

HEAT TRANSFER THROUGH
CAVITY WALLS

A thesis presented for the degree of
Doctor of Philosophy in Chemical Engineering
in the University of Canterbury,
Christchurch, New Zealand.

by

LUFWENDO LISHOMWA

January 1977

QC

320

.L769

1977

Copy 2

"In this work, when it shall be found that much is
omitted, let it not be forgotten that much likewise is
performed"

SAMUEL JOHNSON, A.M.

'Dictionary of the English Language'

Vol. I, page 5, 1755, London

ACKNOWLEDGMENTS

The author wishes to acknowledge the guidance and stimulation provided by his thesis supervisor, Dr J.B. Stott, who first suggested the area of study.

Special thanks are extended to all members of staff of the Chemical Engineering Department, for the many and varied ways in which they assisted in the course of the work; particularly, Dr J. Abrahamson, Mr C.R. Campbell, Mr I.H. Torrens and Mr T.R. Berry. Thanks are also accorded to the staff of the Engineering Library for obtaining many difficult references; in particular, Miss H.C. McCarrigan.

The assistance of Mrs Pearl Thomas and Miss Alison Dunn in the preparation of the final draft is sincerely appreciated.

Finally, the author wishes to thank his lady, Anne Umbers, for her patience and fastidious efforts in the innumerable ways in which she helped with all aspects of the work including the very high quality of the typing.

This work is dedicated to my mother,
Mrs Lyeneno Lishomwa,
and my madame, Anne Umbers

CONTENTS

	<u>Page</u>
ABSTRACT	1
Chapter 1: INTRODUCTION	3
Chapter 2: EQUIPMENT	88
Chapter 3: QUALITATIVE RESULTS	135
Chapter 4: QUANTITATIVE RESULTS	149
Chapter 5: DISCUSSION	185
Chapter 6: CONCLUSION	208
Chapter 7: RECOMMENDATIONS FOR FUTURE WORK . . .	211
NOMENCLATURE	215
REFERENCES	221

Appendices

Appendix A: MISCELLANEOUS DATA	236
Appendix B: CAVITY PROBLEM THEORETICAL DERIVATIONS	244
Appendix C: SURFACE TEMPERATURE SIMULATIONS . . .	270
Appendix D: CALIBRATION OF THERMOCOUPLES	320
Appendix E: SERIES 'A' - EXPERIMENTAL RESULTS . .	330
Appendix F: SERIES 'B' - RAW EXPERIMENTAL DATA AND RESULTS	334
Appendix G: ERROR ANALYSIS	431
Appendix H: NUMERICAL SIMULATION RESULTS	436
Appendix I: LISTING OF THE CAVITY PROBLEM SIMULATION PROGRAM	477

ABSTRACT

The aims of this study were:

- (a) to develop a numerical method and
- (b) to develop an experimental method for the prediction of heat transfer in a cavity in which radiative transfer, gaseous and solid conduction are occurring.

In the experiments, the thermal conductivities of various materials (perspex, durotherm and particle board) were measured to within 1%. The rates of heat transfer across the materials (specimens) were measured for different values of:

- (a) temperature difference across the specimens - ΔT varied between 1°C and 51°C
- (b) material (specimen) thickness - 5.6mm, 9.7mm, 11mm, 12mm and 19mm thick specimens were used
- (c) cavity size - 30.5mm, 34.925mm, 35.5mm and 40.5mm diameter holes were used

The results are presented in graphical and tabular forms (rate of heat transfer versus temperature drop). As expected, the rates of total heat transfer decreased with increases in the hole size and specimen thickness. The effects of radiation transfer were assessed by blocking the holes with aluminium foil. The results showed that radiation transfer was small (about 5% of the total heat transferred).

For four different values of the emissivity of aluminium (0.04, 0.11, 0.2 and 0.5), the method computed:

- (a) the heat transferred by solid conduction - this was

- found to be constant for all values of emissivity
- (b) the heat transferred by gaseous (air) conduction - this too did not vary with emissivity
 - (c) the radiation transferred between the surfaces in the hole - this varied significantly with emissivity
 - (d) the total heat transferred

The results obtained from the numerical simulations are presented in graphical and tabular forms. Depending on the emissivity value used, the percentage of radiation transfer varied between 2 and 15% of the total heat transferred. Correspondingly, the air conduction varied between 9 and 17% of the total heat transferred. Hence solid conduction was the dominant mode of heat transfer (68 to 89% of the total heat transferred).

When using the material durotherm, the experimental and the theoretical results were in agreement within the limits of experimental error. When using perspex, only half of the results were within the limits of experimental error. The discrepancies for the perspex runs varied between 2 and 26%. Reasons are advanced to explain these discrepancies.

CHAPTER 1

INTRODUCTION

1.1	<u>MOTIVATION AND GENERAL OBJECTIVES</u>	7
1.2	<u>RESEARCH UNDERTAKEN</u>	9
1.3	<u>PROBLEM STATEMENT</u>	9
1.4	<u>PRACTICAL APPLICATIONS</u>	12
1.5	<u>OUTLINE OF PRIOR WORK</u>	13
1.5.1	BACKGROUND AND THEORY	13
1.5.1.1	Fundamentals of Heat Transfer	13
1.5.2	REVIEW OF EXPERIMENTAL METHODS	16
1.5.2.1	Heat Transfer Across Vertical and Horizontal Fluid Layers	16
1.5.2.2	General Review of Natural Convection in Cavities - Experimental Studies	20
1.5.2.3	Gas Conduction in Enclosures - Experimental Studies	21
1.5.2.4	Solid Conduction - Experimental Studies	22
1.5.2.5	Radiation Heat Transfer in Enclosures - Experimental Studies	22
1.5.2.6	Concluding Remarks	23
1.5.3	REVIEW OF THEORETICAL METHODS	24
1.5.3.1	Radiative Transfer in Enclosures - Theoretical Studies	24
1.5.3.2	Conduction Heat Transfer - Theoretical Studies	26
1.5.3.2.1	Analytical solutions	26
1.5.3.2.2	Numerical methods	28
	I Finite differences	29
	II Finite elements	32

	III Concluding remarks	33 ⁴
1.5.3.2.3	Other methods of obtaining approximate solutions	34
1.5.3.2.4	Solutions of transient state problems	34
1.5.3.3	Review of Convection Heat Transfer - Theoretical Studies	35
1.5.3.3.1	Empirical studies	36
1.5.3.3.2	Analytical and numerical studies	36
1.5.3.3.3	Theoretical convection studies in the post conductive regime	39
1.5.3.3.4	Concluding remarks	39
1.6	<u>METHOD OF SOLUTION</u>	40
1.6.1	METHOD OF SOLUTION BY EXPERIMENT	40
1.6.1.1	Convection	40
1.6.1.2	Radiation	40
1.6.1.3	Conduction	41
1.6.1.4	Total Heat Transferred	41
1.6.1.5	General Remarks	42
1.6.1.6	Assumptions	42
1.6.2	NUMERICAL SIMULATION OF THE EXPERIMENTS	43
1.6.2.1	Theoretical Basis	43
1.6.2.1.1	Assumptions	43
1.6.2.1.2	Basic transfer equations	44
1.6.2.2	Numerical Solution of Cavity Problem	44
1.6.2.2.1	General description of the procedure	44
1.6.2.2.2	Problem formulation	45

		5
	1.6.2.2.3 Solutions of the equations	49
	1.6.2.2.4 Program flow sheet	51
	1.6.2.2.5 Reliability of solutions	51
1.6.3	SURFACE TEMPERATURE MEASUREMENT	51
	1.6.3.1 General Remarks	51
	1.6.3.2 Sources of Error	54
	1.6.3.3 Prior Work on Error Determination in Surface Temperature Measurement	55
	1.6.3.4 Method of Solution - Surface Temperature Measurement	57
	1.6.3.4.1 Problem statement	57
	1.6.3.4.2 Assumptions	57
	1.6.3.4.3 Physical formulation	57
	1.6.3.4.4 Mathematical formulation	59
	1.6.3.4.5 Numerical solution of the equations	61
	1.6.3.4.6 Numerical simulations carried out	61
	1.6.3.4.7 Quantitative results	71
	1.6.3.4.8 Discussion of the surface temperature results	79
	1.6.3.4.9 Optimal approximations	83
	1.6.3.5 Thermal Contact Resistance	84
	1.6.3.5.1 Prior work on thermal contact resistance	84
	1.6.3.5.2 Method of estimating thermal contact resistance	85
	1.6.3.6 Concluding Remarks	86
1.7	<u>CONCLUSION</u>	87

CHAPTER 1

INTRODUCTION

Heat is defined as energy transferred by virtue of a temperature difference or gradient and is vectorial in the sense that it flows from regions of higher temperature to regions of lower temperature. The basic modes of heat transfer are conduction and radiation.

Conduction is a process by which heat flows from a region of higher temperature to a region of lower temperature within a medium (solid, liquid or gaseous) or between different mediums in direct physical contact. The conduction process takes place at the molecular level and involves the transfer of energy from the more energetic molecules to those with a lower energy level. Irrespective of the exact mechanism, which is by no means fully understood, the observable effect of heat conduction is an equalization of temperature. Conduction is the only mechanism by which heat can flow in opaque solids. Conduction is also important in fluids, but in non-solid mediums it is usually combined with convection, and in some cases with radiation also.

Radiation, or more correctly thermal radiation, is electromagnetic radiation emitted by a body by virtue of its temperature. Thermal radiation is of the same nature as visible light, x-rays and radiowaves, the difference between them being in their wavelengths. The wavelength range normally associated with thermal radiation falls approximately between 0.1 and 100 microns. All solids and liquids, as well as some gases, emit thermal radiation. The intensity of the emissions depends on the temperature and nature of the surface.

Convection, sometimes identified as a separate mode of heat transfer, relates to the transfer of heat from a bounding surface to a fluid in motion, or to the heat transfer across a flow plane within the interior of the flowing fluid. If the fluid motion is induced by a pump, blower, fan, or some similar device, the process is called forced convection. If the fluid motion occurs as a result of the density differences produced by the heat transfer itself, the process is called free or natural convection. Detailed inspection of the heat transfer process in these cases reveals that the basic heat transfer mechanisms are conduction and radiation, both of which are generally influenced by the fluid motion. Convection is most important as the mechanism of energy transfer between a solid surface and a liquid or a gas.

In the solution of heat transfer problems, it is necessary not only to recognize the modes of heat transfer which play a role, but also to determine whether a process is steady or unsteady.

1.1 MOTIVATION AND GENERAL OBJECTIVES

In contrast to conductive and convective heat transfer problems, radiative transfer problems are described, not by differential equations, but by integral equations. Analytical solution of these integral equations, even for the simplest of practical problems, is generally quite difficult and recourse is usually made to numerical methods. When radiant heat transfer and other modes of energy transfer act simultaneously, or interact, the governing equations are non-linear integro-differential equations. Solution of the latter becomes inordinately complex and computer methods are the rule.

Notwithstanding the above, the availability of high-speed digital computers permits great latitude in so far as the level of approach taken in the solution of such problems. Indeed, at one extreme, many complex interaction problems are amenable to solution from first principles with present-day computational capabilities. Such fundamental approaches, however, raise the question as to when this degree of mathematical sophistication is warranted in the solution of problems for engineering purposes. In considering the limited knowledge available about radiation interaction, it appears desirable to employ detailed methods to initially solve simple problems and use the results to delineate the basic physical phenomena. Ideally, the end-product of this approach should be the development of simplified calculational procedures which would be of greater engineering utility in more complex situations.

The primary objective of this study was to develop and demonstrate the validity of a numerical method for the prediction of heat transfer in a cavity in which radiative transfer, gaseous and solid conduction are significant. The study concentrated on finite difference methods for the solution of the primitive equations of motion and energy; an experimental study was also made to verify the analysis.

This work is part of a continuing research effort directed towards an improved general understanding of the physics of processes in which radiative heat transfer interacts with other modes of energy transfer, and the development of improved associated computational procedures. While techniques (4,7,14,137) are currently available for the

solution of simple situations of conduction-radiation interaction problems in two dimensions in an absorbing-emitting media, this work represents a first attempt with a practical geometrical set-up and in three dimensions. Convection-radiation interactions are well summarised by Noble J.J. (3).

As shall become apparent, a survey of available literature revealed that considerable effort has been expended in predicting and measuring heat transfer characteristics in enclosures and cavities; however, a thorough, and simplified method dealing with conduction-radiation interaction was not found in any of this material.

1.2 RESEARCH UNDERTAKEN

The work undertaken in this thesis can be divided into three parts:

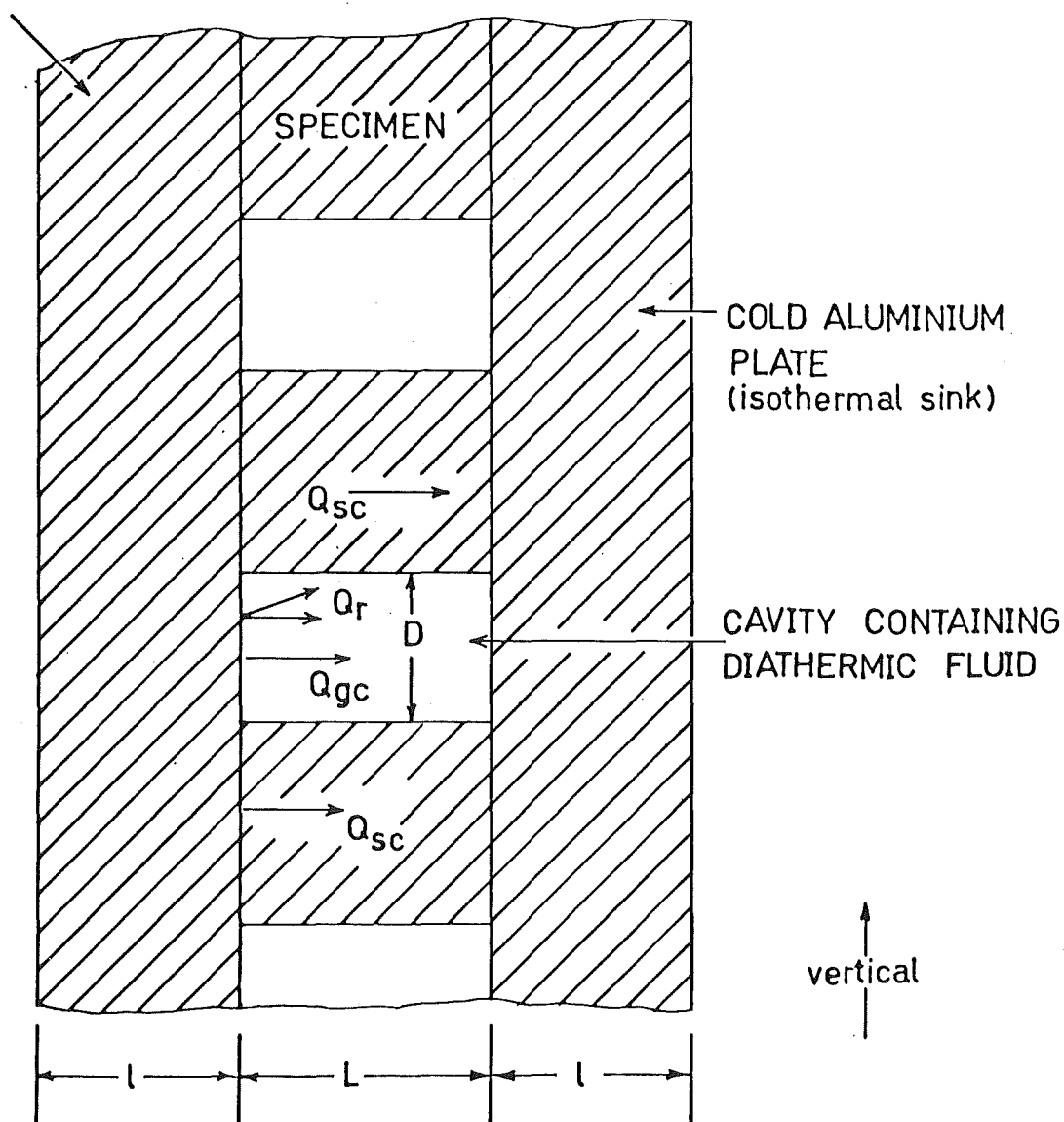
- (1) the design, construction and operation of the experimental equipment (Chapter 2)
- (2) the development of the numerical simulation of the experimental set-up (Chapter 1)
- (3) the comparison and verification of the experimental and theoretical simulations (Chapters 4 and 5)

1.3 PROBLEM STATEMENT

The problem considered is that of the heat transfer mechanisms which occur when a diathermal fluid is contained in a cavity, the walls of which are conducting. Specifically, attention will be given to a cylindrical cavity.

As shown in Figure 1-1, one end of the cylindrical enclosure is an isothermal sink, and the other is an isothermal

HOT ALUMINIUM PLATE
(isothermal source)



Q_{sc} - heat transfer by solid conduction

Q_{gc} - heat transfer by gas conduction

Q_r - heat transfer by radiation

FIGURE 1-1 SKETCH OF A CAVITY SHOWING ITS MAIN COMPONENTS

source zone. Energy is transported from the source to the sink by fluid conduction, solid conduction, and radiative transfer between the walls of the enclosure. Convective transfer is neglected by doing all the work (theoretical and experimental) below the critical Rayleigh number (1,8,11,12). The problem is hereafter referred to as 'the cavity problem'.

As can be shown from dimensional analysis (1,9,10,14,15, 3,17), the cavity problem is a function of the following dimensionless numbers:

1. Aspect ratio of enclosure
2. Grashof number
3. Prandtl number
4. Orientation of gravity
5. Radiation-conduction parameter (or Stark number)
6. Optical thickness (based on a system dimension)
7. Emissivity of the surface
8. Ratio of the absolute source and sink temperatures

It is clear that a complete description of the problem will require considerable theoretical and experimental effort and time. This is partially the reason for the emphasis in this thesis on the numerical and practical aspects of the problem.

The cavity problem is a good test problem for several reasons. First, it is one of the simplest enclosed interaction problems that could be simulated experimentally and theoretically. Second, problems closely associated with the cavity problem have received some attention in the literature. Both theoretical solutions and experimental data are available with which the present work can be compared. Third, there are

many practical applications which can be closely associated with the cavity problem.

1.4 PRACTICAL APPLICATIONS

The mathematical significance of the cavity problem is considered to be at least as important as its practical value and the focus of attention in this thesis is so divided. The cavity problem is of importance in a number of practical situations.

One of the applications is in the thermal insulation field. Radiation transfer and solid conduction are important in determining the effectiveness of thermal insulation (6,13) in cryogenic storage equipment and high temperature thermal protection systems. For example, that used in spacecraft installations - Skylab I for instance. In most cryogenic and space applications, cavities are used to reduce conduction losses and by using low emissivity surfaces in evacuated conditions, reductions in radiation transfer also result. Cavity walled structures are also used to provide high strength -to-weight ratios especially in aircraft. Other areas of insulation engineering where the cavity problem is of significance include building insulation, double-glazing of windows, and the cavities surrounding the core of a nuclear reactor.

A second application is concerned with furnace design. In the steel industry for example, the trend is away from batch production toward large-scale, automated, continuous processes, and therefore the degree of control over furnace conditions must become necessarily finer. As most furnaces

are of cavity wall construction for thermal and economic reasons, using the techniques described in this work, it is possible to get better design methods and operating characteristics for furnaces.

A third area of application that has arisen more recently is in the design of solar energy collectors. In the design of these collectors, particularly the flat plate type, the amounts of radiation, convection and conduction heat transferred from the heated plate must be known in order to compute the efficiency of collection (16,18).

1.5 OUTLINE OF PRIOR WORK

1.5.1 BACKGROUND AND THEORY

Heat transfer processes in enclosures have received increased attention in recent years. Most attention has been to convection transfer in enclosures (natural and forced) (8,18). Conduction and radiation transfers have received very little attention. This section of the work reviews the experimental, numerical and analytical studies on vertical, inclined and horizontal cavities.

1.5.1.1 Fundamentals of Heat Transfer

(1) Definitions:

(a) Thermal Conductivity - is defined as the property of a homogeneous body measured by the ratio of steady-state heat flux (time rate of heat flow per unit area) to the temperature gradient (temperature difference per unit length of heat-flow path) in the direction perpendicular to the area. A material can be considered homogeneous when the value of thermal conductivity is unaffected by variations in specimen thickness

or area over a small temperature range.

To be meaningful, thermal conductivity must be identified with respect to the mean temperature. For a material that is not isotropic, thermal conductivity varies not only with temperature, but also with the direction and orientation of heat flow. Thermal conductivity is usually measured with a material exposed to a definite temperature difference. If the heat flux consists of a convective and radiative as well as a conductive contribution, the thermal conductivity calculated or measured is termed 'effective' or 'apparent'.

(b) Emittance - is the ratio of emission of radiant energy by an opaque material to the emission of a perfect emitter, or blackbody, at the same temperature and under the same geometric and wavelength conditions. Emittance, a practical measure of a material's radiant emission, is distinct from emissivity, a more nearly ideal property obtained by measuring a material whose surface has been carefully prepared to be optically flat.

(2) Basic laws of heat transfer:

The basic physical laws and relations which govern the various mechanisms of heat flow are:

(a) Conduction - the basic relation for heat transfer by conduction was proposed by the French scientist, J.B.J. Fourier, in 1822. It states that q_c , the rate of heat flow by conduction in a material, is equal to the product of the following three quantities:

(i) K , the thermal conductivity of the material

(ii) A , the area of the section through which heat flows by conduction, to be measured perpendicularly to the direction of heat flow

(iii) dT/dx , the temperature gradient at the section

Accordingly, the elementary equation for one-dimensional conduction in the steady-state is written:

$$q_c = -KA \frac{dT}{dx} \quad (1-1)$$

(b) Thermal Radiation - the basic equation for total thermal radiation from the ideal radiator (the 'blackbody') was discovered empirically by Stefan in 1879 and was derived theoretically by Boltzmann in 1884:

$$q_r = \sigma AT^4 \quad (1-2)$$

where q_r is the rate radiant energy emission, W

A is the surface area of the emitting surface, M^2

T is the absolute surface temperature, $^{\circ}K$

σ is the Stefan-Boltzmann constant, $W/M^2/^{\circ}K^4$

Real bodies do not meet the specifications of an ideal radiator but emit radiation at a lower rate than blackbodies. If they emit, at a temperature equal to that of a blackbody, a constant fraction of blackbody emission at each wavelength, they are called gray bodies. The rate of emission of radiant energy of a gray body at a temperature T_1 is:

$$q_r = \sigma A \epsilon T_1^4 \quad (1-3)$$

where ϵ is the emittance of the gray surface.

(c) Convection - in 1701, Newton defined the heat transfer rate q_{co} from a surface of a solid to a fluid by

the equation:

$$q_{co} = h_{co} A (T_s - T_f) \quad (1-4)$$

where q_{co} is the rate of heat transfer by convection, W

A is the heat transfer area, M^2

T_s is the surface temperature, $^{\circ}C$

T_f is the fluid temperature at some specified location (usually far away from the surface), $^{\circ}C$

h_{co} is the surface coefficient of heat transfer (or the convective heat transfer coefficient), $W/M^2^{\circ}C$

1.5.2 REVIEW OF EXPERIMENTAL METHODS

It is mentioned at the outset that little work has been found which is related to measuring heat transfer rates in enclosures with conduction and radiation as the predominant modes. As such, the discussion of prior investigations pertinent to this study is of a general nature.

1.5.2.1 Heat Transfer Across Vertical and Horizontal Fluid Layers

The first systematic experimental investigation - directed at obtaining generalised relationships for the transfer of heat through enclosed, plane air layers - was made by Mull and Reiher (19) in 1930. They measured the steady-state heat transfer rate by natural convection across air layers. Most of their experiments were conducted for horizontal and vertical cavities. Their results were presented in the form of a Nusselt-Grashof number correlation.

The results of Mull and Reiher were represented in a simplified form by Jakob (20,21). It was suggested that there are essentially three regimes of heat transfer occurring

within vertical air layers. At low values of Gr only gaseous conduction occurs and Nu equals unity; the convective flow region can then be divided into laminar and turbulent regimes. The results were again presented in empirical relationships.

In 1951, Peck et al (22), performed a series of experiments on vertical, enclosed gas layers in which the environmental pressure was varied. The radiative, Q_r , and solid conductive, Q_{sc} , components of the total heat flux passing across the cavities were obtained by evacuating the test cell to a pressure of approximately 2×10^{-5} torr. At such vacua, the gaseous conductive and convective heat transfers are completely eliminated. Their experiments could not distinguish Q_r from Q_{sc} . They however, obtained empirical correlations for air, at environmental pressures in the range 1 - 100 torr. Kent (23) used a similar technique to obtain correlations of Nusselt and Rayleigh numbers for horizontal fluid layers in 1972.

De Graaf and Van der Held (9) examined the transfer of heat across enclosed air layers in horizontal, vertical and inclined positions. Attempts were made to determine the convective flow patterns occurring within air layers by means of both a modified shadow-graph technique and smoke methods. It was concluded from these tests that convection did not occur in vertical air layers provided $Gr < 2.78 \times 10^3$, and that if $Gr > 5.55 \times 10^4$ laminar flow existed. When this Grashof number was exceeded, a gradual transition to turbulent flow ensued. The radiation contribution of the total flux transferred across a layer was incorrectly assumed to be the

heat transferred through a horizontal air layer when the hot wall was placed uppermost. The experimental correlations given were in good numerical agreement with those of Jakob.

The thermal insulating values of enclosed air spaces, with particular reference to buildings, have been studied by Robinson and Powlitch (24). Steady-state heat transfer measurements were obtained with enclosing surfaces of differing emissivities at five different inclinations of each cavity and for various directions of heat flow. Values of the combined conduction-convection heat transfer coefficients were plotted against the air layer thickness, with temperature difference as an experimental parameter. They concluded that for a given orientation and temperature difference there is an optimum thickness of air layer at which the thermal resistance of the air space has a maximum value, though at large air thickness values, greater resistances may be encountered.

The first detailed, phenomenological study of the heat transfer processes occurring within vertically-enclosed air layers was presented by Eckert and Carlson (25), who used a Mach-Zehnder interferometer to determine the temperature distribution within the air layers. Three regimes of flow were distinguished in the range $2.92 \times 10^2 < Gr < 1.94 \times 10^5$. The conduction regime was defined to exist when a linear temperature gradient was established in the central portion of the cavity. The conditions under which a core of uniform temperature was established across the cavity, with thermal boundary layers along the hot and cold walls, was termed the boundary layer regime. Between these two regimes the temperature profiles were observed to be curved throughout the complete height of the air layer, indicating that convection

was becoming increasingly significant. This was called the transition regime. In the conduction regime heat is transferred by gaseous conduction only in the central section of the air layer. In the corners of the cavity, convection was found to contribute to the total heat flux across the cavity and local heat transfer coefficients were obtained for these corner regions. Average Nusselt number correlations for the conduction regime, as well as empirical relationships for heat transfer in the boundary layer regime, were presented.

The earliest experiments on the thermal instability phenomenon referred to above were conducted by Thomson (26), and then Benard (27) presented a more complete description of the development of a cellular convection pattern. Consequently, the thermal instability question is generally referred to as the Benard problem. Schmidt and Saunders (28) found that instability and cellular motion within a horizontal layer of fluid ensued when Ra was approximately equal to 1700. When cellular convection occurred, the length of the horizontal side of a cell was found to be approximately twice the layer depth. As Ra was increased beyond its critical value, the temperature gradients at the plane midway between the boundary surfaces decreased to negligible values, indicating that all the heat was being convected. Experiments on layers of different depths showed that on further heating the layer became completely turbulent at $Ra = 4.5 \times 10^4$; the first signs of turbulence occurring at about $Ra = 5 \times 10^3$.

Sadhu and Probert (29) measured steady-state rates of heat transfer outwards across vertical air-filled annular

cavities, with aspect ratios which ranged from 16 to 70, and for several pressures of the contained air. The chosen temperature difference between the isothermal cylindrical walls ranged from 20°K to 180°K . For constant values of the temperature difference, the gaseous conductive, convective and radiative components of the heat leaks across the air gap to the outer cylindrical wall were distinguished and evaluated using a technique which employed the air pressure as the variable. Convection of the air ensued throughout the whole height of the cavity when the Rayleigh number attained a value of 1.6×10^4 .

Edwards (30) measured the rate of heat transfer through air across a rectangular sectioned cavity for different values of temperature difference across the cavity, aspect ratio, angle of inclination of the cavity with respect to the horizontal, and air pressure within the cavity. By reducing the pressure of the air in the cavity from atmospheric to 10^{-3} torr for any given geometrical arrangement, he distinguished between the convective, conductive and radiative components of heat transfer through the gas. He did not, however, distinguish between radiation through the gas and conduction via the cell structure supports. The results were presented in dimensionless form, Nusselt number against Rayleigh number.

1.5.2.2 General Review of Natural Convection in Cavities - Experimental Studies

There have been numerous investigations concerned with natural convection in enclosures. Among the references with

the greatest relevance to the thesis are those of Churchill (12,31,32), Probert (8,33,34,35,36) and Ostrach (37,38). The reader is referred to Drake (39) for a more comprehensive review of more general enclosed natural convection experimental studies.

1.5.2.3 Gas Conduction in Enclosures - Experimental Studies

Most experimental studies of gaseous conduction in enclosures were (and still are) associated with work relating to thermal insulation.

A comprehensive series of experiments on the insulating effectiveness of various materials was carried out by Allcut (40) in 1951. The effects of varying the amounts of air conduction (by varying the density of the fibrous insulation materials) were studied in detail. Although no new theories or methods of evaluating air conduction were obtained, the results provided an experimental basis for future work on thermal insulation. The effects of radiation transfer, convection and air pressure were also studied.

Verschoor and Greebler (41) studied heat transfer of gas conduction and radiation in fibrous insulations. Thermal conductivity measurements were made at atmospheric pressures with four different gases in the insulation samples, and the thermal conductivity with air was studied over a pressure range of 1 micron to 760mm of Hg. Gas conduction was found to be the most important mechanism of heat transfer. A theory of gas conduction in fibrous insulation was developed, which agreed well with experimental results. Theoretical

considerations of heat transfer by radiation (mean free path of radiation calculations) were also confirmed by the experimental thermal conductivity values at low pressures.

Good reviews of gas conduction studies are presented by Tye (6) and Glaser (13).

1.5.2.4 Solid Conduction - Experimental Studies

As mentioned earlier, the thermal conductivity of a material is a measure of heat flow by conduction in the material. Numerous methods are available for the measurement of the thermal conductivity of a solid material (6). The basic method is the guarded hot plate which has been the subject of much experimental and theoretical study (42,43, 44,45).

References worthy of note are Bratis and Novotny (46), Kent (23), Swann (47,48), and various workers at the seventh conference on thermal conductivity measurements (49).

Experimental analogic methods have been used to measure the solid conduction contribution to heat transfer. Schneider (5) used three different analogies (the electrical, the fluid-flow, and the membrane) to measure the solid conduction component in a furnace wall problem. Kreith (1) also describes three different electrical analogies that have been successfully used. A comprehensive review of analog methods is presented by Rohsenow (51).

1.5.2.5 Radiation Heat Transfer in Enclosures - Experimental Studies

In the last two decades, there have been numerous

investigations of the influence of thermal radiation heat transfer in enclosures composed by various surfaces (black, diffuse-gray, specularly reflecting, non-diffuse non-gray, and transparent surfaces) (7,14,52,53). The majority of the publications have been analytical investigations using gas models such as the gray gas, the box or the exponential wide-band model.

At the present time, there are very few existing experimental investigations concerned with radiative transfer in enclosures. Most of these experimental investigations deal with gaseous radiation interactions (54,55,56,57,58).

Allcut (40), Verschoor (41) and Strong (59) measured the effect of thermal radiation in conjunction with thermal insulation studies in fibrous materials. Swann (4) and Stroud (60) measured the effects of thermal radiation in enclosures in their studies of heat transfer across honeycomb core panels.

Sadhu (29) and Edwards (30) in their experimental studies of natural convection in enclosures, measured the amount of radiation flux as well.

1.5.2.6 Concluding Remarks on Experimental Methods of Analysing The Cavity Problem

(a) Conduction - gas conduction has been measured by reducing the working pressure to 10^{-3} torr (13,29,30). Solid conduction is either lumped together with thermal radiation (23,29) occurring in the enclosure, or is reduced (consequently ignored) by using thin walls (61). Other workers (3, 30) used adiabatic cell set-ups and estimated solid conduction

as a loss in heat flux.

(b) Radiation - no work was found in which it was measured or stated quantitatively, it was always associated with solid conduction.

(c) Convection - most workers estimated it by using the Mach-Zehnder interferometer or by difference.

1.5.3 REVIEW OF THEORETICAL METHODS

This review of calculation methods falls into three categories:

(a) Empirical and Semi-empirical - that is, correlations.

(b) Analytical - the formal analytical approach involves the derivation of a mathematical solution for the temperature as a function of space or space-time co-ordinates. The solution must satisfy the characteristic differential equation from which it was derived, and certain initial and boundary conditions imposed by the particular problem itself. Excellent books on this approach are Carslaw and Jaeger (62), Schneider (50), Jakob (21) and Ozisik (63).

(c) Numerical - these methods are associated with obtaining approximate solutions of the steady-state and transient heat transfer equations. Their basis are usually finite difference and finite element approximations.

1.5.3.1 Radiative Transfer in Enclosures - Theoretical Studies

A general analysis of radiant interchange within an enclosure was first devised by Hottel (15). Hottel's early work showed how the problem could be solved if the associated

linear equations could be solved and he suggested the use of matrix methods to do so. A different approach to the problem was offered by Poljak (21,64). Later Oppenheim (65) introduced an electrical analogy to radiant heat transfer which greatly simplified the representation of the problem and he suggested that the electrical network be solved by matrix methods similar to Hottel's. An alternate approach to the cavity problem was given by Gebhart (66). All of the above methods are basically equivalent as demonstrated by Sparrow (67); they are termed 'the net-radiation method'.

Bevans and Dunkle (68) used relaxation methods in solving the resulting equations from the electrical networks of the cavity problem. Stott and Garrod (17,69) produced a method of assessing radiation heater transfer in an enclosure surrounded by several surfaces at different temperatures and containing a number of radiating and absorbing volumes of gas. They showed that the application of an electrical analogy could be made relatively simple by the use of relaxation methods to solve equations describing the analogous electrical resistive network. A computer program was described which solved the problem in general terms and its application to furnace design was outlined.

The net radiation method is formulated in different terms in the various textbooks (51,70), but the basics of the methods are the same. Wiebelt (136) developed integral equations of radiant heat transfer. These equations were solved by numerical and analytical methods. The numerical methods involved taking finite difference approximations for the integral equations which led to the network concept and

hence iterative solving techniques. The analytical approach involved solving the integral equations by successive substitution and variational calculus.

An alternate approach to the analysis of radiative transfer in enclosures is offered by the Monte Carlo method. It is a statistical numerical method. A review of the problems solved in the literature using this method is given by Siegal (14).

Analytical and numerical studies of the interaction of thermal radiation with other modes of heat transfer in enclosures is well reviewed in the work of Novotny (46,56,58).

1.5.3.2 Conduction Heat Transfer - Theoretical Studies

The study of conduction heat transfer is principally concerned with the distribution of temperature or rate of heat flow within a medium. The determination of the temperature field or heat flux constitutes a complete solution.

1.5.3.2.1 Analytical solutions of conduction problems

Analytical solutions are limited in their range of applicability due to their complexity and uncertainty as far as practical boundary conditions are concerned. Many practical two- and three-dimensional engineering problems require numerical methods for their solution. However, assumptions can usually be made in most practical problems which reduce them to simple geometrical shapes with straightforward boundary conditions for which many analytical solutions have been tabulated.

The classical works on analytical heat conduction are considered to be those of Fourier (71) and Carslaw and Jaeger (62). Fourier, of course, laid the foundations of conduction in solids, while Carslaw and Jaeger later described numerous solutions to many different geometries and solutions. This latter work is principally an operational text in that the mathematical methods of solution are only briefly outlined. Carslaw and Jaeger were principally concerned with conduction for its own sake, but other authors such as Arpaci (72) have outlined conduction in an engineering context with the solutions described in more detail.

This work can in no way attempt a complete presentation of the analytical methods available for the solution of the heat conduction problems. What is attempted is a citation of some of the more commonly used and more straightforward procedures employed in engineering practice.

Schneider (50) solved various practical engineering problems using analytical methods, principally Fourier series. One of the problems that he solved that is particularly applicable to this work is that of a temperature field in a nuclear reactor. The solution obtained was only approximate as he used circular harmonics.

The classical approach to an exact solution of the heat conduction equation is the separation-of-variables technique. Kreith (1), Bayley (73) and Myers (74) have given good accounts of this approach. Myers in his text has given a fairly complete and rigorous presentation of alternative methods used in the integration of partial differential

equations. An outline of the mathematical principles required to solve analytical problems is given. Bessel function, Fourier series and Laplace transforms are all presented in simple terms. Examples of the application of these principles to such problems as plane wall and semi-infinite solid conduction are given.

Rohsenow (51) also gives an excellent review of mathematical and practical examples of analytical methods used in conduction heat transfer. A systematic and unified study of methods for solutions of heat conduction problems is given by Ozisik (63). The feature of his book is a systematic tabulation of transforms; inversion formulas for finite, semi-finite and infinite regions, for all combinations of boundary conditions. Through the use of this integral transform technique, the solution of heat conduction problems becomes a comprehensive study.

1.5.3.2.2 Numerical methods

These are methods of obtaining approximate solutions to the heat conduction equation. Most treatments of numerical heat conduction are derived from the more generalised and more rigorous approach of the numerical analyst as advocated by Fox (75), Smith (76), Ames (77), Forsythe (78) and Richtmyer (79). Of the numerical approximation methods available, those employing finite difference approximations are straightforward, are more frequently used, and are generally more applicable than any other. Accordingly, this thesis concentrates on the finite difference approach. However, also briefly described is a relatively new approach known as the 'finite element' method, which is essentially

a variational approach since the solution of the governing differential equation is obtained by minimising some integrated quantity (referred to as a functional) which is evaluated over the whole region of interest.

This method is widely used in structural analysis and although it is not as straightforward conceptually as the finite difference approach, it offers several advantages in the treatment of heat conduction problems, particularly with curved boundaries and normal derivative boundary conditions.

It is common in heat transfer to treat steady-state conduction (involving two or more space variables) and transient heat conduction (involving one or more space variables and time) separately, and this is also done in the numerical analysis of these problems since they form separate classes of partial differential equations. These classes are important in that they classify the nature of the procedure used in their solution. Steady-state problems are elliptical partial differential equations and transient are parabolic. Only solutions of the former are considered in this work.

(I) Finite Differences

(a) Approach - the basic approach consists of overlaying the area of integration with a mesh (usually rectangular or triangular), and in replacing each derivative of the original partial differential equation by a finite difference approximation at each mesh point, in terms of the temperatures of the neighbouring mesh points and writing down an algebraic equation approximating the partial differential equation at that point (80,81,51).

With steady-state heat conduction this process gives N simultaneous algebraic equations for N mesh points in the region, the solution of which provides a numerical value of temperature for each mesh point. In the case of transient heat conduction, the partial differential equation is approximated along one or two rows of mesh points at a time, so that the procedure results in the successive solution of small sets of algebraic equations (51,82).

(b) Physical formulation - the first step in the physical formulation of the problem is to subdivide the system into a number of small but finite subvolumes (1,51,74,80). Each subvolume is assumed to be at the temperature corresponding to its centre. The physical system is replaced by a network of fictitious heat-conducting rods between the centers, or nodal points, of the subvolumes. Once the thermal conductance corresponding to the conductance of the material between nodal points is assigned, the heat flow in the rod network is obtained. This heat flow approximates the flow in the continuous system.

(c) Finite difference approximations - the fundamental operation in the method of finite differences is the replacement of each derivative in the partial differential equation by an algebraic approximation at each discrete point in the region. These finite difference approximations can be of varying degrees of accuracy and can be derived in several different ways: by examination of the heat flow in a differential element, from variational considerations (78) by fitting polynomials through the function values of the neighbouring nodal points and differentiating, or by the use

of Taylor expansions. Myers (74), Bayley (73) and Rohsenow (51) have shown that the latter method is brief, simple, and gives an indication of the accuracy of the approximation.

(d) Formulation of nodal equations - numerous examples exist of the finite difference representation of the main equations. Among the references worthy of note are the works of Dusenberre (80), Kreith (1), Rohsenow (51) and Myers (74). In all these references, radiation and convection boundary conditions, and irregular physical boundaries are considered in detail.

(e) Finite difference equations and their solutions - finite difference methods for solving steady-state heat conduction problems lead to systems of algebraic equations. The solution of the equations is not a trivial matter. In the majority of cases, the equations are linear, so that the coefficients are constants or functions of the independent variables only, and the mathematical procedures of matrix algebra apply. However, some problems, such as those involving temperature-dependent thermal conductivity, and the cavity problem, produce non-linear algebraic equations. The methods of solving the equations can be classed as either direct or iterative.

Emmons (81) presented one of the earliest solutions to the finite difference equations by using the relaxation method of Southwell (83,84). Later, Dusenberre (80) generalised the solutions due to Emmons. Numerous publications (50,51,73,74,1) have represented the relaxation solution. The most common direct method of solution of finite difference equations is via Gaussian elimination.

Bayley and Myers present good accounts of this method. Iterative methods of solution include Gauss-Siedel (relaxation method), Jacobi, successive overrelaxation, and alternating direction implicit methods (50,51).

(II) Finite Elements

The finite element approach was developed and has been extensively used for structural analysis (85,86). It is becoming of increasing importance in other engineering fields such as fluid mechanics and heat conduction (87,88,89).

While the finite difference method represents a direct approach by approximating individual derivatives in the differential equation, the finite element procedure is an approximation applied to the variational form of the partial differential equation, so that, in general, the problem becomes one of finding a function which minimises a 'variational functional' over the field of interest.

The region is divided into a number of elements (usually triangular (86,90) for two-dimensional problems, or tetrahedral (88) for three-dimensional problems), and the unknown function is uniquely specified throughout the field by a discrete number of values associated with the node points of the elements. The value of the function at a particular node point influences only the function at the nodes of the adjacent elements so that the minimization of the functional throughout the whole region results, as with finite differences, in a system of simultaneous equations.

Numerous investigators have dealt with the fundamental concepts of the finite element method. The papers by

Zienkiewicz (85,88) present the finite element formulations well. More recently, Myers (74) has dealt with the subject very fully. Fundamental concepts are presented and two-dimensional steady-state problems are solved. Bayley (73) has used the finite element method to solve the classical gas turbine problem. Zienkiewicz (88) used finite element methods to solve electrical three-dimensional field problems which are analogous to heat transfer problems. He also studied spontaneous ignition (89) using variational techniques.

(III) Concluding Remarks on Finite Difference and Finite Element Methods

Emery and Carson (90) made a study of the accuracy and efficiency of the finite element methods in comparison to the standard finite difference algorithms used for the computation of temperature. Their study was primarily concerned with computational aspects, but their general conclusions seemed to favour the use of the finite element methods rather than finite difference ones. Their study suggested that the primary advantages of the finite element methods were associated with the ease of inputting the required data and the capability of altering the basic accuracy of the method; its major disadvantages were large core memory requirements and lengthy execution times.

Bayley and Myers, both make the points that, although the finite difference and finite element methods occasionally result in identical equations, the finite element method has advantages in the freedom of the shape of elements (that is, the choice of placement of node points in complex regions)

and in the ease with which derivative and mixed boundary conditions on irregularly shaped boundaries can be handled.

1.5.3.2.3 Other methods of obtaining approximate solutions

The theory of complex variables provides the means of obtaining solutions to two-dimensional steady-state heat transfer problems in many situations where analytical procedures are not applicable. The most useful aspect of this theory is its ability of transforming a region in which heat transfer takes place (where, for example, complicated boundary conditions prohibit the use of analysis) into another region, so that the problem can be easily solved (91,92,93). This transformation, which preserves the magnitude and sense of the angles between isothermal boundaries, is called conformal mapping. This theory also provides the fundamentals for graphical solutions. Kreith (1), Schneider (50) and Rohsenow (51) have used graphical methods to solve numerous conduction problems.

1.5.3.2.4 Solutions of transient state problems

Unsteady-state heat transfer problems are characterised by time-dependent heat fluxes and temperature fields. Exact solutions to most practical transient heat transfer problems are rather difficult, if not impossible, to obtain. Thus, the necessity of obtaining an approximate solution to such problems has motivated a considerable effort for developing methods for achieving approximate solutions. The most commonly used of these methods can, in general, be classified in the following four categories:

(1) Method of finite differences - this method has attracted most of the attention in recent years, primarily because it is easily adapted to digital computations (94); consequently, this is the only method that can be used to obtain an approximate solution if a high degree of accuracy is required, or if the problem at hand is of considerable size and complexity.

(2) Graphical methods - were first introduced by Schmidt and Binder (15). In recent years, with the development of computers, the interest in such methods has diminished, though these methods can provide quick answers, and also have the advantages of simplicity and visualization.

(3) Approximate analytical methods - several have been developed (51,73) for obtaining approximate solutions of heat transfer problems in an analytical form. They can be applied to both linear and non-linear problems yielding simple solutions with an accuracy adequate for engineering purposes. The most extensively used are the Integral method first introduced by Goodman and the Biot's variational principle.

(4) Analog methods - these are discussed by Paschakis (51) in great detail.

1.5.3.3 Review of Convection Heat Transfer - Theoretical Studies

As it was the aim of this work to suppress convection in the cavity, the theoretical studies on natural convection pertinent to this study are concerned with heat transfer in the conduction regime only (Ra less than 1709). With this

restriction, little work has been found which is directly applicable.

Natural convection studies in enclosures can be classified as follows:

1.5.3.3.1 Empirical studies

Most of the experimental and numerical investigators of heat transfer in enclosures, presented their results in the form of the Nusselt number - Grashof (or Rayleigh) number correlations (25,70,95,96,97,98). The most up-to-date correlation (May 1976), is that due to Holland (114). The correlation is applicable for all values of the Rayleigh number and agrees well ($\pm 5\%$) with experimental results for angles of inclination to the horizontal less than 60 degrees.

$$\begin{aligned} \text{Nu} = 1 + 1.44 (1 - 1708/\text{Ra} \cos \phi) (1 - \frac{(\sin 1.8\phi)^{1.6} 1708}{\text{Ra} \cos \phi}) \\ + ((\frac{\text{Ra} \cos \phi}{5830})^{0.333} - 1) \end{aligned} \quad (1-5)$$

where Nu = Nusselt number for natural convective heat transfer across the air layer

Ra = Rayleigh number

ϕ = Angle of air layer from horizontal

1.5.3.3.2 Analytical and numerical studies

(A) Vertical layers

Early theoretical analyses of the cavity problem were published by Batchelor (99) and Poots (100).

Batchelor presented a solution valid for nearly square enclosures based on parametric expansion of the temperature field and stream function in powers of the Rayleigh number. As such, his results were valid only for small Rayleigh

numbers or the cases where conduction predominated convection. Poots used a numerical method based on the use of orthogonal polynomials to solve a variant of the cavity problem in which the temperature profiles along the top and bottom of the enclosure varied linearly between the source and sink temperatures. Results were presented for aspect ratios of unity, $Pr = 0.73$ and Rayleigh numbers from 500 through to 10,000. The Poots' correlation was

$$Nu = 1 + (9.8 \times 10^{-8}) Gr^2 \quad (1-6)$$

provided the Grashof number was less than 1390. This result compared favourably with Batchelor's predictions.

Mynett (101) attempted to solve the governing equations by means of a relaxation technique for an aspect ratio of 6 only and for Rayleigh numbers of 100, 1,000 and 10,000 respectively. The partials differentials were replaced by their finite difference equivalents in preparation for the relaxation process, which involved an iterative procedure. The results obtained for Nu agreed closely with those of Batchelor's.

Following Eckert and Carlson (25), various publications (95,102,103,104,105) have used the temperature distribution in the cavity to distinguish between three regimes of flow. At Ra less than 3,000 the computed temperature profile across the cavity was virtually linear, that is, the continuum conduction regime. As Ra increased, convection was found to become increasingly significant and the temperature profiles across the air layer showed a progressive departure from linearity - this is termed the transition regime. Above $Ra = 10,000$, the boundary layer regime ensued.

(B) Horizontal layers

The first analytical treatment aimed at determining the conditions delineating the breakdown of the quiescent state within horizontal fluid layers heated from below was carried out by Lord Rayleigh (106). This work was corroborated and extended by Jeffreys (107,108) and Low (109). From these analyses it was concluded that the sole parameter determining stability was the product of the Prandtl and Grashof numbers, that is, the Rayleigh number. The critical value of Ra (based on the thickness of the fluid layer), above which cellular convection ensues, was computed to be 1709. The fundamental assumptions in these analyses were that (a) density variation effects were negligible except for their influence on the bouyancy; (b) the initial motion was slow; and (c) a linear temperature profile extended across the entire fluid layer at the start of the motion.

More recent studies on convection in enclosures include the work of Churchill and Chu (110). They studied the effect of localised heating in a rectangular channel by solving the partial differential equations for the conservation of mass, energy and momentum numerically using an unsteady-state formulation and the alternating-direction-implicit method. The computations were carried out for $Pr = 0.7$ and Rayleigh numbers between 0 and 100,000. They concluded that (a) the relationship between the circulation pattern and the rate of heat transfer was quite complex and (b) conduction was the predominant mechanism for heat transfer for Ra less than 1,000 even though some circulation occurred for all Ra greater than 0.

Ozoe and Churchill (12) performed a three-dimensional numerical analysis of laminar natural convection in a confined fluid heated from below. They tested three geometrical configurations and compared their results with those of Aziz and Hellums, Catton, and Heitz and Westwater. For the cubical enclosure, the critical Rayleigh number obtained by extrapolation to $Nu = 1$ was 3500, which agrees closely with the computed value of 3446 by Catton (111), and the experimental value of 3700 by Heitz and Westwater (112). For the long square channel, the critical Rayleigh number obtained from extrapolation to $Nu = 1$ was 2300 which agrees reasonably well with the prediction of 2452 by Catton. The results for the analysis of a region between infinite horizontal plates heated from below gave similar results as obtained from earlier two-dimensional computer programs (31).

1.5.3.3.3 Theoretical convection studies in the post conductive regime

Catton (113), Hollands (114) and Buchberg (18) give good reviews of the work that has been done in this area in the last two decades.

1.5.3.3.4 Concluding remarks on natural convection studies in enclosures

It has been conclusively shown by Probert (11) for vertical air layers, that the limit of conduction can be identified solely in terms of the Grashof number ($Gr = 2.2 \times 10^3$) and that the critical Grashof number is independent of the height of the fluid layer.

Rayleigh (106), Jeffreys (107,108) and Low (109) have shown that for horizontal fluid layers, the critical Rayleigh number is 1709. The studies of Ozoe and Churchill (12) tend to come up with critical Rayleigh numbers close to 2300 for confined fluids heated from below.

1.6 METHOD OF SOLUTION

The cavity problem is solved in this work by two distinct methods (a) by an experimental method and (b) by a numerical method.

1.6.1 METHOD OF SOLUTION BY EXPERIMENT

The experiment is required to measure or show the effects of: (a) the thermal conductivity of the specimen; (b) solid conduction; (c) thermal radiation; (d) gaseous conduction; and (e) total heat flow.

1.6.1.1 Convection

As previously mentioned, it was the aim of this work to suppress natural convection. Consequently, all the experiments were to be performed at sub-critical Rayleigh numbers (less than 1700). As calibration runs will show later, by working with specimens of less than 0.75 inches (19.05mm) thick at moderate temperatures, the resulting Rayleigh and Grashof numbers are sub-critical. As no interferometer was available, the no convection assumption could not be checked experimentally.

1.6.1.2 Radiation

Radiation is difficult to measure experimentally (115). As such, the only ways of assessing its importance are by

difference or by showing its varying effects under different conditions. Since conduction and convection were not measured individually or distinguished in this work, the latter method was used. Radiation effects were assessed by varying the

- (i) material
- (ii) material thickness
- (iii) cavity size
- (iv) temperature differences across the cavity
- (v) surface conditions at the ends of the cavity

1.6.1.3 Conduction

Solid conduction could have been measured by imbedding thermocouple wires in the solid slabs used. The introduction of these probes in the solid would have disturbed the heat flux profiles (see section 1.6.3).

Gas conduction could also have been measured by varying the working pressure (below 10^{-3} torr gas conduction negligible (13,30)), however, evacuating holes in the specimens would also have been necessary. They too would have disturbed the heat flow.

Consequently, conduction effects were also only assessed in relation to the total heat transferred under various experimental conditions (see 1.6.1.4 below).

1.6.1.4 Total Heat Transferred

The total heat flow was determined using a guarded hot plate apparatus (5). For a given temperature difference and material, the apparatus was used to measure the thermal conductivity of the material. Holes were then drilled in the

specimen. The guarded hot plate apparatus was again used to find the total heat transferred at the same temperature differences as for the solid specimen experiments. This set of experiments was repeated for various hole sizes, thicknesses of the same material, and for various materials. By blocking the holes with aluminium foil, the effects of radiation were also assessed.

From quantitative heat flux curves of heat transferred against temperature difference for various operating conditions, the effects of solid and gaseous conduction can be distinguished from radiation effects, as the former are linear relationships while the latter are non-linear. A comparison of total heat transferred by experimental and by theoretical work provided a check on the accuracy of the theoretical and experimental analyses.

1.6.1.5 General Remarks

The primary material used in the experiments was 'perspex' acrylic sheet (Imperial Chemical Industries Limited tradename for polymethyl methacrylate). Rationale for this choice, is provided in the next chapter. Other materials used are particle board, rubber, and two types of asbestos cement board (durotherm and syndanyo board).

1.6.1.6 Assumptions

Some of the basic assumptions used in the development of the experimental method of solution are summarised below. Other particular assumptions are discussed as they arise.

(a) Steady-state conditions exist - the recorder showed this condition to be true despite fluctuations in voltage and current which could not be eliminated.

(b) Uni-directional heat flow - the thermocouple wires on each plate proved this to be practically correct.

(c) Heat flow from electrical power input is equally divided between the two specimens. Electrical power was computed from current multiplied by voltage assuming a power factor of one. Also the heat flux was assumed to be area dependent, that is, since the central metered section was 1/4th of total plate area, then 1/4th of the power was associated with this area.

(d) The temperatures indicated by the thermocouple wires are the correct surface temperatures (see section on surface temperature measurement).

(e) The surface temperature of the specimen at the hot end is equal to the surface temperature of the hot plate of the guarded hot plate apparatus. Similarly for the cold end of the apparatus, the specimen temperature is assumed to be the same as the cold plate temperature.

1.6.2 NUMERICAL SIMULATION OF THE EXPERIMENTAL SET-UP

1.6.2.1 Theoretical Basis

1.6.2.1.1 Assumptions

The basic assumptions used in the numerical simulation of the cavity problem are:

- (1) Steady-state conditions exist
- (2) No heat generation - heat sources or sinks in the problem are non-existent
- (3) The physical properties of the system are constant and are calculated at the mean temperatures. For example,

the thermal conductivities of perspex and air are constant (at the mean temperatures).

(4) Zones of constant temperature are associated with each node. Three different zoning systems are used (see Appendix). For solid conduction, the zoning approximations are well known (1,50). For gas conduction, cores of air at constant temperature are considered. For radiation surfaces, the zoning approximations of Hottel (116) are assumed.

(5) The surfaces of the enclosure are assumed to be opaque and diffuse-gray (Appendix). Hence, the emissivity of perspex is taken as 0.9, and that of aluminium taking values of 0.04, 0.11, 0.2 and 0.5 (Appendix).

1.6.2.1.2 Basic transfer equations

The basic equation used for the conduction flow calculations is the Fourier equation (1-1) in three dimensions. For radiant transfer, the Stefan-Boltzmann equation (1-3) is used. The continuity and mass conservation equations are used in all heat balances. Note that for radiant heat transfer in the enclosure, the net-radiation method (14,64) is applied.

1.6.2.2 Numerical Solution of the Cavity Problem

1.6.2.2.1 General description of the procedure

The method used is an iterative one using relaxation techniques. Unknown temperatures are first estimated and the radiation fluxes between radiation regions are calculated. Using these fluxes, heat balances are calculated for each region and temperatures are adjusted until the heat balances

are satisfied. The procedure is repeated until no further worthwhile changes occur. The calculation depends for its success on a technique (discussed later) which ensures convergence of the iterations which calculate the heat balance, whilst simultaneously adjusting the radiation flow changes due to changes in temperature. The convergence, accuracy, and numerical stability of relaxation procedures is well documented in the literature (80,81).

1.6.2.2.2 Problem formulation - finite difference approximations

(a) Heat transfer equations

(i) Choice of grid - the three-dimensional cartesian co-ordinate system used (rectangular parallel-piped or box elements) is shown in the Appendix. The relationship of the grid to the physical layout of the problem is also presented. There are three solid conduction regions, each region has 58 temperature points. Note that due to the symmetry of the problem, only 1/8th of the box element (or zone) is used. Six radiation regions are considered and three air conduction regions (each with four temperature (nodal) points).

The choice of grid presented numerous problems as the hole (or cavity) is cylindrical whereas the solid is rectangular, hence mixed co-ordinate systems at the air-solid interface were necessary. As will be shown later, by using triangular meshes at this boundary, the problem was solved.

(ii) Boundary and initial conditions - at the hot end of the cavity, the temperature was fixed at the experimentally obtained value. At the cold end of the cavity similarly, the

temperature was fixed at T_{cold} . All the other boundaries were taken as zero heat flux regions. In the computer program this was done by putting the conductances associated with fictitious temperatures at zero conductances.

The initial temperatures within the grid were arbitrarily chosen.

(iii) Formulation of the nodal equations - detailed derivations of the equations are given in the Appendix. After completing the subdivision of the system, the thermal conductance K_{ij} between the nodes i and its adjacent j nodes must be calculated. The rate of heat flow q_{ij} (watts) from any node j to the adjacent node i is:

$$q_{ij} = K_{ij} (T_j - T_i) \quad (1-7)$$

The heat balance for the node i gives the equation:

$$\sum_j q_{ij} = \sum_j K_{ij} (T_j - T_i) = 0 \quad (1-8)$$

Using this energy-balance method, equations of the type shown below were obtained for the temperature (T_{299} - Figure B4) of an interior node:

$$\begin{aligned} & \{ \text{CXY}(298)T(298) + \text{CXY}(299)T(300) + \text{CYX}(425)T(425) + \text{CYX}(299) \\ & \quad T(173) + \text{CZX}(285)T(285) + \text{CZX}(299)T(313) \} \\ & \hline & \{ \text{CXY}(298) + \text{CXY}(299) + \text{CYX}(425) + \text{CYX}(299) + \text{CZX}(285) + \text{CZX}(299) \} \\ & \quad - T(299) = 0 \quad (1-8A) \end{aligned}$$

For a surface point, for example, nodal point 158, the radiation heat flow, and the air heat flow had to be taken account of.

Air conduction toward (or away from) the surface is evaluated using equation (1-7). The radiation exchange

within the enclosure is analysed using the net-radiation method. The basic heat balance equations for the net-radiative loss from surface k resulting from radiation in the enclosure are:

$$Q_k = A_k \frac{\epsilon_k}{(1 - \epsilon_k)} (\sigma T_k^4 - q_{o,k}) \quad (1-9)$$

and

$$Q_k = A_k (q_{o,k} - \sum_{j=1}^N F_{k-j} q_{o,j}) \quad (1-10)$$

where Q_k = net radiative loss from surface k , W

ϵ_k = emissivity of surface k

A_k = area of surface k , M^2

$q_{o,k}$ = total radiation leaving surface k , that is,
the radiosity, W/M^2

F_{k-j} = configuration factor

k, j = property of surface j or k

N = number of surfaces in the enclosure

Equations (1-9) and (1-10) are written for each of the six surfaces in the enclosure. This provides 12 equations for 12 unknowns. The radiosities ($q_{o,k}$) are the six unknowns. The remaining six unknowns are the Q 's (since the radiation regions temperatures are assumed (or guessed)). As shown in the Appendix, the Q 's are eliminated giving six equations relating the six unknown q_o 's and the T 's. The resulting system of equations is:

$$\sum_{j=1}^6 (\delta_{kj} - (1 - \epsilon_k) F_{k-j}) q_{o,j} = \epsilon_k \sigma T_k^4 \quad (1-11)$$

With the temperatures given, the q_o 's can be found from (1-11) and on substituting in (1-9), the radiation flows Q_k in the cavity are known.

Once the radiation flows in the cavity are known, using the energy-balance method, equations of the type shown below can be written for all surface points. The equation written below is for surface point 158 - Figure B3; the factor dQ_r/dT arises in getting the solution to converge as discussed in the next section.

$$Q_{r,3} + (dQ_r/dT)_{158} (T(158) - T_i(158) + K_{air,158} (T_{air} - T(158))) = \\ CX(158) (T(158) - T(159)) + CZ(158) (T(158) - T(172)) + CY(158) \\ (T(158) - T(32)) - CY(284) (T(284) - T(158)) \quad (1-12)$$

where $Q_{r,3}$ = radiation flow towards surface point 158

$T(158)$ = temperature of surface point 158 (to be relaxed)

$T_i(158)$ = initial temperature of surface point 158 (before relaxation)

K_{air} = thermal conductance of air associated with surface point 158

$(dQ_r/dT)_{158}$ = approximate change in radiation flow with temperature nodal point 158

the other variables are as described in the nomenclature section

In the computer program, a general expression (equation) was used for determining the nodal equations of interior, surface, and air points (see Appendix).

(b) Thermal conductance equations

For interior points conduction, the thermal conductances are calculated using the formula:

$$K_{ij} = k \left(\frac{A_{ij}}{L_{ij}} \right) \quad (1-13)$$

where k is the thermal conductivity

A_{ij} is the average surface area perpendicular to the direction of heat flow

L_{ij} is the distance between the nodes

The irregular boundaries produced as a result of the presence of the circular hole in the box element used for calculations required special treatment. The thermal conductance between such nodes was calculated by the unified method of Macneal (117). A justification of the use of this method is presented in the Appendix.

For the air thermal conductance calculations, equation (1-13) is written in cylindrical co-ordinates.

$$K_{ij} = 2\pi k L_{ij} / \ln (r_o / r_i) \quad (1-14)$$

The detailed calculations and theory of thermal conductance methods can be found in the Appendix where composite media, and boundary nodes are dealt with.

1.6.2.2.3 Solutions of the equations

(a) Radiation equations - equation (1-11) resulted in a set of six simultaneous equations. Since the right hand side was known and the left hand side consisted of a matrix of coefficients, matrix inversion (Gaussian elimination with total pivoting) was used to find the radiosities. With $q_{o,k}$ found, Q_k was found by substitution into (1-9)

(b) Heat balance equations - the heat balance equations of the form (1-8) and (1-12) are solved by successive over-relaxation. The relaxation procedure of solving potential

flow networks is well known and is only briefly described here (81,83,84). The heat flows into a node are summed, and if not zero, the temperature of the function is adjusted to make the net heat flows zero. Zero net heat flows at all nodes implied the desired steady-state solution had been found.

(c) Convergence technique - as mentioned above, to solve the heat balance equations, they are relaxed, and because these equations describe a potential flow situation, the results converge rapidly.

However, when the new temperatures are used to recalculate radiant fluxes and new heat balances are calculated from these, convergence does not occur between consecutive calculations of regional heat balances and radiant fluxes. Account must be taken, at least approximately, of the change in radiant flux as the temperature being relaxed is changed in the heat balance equations. The method of doing this is as follows.

It has been shown (17,69) that by considering the matrix of equations describing radiant fluxes in the electrical analogy, for any region s , $(dQ_r/dV)_s$ is constant. That is, if all the temperatures are constant, except that of region s , then the radiant flux to s is proportional to the voltage of s alone.

$$\text{But } V_s = \sigma T_s^4 \quad (1-15)$$

where V is the voltage in the electrical analogy, W/m^2

From (1-15),

$$(dV/dT)_s = 4\sigma T_s^3 \quad (1-16)$$

$$\text{and so } (dQ_r/dT)_s = (dQ_r/dV)_s 4\sigma T_s^3 \quad (1-17)$$

Since the radiation flow in the cavity is known before each set of iterations starts, $(dQ_r/dT)_s$ for each region is also known by evaluating equation (1-17). Hence equation (1-12), that is, the surface points heat balance can be solved. In this treatment, (dQ_r/dT) is regarded as being constant during the iteration.

1.6.2.2.4 Program flow sheet

The block diagram of the computer program used to solve the cavity problem is shown in Figure 1-2.

1.6.2.2.5 Reliability of solutions

In the simulation runs, the heat balances were attained to within 0.03%. The grid size was reasonable. It covered all the regions of the cavity problem well (Appendix). The configuration factors used were derived as shown in the Appendix, they were taken for the whole ring and disk rather than for finite radiation surface areas.

1.6.3 SURFACE TEMPERATURE MEASUREMENT

1.6.3.1 General Remarks

It is widely recognised that the output of a sensor such as a thermocouple or a thermometer represents an approximation to the temperature at some location in a fluid or a solid. There is no easy method of attaching a thermocouple to a surface so that it can be guaranteed to indicate the true surface temperature. To do this, it would be necessary to mount the measuring junction so that it could

attain, but not affect, the surface temperature.

(a) Measurement error - a significant difference will exist between the indicated temperature and the 'true' surface temperature, that is, the temperature that the surface would reach if no thermocouple were present. This difference is normally termed a 'measurement error', but it should not be confused with calibration or extension wire errors which are common to all thermocouple measurements. The relationship between the indicated and true surface temperature is often defined by the equation:

$$Z = (T_s - T_i) / (T_s - T_a) \quad (1-18)$$

where Z = installation factor

T_s = true surface temperature

T_i = indicated surface temperature

T_a = temperature of the surrounding or coolant

The value of Z for a particular installation may be calculated or found by experiment.

(b) Installation - in the experimental set-up used in this work, the thermocouple junction is installed in a groove. The groove is filled with araldite so that the surface is restored to its original profile. A thermocouple in a groove normally will have its junction below the surface and will indicate the sub-surface temperature. Details on thermocouple installation of this work are described in Chapter 2.

The measuring junctions of the thermocouples used in this work are made by twisting together bare thermocouple wires and then mounting them in a groove using araldite.

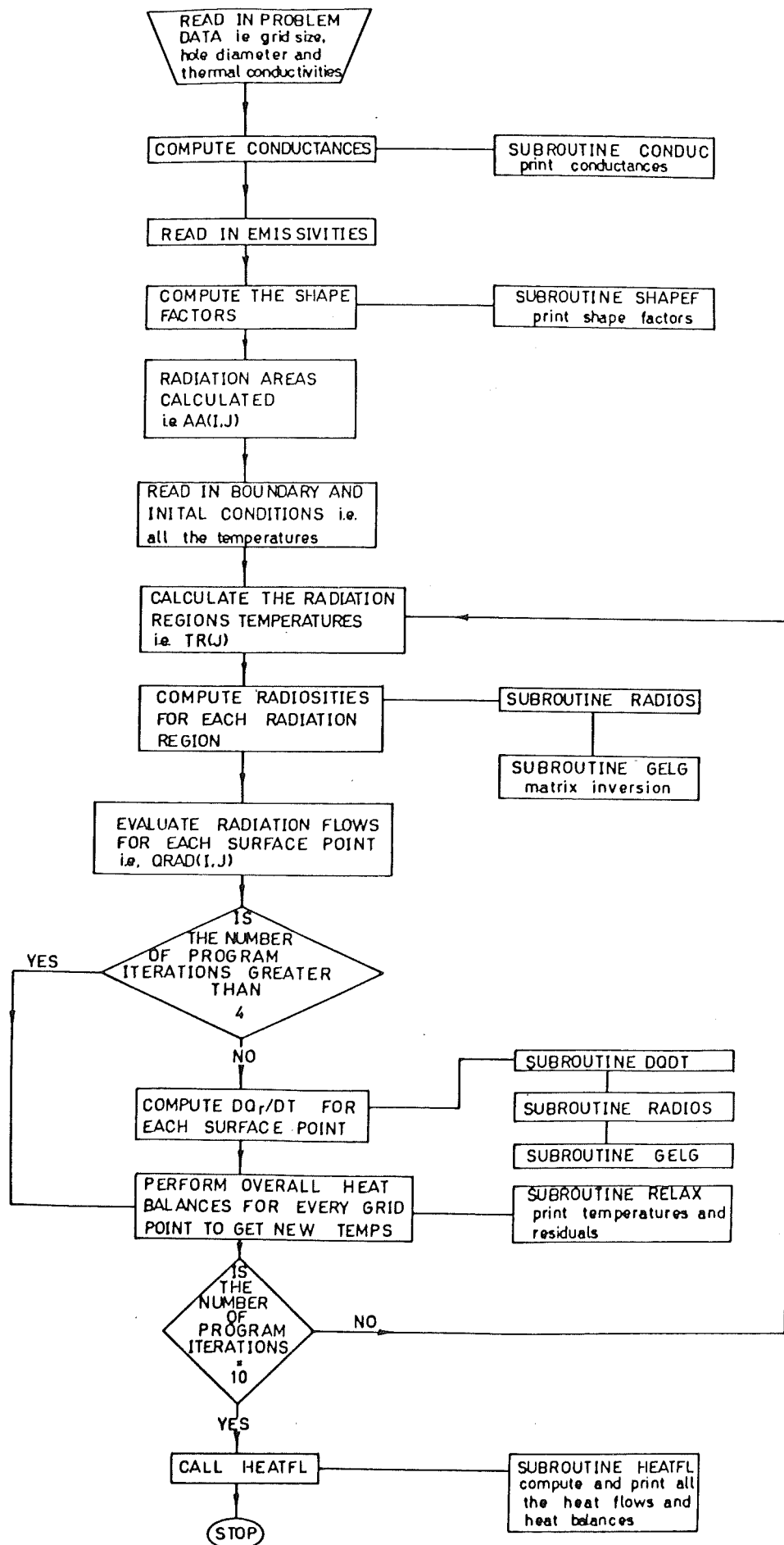


FIGURE 1-2 FLOWSHEET OF THE COMPUTER PROGRAM USED TO SOLVE THE CAVITY PROBLEM

1.6.3.2 Sources of Error

When a thermocouple is attached to a surface, its presence alters the heat transfer characteristics of the surface and normally will change the temperature distribution. This causes an error which is referred to as the perturbation error.

Causes of perturbation error are:

(i) The heat transfer characteristics of the surface are changed by the installation of the thermocouple. That is, the surface emissivity and effective conductivity will be altered and/or the wires act as fins providing additional heat transfer paths - the so called 'conduction error of thermocouples' (118).

As will be shown later, the presence of another material, that is, the adhesive araldite, causes a distortion of heat flow in the immediate vicinity of the measuring junction.

(ii) Thermal contact resistance between the junction and the surface causes a temperature gradient which prevents the measuring junction from attaining the correct temperature.

Other causes of uncertainty in the measurement of surface temperatures include:

- the possibility of the thermocouple junction being in a small air pocket.

- the position of the thermocouple junction in relation to local inhomogeneities in the surface of the sample; and also the uncertainty in the exact position of the junction relative to the surface.

- different and possibly varying thermal resistances between the samples and the plates at the positions where the thermocouple wires are installed.

- although not discussed in this Chapter (see Chapter 2 and the Appendix), the errors associated with thermocouple measurements, such as deviations from standard emf and lead wire errors, must be taken into consideration.

1.6.3.3 Prior Work on Error Determination in Surface Temperature Measurement

The perturbation error must be determined if the surface temperature must be known with a high degree of accuracy. The error, and hence the correction factor, has been determined by various investigators using the following methods for steady-state conditions:

(a) Direct calculation - The direct calculation of the error involves solving the heat flow equation for the measuring junction and surface geometry (115). Simplifying assumptions are made, and the results interpreted in relation to them. Numerous publications (20,50,118,119,120) have used this approach and have clearly shown the major sources of error. They also indicated means of reducing these errors. Singh (121) recently (August 1976) used this approach to calculate the error in temperature measurements due to conduction along the sensor leads and compared theoretical results with experimental results and obtained good agreement.

(b) Analog methods - Analog methods of solving the heat transfer equations using resistance or resistance-capacitance networks have been used to indicate the overall

temperature distribution (50,120,122,123). These methods have shown the perturbation effects of the thermocouple clearly. They have, however, also shown that they are difficult methods to make flexible, and so they required a number of analog models to simulate various heat transfer conditions.

(c) Relaxation methods - Although these methods have been mentioned in the literature as being suitable for error determination calculations in surface temperature measurements, no work was found that applied them. As will be shown later, they were used in this work to solve the heat transfer equations associated with surface temperature determination (section 1.6.3.4).

(d) Experimental methods - Direct experimental measurement on the installation has been found to be one of the most satisfactory ways of accurately determining the perturbation error (118). Care and precision had to be taken to simulate the service conditions exactly as changes in any variable significantly affected the results. The major problem found was in determining the true surface temperature. This has been discussed extensively in the literature (123,124,125,126,127,128).

Baker (129) has discussed surface temperature measurement techniques, errors and minimisation of errors in numerous practical installations. The work of Eckert and Goldstein (115) is noteworthy in this respect too.

1.6.3.4 Method of Solution - Surface Temperature Measurement

1.6.3.4.1 Problem statement

The objectives of this part of the thesis are:

- (1) to determine whether the temperatures indicated by the thermocouple wires were the true surface temperatures.
- (2) to determine the temperature profiles of the aluminium plates (hot and cold) in the presence and absence of the thermocouple grooves.
- (3) to test the hypothesis that the aluminium plates were so large in size in comparison to the thermocouples, thermocouple grooves, and araldite adhesive that their presence could be ignored.

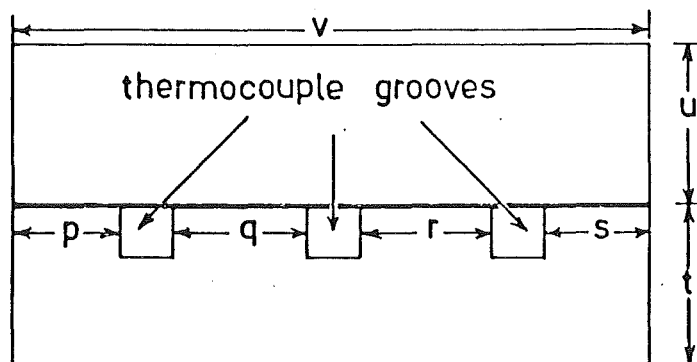
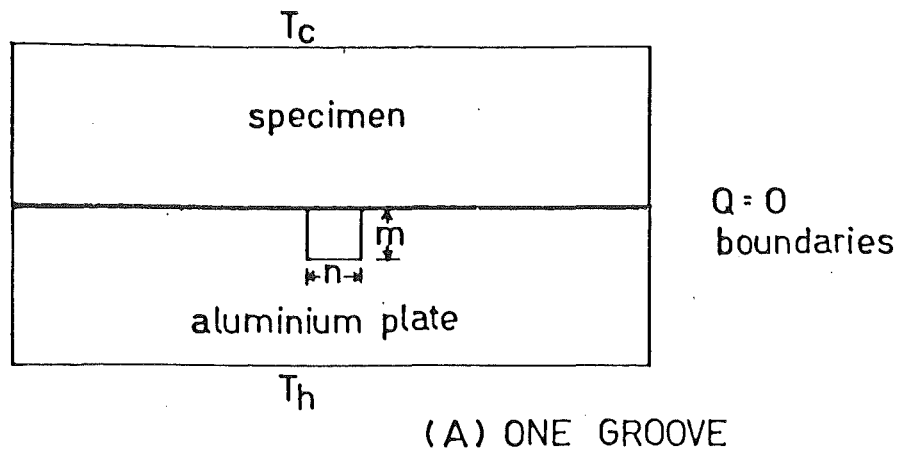
1.6.3.4.2 Assumptions

The general assumptions used in formulating the solution to the problem outlined above are:

- (a) most of the finite difference assumptions outlined in section 1.6.2.1.1, that is, zones of constant temperature, physical properties of the system evaluated at average temperatures, and no heat generation
- (b) steady-state, two-dimensional flow
- (c) zero heat flux at two of the boundaries and fixed temperatures at the other two boundaries

1.6.3.4.3 Physical formulations

In simulating the surface temperature measurements, a cross-sectional view of the hot guarded plate apparatus was considered (see Chapter 2). Considered were three basic physical arrangements of different linear dimensions - Figure (1-3).



(B) THREE GROOVES

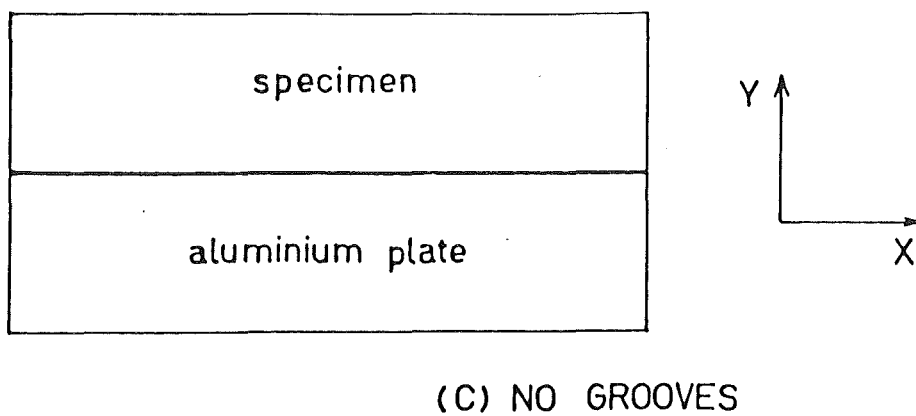


FIGURE 1-3 SKETCHES OF THE TWO DIMENSIONAL CONFIGURATIONS USED IN THE SURFACE TEMPERATURE SIMULATIONS

(a) One groove - the aluminium plate was assumed to have only one thermocouple groove of various dimensions.

(b) Three grooves - the aluminium plate with three grooves (as used in the experiment) was considered.

(c) No grooves - the aluminium plates were assumed to have no groove (or grooves) in them. This arrangement gave the theoretically ideal results, that is, the temperature profiles that were assumed in the calculation of the results in Chapter 4.

The finite-difference approximations to the problem were set up by dividing the physical arrangements mentioned above into nodes as shown in the Appendix.

1.6.3.4.4 Mathematical formulation

(i) General description of the procedure - the method used is an iterative one using relaxation techniques. From the physical formulation, finite difference approximations are applied to the Fourier equation (1-1) in two dimensions. The resulting finite difference equations are solved using successive overrelaxation by first guessing all the unknown temperatures; the boundary conditions are, of course, known. Using these temperatures, heat balances are calculated for each region and temperatures are adjusted until the heat balances are satisfied. This procedure is repeated until no further worthwhile changes occur.

(ii) Finite difference approximations - as the only mode of heat flow in opaque solid materials is conduction, the basic heat transfer equation used is the Fourier equation. Consequently, the nodal equations are derived

from equations (1-7) and (1-8). Using the heat balance method for a region, the resulting relaxation equation is of the exact form as equation (1-8A). The only difference is that now it is in two dimensions and not three, hence fewer terms.

Applying equations (1-7) and (1-8) to nodal point $i+m$ for example, the resulting relaxation equation is:

$$\frac{(CA_{i+m-1} T_{i+m-1}) + (CA_{i+m} T_{i+m+1}) + (CU_i T_i) + (CU_{i+m} T_{i+2m})}{(CA_{i+m-1} + CA_{i+m} + CU_i + CU_{i+m})} - T_{i+m} = 0 \quad (1-19)$$

where m = number of nodal points in the x-direction

(Figure 1-3)

CA_i = thermal conductance between nodal points i and $i+1$ in the x-direction, $W/^\circ C$

CU_j = thermal conductance between nodal points j and $j+m$ in the y-direction, $W/^\circ C$

T_k = temperature of nodal point k in degrees celsius

As shown from Figure 1-3, the specimens considered are rectangular in cross-section, consequently, the choice of grid was no problem, a rectangular grid was used. The various sizes of the mesh are shown below. In all runs, nodal points were concentrated in regions of high temperature gradients.

The boundary conditions used were zero heat flux at the edges as indicated in Figure 1-3. To obtain the boundary temperatures, fictitious temperature nodes were used whose

thermal conductances were put at zero, and their equations were neither formulated nor relaxed (see Appendix). In a few runs, the boundary conditions of constant edge temperature were used in attempts to verify the program.

(iii) Thermal conductance equations - the equations used for evaluating the conductances are exactly the same as those used for the cavity problem solutions, that is, equation (1-13).

1.6.3.4.5 Numerical solution of the equations

All the equations obtained are of the form of equation (1-19), that is, they are linear heat balances. As previously mentioned, successive overrelaxation was used to solve them.

The program flow sheet used to solve the equations is shown below.

1.6.3.4.6 Numerical simulations carried out

Numerous computer runs were used to simulate the surface and experimental conditions (both physical and thermal conditions), in order that surface temperature profiles, and true surface temperatures could be obtained. In this work, only a few of these simulation runs are presented. Sixteen different simulation runs are presented in two parts. The first part consists of runs numbered 1 to 10. These simulate conditions that are not used in the experiment, but are physically close to the experimental conditions. For example, runs 1 and 2 simulate thermocouple grooves of linear

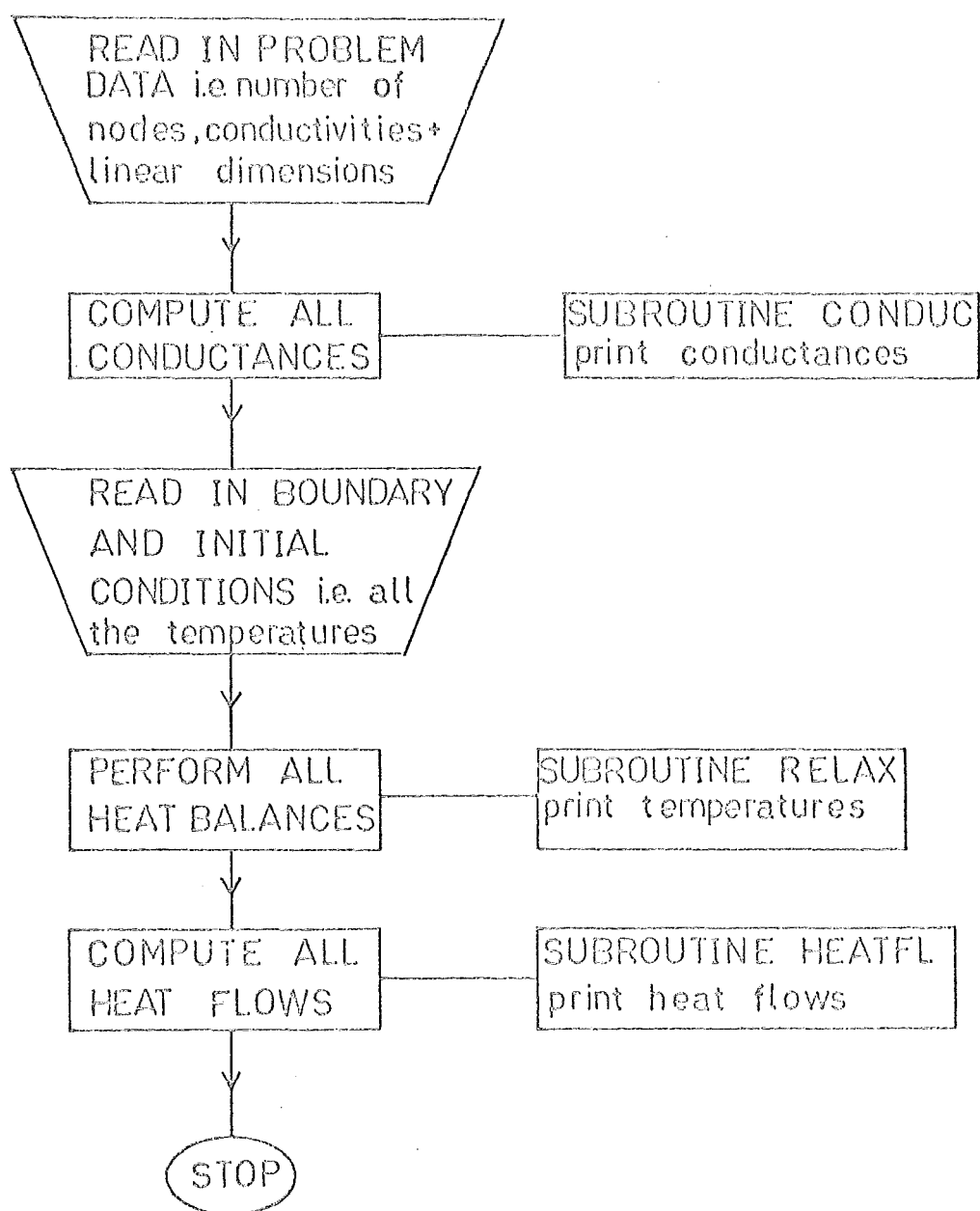


FIGURE 1-4 FLOWSHEET FOR SURFACE TEMPERATURE SIMULATION PROGRAM

dimensions 5mm by 5mm. In the experiment, the actual size of the grooves is 2.38mm by 2.38mm. Simulation runs numbered 11 to 16, correspond exactly to the experimental conditions. For example, run 12 uses thermocouple grooves of 2.38mm by 2.38mm. These runs (11 to 16) make up the second part of the simulation.

SIMULATION RUNS - PART I

(a) Runs 1 and 2 - in these two runs, aluminium inserts of two sizes were put in the one groove configuration of Figure 1-5. In run 1, the aluminium insert is 3mm by 4mm, that is, $a = b = 1\text{mm}$. In run 2, it is 4.99mm by 4mm, that is, $a = 0.005\text{mm}$ and $b = 1\text{mm}$.

In each run, the linear dimensions used are:

$$u = 3\text{mm}$$

$$t = 8\text{mm}$$

$$v = 19\text{mm}$$

$$m = n = 5\text{mm}$$

The grid used in each run has the same number of nodal points in the x-direction, that is, $M = 20$, and those in the y-direction, that is, $N = 11$ (see Appendix). The distance between any two nodal points both in the x and y directions is 1mm. The assumed thermal conductivities are:

$$\text{for aluminium, } k = 200 \text{ W/M}^{\circ}\text{C}$$

$$\text{araldite, } k = 0.7 \text{ W/M}^{\circ}\text{C}$$

$$\text{specimen, } k = 1 \text{ W/M}^{\circ}\text{C}$$

Run 1 simulates the case where araldite is present on the sides of the groove in bulk, and the aluminium insert

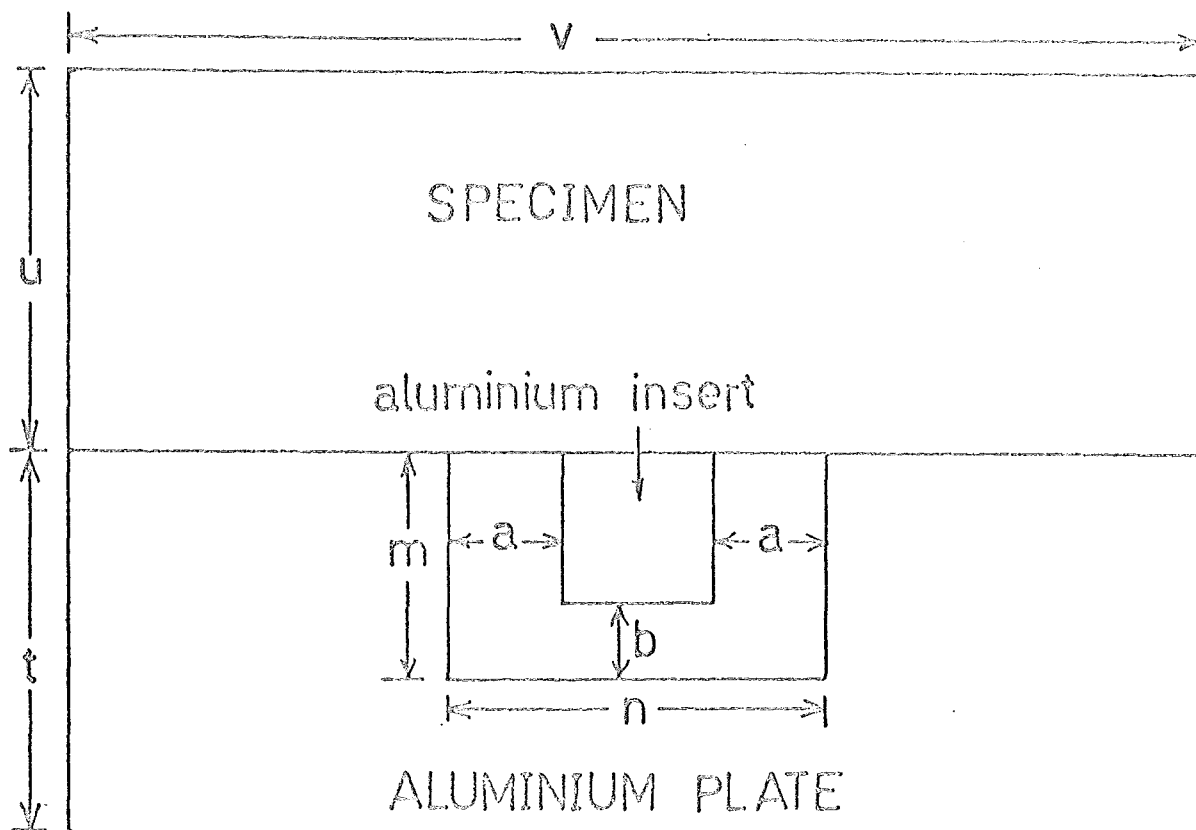


FIGURE 1-5 SKETCH OF THE PHYSICAL CONFIGURATION USED IN RUNS 1 and 2

does not fit tightly in the thermocouple groove. The 1mm gap at the bottom of the groove ('b'), is large enough to accommodate the 36 gauge thermocouple wires.

Run 2 simulates the case where the aluminium insert is machined to close tolerances so that it fits tightly in the thermocouple groove, leaving very little room (0.005mm) for any araldite to get caught between the insert and the aluminium plate. Again, enough room is left at the bottom of the cavity to accommodate the thermocouple wires.

(b) Runs 3 and 4 - these two runs were used to show the differences between the two possible boundary conditions. Run 3, like all the other simulation runs, uses zero heat flux boundary conditions at the edges, while run 4 uses constant temperature conditions at the edges (assumes uniform heat flux). The grid used is exactly the same as that used for runs 1 and 2, that is, $M = 20$ and $N = 11$. The thermocouple groove used in each run is a 2.38mm square groove with no aluminium insert. The groove is full of araldite of assumed thermal conductivity $0.167 \text{ W/M}^{\circ}\text{C}$ for run 3 and $0.282 \text{ W/M}^{\circ}\text{C}$ for run 4. The thermal conductivity of the specimen is taken as $0.167 \text{ W/M}^{\circ}\text{C}$ in both runs, and that of aluminium as $238.4 \text{ W/M}^{\circ}\text{C}$. The linear dimensions used as referred to in Figure 1-3A are:

$$u = 1.428\text{mm}$$

$$t = 3.808\text{mm}$$

$$v = 9.044\text{mm}$$

$$m = n = 2.38\text{mm}$$

General remarks about simulation runs 5 to 10:

(i) Boundary conditions - for all runs, the hot

boundary temperature was taken as 45.14°C and the cold boundary as 43°C . Zero heat flux boundary conditions were taken for the remaining two boundaries.

(ii) Thermal conductivities - the thermal conductivity of aluminium at the mean temperature was taken as $238.4 \text{ W/M}^{\circ}\text{C}$, that of araldite was taken as $0.282 \text{ W/M}^{\circ}\text{C}$ and that of the specimen as $0.167 \text{ W/M}^{\circ}\text{C}$. See the Appendix for the verifications of these values.

(iii) Program constants - the overrelaxation factor used in all runs was 1.26. All the temperatures were relaxed to within 0.005°C .

(c) Runs 5 and 6 - for run 5, the one groove configuration of Figure 1-3A was used. The thermocouple groove considered in this run is 2.38mm square. In run 6, there is no groove, that is, the place where the groove would have been is completely filled up by aluminium, corresponding to Figure 1-3C. Run 6 results gave the ideal complement to the results of run 5. The latter shows the effects of having a thermocouple groove, while the former shows the ideal case where the groove does not exist.

The grids used for both runs had $M = 20$ and $N = 26$. The dimensions used are:

$$m = 2.38\text{mm}$$

$$v = 9.044\text{mm}$$

$$t = 6.188\text{mm} \text{ (this corresponds approximately to the thickness of the aluminium plates used in the experiment)}$$

$$u = 6.188\text{mm} \text{ (this corresponds approximately to the } 1/4" \text{ PMMA specimens used in the experiment)}$$

(d) Runs 7 and 8 - as one thermocouple groove was used in both these runs, Figure 1-3A applies. For run 7, the groove depth is taken to be twice the actual experiment groove depth, that is, $m = 4.76\text{mm}$, while the breadth of the groove is halved, that is, $n = 1.19\text{mm}$. This run was used to simulate a deep narrow thermocouple groove.

For run 8, however, the depth of the groove is kept at 2.38mm (experimental value), but the breadth is halved, that is $n = 1.19\text{mm}$.

For both runs 7 and 8, the grid used had $M = 20$ and $N = 26$. The other linear dimensions are:

$$t = u = 6.188\text{mm}$$

$$v = 4.522\text{mm}$$

Using runs 5, 6, 7, and 8, the effects of one groove of various dimensions on the surface temperatures were deduced. The effects of having three thermocouple grooves in the aluminium plates are now investigated.

(e) Runs 9 and 10 - run 9 simulates the experimental set-up exactly. Three grooves are considered in the simulation, hence Figure 1-3B is applicable. The linear dimensions used are exactly those mentioned in Chapter 2. They are summarised as follows:

$$n = m = 2.38\text{mm}$$

$$t = 6.35\text{mm} \left(\frac{1}{4}''\right)$$

$$u = 6.35\text{mm}$$

$$p = s = 125.4\text{mm}$$

$$r = q = 71.44\text{mm}$$

$$v = 400.82\text{mm}$$

Run 10 is the ideal experimental set-up with no thermocouple grooves, so that it provides the ideal results for complementing the actual results of run 9. The linear dimensions are exactly the same as those for run 9, except that m and n are not applicable of course, Figure 1-3C.

The grids used for both runs are with $M = 32$ and $N = 13$. (See the Appendix for conductance evaluation details for regions with thermocouple grooves in them (run 16)).

Table 1-1 summarises the surface temperature computer simulation runs numbered 1 to 10. In the table, all the linear dimensions are in millimeters and the symbols used are referred to Figure 1-3.

SIMULATION RUNS - PART II

As previously mentioned, computer runs numbered 11 to 16 constitute this part of the simulation. For all these runs, the following conditions are used:

(i) Boundary conditions - the hot boundary temperature was taken as 45.14°C , and the cold boundary as 43.0°C . Zero heat flux boundary conditions were used for the remaining two other boundaries.

(ii) Thermal conductivities - the thermal conductivity of aluminium at the mean temperature was taken as $238.4 \text{ W/M}^{\circ}\text{C}$, that of araldite as $0.282 \text{ W/M}^{\circ}\text{C}$, and that of the specimen (perspex) as $0.167 \text{ W/M}^{\circ}\text{C}$.

(iii) Program constants - the overrelaxation factor was 1.26 and all the temperatures were relaxed to within 0.005°C .

TABLE 1-1

Qualitative Results of the Surface Temperature Simulation Runs 1 to 10

Simulation Run Number	Number of Grooves	Groove Dimensions in mm		Linear Dimensions of the Physical Layout in mm Figure 1-3			Grid Size		Boundary Conditions in °C		Thermal Conductivities in W/M °C			General Comments
		m	n	t	u	v	M	N	Th	Tc	aluminium	araldite	specimen	
1	1	5	5	8	3	19	20	11	100°C	20°C	200	0.7	1.0	3mm x 4mm aluminium insert put in groove
2	1	5	5	8	3	19	20	11	100°C	20°C	200	0.7	1.00	4.99mm x 4mm aluminium insert put in the groove
3	1	2.38	2.38	3.808	1.428	9.044	20	11	45.14	43.68	238.4	0.167	0.167	constant temperature boundary conditions
4	1	2.38	2.38	3.808	1.428	9.044	20	11	45.14	43.68	238.4	0.282	0.167	
5	1	2.38	2.38	6.188	6.188	9.044	20	26	45.14	43.00	238.4	0.282	0.167	this run simulates the experiments approximately
6	no groove is present, solid aluminium covers where the groove should have been			6.188	6.188	9.044	20	26	45.14	43.00	238.4	0.282	0.167	this run gives the ideal temperature profile for run 5
7	1	4.76	1.19	6.188	6.188	4.522	20	26	45.14	43.00	238.4	0.282	0.167	a deep narrow groove is simulated
8	1	2.38	1.19	6.188	6.188	4.522	20	26	45.14	43.00	238.4	0.282	0.167	a narrow groove is simulated
9	3	2.38	2.38	6.35	6.35	400.82	32	13	45.14	43.0	238.4	0.282	0.167	16 nodal points put in each groove
10	no grooves are present, solid aluminium covers where the grooves should have been			6.35	6.35	400.82	32	13	45.14	43.0	238.4	0.282	0.167	no grooves are present - this gives the ideal temperature profile for run 9

(iv) Linear dimensions - the linear dimensions as referred to Figure 1-3 are as follows:

$$t = u = 6.35\text{mm}$$

$$p = s = 125.4\text{mm}$$

$$r = q = 71.44\text{mm}$$

$$v = 400.82\text{mm}$$

The number of grooves and the groove dimensions varied with each run, consequently the values of q and r for example were applicable only when three grooves were considered. The grid used for all the runs had $M = 32$ and $N = 17$.

(a) Run 11 - in this run, one groove $2.38\text{mm} \times 2.38\text{mm}$ is considered with a $1.5875\text{mm} \times 1.5875\text{mm}$ ($1/16"$ square) aluminium insert in it. The dimensions in the groove region are thus:

$$m = n = 2.38\text{mm}$$

$$a = 0.39625\text{mm} \text{ (1/64")}$$

$$b = 0.7925\text{mm} \text{ (1/32")}$$

This run simulates a possible configuration of the apparatus with very small gaps on the sides of the groove and a gap at the bottom of the groove large enough to fit the thermocouple wires.

(b) Run 12 - in this run, one groove $2.38\text{mm} \times 2.38\text{mm}$ is considered. This simulates another possible experimental set-up in which only one groove rather than three could have been used.

(c) Run 13 - three grooves are considered of shallow depth but same width (or breadth) as used in the experiment. The linear dimensions of the grooves being:

$$m = 0.952\text{mm}$$

$$n = 2.38\text{mm}$$

(d) Run 14 - one deep groove is considered in this configuration, the width is exactly the same as used in the experimental set-up. The linear dimensions of the groove are:

$$m = 5.026\text{mm}$$

$$n = 2.38\text{mm}$$

(e) Run 15 - in this run, the ideal temperature profile for all the other simulation runs of Part II is presented. No grooves are present in this simulation, only solid aluminium. Since the experimental set-up linear dimensions are used, this run represents the ideal temperature profile for the experimental set-up used in this thesis.

(f) Run 16 - this run represents the experimental set-up as it is in this work (Chapter 2). Three grooves of 2.38mm x 2.38mm linear dimensions are considered.

Table 1-2 presents a summary of all the simulation runs of Part II, that is, runs numbered from 11 to 16. As all the linear dimensions, grid sizes, boundary conditions, and thermal conductivities are the same for each run, only the groove characteristics are presented in the table shown.

1.6.3.4.7 Quantitative computed
results of the surface temperature simulation runs

The surface temperature results are presented in tabular form (Tables 1-3 to 1-8), with the positions of the thermocouple grooves as indicated in the tables of results. As the simulations of runs 11 to 16 approximated the experimental conditions, only this range of results is presented in this section. The results of simulation runs 1 to 10 are presented in the Appendix, where the computer listings with the various

TABLE 1-2

Qualitative Results of the Surface Temperature Simulation Runs
Numbers 11 to 16

Simulation Run Number	Number of Grooves	Groove Dimensions in mm		Comments
		m	n	
11	1	2.38	2.38	1/16" x 1/16" aluminium insert in groove
12	1	2.38	2.38	Simulating one groove instead of three
13	3	0.952	2.38	Simulating three shallow grooves
14	1	5.026	2.38	Simulating one deep groove
15	No grooves are present, solid aluminium covers where the grooves should have been			Ideal temperature profiles
16	3	2.38	2.38	Actual experimental set up used in this work

Figure 1-3
Temperature profile of simulation run 11 showing
the 1 groove configuration with a 1.6mm x 1.6mm
aluminium insert in the groove

[illegible]

TABLE 1-1.
Temperature profile of simulation run 12
showing the 1 groove configuration

[illegible]

TABLE 2-5
Temperature profile of simulation run 13
showing the 3 shallow groove configuration

[illegible]

TABLE 1-7
Temperature profile of simulation run 15
showing the ideal temperature profile of
the no groove configuration

[illegible]

TABLE 1-3

78

problem data used, for example, conductances and heat flows are also presented.

1.6.3.4.8 Discussion of the surface temperature results

In this part of the thesis, the effects of having thermocouple grooves in the aluminium plates are discussed. The optimal number and dimensions of the grooves are also discussed. However, not discussed are the effects of actually having the thermocouple wires in the grooves. That is, although the dimensions of the thermocouple wires are taken into consideration in the dimensioning of the simulation grooves, their actual physical presence is ignored. The conduction errors, and the thermal conductivities due to the thermocouple wires are ignored in the simulations.

As expected (see the discussions of prior work done on surface temperature measurement), if a thermocouple groove is introduced, the temperature profile of the surface is distorted. Table 1-4 (showing the results of a one-groove configuration) shows this clearly. Without the thermocouple groove, all the temperatures in the aluminium block are equal to 45.14°C (run 15), however, once a thermocouple groove is introduced, temperature gradients result. This phenomena is also shown clearly by run 16 where three grooves are present (runs 5 and 6 in the Appendix show this effect also). In the grooves, the temperature at the specimen-araldite interface is 45.03°C , and it increases towards the aluminium surface temperature of 45.14°C at the bottom of the groove. This comment applies to all other runs with grooves in them, the exception being run 7. Since the introduction of a thermo-

couple groove (or grooves) causes very significant temperature and heat flux profile distortions (all runs except 6, 10 and 15), the exact positioning of a thermocouple in a groove is important in ascertaining the true surface temperature. For example, if in run 12 (driving force $dT = 2.14^{\circ}\text{C}$) a thermocouple measuring junction was positioned 0.952mm from the side of the groove and at a depth of 0.952mm from the bottom of the groove, the temperature it would indicate, assuming no conduction and other thermocouple wire errors (as discussed in section 1.6.3.2), would be 45.12°C . The true (or correct) surface temperature being 45.14°C (from runs 12 and 15). The true surface temperature being defined as the temperature of the surface when no thermocouple grooves are present (Figure 1-3C). For example, 45.14°C for run 15.

The introduction of an aluminium insert in the groove tends to smooth out the sharp temperature gradient at the araldite-specimen interface. Runs 11 and 12 show this effect clearly. In run 12, where the insert is not present, the specimen does not have a large influence on the temperature gradient in the groove. However, with the aluminium insert in the groove (run 11), the specimen seems to have a very significant effect on the temperature distribution in the groove. In fact, in run 11, the temperature at 0.476mm from the bottom of the groove is 44.54°C which is significantly different from the correct aluminium surface temperature of 45.14°C . While the presence of an aluminium insert in the groove helps to smooth out the sharp temperature gradients at the araldite-specimen interface, it does not

help to bring the thermocouple wires in the groove any closer to monitoring the correct surface temperature. Runs 1 and 2 also verify this fact. In run 1, for example, the true surface temperature is between 98.85°C and 98.98°C , while the thermocouple wires placed at the bottom of the groove would indicate a reading between 91.2°C and 99.79°C . As a consequence, in the experimental set-up (Chapter 2) used in this work, no aluminium inserts were put in the thermocouple grooves.

The temperature profile in the thermocouple groove obtained when using the one groove configuration (Figure 1-3A) is exactly the same as that obtained when using the three groove configuration (Figure 1-3B). The araldite-specimen interfacial temperatures are the same in both cases too. Runs 12 and 16 verify these statements. For instance, in run 12, the temperature at 0.476mm from the bottom of the groove is 45.13°C . This is exactly the same temperature indicated in the three groove configuration (run 16) at the same groove position. In the experimental set-up, the three groove configuration is thus adopted (justifications for this choice of configuration is presented in the next section).

Three shallow thermocouple grooves (run 13), do not give very good estimates of the true surface temperatures. They give far worse estimates than run 16 (that is, the adopted configuration for the experimental set-up). In run 13, the temperature indicated at a depth of 0.476mm from the bottom of the shallow thermocouple groove is 45.10°C . This is as compared to 45.13°C for run 16, and 45.14°C for the true surface temperature, run 15.

One deep groove (simulation) gives the desired result, subject to the measuring junction being placed less than 0.476mm from the bottom of the groove. At this distance from the bottom of the groove, the temperature is equal to the surface temperature. From run 14, at a distance of 0.476mm from the bottom of the groove, the indicated temperature is 45.14°C which is the correct surface temperature. Run 7 shows that for a deep groove, the other linear dimensions, that is, the width of the solid material on either side of the groove needs to be large before the surface temperature can be attained at the bottom of the groove. In run 7, a deep narrow groove with the other linear dimensions small is considered. The true surface temperature is close to 44.13°C , but the indicated temperature at the bottom of the groove is close to 44.75°C .

Reliability of the Solutions

Numerous simulation runs were devised to verify the validity and accuracy of the computer solutions. Apart from the simulation runs already discussed above (runs 1 to 16) in which different problems were solved, many other runs were performed with the following conditions:

- (1) different initial and boundary conditions
- (2) different tolerances of the temperature accuracies, that is, the tolerances were sometimes put as low as 10^{-6}
- (3) different grid sizes (in the runs 1 to 16, different sizes were used)
- (4) different relaxation parameters - the problem was solved both by overrelaxation, that is, W greater than 1 and less than 2; and by underrelaxation, W was put at 0.8

In all cases, the computed temperatures had converged and the heat balances satisfied. Since the computer program converged under all these trying conditions, the program was verified.

1.6.3.4.9 Optimal approximations

Although one deep thermocouple groove (run 14) gave a better approximation of the true surface temperature (see below) in the experimental set-up (Chapter 2), three grooves were used (exactly as set out in run 16). The three groove configuration was chosen for three primary reasons.

(1) More thermocouple wires could be put in the three grooves (9 thermocouples), and as the grooves were spread over a large area of the aluminium plates, they gave a better estimate of the temperature of the aluminium plate. By having more thermocouple wires, inherent experimental errors (for example, the uncertainty in the exact positions of the measuring junctions in the grooves) were averaged (smoothed) out.

(2) The experiments undertaken using the guarded hot plate apparatus were based on the assumption that uni-directional heat flow existed (section 1.6.1.6). To verify this assumption, the temperatures at various positions of the aluminium plates were required. The three groove configuration fulfilled this requirement.

(3) The temperatures indicated in the three groove configuration were not far removed from the true surface temperatures (and also those indicated by the one groove configuration) bearing in mind that thermocouple circuits

at their best performances give temperatures accurate to within $\pm 0.02^{\circ}\text{C}$. This figure was also the indicated maximum deviation from the true surface temperature in the groove (discussed above - runs 11 to 16) at temperatures between 45.14°C and 43.0°C . (These are typical experimental temperatures for $\frac{1}{4}$ " perspex as the specimen - experiments series A.)

1.6.3.5 Thermal Contact Resistance

At the interface between two materials held together in unbonded contact, there is a resistance to heat flow due to imperfect contact. This thermal resistance between the two surfaces is called the contact resistance. In the experimental set-up used in this work (Chapter 2), the specimen (usually perspex) is in contact with the hot and cold aluminium plates of the hot guarded plate apparatus. As a result, there are contact resistances between the specimen and the aluminium plates. Estimates of the magnitudes and hence importance of these resistances were required.

1.6.3.5.1 Prior work on thermal contact resistance

Although the thermal conduction contribution to heat transfer at contacts has been recognised for a long time, the amount of scientific and engineering work performed to understand this problem has been fairly limited.

Cetinkale and Fishenden (130) are among some of the earliest workers in this field. They described measurements of the thermal contact conductance for steel, brass and aluminium surfaces ground to various degrees of roughness,

and with air, spindle oil, or glycerol between the contacting surfaces. They measured the contact conductances for a range of contact pressures. Reasonable agreement was also obtained between the experimental results and an approximate analytical solution for which the surface roughness, the thermal conductivities of the metal and fluid, the applied pressure, the hardness of the softer metal, and the mean contact temperature must be known.

Other investigators worthy of note who have dealt with this subject in detail include: Fried (131), Fenech and Rohsenow (132) and Mikic (133,134). A thorough review of the subject of interfacial resistance is dealt with more recently by Fried E. in Tye's book (135).

1.6.3.5.2 Method of estimating the thermal contact resistance

Heat transfer through an interface takes place by combined mechanisms of conduction across true contact points, conduction across entrapped interstitial fluid, and radiation across interstitial gaps. Resulting overall conductance of the joint is therefore a function of the materials in contact (conductivity, surface finish, flatness, and hardness), the contact pressure, the mean temperature and heat flux across joint, the nature of interstitial fluid (liquid, gas, vacuum), and the presence of oxide films.

Various publications (51,132) have presented graphs of thermal interface conductance data for various materials under different conditions. None of the conditions or the data presented simulated the experimental conditions used in this work. As a result, using the guarded hot plate apparatus

with perspex as the specimens, experiments were performed to try to determine the surface contact conductance in this work. The details and results of these runs will be presented in Chapters 3 and 4. * However, briefly the runs consisted of measuring the thermal conductivities of perspex pieces with no lubrication on them, and then lubricating them with a light oil on both faces and measuring the thermal conductivities again. The light oil film provided good thermal contact between the specimens and the aluminium plates. The differences in thermal conductivities between the two runs should have given estimates of the effects of surface conductances. As will be seen in Chapter 4, no significant difference between the runs resulted. Consequently, no estimate of the surface contact resistance was obtained.

1.6.3.6 Concluding Remarks on Surface Temperature Measurement

Since the thermal contact resistance is small and can be neglected, the only source of error in determining the temperatures of the specimens is in the measurement of surface temperature. By careful design, the thermocouple measuring junctions can be made to monitor the surface

* In Laboratory experiments in the Chemical Engineering Department, University of Canterbury involved with measuring surface temperatures of apparatus using thermocouples attached to copper contact shoes, it had been found that silicone grease between the copper shoe and the surface being measured significantly increased the accuracy of the measurements.

temperature to within $\pm 0.02^{\circ}\text{C}$ of the true value. From the numerical simulation runs, the optimal number of thermocouple grooves was found to be three, and the best location of the measuring junctions was found to be at a distance of not more than 0.476mm from the bottom of the 2.38mm square groove.

1.7 CONCLUSION

To analyse the cavity problem fully, separate experimental measurements of gas conduction, solid conduction and radiation heat flows are required. As research into the cavity problem continued, it became clear that a complete solution to the problem would take years to complete. As a result, the work outlined in this thesis was directed at providing the theoretical and experimental basis for future work.

The experimental apparatus was designed, built and tested. The discrepancies between the experimental and the theoretical results varied between 2 and 26%. The experimental error was 12%.

CHAPTER 2EQUIPMENT

2.1	<u>THE APPARATUS AND EXPERIMENTAL TECHNIQUE</u>	91
2.2	<u>EQUIPMENT DESIGN CONSIDERATIONS</u>	91
2.2.1	GENERAL REMARKS	91
2.2.2	DESIGN CONSIDERATIONS OF LOW TEMPERATURE GUARDED HOT PLATE	92
2.2.2.1	Design of the Plates	92
2.2.2.2	Design of the Heating Circuit	93
2.2.2.3	Surface Temperature Measuring	94
2.2.2.4	Sample Requirements	95
2.2.2.5	Miscellaneous Design Requirements	95
2.3	<u>DESCRIPTION OF APPARATUS</u>	96
2.3.1	LOW TEMPERATURE GUARDED HOT PLATE	101
2.3.1.1	Hot Plate	101
2.3.1.2	Cold Plate	103
2.3.1.3	Miscellaneous Plate Details	103
2.3.2	TEMPERATURE MEASURING EQUIPMENT	105
2.3.2.1	Thermocouple Wires	105
2.3.2.2	Thermocouple Circuit	106
2.3.2.3	Thermocouple Circuit Equipment	106
2.3.2.4	Reference Junction	109
2.3.3	ELECTRICAL POWER SUPPLY EQUIPMENT	109
2.3.3.1	D.C. Regulated Power Supply	111
2.3.3.2	A.C. Regulated Power Supply	111
2.3.3.3	Heating Element	111
2.3.3.4	Power Measuring Instruments	112
2.3.4	AUXILIARY EQUIPMENT	112
2.3.4.1	The Thermostatic Bath	112
2.3.4.2	Miscellaneous Equipment	113

2.3.5	SPECIMENS	113
2.4	<u>CALIBRATION OF EQUIPMENT</u>	114
2.4.1	CALIBRATION OF THERMOCOUPLES	114
2.4.1.1	Working Standard	115
2.4.1.2	Measurement of emf	115
2.4.1.3	Calibration Using Comparison Method	115
2.4.1.4	Procédure of Calibration Using the Comparison Method	116
2.4.1.5	Method of Interpolating Between Calibration Points	119
2.4.1.6	Discussion of Calibration Uncertainties	120
2.4.1.6.1	Uncertainties which influenced the observations	120
2.4.1.6.2	Uncertainties due to interpolation between calibration points	121
2.4.1.7	Concluding Remarks	122
2.4.2	CALIBRATION OF REFERENCE JUNCTION	122
2.4.2.1	General Comments	122
2.4.2.2	Working Standard	122
2.4.2.3	Calibration Method	122
2.4.2.4	Calibration Results	123
2.4.2.5	Concluding Remarks	123
2.4.3	CALIBRATIONS OF INSTRUMENTS USED WITH THERMOCOUPLES	123
2.4.4	CALIBRATION OF POWER SUPPLY EQUIPMENT	124
2.4.5	CALIBRATION OF PLATES	125
2.4.5.1	Flatness of the Plates	125

2.4.5.2	Temperature Drops Across The Specimens	125
2.4.5.2.1	Determination of 'temperature-drop' differences	126
2.4.5.2.2	Results of the positioning experiments	128
2.4.5.2.3	Concluding remarks	130
2.5	<u>EXPERIMENTAL PROCEDURE</u>	130
2.5.1	APPARATUS PREPARATION	130
2.5.2	ASSEMBLY OF APPARATUS	131
2.5.3	OPERATION OF APPARATUS	132
2.5.4	EXPERIMENTAL DETERMINATIONS	133
2.5.4.1	Thermal Conductivity	133
2.5.4.2	Thermal Conductance	133
2.5.4.3	Thermal Conductance with Aluminium Foil in the Holes	134

CHAPTER 2

EQUIPMENT

2.1 THE APPARATUS AND EXPERIMENTAL TECHNIQUE

In the tests it was necessary to generate, control, and measure the following systems: thermal conductivity of specimen material, heat flux, isothermal faces, cell orientation (shape and size as well), and material (type and thickness).

2.2 EQUIPMENT DESIGN CONSIDERATIONS

2.2.1 GENERAL REMARKS

(1) Maximum and minimum working temperatures - two different types of guarded hot plate apparatus are described in the literature (6). The low temperature guarded hot plate, which has metal surface plates and a definite guard gap, is generally used for measurements over the approximate temperature range 90° to 600°K . The high temperature guarded hot plate, which may or may not have metal surface plates, and may or may not have a definite guard gap, is ordinarily used for measurements where the hot plate temperature is greater than 550°K and less than 1350°K . In this work, the low temperature guarded hot plate apparatus was used since the materials available locally were of the building, refrigeration, and other constructional varieties (temperature range 200 to 400°K).

(2) As previously mentioned (Chapter 1), it is practically impossible to distinguish between the solid conduction contribution to the total heat transferred and

the thermal radiation contribution experimentally in the cavity problem. As such, the experiments had to be designed so that they could be performed in two parts. The first part of each experimental series of runs was concerned with measuring heat transfer rates in an opaque solid - where solid conduction is the only mechanism of heat transfer. The second part of the experiments also measured the rates of heat transfer for the same temperature differences as those used in the first part, the difference being that holes were drilled in the opaque solids to induce radiation and gaseous conduction. For different temperature differences, hole sizes, thicknesses of material and materials, different ratios of radiation to solid conduction were obtained. Hence the radiation and solid conduction contributions to the total heat transferred could be assessed.

As a result, the apparatus was designed so that:

- (a) it could accommodate various sizes of materials (specimens)
- (b) dismantling and assembling of the test stack could be done quickly and easily

2.2.2 DESIGN CONSIDERATIONS OF LOW TEMPERATURE GUARDED HOT PLATE

The general features of the metal surfaced guarded hot plate are shown schematically in Figure 2-4.

2.2.2.1 Design of the Plates

The materials of construction of the plates had to withstand the operating temperatures. As the maximum operating temperature is 600°K , most metals would suffice.

The plates had to be:

(a) of sufficient thickness such that warping would not result

(b) made of non-corroding metal of high thermal conductivity

(c) of constant surface properties - the emissivity of the plates had to be of constant value during the experimental runs

(d) rigid enough to retain their linear dimensions and flatness during all operating conditions

Other design considerations for the plates include:

(i) methods of attaching the heating elements to the hot plates so that the electrical power dissipated could be divided evenly between the two specimens

(ii) adequate cooling for the heat dissipated by the heating elements

(iii) methods of attaching thermocouple wires to both the hot and cold plates

2.2.2.2 Design of the Heating Circuit

The various components used in the heating circuit had to:

(a) withstand the operating temperatures

(b) provide a steady heat input into the hot plates; this electrical supply is required not to interfere with the operations of the thermocouple wires

(c) provide enough electrical power to heat both the central metering section and the guard ring areas of the plates

Methods of measuring the electrical power had also to be considered.

2.2.2.3 Surface Temperature Measuring

The analyses of surface temperature measurement errors in Chapter 1 have shown some procedures that should be followed in order to obtain better estimates of surface temperatures. These procedures and the specifications of surface temperature measuring given in the A.S.T.M. Standard C177-71 (5) are considered as the design requirements in ascertaining the correct surface temperature measurements in the experiment. They are summarised as follows:

- (1) Use the smallest possible installation (thermocouple wires and grooves) to avoid perturbation errors.
- (2) Bring the thermocouple wires away from the junction along an isotherm for at least 20 wire diameters to reduce conduction errors. The use of thin thermocouple wires or thermocouple wires with low thermal conductivity will also reduce this error.
- (3) Locate the measuring junction, as mentioned in Chapter 1, at the optimal position.
- (4) Design the installation so that it causes a minimum disturbance of change in the emissivity of the surface, to avoid changes in radiative heat transfer.
- (5) Design the installation so that the total response is fast enough to cause negligible lag for the transients expected in service.
- (6) Reduce the thermal resistance between the measuring junction and the surface to as low a value as possible.

Other design considerations of surface temperature measuring include: having enough thermocouple wires in the central section of the plates, and also having a means of

finding the temperature differences between the central section and the guard ring areas.

2.2.2.4 Sample Requirements

The test sample should be composed of two similar pieces (specimens) of a requisite uniform thickness and cross-section. These pieces should be as flat as possible so that intimate contact between specimens and plates can be achieved. The physical properties of the specimens must be constant over the operating temperature range, for example, the moisture content should be constant, and so should the linear dimensions. The specimens should have a low thermal conductivity so that adequate temperature differences can be achieved. As holes will be drilled in the specimens, they need to be machineable.

These pieces (specimens) should be cut so that they represent areas equivalent to the central and guard sections respectively. This serves two purposes:

(1) The area, A , used in the calculation of the thermal conductivity (conductance) is clearly defined in terms of the side of the central piece rather than including an additional half the gap width.

(2) Radial conduction is reduced and a more uniform temperature distribution throughout the sample can be maintained.

2.2.2.5 Miscellaneous Design Requirements

- Provide means for (i) imposing a reproducible constant pressure of the plates against the specimens to promote good thermal contact. (ii) measuring the effective thicknesses

and other linear dimensions of the specimens.

- Provide means of reducing heat losses from the outer edges of the guard section and the specimen.

- Provide a cabinet or enclosure to surround the guarded hot plate. This enclosure should maintain the desired interior air temperature and the dew point in order that condensation is prevented. It also must allow the heat generated in the enclosure to escape at a sufficient rate at the operating temperatures.

2.3 DESCRIPTION OF APPARATUS

The general layout of the installation is shown in Figures 2-1 and 2-2. Electrical energy is supplied into the guarded hot plate apparatus from the mains A.C. supply through an A.C. regulator and a D.C. regulator. This power input is measured using a digital voltmeter and a digital ammeter. Using the nine thermocouple wires on each face of the isothermal plates, the temperature of each plate is known by monitoring the thermocouple wire outputs using a Cambridge Laboratory precision potentiometer. The thermocouple measuring circuit is shown in detail in Figure 2-9. The environmental conditions are kept constant by immersing the guarded hot plate set in a stainless box in a well stirred water thermostatic bath kept at 31°C . The thermostatic bath is kept at this constant temperature by using cooling coils (from the main cold water supply), an immersion heater, and a bias heater connected to a temperature controller. Since the room in which the experiments were performed was air conditioned (room temperature was $22^{\circ}\text{C} \pm 3^{\circ}\text{C}$), all the thermocouple circuit junctions were assumed



FIGURE 2-1

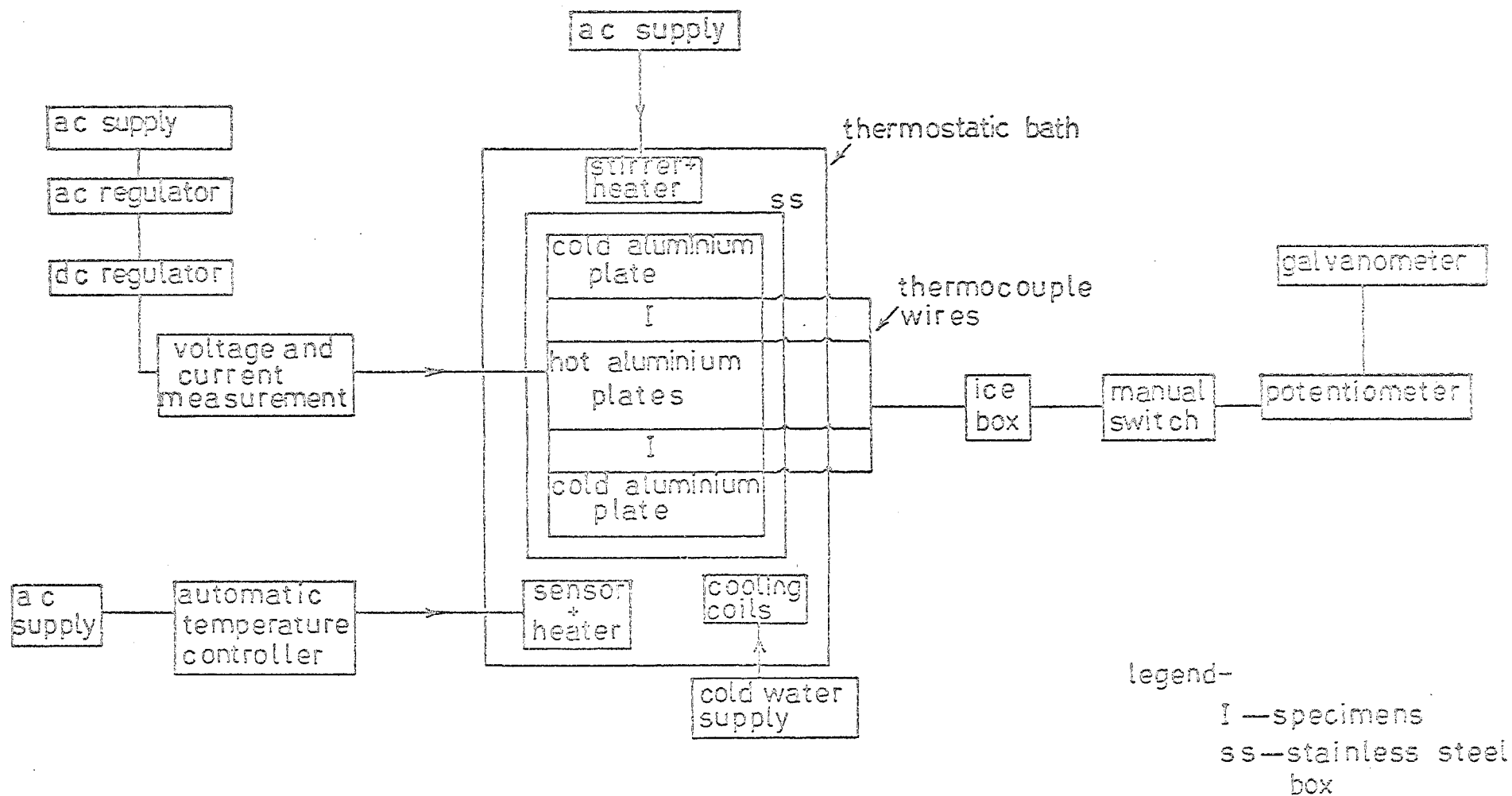


FIGURE 2-2 FLOW DIAGRAM OF THE INSTALLATION

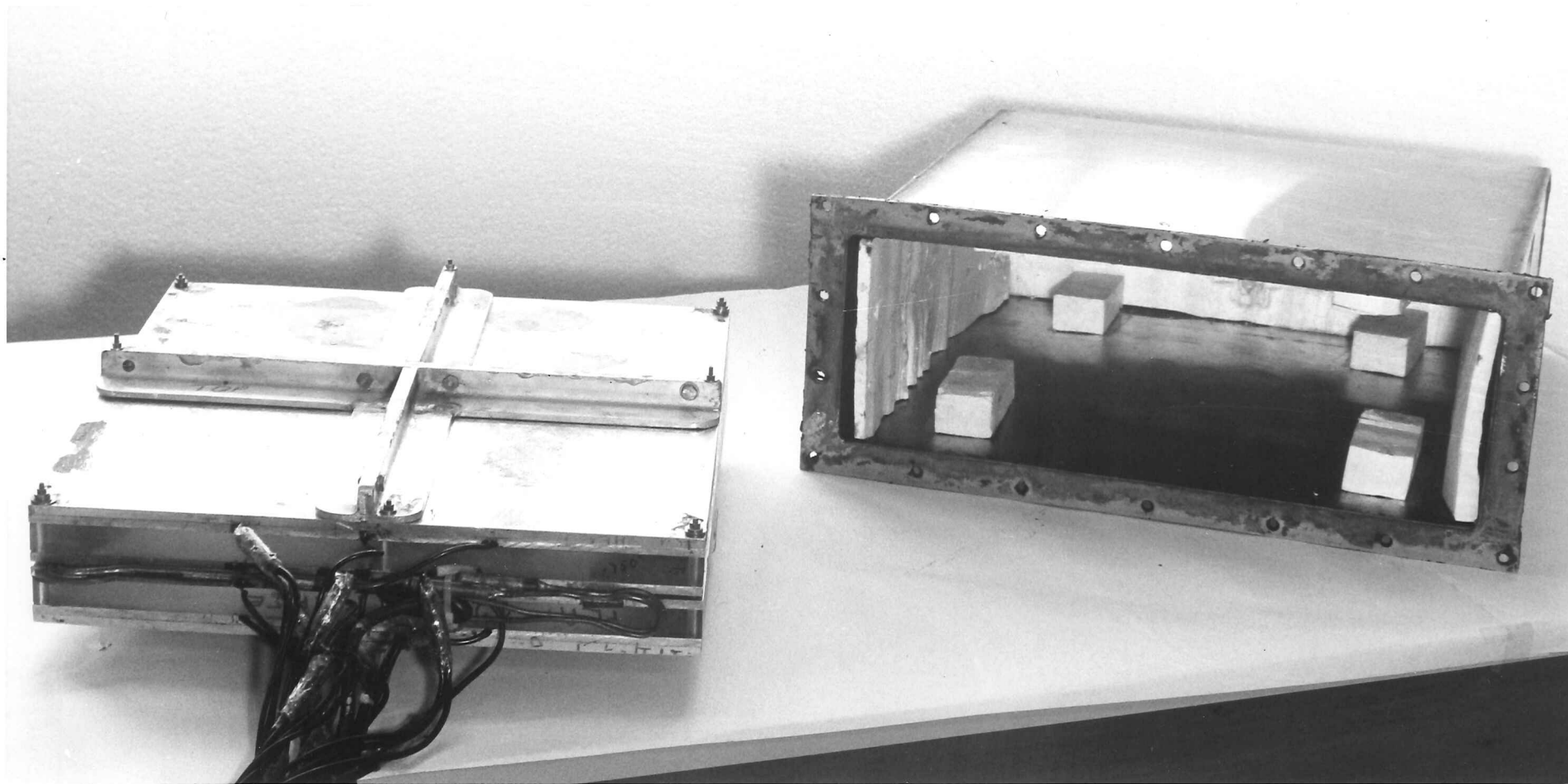
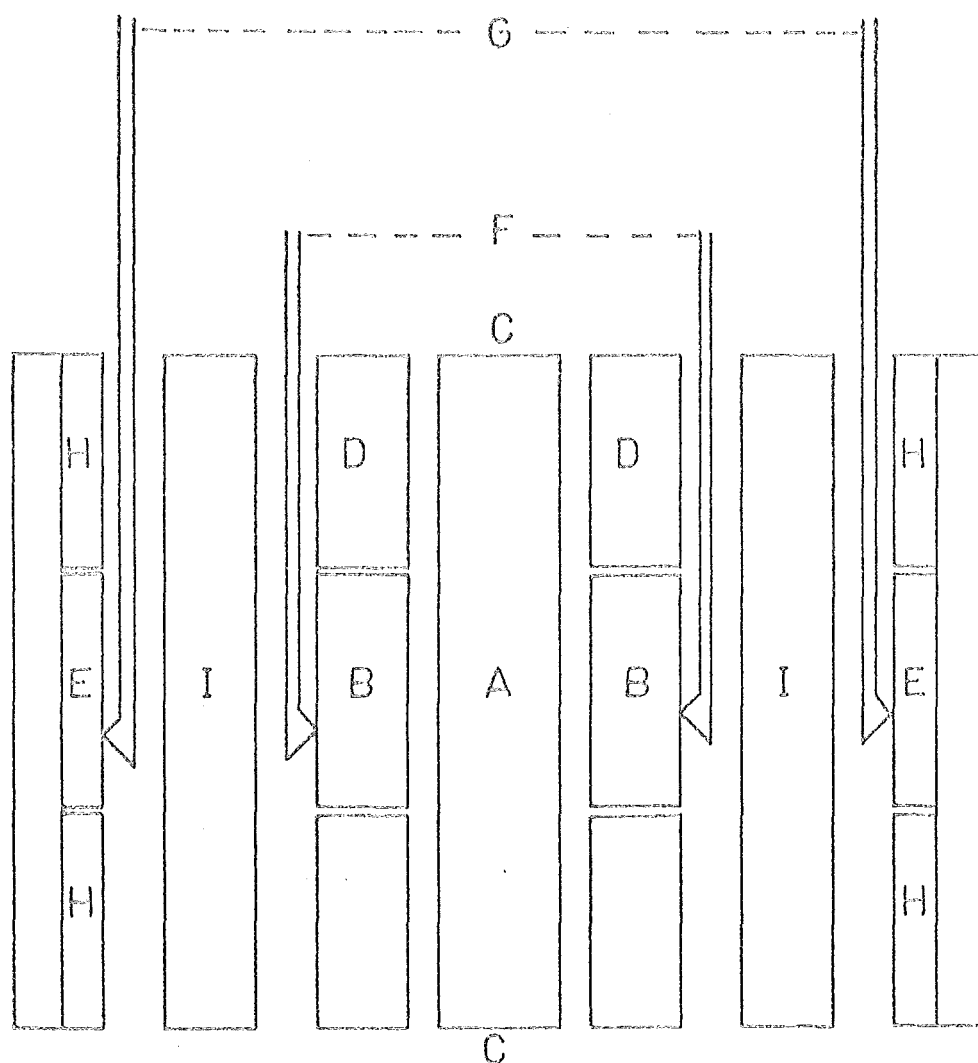


FIGURE 2-3



- A—central heater core—the same coil is used to heat the metered section B and the guard section D
- B—central surface plates—aluminium hot plates metered area
- C—guard heater area of the main heater A
- D—guard surface plates (aluminium hot plates)
- E—cold aluminium plates
- F—heating unit surface thermocouples
- G—cooling unit surface thermocouples
- H—guard area of the cold aluminium plates
- I—test specimens

FIGURE 2-4 SCHEMATIC ASSEMBLY OF THE LOW TEMPERATURE GUARDED HOT PLATE

LEGEND FOR FIGURE 2-5

1. Thermostatic water bath
2. Stirrer assembly
3. Controlled heater
4. Main water bath heater
5. Thermister probe connected to temperature controller
6. Water
7. Stainless steel box (enclosure) containing the
 guarded hot plate
8. Polystyrene edge insulation
9. Polystyrene studs
10. Air contained in the box
11. Cold aluminium plate
12. Test specimen
13. Hot aluminium plate

to be at the same temperature.

The individual equipment items are presented below.

2.3.1 LOW TEMPERATURE GUARDED HOT PLATE

The major part of the equipment used in this work consisted of the low temperature guarded hot plate apparatus. This apparatus was adapted from one designed by Gilbo (2) in 1957. It meets the requirements of the A.S.T.M. method C177. The guard heaters used to ensure uni-directional heat flow in the A.S.T.M. method are replaced by an envelope hot plate (Figure 2-4). Also the isothermal heat sink provided by a circulating liquid in the A.S.T.M. method is now provided by enclosing the outer faces of the conductivity cell in sheets of high conductivity material (aluminium) and placing the whole unit inside a stainless steel box, in a tank of coolant (Figure 2-5).

2.3.1.1 Hot Plate

The general features of the aluminium hot plate are shown in Figure 2-7. The aluminium plates are 398.5mm square, and are of thicknesses 6.35mm ($\frac{1}{4}$ ") on either side of the 3.1mm diameter pyrotenax heating cable. The metered central section and the guard section are of almost equal area and are separated by a gap of 1.6mm ($1/16$ "). The metered central section is 200mm square with a set of nine thermocouple wires (36 gauge copper-constantan) in accurately machined (150mm x 2.38mm x 2.38mm) grooves. The positions of the thermocouple wires in the grooves are shown in Figure 2-7. The measuring junction of each thermocouple pair was placed as close as possible to the bottom of the groove. Both

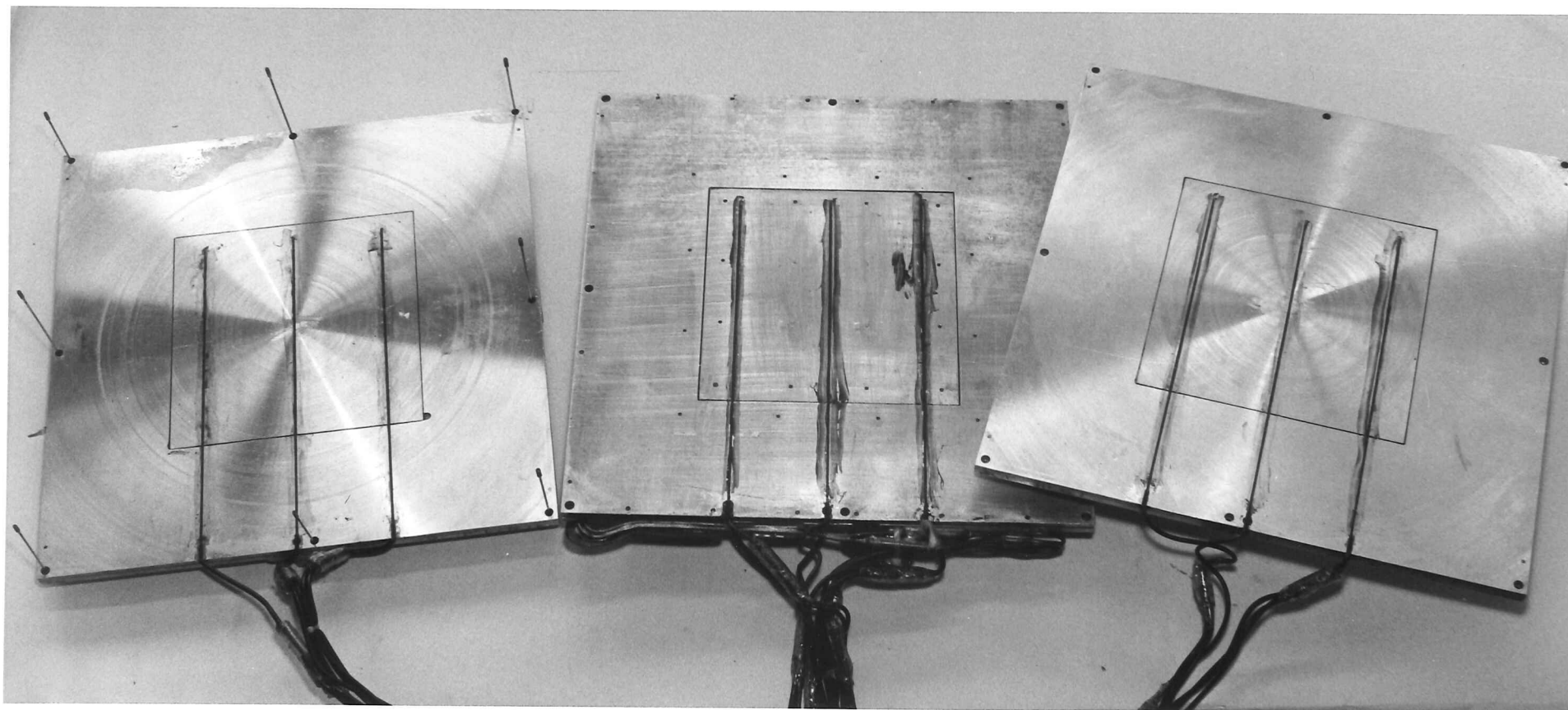


FIGURE 2-6

faces of the aluminium hot plate were machined to within $\pm 0.03\text{mm}$ ($0.001''$). Heat was supplied to the hot plate by 30 metres of pyrotenax heating cable (specifications in section 2.3.3). The cable was kept a constant diameter by the aluminium studs shown in Figure 2-7B.

2.3.1.2 Cold Plate

A section through the aluminium cold plates is shown in Figure 2-8. The heat sink (aluminium cold guarded plates) is made from two sheets of aluminium $398.5\text{mm} \times 398.5\text{mm} \times 6.35\text{mm}$. These two sheets of aluminium were held together by eight aluminium screws on the outer edges of the plates, and by metal-to-metal adhesive in the centre of the plates. As in the hot plates, a metered central section and a guard section were provided. In fact, the plan view of each heat sink ('E' in Figure 2-4) is exactly the same as the plan view of the hot guarded plates (Figures 2-6 and 2-7).

2.3.1.3 Miscellaneous Plate Details

The cold plate construction described above was found to provide adequate cooling for the temperatures desired. The cold aluminium plates maintained a lower uniform temperature than that of the heating unit by thermal air insulation provided on the outermost faces. Polystyrene edge insulation was provided as shown in Figure 2-5. Polystyrene insulation was not used all around the apparatus because of the low temperature drops across the specimens (perspex especially). Consequently, to get large temperature drops, air was used as the thermal insulator. Experimental runs with fibreglass insulation right around the apparatus are described in Chapter 3.

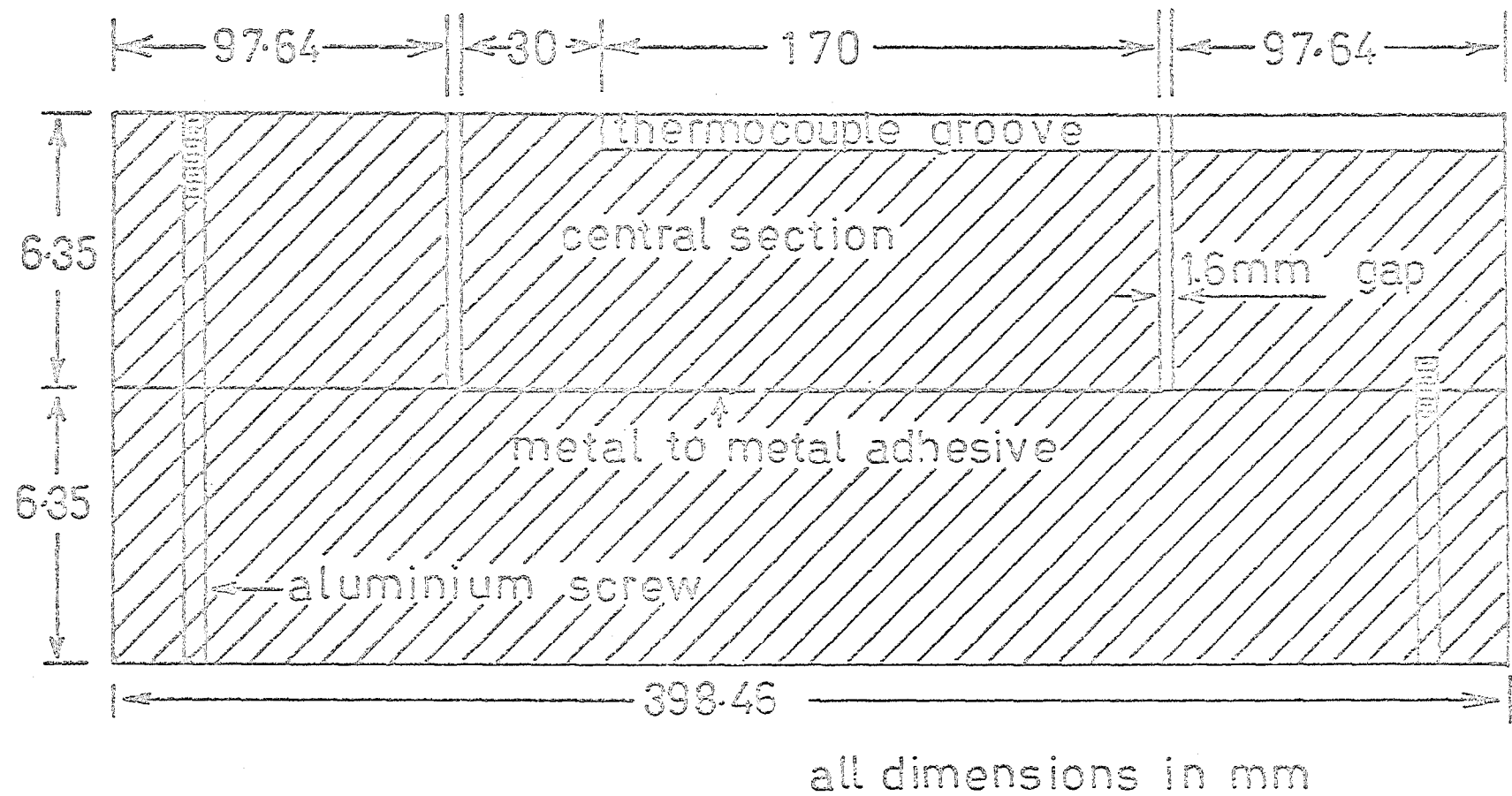


FIGURE 2-8 SECTION THROUGH COLD GUARDED PLATE

Figure 2-3 shows the guarded hot plate apparatus assembled. The aluminium support crossbars (one on top and the other at the bottom) are used for providing (a) rigidity to the assembled apparatus and (b) good thermal contact between the aluminium plates and the specimens. The plates are held together by using 1.6mm (1/16") stainless steel studs of varying lengths according to the thickness of the specimens. The studs are in 6.35mm (1/4") holes so that they do not touch the aluminium plates. If they touched the aluminium plates, they would provide thermal short circuits for the heat flows.

Figure 2-6 shows the apparatus dismantled.

2.3.2 TEMPERATURE MEASURING EQUIPMENT

The surface temperatures of the guarded hot plate apparatus were measured using copper-constantan thermocouple wires. The reference junction, room, and water bath temperatures were measured by mercury-in-glass calibrated thermometers.

2.3.2.1 Thermocouple Wires

The thermocouple wires used were numbered from 1 to 37. Number 37 was the reference junction pair (Figure 2-9). Apart from showing the unassembled plates, Figure 2-6 also shows the guarded hot plate laid out in order of assembly. The thermocouple wires attached to the cold aluminium plates shown on the right in Figure 2-6 were numbered 1 to 9. The wires fixed on the top of the hot plate in Figure 2-6 were numbered 10 to 18. Those on the bottom of this plate were numbered 19 to 27. The wires attached to the cold plate shown on the left (with the aluminium studs in the Figure)

were numbered 28 to 36.

36 gauge copper wire was used as the positive leg of each pair and constantan as the negative leg. The copper wire was cotton-covered as supplied by British Driver Harris Company Limited. For thermocouple wires numbered 1 to 32, 36 gauge cotton-covered constantan wires was used, and for wires numbered 33 to 37, 39 gauge cotton-covered constantan wire was used. The differences between the resulting thermocouple pairs are discussed in the calibration section.

2.3.2.2 Thermocouple Circuit

Figure 2-9 shows the thermocouple circuit used. For ease of numbering the measuring junctions associated with each thermocouple pair, a measuring counter 'i' is used in Figure 2-9. For thermocouple wires numbered 1 to 9, $i = 1$; for wires 10 to 18, $i = 10$; for wires 19 to 27, $i = 19$; and for thermocouple wires numbered 28 to 32, $i = 28$. The terminal block three metres away from the measuring junctions was maintained at a uniform temperature by insulating with polystyrene and fibreglass insulation. All the junctions including one from the reference junction were brought to it. Copper wires were then led to the insulated double pole selector switch and on to the potentiometer.

2.3.2.3 Thermocouple Circuit Equipment

The thermocouple selector switch is a 'CROPICO' - 2 pole, 50 position manual rotary switch with a motorised option which was not used. The switch has gold-silver alloy contacts on copper studs ensuring low invariable contact resistance and negligible thermal emfs. This switch is model S.P.2, instrument number 20085 and was supplied by

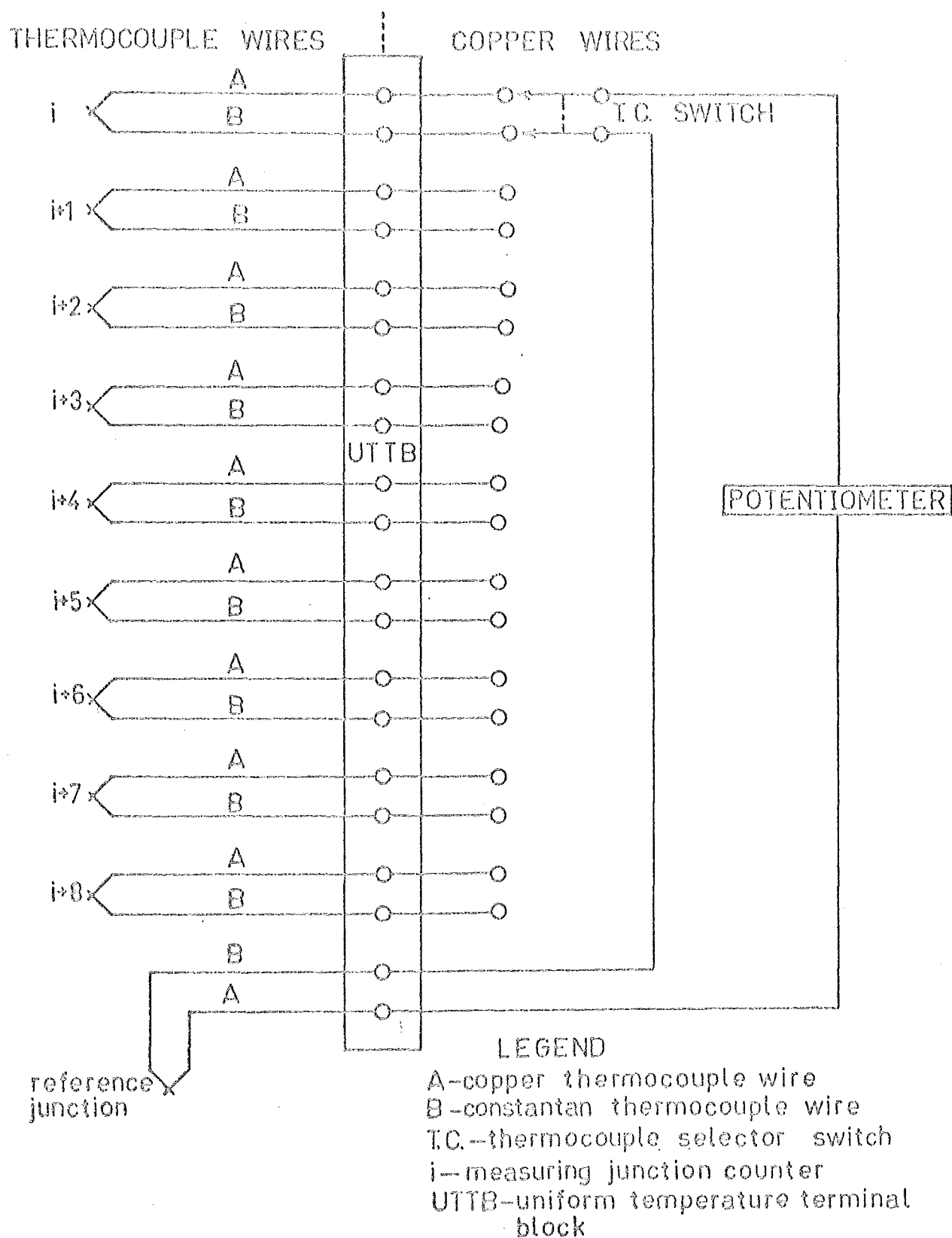


FIGURE 2-9 THERMOCOUPLE MEASURING CIRCUIT

Croydon Precision Instrument Company.

The potentiometer used for measuring the thermocouple wire outputs was a Cambridge Laboratory precision potentiometer, type 44228. This potentiometer was designed primarily for the measurement of d.c. potentials up to 101mV. Two potential dials are provided. The main potential dial controls a multi-point switch that has 100 steps of 1mV, each step being defined by a light, positive 'click stop'. The contact surfaces of the switch are plated with rhodium. The fine potential dial, controlling a calibrated slide wire, has a range of -0.05mV to +1.05mV, giving an overlap of 0.05mV above and below each step of the main potential dial. It is divided at intervals of 0.01mV, allowing estimations of 0.002mV, and can be turned continuously through maximum back to minimum reading.

The galvanometer fitted with the potentiometer was disconnected from the potentiometer terminals by removable links. A Kipps-Zonen galvanometer with about twenty times the sensitivity of the Cambridge galvanometer was connected to the potentiometer terminals. The Kipps-Zonen ('microva') galvanometer used had a full scale deflection of 20cm for a measuring range of 2 microamps at an internal resistance of 125 ohms.

The specifications of the potentiometer can be summarised as follows:

Range: 101mV

Voltage Subdivisions: 100 steps of 1mV (main dial)

110 divisions of 0.01mV over

range of -0.05 to +1.05mm

(fine dial)

Accuracy: $\pm 0.1\%$ or $\frac{1}{2}$ slidewire division (0.005mV),
whichever is the greater

Discrimination: 0.002mV

Resistance: 200 ohms/V

2.3.2.4 Reference Junction

The reference junction built was based on the constant temperature ice bath model E962 designed by the Rosemount Engineering Company Ltd. The reference junction set-up is shown in Figures 2-1 and 2-10. The ice bath consists of a 3.5 litre dewar flask, surrounded by polystyrene insulation. The dewar flask is 200mm deep and is of 150mm inside diameter. Distilled water and flaked ice made therefrom are used as the bath medium. The reference junction thermocouple wires are contained in a 3mm O.D. x 2mm I.D. glass tube. The tube is tapered to 1mm O.D. at the measuring junction end. The reference junction thermocouple pair was immersed to a depth of 150mm.

Agitation of the ice bath medium was not required (see section 2.4). The ice bath temperature was measured by a calibrated mercury-in-glass (-20°C to $+20^{\circ}\text{C}$) thermometer.

2.3.3 ELECTRICAL POWER SUPPLY EQUIPMENT

The maximum available d.c. voltage (power) supply was 50 volts. As a result, when more than 50 volts was required, the flow diagram shown in Figure 2-2 had to be modified. The d.c. regulator was replaced by a rheostat (variac). The supply to the hot guarded plate was then regulated 230 volts a.c. mains supply.

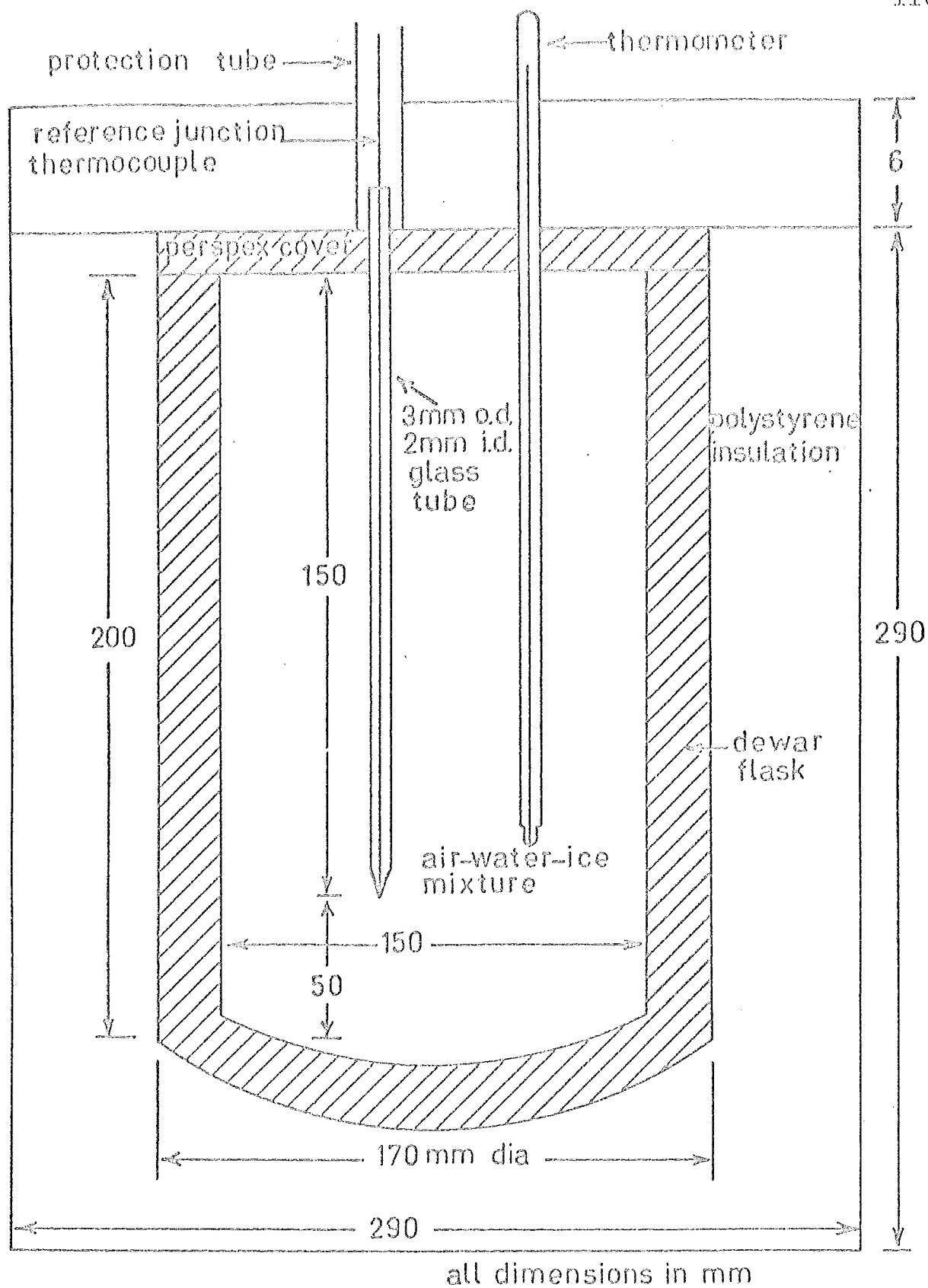


FIGURE 2-10 ICE BATH FOR REFERENCE JUNCTION

2.3.3.1 D.C. Regulated Power Supply

A Redfern regulated power supply series 51/3, 0-50 volts and 0-20 amps was used for the power supply to the hot plate. This unit converts 230 volts a.c. 50 cycles to 50 volts d.c. at 20 amps. The line voltage regulation is $\pm 0.01\%$, and the maximum ripple is 1mV RMS.

Direct current was the preferable power supply because it can be more accurately measured and is more steady than a.c. supply.

2.3.3.2 A.C. Regulated Power Supply

When a.c. power was required, the Sorenson a.c. voltage regulator model LT-1000-25 (used as the first stage voltage regulator in the d.c. circuit (Figure 2-2)), was used for the power supply to the hot plate.

The specifications of the Sorenson are:

Input Voltage: 230 volts a.c. mains

Output Voltage: 220-240 volts a.c. adjustable

Regulation Output: $\pm 0.1\%$ for changes in input voltage
 $\pm 0.01\%$ for changes in load current

Distortion: 3%

Time Constant: 0.1 second

Power Factor Range: 0.9 leading to 0.7 lagging

2.3.3.3 Heating Element

Pyrotenax heating cable model HCH-1L-500 was used in heating the hot plates. The specifications for heating cable are:

Cable Diameter: 3.1mm

Resistance: 0.5 ohms per metre at 20°C

Maximum Working Temperature: 250°C

Maximum Voltage: 600 volts

2.3.3.4 Power Measuring Instruments

Two Data Precision Corporation miniature digital multimeters model 245 were used to measure the current and voltage into the aluminium hot plates.

These 4½ digit multimeters are for measuring d.c. or a.c. voltage, d.c. or a.c. current, or resistance with 0.005% resolution in 21 ranges and 100% overrange.

2.3.4 AUXILIARY EQUIPMENT

2.3.4.1 The Thermostatic Bath

The tank containing the cooling water was made out of stainless steel. The tank is 51cm x 51cm x 51cm. The agitation of the water in the tank was achieved by using a 10cm, 6 blade impeller driven by a 100 watt motor. The tank was insulated by 6.35mm thick polystyrene all around, with the top covered by 6.35mm thick sheets of perspex.

The temperature of the water in the tank was kept at a constant value by using a proportional controller. The maximum power output of the controller was 1500 watts. The controlled immersion heater had a resistance 50.5 ohms while the main uncontrolled water heater had a resistance of 35.6 ohms. The temperature sensor connected to the controller was a thermistor probe of resistance 10 kilo-ohms.

The stainless steel container (box) for enclosing the guarded hot plate apparatus under water was made out of 14 gauge stainless steel. The box was of dimensions 44.5cm x

15.24cm x 44.5cm. The flanged cover of the box had a 1.91cm I.D. x 15cm stainless tube for passing the thermocouple wires in and out of the box. The box was made water tight by using a gasket, gasket-sealing compound, and 18 bolts in the flange assembly.

The thermostatic bath is shown in Figure 2-11.

2.3.4.2 Miscellaneous Equipment

During the experimental runs, to establish when steady-state conditions had been attained, a graphical output from a thermocouple pair was obtained on a Kipps and Zonen BD5 recorder. The micrograph BD5 was primarily designed for recording a wide range of currents and voltages from 20nA and 20 microVolts full scale deflection up to 0.1mA and 0.1 volts full scale deflection. The accuracy of this recorder is better than 0.5% f.s.d.

During the experimental runs in which a.c. power was used, the transformer used to reduce the mains voltage from 230 volts to the desired value, was a Yokohama Electric Works Ltd, Voltac-type-SB-5, 0 to 260 volts, 5 amp variac.

The thicknesses of all the specimens were measured using a micrometer screw gauge. The other linear dimensions were measured using a steel ruler.

2.3.5 SPECIMENS

Polymethyl methacrylate (perspex) was the primary material used. Other materials used were durotherm (asbestos cement board), particle board, syndanyo board, and polystyrene (to a less extent). In the calibration runs, rubber

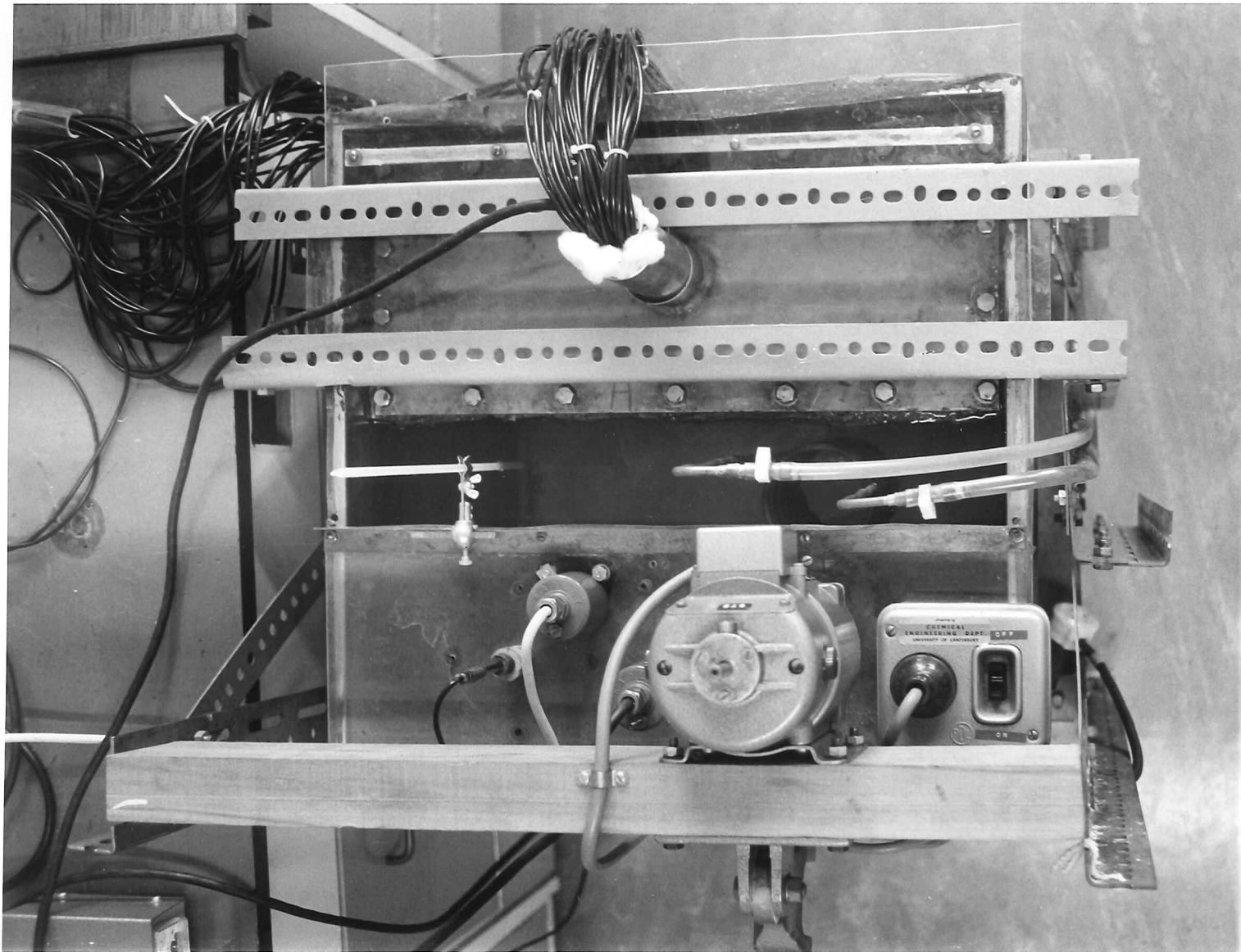


FIGURE 2-11

and cork board were also used but these were abandoned. Figure 2-12 shows some of the specimens used in the experiments. The specimens shown in the Figure have all had holes drilled in them. The 5.64mm thick perspex sheet also shows the aluminium foils put in the holes in an attempt to reduce radiation in the holes.

The specimens were all cut to the same size as the guarded hot plate, that is, 398.5mm square. The nominal specimen thicknesses were: 6.35mm, 12.7mm, and 19.05mm. The actual thicknesses of the individual plates are in the Appendix.

2.4 CALIBRATION OF EQUIPMENT

All the equipment used in this work was tested and calibrated prior to the main experimental runs (runs 1 to 738).

2.4.1 CALIBRATION OF THERMOCOUPLES

The calibration of a thermocouple consists of the determination of its electromotive force (emf) at a sufficient number of known temperatures so that, with some accepted means of interpolation, its emf will be known over the entire temperature range in which it is to be used. The process requires a standard thermometer to indicate temperatures on a standard scale, a means for measuring the emf of the thermocouple, and a controlled environment in which the thermocouple and the standard can be brought to the same temperature.

Much of the material described in this section including the techniques used are based on the methods of The National

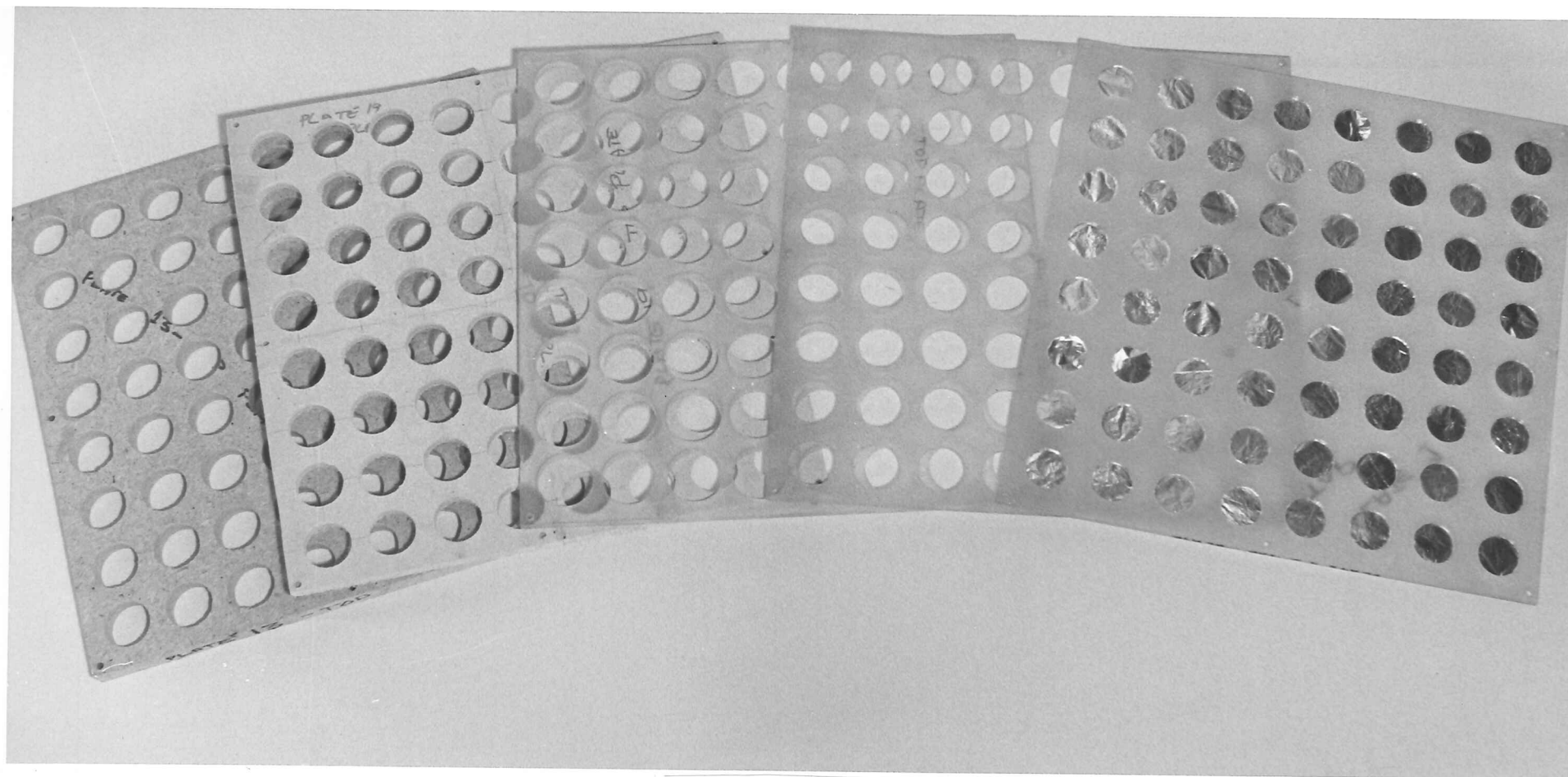


FIGURE 2-12

Bureau of Standards (138) and The National Physical Laboratories (139). Other useful references in the calibration of thermocouples are Billing (140), American Institute of Physics (118) and Baker (129).

2.4.1.1 Working Standard

The working standard used for the calibration of the thermocouple wires was the Rosemount Engineering Company platinum resistance thermometer model WS104. This thermometer was calibrated by the National Physical Laboratory in England in 1970, and by the New Zealand Department of Scientific and Industrial Research in late 1975. The former calibration was the more superior and complete. The latter was not conclusive, but it showed that the calibrations of 1970 were still valid. The brief specifications are presented here.

Temperature Range: -183°C to 500°C

Ice Point Resistance: 25.4899 ohms

25.4893 ohms

The results of the National Physical Laboratory calibrations are presented in the Appendix.

2.4.1.2 Measurement of emf

One of the factors in the accuracy of the calibration of a thermocouple, is the accuracy of the instrument used to measure the emf. In this work, the Cambridge potentiometer described in section 2.3.2.3 was used.

2.4.1.3 Calibration Using Comparison Method

The success of this method depends upon the ability of bringing the measuring junction of the thermocouple to the

same temperature as the actuating element of the standard platinum resistance thermometer.

The maximum service temperature of perspex is 80°C . As a result, the temperature range of the work carried out was 0 to 80°C , and consequently, water was used as the bath medium.

The bath used is the same one described in section 2.3.4.1. The protection tube for immersion in the water bath is shown in Figure 2-13. The tube is drilled in a block of 70mm diameter x 360mm aluminium. The calibration zone is 10mm diameter by 245mm deep. Once the platinum resistance thermometer and the thermocouple wires have been inserted into it, the protection tube is filled with copper filings.

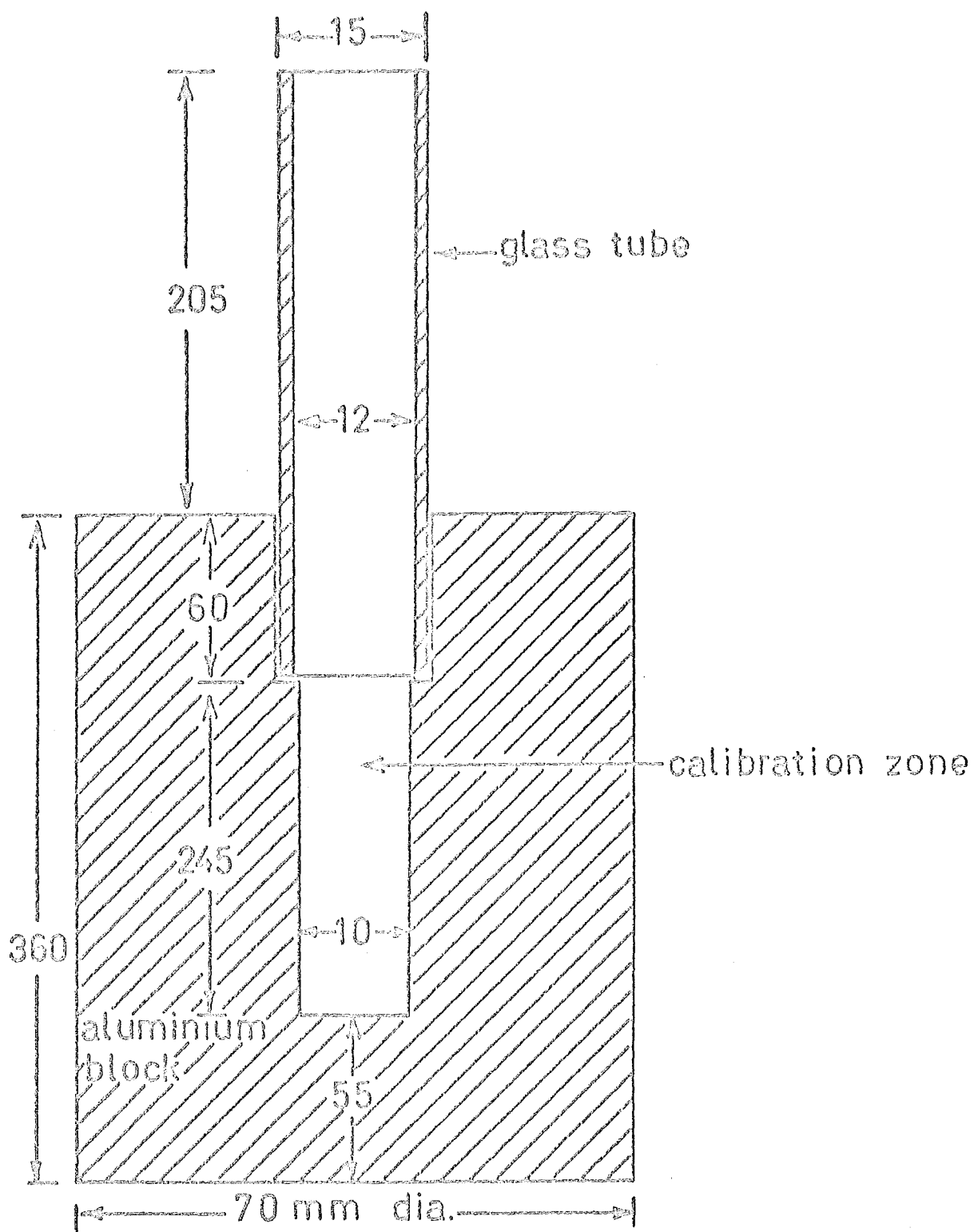
The reference junction described in section 2.3.2.4 and a three litre commercial dewar flask (10cm diameter x 40cm deep) were compared. Both were found to be suitable for the calibration of the thermocouples.

2.4.1.4 Procedure of Calibration Using the Comparison Method

(1) The water bath and the aluminium protection tube were maintained at a temperature close to the calibration temperature.

(2) The reference junctions described above were set up.

(3) The platinum resistance thermometer and the Model VLF 51A precision comparison bridge for resistance thermometry were set up. (Details in the Appendix.) The



all dimensions in mm

FIGURE 2-13 THERMOCOUPLE CALIBRATION
BLOCK

various zero checks on the comparison bridge were performed.

(4) The ice point was checked by inserting the platinum resistance thermometer in the dewar flask.

(5) The platinum resistance thermometer and the four thermocouple wires numbers 5, 23, 33 and 35 were inserted in the protection tube which was already immersed in the water bath. Copper filings completely filled the calibration zone. The reference junction thermocouple wire (wire number 37) was put in the dewar flask (section 2.3.2.4).

(6) The water bath was brought to the required bath temperature using the controller and the bath thermometer ($\pm 0.1^{\circ}\text{C}$). To ascertain when steady-state conditions had been attained, a graphical output from the thermocouple wires was obtained on a Hitachi two pen recorder and also by monitoring visually the controller fluctuations and the water bath temperature.

(7) Once steady-state was attained, the apparatus was left running in this condition for one hour. Monitoring the bath temperature with the thermometer and the Hitachi recorder was continued throughout this period.

(8) After equipment had been at steady-state for one hour, the following were noted down:

(a) the resistance ratio of the platinum resistance thermometer to the standard resistor. This gives the bath temperature ex platinum resistance thermometer.

(b) the thermocouple wire outputs in millivolts

(c) the water bath temperature using the 1/10th of a degree mercury-in-glass thermometer

(d) the room temperature using the two wall thermometers

(e) cooling water rate, bias heater voltage, and the controller setting

(9) The apparatus was again left running at the steady conditions for a further hour. Procedure steps 7 and 8 were repeated.

(10) After two sets of readings were noted down for the same operating conditions, step 6 and the subsequent steps were repeated.

The relationship between the temperature and emf of copper-constantan thermocouples has been very well established in the literature in the range -190°C to $+300^{\circ}\text{C}$ (138,141). In the range 0°C to 100°C , the relationship is a straight line. As a result, the calibration runs used in this work used water bath temperatures in the range 25°C to 55°C .

2.4.1.5 Method of Interpolating Between Calibration Points

After a thermocouple has been calibrated at a number of points, the next requirement is a convenient means of obtaining corresponding values of emf and temperature at other points. Various interpolating methods are available in the literature (118,138,141).

For the copper constantan thermocouples used, the empirical relationship of the National Bureau of Standards (138) was used.

$$e = aT + bT^2 + c \quad (2-1)$$

where e = emf in millivolts

T = temperature in $^{\circ}\text{C}$

a and b are calibration constants

c is also a calibration constant which should be equal to zero

As mentioned in section 2.3.2, two different gauges of constantan wire were used in the experiment. Consequently, two calibration equations (and tables) resulted. Recall that thermocouple wires numbered 1 to 32 used 36 gauge constantan wire, whereas the wires numbered 33 to 37 used 39 gauge constantan wire. The calibration equations obtained are:

(a) for thermocouple wires 5 and 23:

$$e = 0.02786 + 0.03742 T + 0.00004287 T^2 \quad (2-2)$$

(b) for thermocouple wires 33 and 35:

$$e = -0.007268 + 0.03905 T + 0.00004037 T^2 \quad (2-3)$$

2.4.1.6 Discussion of Calibration Uncertainties

The several factors which contributed to the uncertainties in the emf versus temperature relationships given above may be grouped into two kinds.

2.4.1.6.1 Uncertainties which influenced the observations

- the accuracy attained at each calibration point was dependent upon the degree to which the platinum resistance thermometer and the thermocouples were maintained at the same temperature

- the accuracy of the platinum resistance thermometer

(the ice point was the only check)

- the stability and homogeneity of the 36 gauge wires
- the accuracy of the emf measure (potentiometer accuracy)

2.4.1.6.2 Uncertainties due to interpolation between calibration points

Interpolation between calibration points was based on the assumption that emf changes slowly and smoothly with temperature. Table 2-1 shows some temperatures obtained by evaluating equations 2-2 and 2-3 for experimental values of emf. The temperatures indicated by the platinum resistance thermometer are also presented. As can be seen from the results, the experimentally determined temperatures (the platinum resistance thermometer results) and the empirical (using interpolation equations) temperatures agree to within $\pm 0.04^{\circ}\text{C}$. This is also the accuracy to which thermocouple wires can be relied on to retain their calibration.

TABLE 2-1
Experimentally and Empirically Determined Temperatures

Thermocouple Wire Outputs				Platinum Resistance Temperature in °C
Wires No 5 and 23		Wires No 33 and 35		
Average mV Output	Empirical Temperature °C	Average mV Output	Empirical Temperature °C	
1.031	25.58	1.071	25.56	25.58
1.192	30.08	1.204	30.08	30.06
1.437	36.16	1.458	36.17	36.17
1.688	42.32	1.718	42.33	42.30
1.856	46.39	1.8905	46.38	46.37
2.0185	50.30	2.058	50.28	50.31

The American Society for Testing and Materials manual. STP470A (142) presents a very good review of uncertainties due to interpolation between calibration points.

2.4.1.7 Concluding Remarks

The emf-temperature relationships for the two types of thermocouple wires used in this work are given in quadratic equation form (Equations 2-2 and 2-3). The relationships are also presented in tabular form in the Appendix. In the computation of experimental results in Chapter 4, the temperatures are found by solving the quadratic equations.

The temperatures evaluated from the quadratic equations are accurate to $\pm 0.04^{\circ}\text{C}$.

2.4.2 CALIBRATION OF REFERENCE JUNCTION

2.4.2.1 General Comments

If a proper technique is used, the uncertainty in the reference junction temperature can be made negligibly small. With extreme care, the ice point can be reproduced to 0.0001°C (142).

2.4.2.2 Working Standard

The platinum resistance thermometer described in section 2.4.1.1 was the working standard.

2.4.2.3 Calibration Method

The reference junction described in section 2.3.2.4 was used. The flask was filled with ice and its temperature determined using the platinum resistance thermometer. The results obtained were also compared with those obtained when the commercial three litre flask was used.

Experimental runs were also performed in which a stirrer was used. The above procedure was repeated at different times of the day and on different days.

2.4.2.4 Calibration Results

A typical set of ice point determinations is shown below.

TABLE 2-2
Ice Point Calibrations

Date	Reference Junction Temp. °C	Commercial Dewar Flask Temp. °C
08-12-75	0.001506	0.001511
08-12-75	-0.008277	-0.008476
08-12-75	-0.007274	-0.006910
08-12-75	-0.006521	-0.006800
22-12-75	0.000502	0.000504

The ice point readings with the reference junction media being stirred were not successful due to the stirrer motor noise causing fluctuations in the precision comparison bridge null meter.

2.4.2.5 Concluding Remarks

The reference junction used in all the experimental runs in this work was kept at 0°C (-0.008°C to 0.007°C).

2.4.3 CALIBRATIONS OF INSTRUMENTS USED WITH THERMOCOUPLES

The Cambridge potentiometer described in 2.3.2.3 was the instrument used to provide a measure of any unknown electromotive force. As no standard potential measuring

instrument was available, the calibration of the potentiometer consisted of comparing its emf outputs against those of other available potentiometers.

Table 2-3 shows a typical set of results. Potentiometer 'A' represents the one used in the experiments, and 'B' represents another Cambridge potentiometer.

TABLE 2-3
Comparison of Two Cambridge Potentiometers

Thermocouple Wire Number	Potentiometers	
	A	B
5	1.332mV	1.335mV
23	1.332mV	1.329mV
33	1.349mV	1.345mV
35	1.349mV	1.345mV
5	1.583mV	1.584mV
33	1.608mV	1.605mV

Numerous other test runs were performed to validate the readings indicated by the potentiometer. These included comparing the potentiometer readings with those of a solar-tron digital datalogger, and those shown by the Data Precision Corporation digital multimeters.

The Kipps-Zonen galvanometer was, of course, not calibrated since it was used to indicate the presence of a current, and readings were only made when no perceptible current was passing through it.

2.4.4 CALIBRATION OF POWER SUPPLY EQUIPMENT

As the experiments were performed at steady-state, it

was essential to have constant power supply. The regulations in the supply achieved are indicated in the various experimental runs in the Appendix. Better regulation was achieved through isolation of all the electrical equipment via transformers.

The two digital multimeters used for the current and voltage measurements were calibrated against a standard digital multimeter. For both meters and for all ranges, the indicated readings were exactly the same as those of the standard. These calibration checks were undertaken at various stages of the experimental work.

2.4.5 CALIBRATION OF PLATES

In any guarded hot plate apparatus, it is absolutely essential to get the plates as identical as possible.

2.4.5.1 Flatness of the Plates

Trial experimental runs with unmachined perspex pieces were carried out (experiment series A - Chapter 3). It was found necessary to machine the perspex pieces due to the variations in thicknesses of as received specimens. All the perspex specimens used in the experiments (series B and some of series A) were machined flat to within $\pm 0.03\text{mm}$ (0.001").

The flatness of the aluminium plates has already been discussed (section 2.3).

2.4.5.2 Temperature Drops Across The Specimens

One of the factors noted during pre-trial and trial runs was the difference in temperature drops between the two specimens ('a' and 'b' in Figure 2-5). For example, results

shown in Table E1.

Mathematically,

$$(mv_{10-18} - mv_{1-9}) \text{ is not equal to } (mv_{19-27} - mv_{28-36})$$

(2-4)

where mv_{i-i+8} is the average millivolt reading of thermocouple wires i to $i+8$.

Equation 2-4 unfortunately held for all the runs. The causes of the 'temperature-drop' differences could have been:

- (1) differences between the specimens
- (2) the assumption of even heat flux distribution between the two specimens not being true
- (3) different positions of the thermocouple wires
(This was highly unlikely since each plate had nine different thermocouple wires.)
- (4) different external heat flow resistances
(resistances due to insulation in the enclosure)
- (5) differences between the aluminium plates
- (6) arrangement of the apparatus - the positioning of the guarded hot plate in the enclosure and in the bath

The above uncertainties were experimentally investigated.

2.4.5.2.1 Determination of 'temperature-drop' differences

In an attempt to get the temperature drops across the specimens to be the same, an extensive experimental and theoretical program was undertaken.

The uncertainty due to the specimen physical and chemical structures was minimised by cutting the perspex pieces from the same large sheet. During any set of experimental runs, it

was also decided to do a check on the effect of the specimen position in relation to the aluminium plates. After each experimental run, the specimen positions were exchanged. In Figure 2-5, specimen 'a' was put where specimen 'b' was and vice versa. Readings were again taken.

The heat flux distribution uncertainty was minimised by putting aluminium studs in the hot plate (Figure 2-7). Physical and chemical differences between the aluminium plates used were minimal. All the aluminium plates used in the guarded hot plate apparatus were made from the same sheet of material.

The effect of the external resistance on the temperature drops was investigated by using three types of insulation systems in the box.

- (i) sheets of polystyrene completely enclosed the guarded hot plate
- (ii) fibreglass insulation instead of polystyrene
- (iii) air was also used instead of polystyrene

The use of plastic bags instead of the stainless steel box was also investigated unsuccessfully. The bags kept on getting torn regardless of the number used.

The effect of the arrangement of the apparatus was thoroughly investigated. Using 6.35mm thick perspex pieces, six arrangements were considered. With reference to Figure 2-5, the side of the stainless steel box nearest to the cold aluminium plate labelled 11a was labelled Side 'a'.

Run I - The apparatus was arranged as shown in Figure 2-5. However, the polystyrene studs ('9') were replaced by sheets

of polystyrene completely filling the box.

Run II - The arrangement of Figure 2-5 was used.

Run III - Same as run II but at a different voltage and current setting, consequently, different temperature drops.

Run IV - The guarded hot plate apparatus was rotated inside the box. The cold aluminium plate 11b was now closest to side 'a' of the stainless steel box.

Run V - The same arrangement as run IV except that the specimens 'a' and 'b' were swapped. The former specimen was now closest to side 'a' of the box.

Run VI - The same arrangement as run V except that the stainless steel box with all its contents was completely rotated during this run. Side 'a' of the box was now closest to the stirrer assembly in Figure 2-5.

2.4.5.2.2 Results of the positioning experiments

Table 2-4 shows:

(a) the average temperature of each plate for all the six runs

(b) the corresponding temperature drops across the specimens

(c) the thermocouple wires used in determining the surface temperature

Experimental Observations - From the experimental results presented in Table 2-4, the following points arise:

(1) The temperature of cold plate 11a is always greater than that of cold plate 11b.

(2) Within the thermocouple calibration error limits ($\pm 0.04^{\circ}\text{C}$), the two hot aluminium plates 13a and 13b have

TABLE 2-4

Results of Positioning Arrangement Experiments

Run	Temperature of cold plate 11a Thermocouple Wires numbers 1-9		Temperature of hot plate 13a Thermocouple Wires numbers 10-18		Temperature Drop Across Specimen	Temperature of hot plate 13b Thermocouple Wires numbers 19-27		Temperature of cold plate 11b Thermocouple Wires numbers 28-32		Temperature Drop Across Specimen	Difference in 'Temperature-Drops'
	mV	°C	mV	°C	°C	mV	°C	mV	°C	°C	°C
I	1.970	49.12	2.051	51.06	1.94 (a)	2.050	51.04	1.950	48.64	2.40 (b)	0.46
II	1.770	44.30	1.861	46.50	2.20 (a)	1.862	46.52	1.762	44.10	2.42 (b)	0.22
III	1.952	48.71	2.080	51.77	3.06 (a)	2.081	51.80	1.943	48.49	3.31 (b)	0.25
IV	1.947	48.59	2.075	51.66	3.07 (a)	2.077	51.70	1.941	48.44	3.26 (b)	0.19
V	1.943	48.49	2.071	51.56	3.07 (b)	2.072	51.58	1.939	48.40	3.18 (a)	0.11
VI	1.949	48.64	2.078	51.73	3.09 (b)	2.079	51.75	1.945	48.54	3.21 (a)	0.12

Note: The letter in the brackets refers to the specimen used. For example:

1.94°C (a) - refers to the temperature drop across specimen 'a'

3.07°C (b) - refers to the temperature drop across specimen 'b'

equal temperatures. Consequently, the even heat flux assumption was verified.

(3) The temperature difference of the specimen held between plates 11a and 13a is always less than that of the specimen held between plates 11b and 13b. This naturally follows from points (1) and (2).

(4) The more the insulation put in the box, the lower the temperature difference across the specimen. This point is further verified in Chapter 4. From runs II and III, as expected, the higher the working temperature, the higher the difference in 'temperature-drops' between the two specimens.

2.4.5.2.3 Concluding remarks

It was not possible to get the temperature differences across the specimens the same. Equation 2-4 was not able to be falsified. The insulation in the box was at first thought to have been the source of temperature differences between the two cold aluminium plates 11a and 11b. This point was later nullified by the experimental runs with durotherm at high temperatures using both air insulation and fibreglass insulation. These results are discussed in Chapter 5.

The 'temperature-drop' difference between any two specimens was incorporated in the overall experimental error.

2.5 EXPERIMENTAL PROCEDURE

2.5.1 APPARATUS PREPARATION

Once the apparatus had been built, tested and calibrated, the main experimental runs started.

(1) A material (specimen) of correct thickness was

chosen, usually perspex.

(2) Two pieces of the material 398.5mm square were cut from the same sheet.

(3) The pieces were machined to the same thickness to within $\pm 0.03\text{mm}$. The pieces were also marked so that they could be distinguished. For example, 6.35mm nominal thickness perspex pieces were marked 'plates 1 and 2'.

(4) The correct length studs for clamping the guarded hot plate were screwed in the appropriate cold aluminium plate.

2.5.2 ASSEMBLY OF APPARATUS

(1) The marked specimens were put between the appropriate plates.

(2) Using the four corner studs, the plates were clamped lightly.

(3) The guarded hot plate was then clamped firmly using the four middle studs and the support crossbars. The four corner studs were also tightened firmly.

(4) The guarded hot plate was then put in the stainless steel box (enclosure).

(5) Using the gasket compound, the gasket, and eighteen bolts, the box was made water tight by bolting the flange cover on top.

(6) The box containing the guarded hot plate was immersed in the water bath (Figure 2-11).

(7) The water bath was brought to temperature (31°C) using the controller, bias heater, cooling water and the stirrer.

The guarded hot plate was then connected to the electrical

power supply. The temperature of the guarded hot plate was monitored on the Kipps-Zonen BD5 recorder.

2.5.3 OPERATION OF APPARATUS

The operating procedure was adopted from that outlined in the A.S.T.M. Standard C177-71.

For any test, the temperature difference between the hot and cold surfaces of the specimen was adjusted by varying the power supply. From trial experimental runs using perspex, three voltage settings were chosen. These were 17 volts, 35.4 volts and 44.6 volts. During later experimental runs, higher voltages (55 volts and 63 volts) were used. For other materials, syndanyo board, for example, 132 volts was one of the voltage settings used.

The operating procedure was:

(a) A voltage setting was chosen. The apparatus was left running at this setting until steady-state was attained (usually after 36 to 48 hours).

(b) Once the Kipps-Zonen recorder indicated steady-state, the following were noted down:

(i) the room temperature using the two wall thermometers

(ii) the time of day

(iii) the water bath temperature

(iv) the reference junction temperature

(always 0°C)

(v) the current and voltage - using the two digital multimeters

(vi) all the thermocouple wire outputs (numbers 1 to 36) using the Cambridge potentiometer

(vii) after all the thermocouple wire outputs were taken, steps (i) to (v) were again repeated - (thus all the environmental conditions were noted down before and after each set of millivolt readings)

The above procedure ((i) to (vii)) was repeated every hour, thirteen times for every voltage setting. Note that after all the perspex experimental runs, the procedure was repeated every half hour and only eight times for durotherm, wood, syndanyo board and polystyrene runs.

2.5.4 EXPERIMENTAL DETERMINATIONS

2.5.4.1 Thermal Conductivity

Once a material had been chosen and prepared, its thermal conductivity was determined at various mean temperatures (various voltage settings). For example, the thermal conductivity of durotherm (plates 19 and 20) was determined at 66°C , 80°C , 92°C and 130°C . During some of the thermal conductivity determinations, especially perspex runs, the positions of the specimens were altered by exchanging them exactly as described in run IV (section 2.4.5.2.1). The exchanging was a means of getting an estimate of the experimental error.

2.5.4.2 Thermal Conductance

Once the thermal conductivity of the material was known at various temperatures, the following procedure was adopted:

(i) A hole size to be investigated was chosen. For perspex specimens, the initial hole size chosen was 30.5mm diameter.

(ii) Holes were drilled in the specimen in a regular

pattern (square pitch) as shown in Figure 2-12.

(iii) The thermal conductances of the specimens with holes in them were determined as described above (2.5.3).

(iv) The hole size in the specimens was increased. For perspex pieces, 35.5mm diameter holes were used. Step (iii) was then repeated. For perspex plates 5 and 6, 40.5mm diameter holes were also used.

For durotherm, only one size hole was used (34.925mm diameter).

2.5.4.3 Thermal Conductance With Aluminium Foil in the Holes

For perspex specimens with 30.5mm holes, aluminium foil inserts were placed in the centre of each hole, and the thermal conductance was measured.

CHAPTER 3QUALITATIVE RESULTS

3.1	<u>QUALITATIVE EXPERIMENTAL RESULTS</u>	136
3.1.1	EXPERIMENTS - SERIES A	136
3.1.2	EXPERIMENTS - SERIES B	138
3.1.2.1	The Determination of the Thermal Conductivity of Perspex	138
3.1.2.2	The Determination of the Thermal Conductance of Perspex With 30.5mm Holes Drilled	139
3.1.2.3	Miscellaneous Experimental Runs	140
3.2	<u>SCOPE OF THE THEORETICAL RESULTS</u>	146

CHAPTER 3

QUALITATIVE RESULTS

This chapter deals with descriptions, aims and scope of the results obtained from both the experimental and the theoretical runs.

3.1 QUALITATIVE EXPERIMENTAL RESULTS

The apparatus being basically complete, and calibrated, experimental runs were carried out in two series.

3.1.1 EXPERIMENTS - SERIES A

This series of runs was carried out as a trial for the apparatus. The numerous experiments carried out will not be described individually since many of them proved abortive. This series of runs provided the basis for the major modifications that the apparatus underwent before the main experimental runs (Series B).

The first few runs used 6.35mm thick sheets of rubber as the specimens. Spacers were used to compress the two specimens to the same thickness. The cold surface of the rubber specimens was kept at 33°C and the hot surface at 39°C. Large differences (50-75%) between the two specimens were observed. These were probably due to the unequal compressions resulting from the different specimen widths. The rubber specimens were also run at high temperatures ($T_{\text{hot}} = 91^{\circ}\text{C}$ and $T_{\text{cold}} = 80^{\circ}\text{C}$). At these high temperatures the experimental results were invalidated by thermal creep of the rubber specimens (143). Since rubber gave results which were not compatible within experimental error limits, it was abandoned as a specimen.

Runs with cork board as the specimen material were tried next. The 6.35mm thick cork board specimens were clamped between the aluminium plates which were put in plastic bags and then immersed under water. The plastic bags ensured an intimate contact between the aluminium plates and the water in the bath as hydrostatic pressure removed all the air in the bags. Even at low temperatures, the resulting temperature drops across the specimens were high. When the specimen hot surface was at 45.3°C , the corresponding cold surface temperature was 35.2°C . These temperature drops were very propitious. The ability of the cork board to retain its chemical composition was in doubt as the esters used in the adhesives to hold the board together were smelt after two hours' heating. Although the plastic bags (five layers used at a time) ensured thermal equilibrium within three hours, most runs had to be abandoned since the bags leaked.

With the rubber and cork board specimens abandoned, the next available material tried was perspex. Runs with 6.35mm thick clear and translucent (white opal) perspex specimens unmachined were undertaken. The specimens were enclosed in plastic bags instead of the stainless steel box. The clear perspex runs were completed without the bags leaking. However, sometime during the white perspex runs, the bags leaked. Consequently, the white perspex results presented in the Appendix are suspect. Since only one thickness of translucent perspex was available, it was decided not to use it in the main experimental runs.

The clear perspex runs described above were so successful that it was decided to drill 30.5mm diameter holes in them

and measure the resulting conductances. The runs were performed using the 5.94mm and 5.74mm thick specimens. Fortunately, the plastic bags did not leak during this set of runs. The results are presented in the Appendix.

From the qualitative and quantitative results of experiment Series A, it was decided:

- (a) to machine all specimen pieces before runs
- (b) to abandon plastic bags in favour of the stainless steel box enclosure which was proven to be water tight but took longer to reach thermal equilibrium

3.1.2 EXPERIMENTS - SERIES B

This series of runs constitutes the main and final experiments undertaken in this work. The detailed results are in the Appendix. Sample calculated results are presented in Chapter 4. The runs are numbered from 1 to 738. For the various experiments, Tables 3-1 to 3-5 show:

- (a) the specimens used - numbers and thicknesses
- (b) the specimen positions in the guarded hot plate
- (c) the conditions of the experiments - mean temperatures (heater voltage settings)

The experiments fall into three broad classes.

3.1.2.1 The Determination of the Thermal Conductivity of Perspex

During runs 1 to 158, the thermal conductivities of 5.6mm and 11mm thick perspex pieces were determined. The 5.6mm thick specimens were numbered plates 1, 2, 3, and 4. The 11mm thick specimens were numbered plates 5, 6, 7, and 8.

With reference to Figure 2-5, the specimens were

positioned in the guarded hot plate apparatus as follows:

(a) the even numbered specimens were placed between the aluminium plates 11b and 13b

(b) while the odd numbered specimens were placed between the aluminium plates 11a and 13a

(c) as previously mentioned (Chapter 2), the specimen positions were exchanged for at least one run to get an estimate of the experimental error

Statements (a) and (b) above can be expressed as follows:

For even numbered specimens:

$$\text{cold surface temperature} = mv_{28-36} \quad (3-1)$$

$$\text{hot surface temperature} = mv_{19-27} \quad (3-2)$$

where mv_{i-i+8} is the average millivolt reading of thermocouple wires i to $i+8$.

For odd numbered specimens:

$$\text{cold surface temperature} = mv_{1-9} \quad (3-3)$$

$$\text{hot surface temperature} = mv_{10-18} \quad (3-4)$$

The above comments refer to all the other runs as well (runs 1 to 738).

3.1.2.2 The Determination of the Thermal Conductance of Perspex With 30.5mm Holes Drilled

The perspex specimens used in runs 1 to 158 had 30.5mm holes drilled in them. In runs 159 to 457, the thermal conductances of these specimens were determined. Some of the experimental runs involved perspex pieces with aluminium foil inserts in the holes. The presence of the aluminium foil inserts is indicated in Table 3-2 by an asterisk next to the

run number.

3.1.2.3 Miscellaneous Experimental Runs

These cover runs 458 to 738 and they consist of the following:

(a) thermal conductivity and conductance determinations of 20mm thick particle board (plates numbered 13 and 14)

(b) thermal conductivity determinations of 19mm (nominal thickness 3/4") thick perspex (plates numbered 9 and 10)

(c) thermal conductivity determinations of 9.7mm thick syndanyo board (plates numbered 15 and 16)

(d) thermal conductivity and conductance determinations of durotherm (plates numbered 19 and 20)

(e) thermal conductance determinations of perspex plates 5 and 6 (11mm thick) with various hole sizes and at various mean operating temperatures

(f) thermal contact resistance determinations using 19mm thick perspex sheets (plates 11 and 12)

(g) thermal conductance determinations across air spaces - the hot and cold aluminium plates of the guarded hot apparatus were separated by 5 spacers (5mm diameter x 11mm long). (The spacers were numbered fictitious plates 21 and 22.)

(h) thermal conductivity determinations of 12.7mm thick polystyrene (plates numbered 17 and 18)

Runs 458 to 738 are summarised in Tables 3-3, 3-4 and 3-5.

TABLE 3-1

Runs 1 to 158 -- Thermal Conductivity of Perspex Determination
(Experimental Conditions)

Runs	Specimens Nominal Thickness mm	Specimen Held Between Aluminium Plates		Approximate Mean Temperature °C	Voltage Setting Volts
		11a and 13a	11b and 13b		
1 - 14	5.6	1	2	50	35.4
15 - 28	5.6	3	4	50	35.4
29 - 42	5.6	3	4	36	17.0
43 - 55	5.6	3	4	60	44.6
56 - 68	5.6	4	3	50	35.4
69 - 80	5.6	2	1	50	35.4
81 - 93	11	5	6	50	35.4
94 - 106	11	5	6	36	17.0
107 - 119	11	5	6	60	44.6
120 - 132	11	6	5	50	35.4
133 - 145	11	7	8	50	35.4
146 - 158	11	8	7	50	35.4

TABLE 3-2

Runs 159 to 457 - Thermal Conductance of Perspex With
30.5mm Holes (Experimental Conditions)

Runs	Specimens Nominal Thickness mm	Specimen Held Between Aluminium Plates		Approximate Mean Temperature °C	Voltage Setting Volts
		11a and 13a	11b and 13b		
159 - 171	11	5	6	50	35.4
172 - 184	11	5	6	36	17.0
185 - 197	11	5	6	60	44.6
198 - 210	11	6	5	50	35.4
211 - 223	11	7	8	50	35.4
224 - 236	11	8	7	50	35.4
237 - 249*	11	5	6	50	35.4
250 - 262*	11	5	6	36	17.0
263 - 275*	11	5	6	60	44.6
276 - 288*	11	6	5	50	35.4
289 - 301*	11	7	8	50	35.4
302 - 314*	11	8	7	50	35.4
315 - 327	5.6	3	4	50	35.4
328 - 340	5.6	3	4	36	17.0
341 - 353	5.6	3	4	60	44.6
354 - 366	5.6	4	3	50	35.4
367 - 379	5.6	1	2	50	35.4
380 - 392	5.6	2	1	50	35.4
393 - 405*	5.6	3	4	50	35.4
406 - 418*	5.6	3	4	60	44.6
419 - 431*	5.6	3	4	36	17.0
432 - 444*	5.6	4	3	50	35.4
445 - 457*	5.6	1	2	50	35.4

* - runs with aluminium foil inserts in the holes

TABLE 3-3
Runs 458 to 583 - Experimental Conditions

Runs	Specimens Nominal Thickness mm	Specimen Held Between Aluminium Plates		Approximate Mean Temperature °C	Voltage Setting Volts	Comments
		11a and 13a	11b and 13b			
458 - 470	19	13	14	55	50.0	Particle board conductivity determinations
471 - 483	19	14	13	55	50.0	Same comment as above, but specimens exchanged in guarded hot plate
484 - 496	19	9	10	55	50.0	Perspex conductivity determinations
497 - 509	19	9	10	45	35.4	Same comment as above, but at a lower temperature
510 - 522	19	10	9	55	50.0	Same as runs 484 - 496, but specimens exchanged in apparatus
523 - 535	19	13	14	55	50.0	Particle board with 35.5mm holes, conductance determinations
536 - 543	9.7	15	16	52	50.0	Syndanyo board conductivity determinations
544 - 548	9.7	15	16	110	132.0	Same comment as above, but at a higher temperature
549 - 555	11	5	6	45	35.4	Perspex with 35.5mm holes, conductance determinations
556 - 562	11	5	6	52	44.6	Same comment as above, but at a higher temperature
563 - 567	12.7	17	18	50	35.4	Polystyrene conductivity determinations
568 - 575	11	5	6	61	55.0	Perspex with 35.5mm holes, conductance determinations at 60°C
576 - 583	11	5	6	70	64.0	Same comment as above, but at a temperature close to the maximum working temperature

TABLE 3-4

Runs 584 to 664 - Thermal Conductivity and Conductance of Durotherm (Experimental Conditions)

Runs	Specimens Nominal Thickness mm	Specimen Held Between Aluminium Plates		Approximate Mean Temperature °C	Voltage Setting Volts	Comments
		11a and 13a	11b and 13b			
584 - 588	12	19	20	66	64	Runs 584 - 604: The determination of the thermal conductivity of durotherm at various voltage settings - hence various mean temperatures.
589 - 594	12	19	20	92	90	
595 - 598	12	19	20	130	120	
599 - 604	12	19	20	80	80	
605 - 610	12	19	20	69	64	Runs 605 - 634: The determination of the thermal conductance of durotherm with 34.925mm holes drilled. Mean temperatures close to those of runs 584 - 604.
611 - 616	12	19	20	84	80	
617 - 622	12	19	20	97	90	
623 - 628	12	19	20	137	120	
629 - 634	12	19	20	76	70	
635 - 640	12	19	20	78	64	Runs 635 - 664: The guarded hot plate apparatus was completely surrounded by fibreglass insulation in the box. Again durotherm with 34.925mm holes was used as the material at various mean temperatures.
641 - 646	12	19	20	86	70	
647 - 652	12	19	20	99	80	
653 - 658	12	19	20	114	90	
659 - 664	12	19	20	160	120	

TABLE 3-5
Runs 665 to 738 - Experimental Conditions

Runs	Specimens Nominal Thickness mm	Specimen Held Between Aluminium Plates		Approximate Mean Temperature °C	Voltage Setting Volts	Comments
		11a and 13a	11b and 13b			
665 - 669	11	21	22	45	35.4	Runs 665 - 678: 11mm long spacers separated the aluminium plates. The thermal conductance due to the entrapped air was measured at various temperatures.
670 - 674	11	21	22	50	44.6	
675 - 678	11	21	22	66	64.0	
679 - 684	11	5	6	45	35.4	Runs 679 - 702: 11mm thick perspex pieces with 40.5mm holes had their thermal conductances measured at various temperatures.
685 - 690	11	5	6	52	44.6	
691 - 696	11	5	6	61	55.0	
697 - 702	11	5	6	70	64.0	
703 - 708	19	11	12	45	35.4	Runs 703 - 720: Thermal conductivities of 19mm thick perspex pieces were determined at the three temperatures.
709 - 714	19	11	12	52	44.6	
715 - 720	19	11	12	61	56.0	
721 - 726	19	11	12	45	35.4	Runs 721 - 738: Oil was smeared on both faces of the 19mm thick perspex pieces. The thermal conduc- tivities of the specimens were again determined at the same mean temperatures as in runs 703 to 720.
727 - 732	19	11	12	52	44.6	
733 - 738	19	11	12	61	56.0	

3.2 SCOPE OF THE THEORETICAL RESULTS

The results obtained in the experiments were used in the theoretical simulations. For example, run 172 was used to represent the results obtained for thermal conductance measurements of 11mm thick perspex pieces (5 and 6) with 30.5mm holes (runs 172 to 184). The experimental runs provided the following variables for the computer program:

- (a) the boundary conditions - the hot and cold temperatures of the specimens
- (b) the linear dimensions of the specimens - thicknesses and radii of the holes
- (c) from (a), the thermal conductivities of the specimens (from runs 1 to 158) were known - the thermal conductivities of air at the mean temperatures were also known

The only variable that the experimental runs did not provide for the computer simulations, was the emissivity. The emissivity of perspex used in this work was experimentally measured by Dunkle R.V. in Australia (144). However, the emissivity of aluminium was unknown. To overcome this problem, all the computer simulations were performed using four different aluminium emissivities. The chosen emissivity values were 0.04, 0.11, 0.2 and 0.5.

The numbering system used for the computer simulation runs is:

If run number = 897X, then the simulation data used is based on experimental run 897. X denotes value of the aluminium emissivity used.

If X = A, then 0.04 was used
= B, then 0.11 was used
= C, then 0.2 was used
= D, then 0.5 was used

Table 3-6 shows the computer simulation runs. The letter after each simulation run number is omitted as in all cases the four aluminium emissivities were used.

TABLE 3-6
Results Used For Numerical Simulation Runs

Simulation Run	Temperature of Specimen Face		Thermal Conductivity in W/M ^o C		Comments
	Hot ^o C	Cold ^o C	Specimen	Air	
159	53.32	48.68	0.2053	.02784	11mm thick perspex specimens (plates 5 and 6) with 30.5mm holes at mean temperatures of 36, 50 and 60 ^o C
172	36.48	35.67	0.2053	.02680	
186	61.76	56.25	0.2053	.02844	
201	51.99	48.25	0.2053	.02780	11mm thick perspex with 30.5mm holes at 50 ^o C with specimen positions swapped
315	50.89	48.73	0.2000	.02779	5.6mm thick perspex specimens (plates 3 and 4) with 30.5mm holes at mean temperatures of 36, 50 and 60 ^o C
331	36.36	35.82	0.2000	.02680	
341	61.78	58.37	0.2000	.02852	
549	47.67	43.41	0.2000	.02749	11mm thick perspex specimens (plates 5 and 6) with 35.5mm holes at mean temperatures of 42, 52, 61 and 70 ^o C
556	56.27	49.64	0.2000	.02801	
568	66.20	56.10	0.2000	.02859	
576	76.68	63.25	0.2000	.02921	
605	77.07	60.94	0.2040	.02914	12mm thick durotherm specimens (plates 19 and 20) with 34.925mm holes at mean temperatures of 69, 84, 97 and 137 ^o C
611	96.09	72.43	0.2040	.03020	
617	112.57	82.26	0.2040	.03110	
624	162.77	111.23	0.2040	.03371	
629	86.21	66.51	0.2040	.02966	
679	47.34	42.59	0.2000	.02744	11mm thick perspex specimens (plates 5 and 6) with 40.5mm holes at mean temperatures of 45, 52, 61 and 70 ^o C
686	55.94	48.42	0.2000	.02796	
692	66.76	55.63	0.2000	.02859	
698	78.36	63.14	0.2000	.02926	

CHAPTER 4QUANTITATIVE RESULTS

4.1	<u>EXPERIMENTAL RESULTS</u>	150
4.1.1	THERMAL CONDUCTIVITY RESULTS	150
4.1.2	THERMAL CONDUCTANCE RESULTS FOR SPECIMENS WITH 30.5mm HOLES	155
4.1.3	THERMAL CONDUCTANCE RESULTS FOR SPECIMENS WITH ALUMINIUM FOIL IN THE HOLES	155
4.1.4	THERMAL CONDUCTANCE RESULTS FOR SPECIMENS WITH 35.5mm HOLES	161
4.1.5	THERMAL CONDUCTANCE RESULTS FOR SPECIMENS WITH 40.5mm HOLES	161
4.1.6	THERMAL CONDUCTANCE RESULTS FOR DUROTHERM SPECIMENS	161
4.1.7	QUANTITATIVE EXPERIMENTAL CURVES	161
4.1.8	MISCELLANEOUS EXPERIMENTAL RESULTS	166
4.2	<u>THEORETICAL RESULTS</u>	166
4.2.1	TEMPERATURE AND HEAT FLUX PROFILES	168
4.2.2	HEAT BALANCES	171
4.2.3	RADIATIVE TRANSFER	171
4.2.4	TOTAL HEAT TRANSFERRED	171
4.3	<u>COMPARISON OF EXPERIMENTAL AND THEORETICAL RESULTS</u>	178

CHAPTER 4

QUANTITATIVE RESULTS

This chapter presents the results obtained from the developed experimental and theoretical solutions of the cavity problem.

4.1 EXPERIMENTAL RESULTS

Sample experimental results from each series of runs (Series B) are presented in this section. The complete set of results is presented in the Appendix.

4.1.1 THERMAL CONDUCTIVITY RESULTS

The measured thermal conductivities for the various materials are given below.

Table 4-1 shows the thermal conductivities of 5.6mm and 11mm thick perspex specimens (plates 1, 2, 3 and 4; and plates 5, 6, 7 and 8 respectively). The thermal conductivities are evaluated using the mean aluminium plate temperatures as described by equations 3-1 to 3-4 (see Appendix for sample calculation). As with all the other tables in this chapter, the specimen mentioned first was held between aluminium plates 11a and 13a; while the specimen mentioned last in each run was held between aluminium plates 11b and 13b (see Chapter 3). N.B. - later references to 'specimen position' refer to these alternative specimen positions.

The differences in the temperatures of the cold aluminium plates 11a and 11b, as previously mentioned (Chapter 2), are clearly shown in Table 4-1. For example, in run 2 the temperature of the cold aluminium plate 11a is 49.43°C , whereas that of plate 11b is 49.35°C . The temperature

TABLE 4-1
Thermal Conductivities of
5.6mm and 11mm Thick Perspex Plates

Experimental Run Number	Specimen Plate Number	Thickness of Specimen mm	Temperature of Specimen Surface		Temperature Drop Across Specimen °C	Mean Specimen Temperature °C	Electrical Power Into Specimen W	Thermal Conductivity W/M°C
			Hot °C	Cold °C				
2	1	5.69	51.10	49.43	1.66	50.26	2.299	0.1968
	2	5.54	51.12	49.35	1.78	50.23	2.299	0.1792
16	3	5.66	51.27	49.61	1.66	50.44	2.297	0.1965
	4	5.64	51.29	49.45	1.84	50.37	2.297	0.1757
30	3	5.66	37.14	36.72	0.42	36.93	0.526	0.1789
	4	5.64	37.15	36.68	0.47	36.92	0.526	0.1583
44	3	5.66	61.61	59.07	2.546	60.34	3.651	0.2030
	4	5.64	61.62	58.58	3.035	60.1	2.651	0.1696
57	4	5.64	52.24	50.47	1.76	51.35	2.31	0.1846
	3	5.66	52.28	50.54	1.75	51.41	2.31	0.1872
70	2	5.54	52.01	50.25	1.75	51.13	2.303	0.1817
	1	5.69	52.04	50.34	1.70	51.19	2.303	0.1923
82	5	11.15	51.7	48.58	3.12	50.14	2.289	0.2045
	6	11.20	51.75	48.84	2.906	50.29	2.289	0.2205
95	5	11.15	36.84	36.12	0.72	36.48	0.528	0.2043
	6	11.2	36.85	36.16	0.69	36.51	0.528	0.2153
108	5	11.15	62.58	57.55	5.03	60.06	3.632	0.2015
	6	11.20	62.65	58.11	4.54	60.38	3.632	0.2239
121	6	11.20	52.55	49.64	2.91	51.09	2.284	0.2197
	5	11.15	52.54	49.28	3.26	50.91	2.284	0.1955
134	7	11.21	52.4	49.24	3.16	50.82	2.296	0.2038
	8	11.17	52.46	49.39	3.071	50.93	2.296	0.2068
147	8	11.17	51.94	48.75	3.20	50.34	2.303	0.2013
	7	11.21	51.99	48.9	3.08	50.45	2.303	0.2094

difference between the two plates is enough to cause a significant difference between the two resulting thermal conductivities of the specimens (0.1968 and 0.1792 W/M⁰C).

In the Appendix the mean thermal conductivities and the corresponding standard deviations for each series of runs are worked out. Table 4-2 shows the means and standard deviations of the thermal conductivities of runs 1 to 158. The table also shows the resulting different thermal conductivities of the same specimens depending on the specimen position in the guarded hot plate. This effect was also observed for all the other runs using different specimens.

Table 4-3 shows the mean thermal conductivities measured for the other specimens used in the experiments. Among the results are those of perspex plates 11 and 12. In runs 703 to 720 the thermal conductivities of these two plates were found. At 61⁰C, for example, the thermal conductivities measured were 0.2319 and 0.2270 W/M⁰C respectively. The resulting thermal conductivities in runs 721 to 738 show the effect of having oil smeared on the perspex plates in an attempt to improve the thermal contact between the aluminium plates and the perspex specimens. At the same temperature of 61⁰C, the conductivities are 0.2362 and 0.2261 W/M⁰C. These conductivities are not significantly different from those obtained without oil on the plate surfaces. Consequently, the thermal contact resistance between the specimens and the aluminium plates was verified to be negligible. Runs 665 to 678 show the resulting conductances across the air spaces separating the aluminium

TABLE 4-2
Mean Thermal Conductivities of
5.6mm and 11mm thick perspex plates

Run	Specimen Plate Number	Thermal Conductivity W/M ² C		Specimen Temperature C	
		Mean	Std Deviation	Mean	Std Deviation
1 - 14	1	0.1934	.0019	50.40	.09
	2	0.1777	.0015	50.38	.10
69 - 80	2	0.1812	.0016	50.96	.14
	1	0.1946	.0018	51.03	.14
15 - 28	3	0.1965	.0011	50.48	.04
	4	0.1765	.0012	50.41	.03
56 - 68	4	0.1825	.0019	51.39	.15
	3	0.1856	.0022	51.44	.15
29 - 42	3	0.1942	.0172	36.55	.22
	4	0.1775	.0124	36.54	.23
43 - 55	3	0.2031	.0007	60.37	.05
	4	0.1730	.0013	60.16	.05
81 - 93	5	0.2053	.0021	50.26	.16
	6	0.2193	.0018	50.41	.15
120 - 132	6	0.2195	.0022	50.87	.21
	5	0.1953	.0028	50.69	.20
94 - 106	5	0.2010	.0042	36.51	.08
	6	0.2086	.0069	36.53	.08
107 - 119	5	0.2030	.0022	59.78	.34
	6	0.2232	.0018	60.08	.34
133 - 145	7	0.2053	.0016	50.67	.22
	8	0.2113	.0019	50.77	.22
146 - 158	8	0.2035	.0011	50.20	.13
	7	0.2123	.0021	50.30	.12

TABLE 4-3
Thermal Conductivities of
Miscellaneous Materials

Run	Specimen Plate Number	Material	Thermal Conductivity in W/M°C at Specified Temperature				Comments
			45°C	52°C	55°C	Other	
484 - 509	9	Perspex	0.2203	-	0.2251	-	
	10	Perspex	0.2247	-	0.2247	-	
703 - 720	11	Perspex	0.2300	0.2301	-	0.2319 (61°C)	
	12	Perspex	0.2225	0.2240	-	0.2270 (61°C)	
721 - 738	11	Perspex	0.2328	0.2352	-	0.2362 (61°C)	Oil was smeared on both surfaces of the specimen - to determine the surface contact resistance
	12	Perspex	0.2202	0.2231	-	0.2261 (61°C)	
458 - 470	13	Particle Board	-	-	0.1663	-	
	14	Particle Board	-	-	0.1696	-	
536 - 548	15	Syndanyo Board	-	0.6947	-	0.8044 (110°C)	
	16	Syndanyo Board	-	0.6167	-	0.6881 (110°C)	
563 - 567	17	Polystyrene	-	-	-	0.0522 (49°C)	
	18	Polystyrene	-	-	-	0.0513 (49°C)	
584 - 604	19	Durotherm	0.2075 (66°C)	0.2093 (93°C)	0.2120 (130°C)	0.2033 (80°C)	
	20	Durotherm	0.1976 (66°C)	0.1998 (92°C)	0.2018 (130°C)	0.1956 (80°C)	
665 - 678	21	Air	0.0631	0.0669	-	0.0750 (66°C)	Spacers were used to sepa- rate the aluminium plates The values tabulated are conductance results.
	22	Air	0.0628	0.0664	-	0.0750 (66°C)	

plates. As mentioned in Chapter 3, spacers held the aluminium plates apart. The results shown in Table 4-3 are not true thermal conductivities of air since natural convection must have been occurring in the large stainless box enclosing the guarded hot plate. Radiative transfer between the aluminium plates also occurred.

From reference 146, the thermal conductivity of air is:

Temperature	Thermal Conductivity W/M ⁰ C
45 ⁰ C	0.0276
52 ⁰ C	0.0279
66 ⁰ C	0.0290

4.1.2 THERMAL CONDUCTANCE RESULTS FOR SPECIMENS WITH 30.5mm HOLES

The measured thermal conductances for the 5.6mm and 11mm thick perspex specimens (plates 3, 4, 5 and 6) with 30.5mm holes are given below. The presented results (Table 4-4) are of the runs used in the computer simulations.

The thermal conductance evaluated is the effective conductivity as defined in Chapter 1 (1.5.1.1), that is, the sum of air conductance, solid conductance, and the radiation contribution in the holes.

4.1.3 THERMAL CONDUCTANCE RESULTS FOR SPECIMENS WITH ALUMINIUM FOIL IN THE HOLES

As described in Chapter 3, aluminium foil was used to divide the holes into two. (A single aluminium foil disc of slightly larger diameter than the hole was held using perspex glue at exactly half the specimen thickness in the

TABLE 4-4
Thermal Conductance Results For
Perspex Specimens With 30.5mm Holes

Experimental Run Number	Specimen Plate Number	Temperature of Specimen Surface		Temperature Drop Across Specimen C	Electrical Power Into Specimen W	Thermal Conductance W/M ^o C
		Hot ^o C	Cold ^o C			
159	5	52.32	48.47	3.65	2.294	0.175
	6	52.29	48.25	4.04	2.294	0.159
172	5	36.48	35.68	0.80	0.526	0.181
	6	36.50	35.60	0.90	0.526	0.162
186	5	61.75	56.24	5.51	3.620	0.183
	6	61.74	55.55	6.19	3.620	0.164
201	6	51.98	48.25	3.73	2.301	0.172
	5	52.00	48.04	3.96	2.301	0.162
315	3	50.89	48.74	2.15	2.289	0.150
	4	50.97	48.74	2.23	2.289	0.145
331	3	36.35	35.82	0.53	0.528	0.140
	4	36.39	35.84	0.55	0.528	0.136
341	3	61.78	58.38	3.40	3.630	0.151
	4	61.81	58.30	3.51	3.630	0.146

TABLE 4-5

Thermal Conductance Results For Perspex Specimens
With Aluminium Foil In The 30.5mm Holes

Experimental Run Number	Specimen Plate Number	Temperature Of Specimen Surface		Temperature Drop Across Specimen °C	Electrical Power Into Specimen W	Thermal Conductance W/M°C.
		Hot °C	Cold °C			
237	5	51.60	47.92	3.68	2.296	0.174
	6	51.58	47.46	4.12	2.296	0.156
250	5	36.33	35.44	0.89	0.527	0.166
	6	36.33	35.38	0.95	0.527	0.155
263	5	61.87	56.09	5.78	3.64	0.176
	6	61.87	55.35	6.52	3.64	0.156
276	6	52.66	48.83	3.83	2.302	0.169
	5	52.65	48.42	4.23	2.302	0.152
289	7	52.26	48.23	4.03	2.288	0.159
	8	52.30	48.49	3.81	2.288	0.168
302	8	52.00	47.99	4.01	2.277	0.158
	7	52.04	48.34	3.70	2.277	0.173
393	3	51.10	48.86	2.24	2.296	0.145
	4	51.16	49.00	2.16	2.296	0.150
406	3	61.10	57.52	3.58	3.635	0.144
	4	61.21	57.82	3.39	3.635	0.151
419	3	36.66	36.09	0.57	0.524	0.131
	4	36.68	36.19	0.49	0.524	0.151
432	4	51.33	49.10	2.23	2.281	0.144
	3	51.35	49.21	2.14	2.281	0.151
445	1	50.58	48.63	1.95	2.284	0.166
	2	50.58	48.18	2.40	2.284	0.132

TABLE 4-6
Thermal Conductance Results For
Specimens With 35.5mm Holes

Experimental Run Number	Specimen Plate Number	Temperature Of Specimen Surface		Temperature Drop Across Specimen °C	Electrical Power Into Specimen W	Thermal Conductance W/M°C
		Hot °C	Cold °C			
523	13	64.04	48.61	15.43	4.487	0.143
	14	64.05	49.14	14.92	4.487	0.148
549	5	47.66	43.42	4.25	2.292	0.150
	6	47.68	43.30	4.39	2.292	0.146
556	5	56.27	49.63	6.63	3.650	0.153
	6	56.29	49.38	6.91	3.650	0.148
568	5	66.13	56.17	9.97	5.548	0.155
	6	66.20	56.07	10.13	5.548	0.153
576	5	76.69	63.25	13.44	7.518	0.156
	6	76.78	63.29	13.49	7.518	0.156

TABLE 4-7
Thermal Conductance Results For
Perspex Specimens With 40.5mm Holes

Experimental Run Number	Specimen Plate Number	Temperature Of Specimen Surface		Temperature Drop Across Specimen °C	Electrical Power Into Specimen W	Thermal Conductance W/M°C
		Hot °C	Cold °C			
679	5	47.34	42.59	4.74	2.272	0.134
	6	47.34	42.48	4.86	2.272	0.131
686	5	55.94	48.42	7.51	3.633	0.135
	6	55.96	48.27	7.70	3.633	0.132
692	5	66.76	55.63	11.12	5.432	0.136
	6	66.80	55.45	11.35	5.432	0.134
698	5	78.36	63.14	15.22	7.600	0.139
	6	78.41	62.93	15.47	7.600	0.138

TABLE 4-8
Thermal Conductance Results For
Durotherm Specimens With 34.925mm Holes

Experimental Run Number	Specimen Plate Number	Temperature Of Specimen Surface		Temperature Drop Across Specimen °C	Electrical Power Into Specimen W	Thermal Conductance W/M°C
		Hot °C	Cold °C			
605	19	77.07	60.94	16.12	7.691	0.144
	20	77.15	59.82	17.32	7.691	0.135
611	19	96.09	72.43	23.66	11.528	0.147
	20	96.23	71.01	25.22	11.528	0.138
617	19	112.57	82.26	30.29	14.928	0.149
	20	112.76	80.83	31.93	14.928	0.142
624	19	162.77	111.23	51.54	27.069	0.158
	20	163.13	109.73	53.41	27.069	0.154
629	19	86.21	66.51	19.70	9.226	0.141
	20	86.34	65.87	20.48	9.226	0.137
635	19	84.76	70.95	13.81	7.445	0.163
	20	84.79	68.54	16.24	7.445	0.139
641	19	94.39	77.72	16.67	9.146	0.166
	20	94.43	74.82	19.61	9.146	0.141
647	19	109.35	88.31	21.05	11.790	0.169
	20	109.41	84.75	24.65	11.790	0.145
653	19	126.61	100.49	26.11	14.910	0.172
	20	126.67	96.24	30.43	14.910	0.148
659	19	183.50	139.97	43.52	26.840	0.186
	20	183.63	133.65	49.98	26.840	0.163

hole - see Figure 2-12.) This was done only for runs using 5.6mm and 11mm thick perspex specimens with 30.5mm holes. Table 4-5 presents a sample of the results.

4.1.4 THERMAL CONDUCTANCE RESULTS FOR SPECIMENS WITH 35.5mm HOLES

Particle board specimens (plates 13 and 14) and 11mm thick perspex specimens (plates 5 and 6) had 35.5mm holes drilled in them. The measured thermal conductances are shown in Table 4-6.

4.1.5 THERMAL CONDUCTANCE RESULTS FOR SPECIMENS WITH 40.5mm HOLES

The thermal conductances of perspex plates 5 and 6 with 40.5mm holes are shown in Table 4-7.

4.1.6 THERMAL CONDUCTANCE RESULTS FOR DUROTHERM SPECIMENS

Table 4-8 shows the thermal conductances of durotherm with 34.925mm holes. The results in the run range 605 to 634 were obtained using polystyrene and air insulation in the stainless steel box. Those in the range 635 to 664 were obtained using fibreglass insulation.

4.1.7 QUANTITATIVE EXPERIMENTAL CURVES

Figures 4-1 to 4-3 summarise the above results and some associated data. They show the temperature differences across the specimens as functions of the heater wattage - the slopes being measures of conductances.

Figure 4-1 shows the effect of specimen thickness on the heat transfer rate for solid material and material with the same hole size (30.5mm diameter).

Figure 4-2 shows the effect of hole size on the same

FIGURE 4-1 HEAT FLUX Vs TEMPERATURE DROP

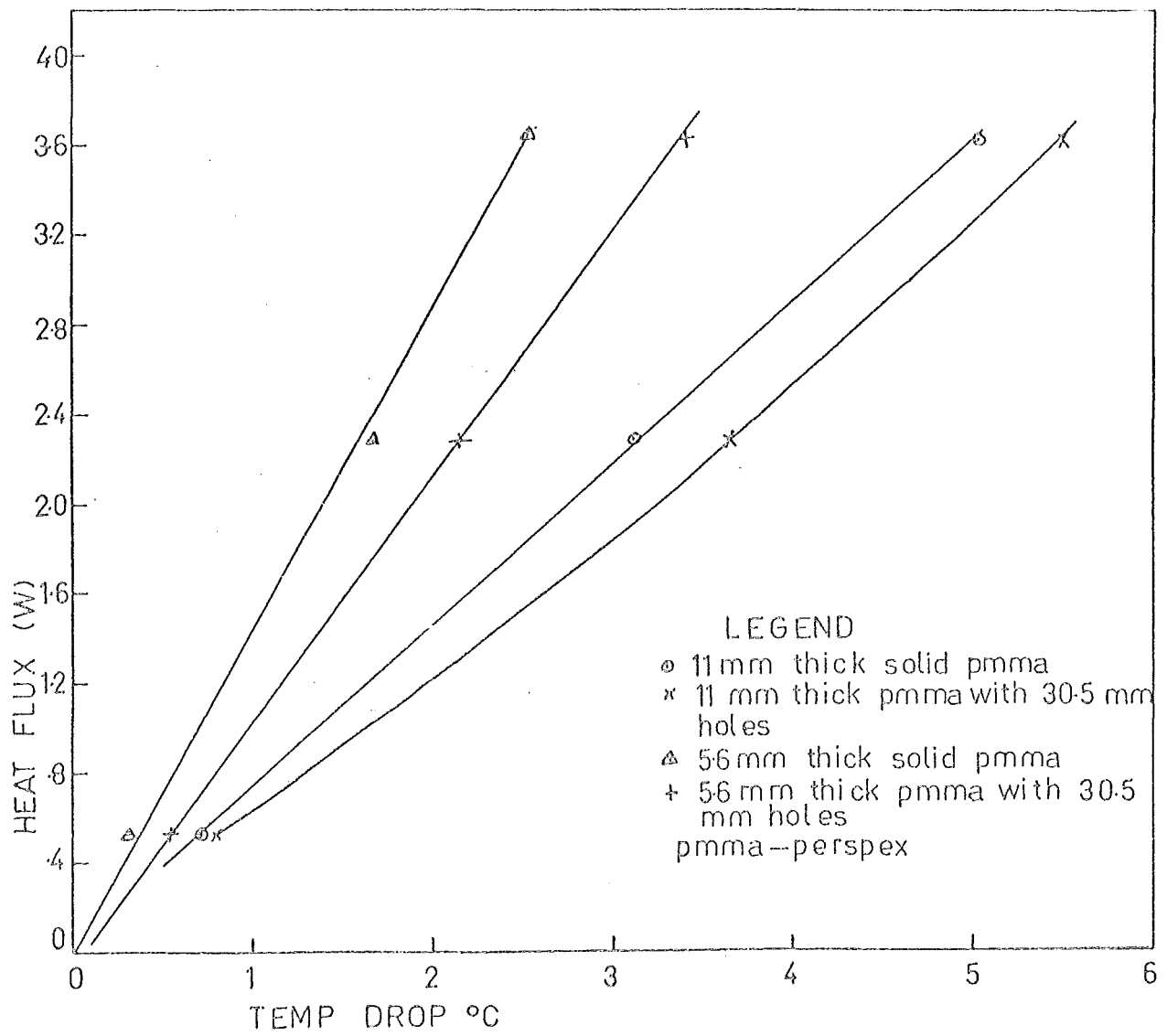


FIGURE 4-2 HEAT FLUX Vs TEMP DROP (11mm thick pmma various hole diameters)

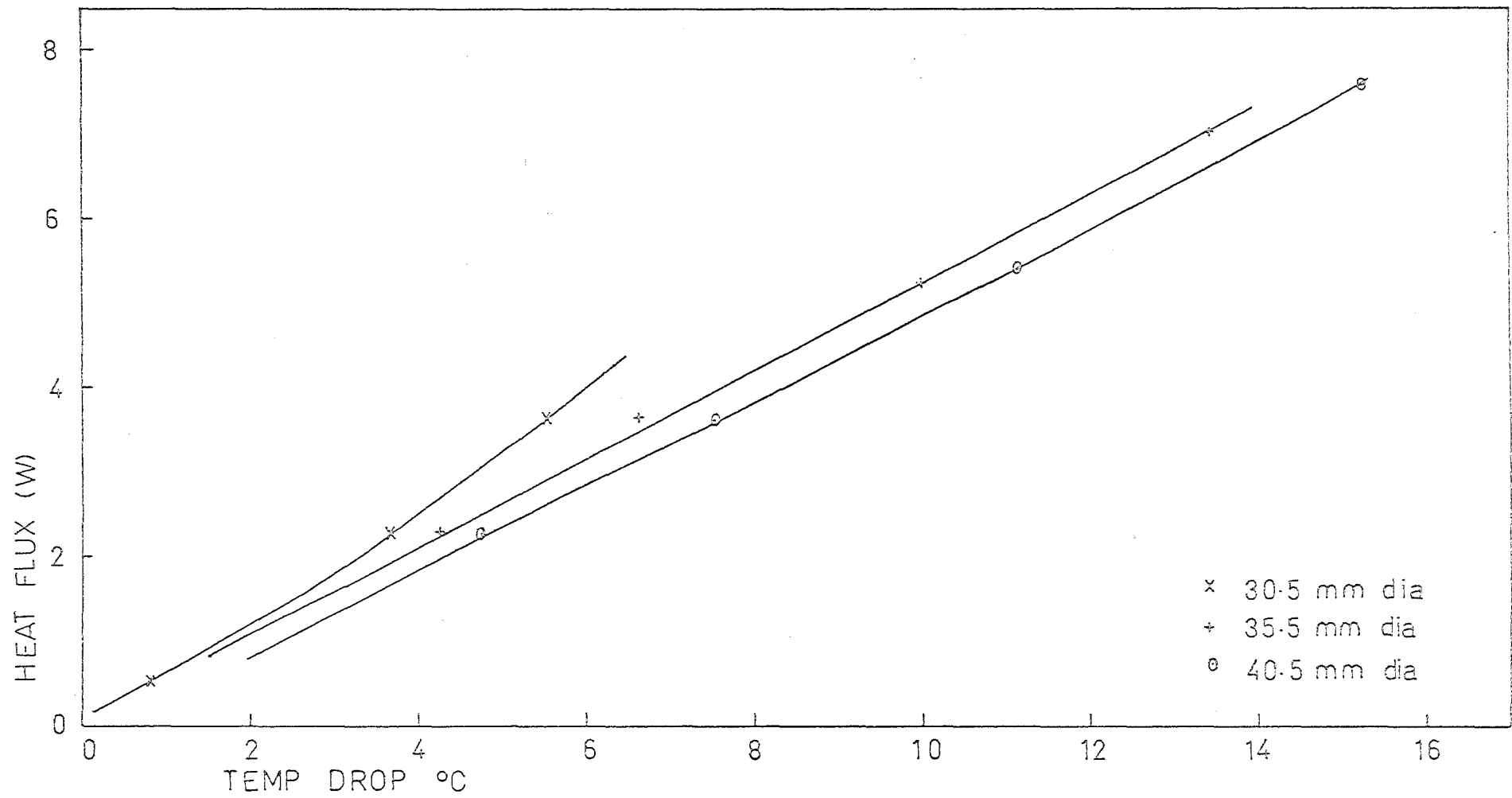


FIGURE 4-3 HEAT FLUX Vs TEMP DROP (durotherm)

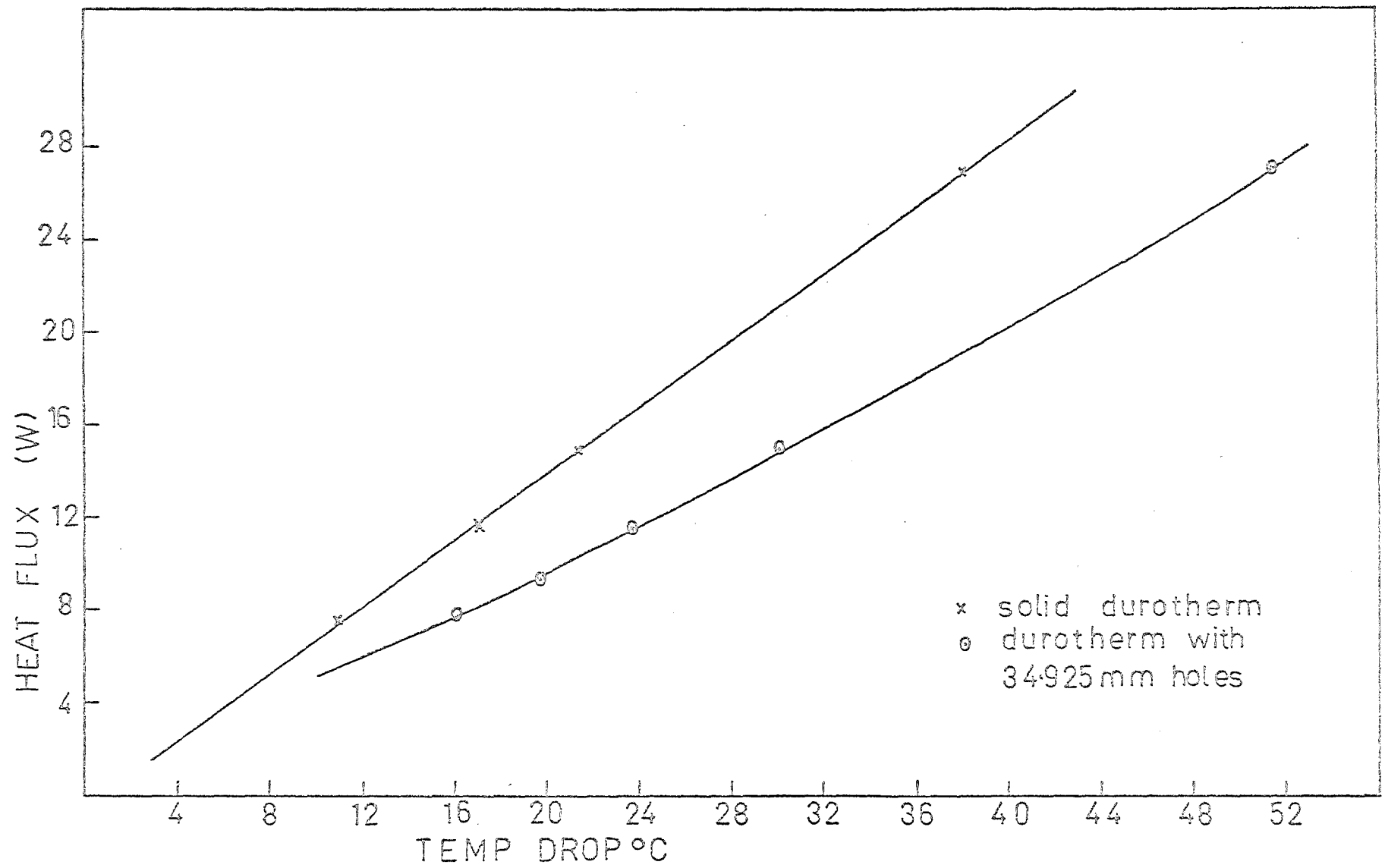


TABLE 4-9

Grashof And Rayleigh Numbers

Run	Gr	Ra
159	465	326
172	126	88
186	625	438
201	480	336
315	37	26
331	11	8
341	51	36
549	584	409
556	819	573
568	1113	779
576	1313	919
605	2052	1437
611	2470	1729
617	2692	1884
624	2886	2020
629	2275	1593
679	657	460
686	939	657
692	1226	858
698	1474	1032

specimen (plates 5 and 6).

Whereas the first two Figures used perspex specimens, the last Figure (Figure 4-3) used durotherm.

4.1.8 MISCELLANEOUS EXPERIMENTAL RESULTS

The Grashof and Rayleigh numbers associated with the experimental runs used in the theoretical simulations are evaluated in the Appendix. Table 4-9 presents them.

4.2 THEORETICAL RESULTS

Conduction heat flow in all directions varies from node to node. We know the conducted heat entering from the hot aluminium plate and leaving via the cold aluminium plate. Because of heat flow parallel to the aluminium plates, the total heat conducted perpendicular to the plates varies from layer to layer (Figures 4-6 and 4-7). We can define conduction heat flow across any plane parallel to the aluminium plates. The conduction heat flows tabulated and used in the diagrams are defined in each table and on each diagram.

Radiation can be defined as either the radiation leaving the hot end disc and touching cylinder or the radiation coming to the cold end disc and touching cylinder. The case used is defined for each Table and Figure. (Note that the sign convention used is that heat flow towards a nodal point is considered positive.)

The computed results of the simulation runs are presented in Table 4-10. They are:

(i) Heat transferred by solid conduction - this is the net heat flow crossing a given Z-X plane, perpendicular to the

TABLE L-10

Results Of The Numerical Simulations

Run	Emissivity = 0.04 Heat Transferred (Watts)				Emissivity = 0.11 Heat Transferred (Watts)				Emissivity = 0.2 Heat Transferred (Watts)				Emissivity = 0.5 Heat Transferred (Watts)			
	Solid	Air	Radiation	Total	Solid	Air	Radiation	Total	Solid	Air	Radiation	Total	Solid	Air	Radiation	Total
159	1.761	0.175	0.0456	1.981	1.760	0.175	0.057	1.991	1.758	0.175	0.072	2.005	1.755	0.175	0.130	2.059
172	0.381	0.023	0.009	0.413	0.381	0.023	0.011	0.415	0.381	0.023	0.014	0.418	0.380	0.023	0.025	0.429
186	2.584	0.167	0.074	2.825	2.583	0.167	0.092	2.842	2.581	0.167	0.117	2.865	2.576	0.167	0.212	2.955
201	1.787	0.155	0.047	1.989	1.786	0.155	0.058	1.999	1.785	0.155	0.073	2.014	1.782	0.155	0.133	2.070
315	1.856	0.141	0.016	2.053	1.856	0.141	0.023	2.06	1.856	0.141	0.033	2.07	1.856	0.141	0.0716	2.108
331	0.476	0.028	0.004	0.507	0.476	0.028	0.005	0.508	0.476	0.028	0.007	0.510	0.475	0.028	0.016	0.519
341	2.581	0.176	0.028	3.185	2.581	0.176	0.04	3.197	2.580	0.176	0.057	3.214	2.580	0.176	0.124	3.28
549	1.637	0.169	0.061	1.867	1.636	0.169	0.078	1.883	1.635	0.169	0.102	1.906	1.632	0.169	0.193	1.993
556	2.647	0.426	0.102	3.175	2.645	0.426	0.131	3.202	2.642	0.426	0.170	3.239	2.635	0.426	0.322	3.383
563	3.542	0.532	0.167	4.641	3.539	0.532	0.214	4.685	3.536	0.532	0.279	4.746	3.525	0.532	0.528	4.985
576	5.222	0.607	0.242	6.071	5.218	0.607	0.310	6.134	5.213	0.606	0.402	6.221	5.196	0.606	0.761	6.563
605	5.978	0.605	0.3	6.883	5.971	0.605	0.378	6.954	5.964	0.604	0.482	7.05	5.939	0.603	0.886	7.429
611	8.759	0.921	0.503	10.223	8.787	0.921	0.632	10.340	8.772	0.920	0.808	10.5	8.727	0.918	1.484	11.128
617	11.311	1.217	0.718	13.245	11.29	1.216	0.903	13.41	11.267	1.215	1.155	13.636	11.197	1.212	2.121	14.53
624	19.44	2.253	1.656	23.350	19.38	2.25	2.087	23.718	19.312	2.247	2.672	24.230	19.122	2.237	4.913	26.272
629	7.313	0.753	0.351	8.457	7.304	0.752	0.492	8.548	7.293	0.752	0.628	8.673	7.259	0.750	1.154	9.164
679	1.401	0.210	0.060	1.69	1.4	0.21	0.105	1.715	1.399	0.21	0.139	1.749	1.40	0.21	0.274	1.880
686	2.353	0.719	0.135	3.247	2.350	0.719	0.178	3.288	2.387	0.719	0.237	3.343	2.378	0.719	0.466	3.563
692	3.472	0.899	0.217	4.589	3.468	0.899	0.286	4.654	3.464	0.899	0.381	4.745	3.450	0.898	0.749	5.098
698	4.672	0.994	0.324	5.991	4.666	0.994	0.427	6.087	4.659	0.994	0.567	6.220	4.638	0.993	1.116	6.747

plane. Unless otherwise indicated, in all the Tables and Figures presented in this chapter, the heat transferred by solid conduction is the sum of the heat flows in conduction zone C2 - Figure B1.

(ii) Heat transferred by air conduction - this is defined in exactly the same way as described above (i). Unless otherwise indicated, heat transferred by air conduction is the sum of the air heat flows in the hole in the 'air-conduction' region corresponding to solid conduction region C2. In Figures B7 and B8, the net heat flows associated with air nodal points 129, 131, 157 and 183; and surface nodal points 132, 145, 158, 171 and 184.

(iii) Heat transferred by radiation between the surfaces in the holes - this is the net radiative loss from the surfaces associated with the conduction region as described above. For example, if solid conduction region C2 is considered, the corresponding radiation regions are 1, 2 and half of 3 (Figure B6).

(iv) The total heat transferred by the above three methods.

The results are presented for the four emissivity values of aluminium chosen. In Appendix H, the heat flows of all the solid, air and radiation regions are presented (Run 568A).

4.2.1 TEMPERATURE AND HEAT FLUX PROFILES

The temperatures of the nodal points in conduction region C2 (Figure B1) are shown in Figure 4-4. The results used are those of numerical simulation run 692A (emissivity of aluminium = 0.04). Similarly, Figure 4-5 shows the

FIGURE 4-4
Temperatures of Conduction Region C2
Numerical Simulation Run 692A

62.965	62.977	62.998	63.020	63.033	63.040	63.043	63.045	63.045	63.046	63.047	63.047
62.955	62.969	62.993	63.018	63.032	63.039	63.043	63.045	63.045	63.046	63.047	
62.923	62.943	62.976	63.011	63.028	63.037	63.042	63.044	63.044	63.046		
62.859	62.893	62.943	62.977	63.021	63.033	63.039	63.041	63.041			
	62.868	62.927	62.991	63.018	63.032	63.038	63.041				
		62.861	62.967	63.005	63.025	63.034					
			62.884	62.970	63.009						
				62.878							

FIGURE 4-5
Temperatures of Conduction Region C3
Numerical Simulation Run 692A

59.335	59.333	59.331	59.331	59.333	59.335	59.336	59.336	59.336	59.337	59.337	59.337
59.339	59.336	59.333	59.332	59.333	59.334	59.336	59.336	59.336	59.337	59.337	
59.353	59.347	59.338	59.334	59.333	59.334	59.335	59.336	59.336	59.336		
59.384	59.37	59.351	59.338	59.335	59.335	59.335	59.335	59.335			
	59.383	59.358	59.34	59.335	59.335	59.335	59.335				
		59.389	59.349	59.338	59.335	59.335					
			59.387	59.35	59.338						
				59.39							

temperatures in conduction region C3. Using the temperature profile data in the Appendix, temperature profiles for the other runs could be similarly presented.

Since every nodal point had six 'conduction-rods' connected, six heat flows were associated with each point. With fifty eight nodal points in the solid, the heat flux profiles could not be fully presented. Figures 4-6 and 4-7 show some of the heat flows using run 692A results. Only Z and X direction heat flows are shown.

4.2.2 HEAT BALANCES

The heat balances of a few nodal points (run 698) are presented in Table 4-11. Every simulation run had the heat balances and the corresponding 'out-of-balance' error calculated. In all runs, the 'out-of-balance' error was less than 0.03% of the heat flow through the node.

4.2.3 RADIATIVE TRANSFER

The radiation flows shown in Table 4-10 are re-presented in Table 4-12.

The results of 11mm thick perspex plates with 35.5mm holes (runs 549, 556, 568 and 576) are graphically shown in Figure 4-8.

Using the emissivity value of aluminium of 0.11, the effect of the three hole sizes in the 11mm thick perspex specimens is shown in Figure 4-9.

4.2.4 TOTAL HEAT TRANSFERRED

The contributions of each mechanism of heat transfer in the cavity problem are shown in Figures 4-10 to 4-12.

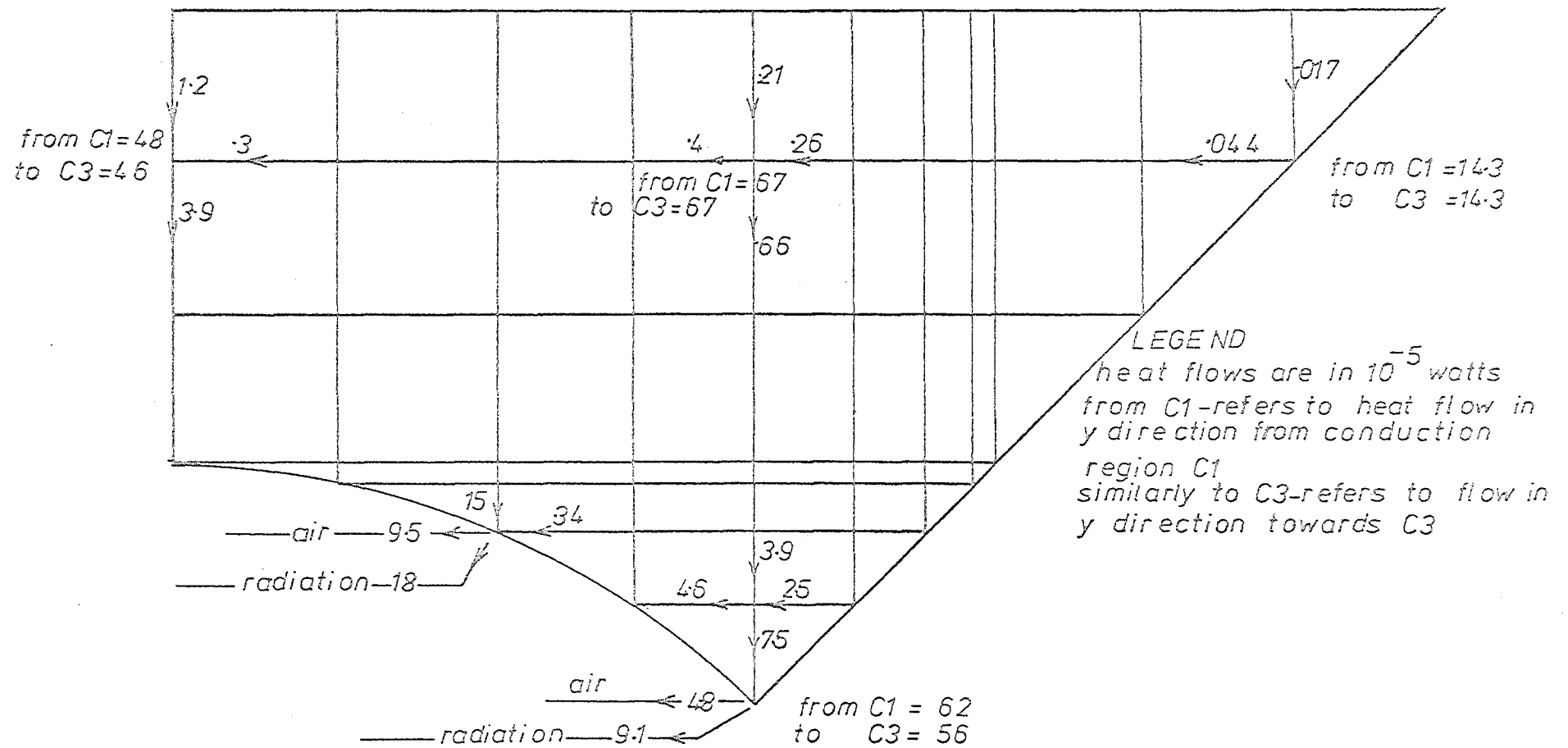


FIGURE 4-6 HEAT FLOWS FOR RUN 692A - CONDUCTION REGION C2

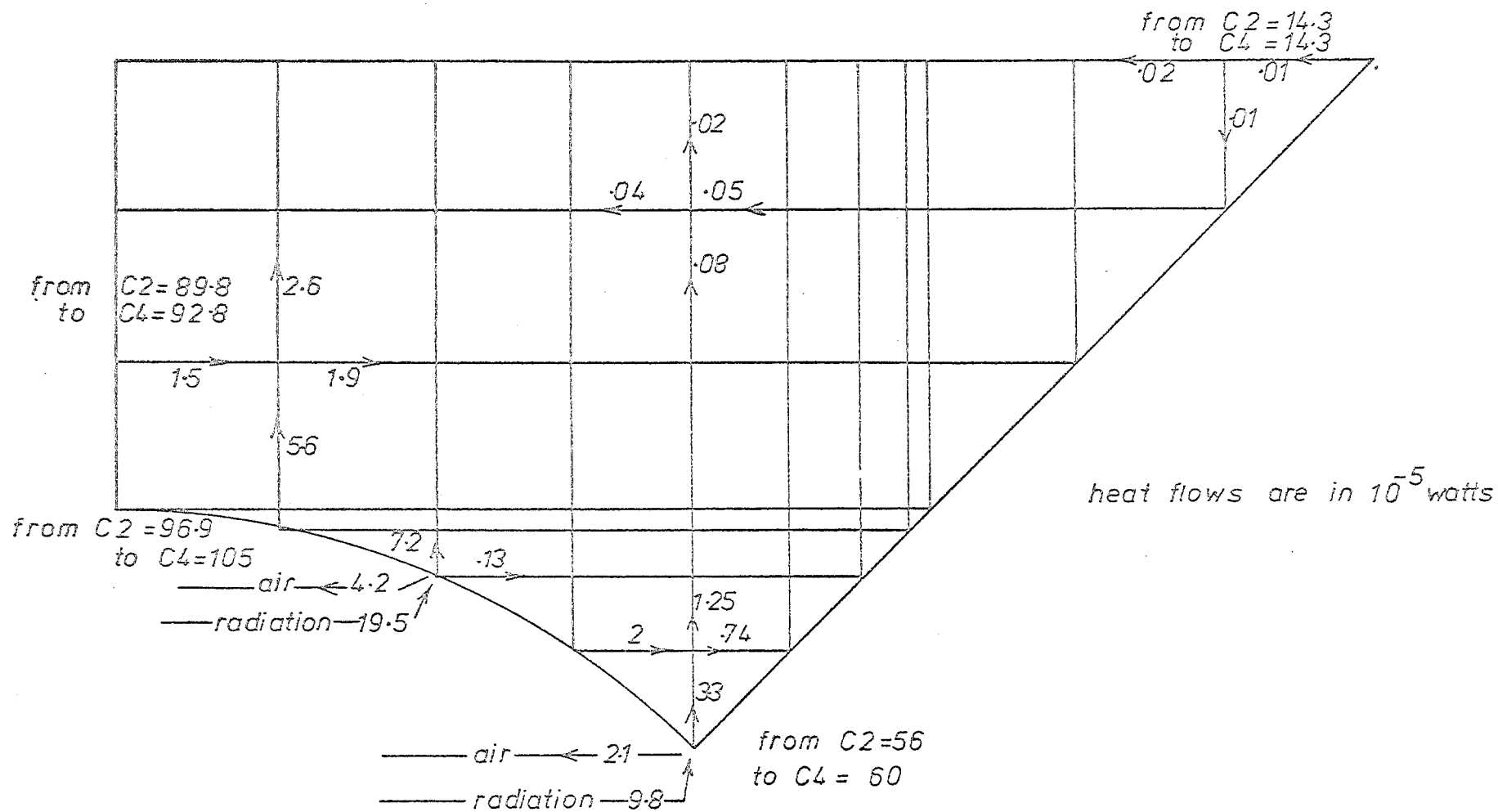


FIGURE 4-7 HEAT FLOWS FOR RUN 692A—CONDUCTION REGION C3

TABLE 4-11
Heat Balances

Nodal Point Number	Heat Into The Point (Watts)				Heat Conducted Away From Point (Watts)				% Error
	QYX(K+126)	QXY(K-1)	QZX(K-14)	Total	QYX(K)	QXY(K)	QZX(K)	Total	
129	-.535E-03	-.52E-05	0	-.54E-03	-.577E-03	.157E-04	.21E-04	-.54E-03	0
132	-.776E-03	-.23E-04 ⁺	-.136E-03*	-.935E-03	-.85E-03	-	.84E-04	-.935E-03	0
158	-.13E-02	-.46E-04 ⁺	-.27E-03*	-.167E-02	-.149E-02	-.37E-05	-.17E-03	-.167E-02	0
174	-.59E-03	-.53E-05	-.24E-04	-.615E-03	-.59E-03	-.319E-05	-.18E-04	-.615E-03	0.003
200	-.117E-02	-.819E-05	-.82E-04	-.126E-02	-.12E-02	-.90E-05	-.419E-04	-.126E-02	0

where: + - air conduction heat flows

* - radiation heat flows

% Error - $\frac{(\text{Heat into point} - \text{Heat out of point}) \times 2 \times 100}{(\text{Heat into point} + \text{Heat out of point})}$

K - nodal point counter

TABLE 4-12
Computed Radiation Heat Flows

Run	Temperature Drop Across Specimen °C	Radiation Heat Flow (Watts) For The Following Emissivities				Comments
		0.04	0.11	0.2	0.5	
159	3.65	0.046	0.057	0.072	0.130	11mm thick perspex plates (5 and 6) with 30.5mm holes
172	0.8	0.009	0.011	0.014	0.025	
186	5.51	0.074	0.092	0.117	0.212	
315	2.15	0.016	0.023	0.033	0.072	5.6mm thick perspex plates (3 and 4) with 30.5mm holes
331	0.53	0.004	0.005	0.007	0.016	
341	3.40	0.028	0.040	0.057	0.124	
549	4.25	0.061	0.078	0.102	0.193	11mm thick perspex plates (5 and 6) with 35.5mm holes
556	6.63	0.102	0.131	0.170	0.322	
568	9.97	0.167	0.214	0.279	0.528	
576	13.44	0.242	0.310	0.402	0.761	
605	16.12	0.300	0.378	0.482	0.886	12mm thick durotherm plates (19 and 20) with 34.925mm holes
611	23.66	0.503	0.632	0.808	1.484	
617	30.29	0.718	0.903	1.155	2.121	
624	51.54	1.656	2.087	2.672	4.913	
629	19.70	0.390	0.492	0.628	1.154	
679	4.74	0.080	0.105	0.139	0.274	11mm thick perspex plates (5 and 6) with 40.5mm holes
686	7.51	0.135	0.178	0.237	0.466	
692	11.12	0.217	0.286	0.381	0.749	
698	15.22	0.324	0.427	0.567	1.116	

FIGURE 4-8 RADIATIVE TRANSFER Vs TEMP DROP FOR VARIOUS EMISSIVITY (pmma with 35.5mm holes)

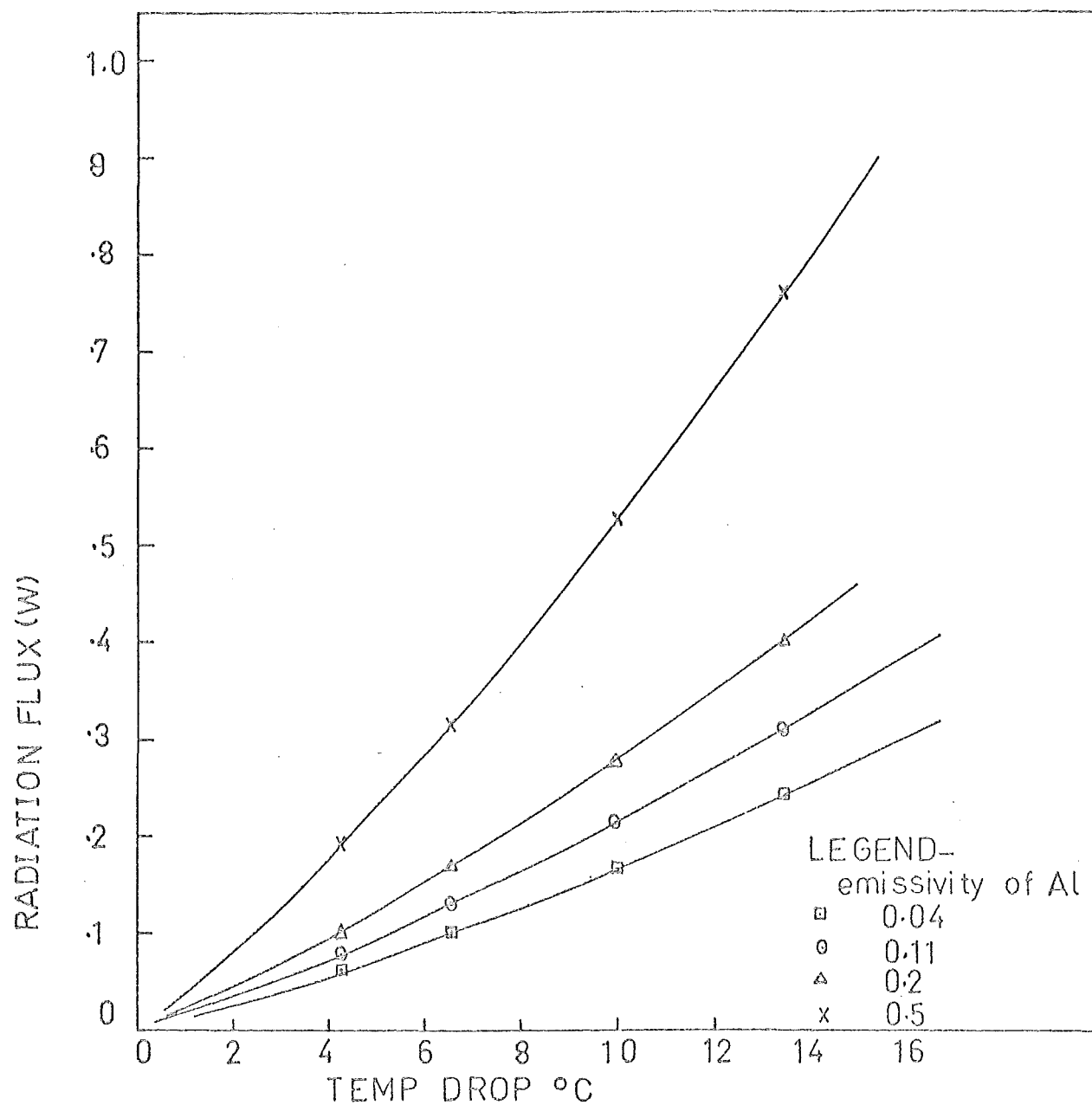
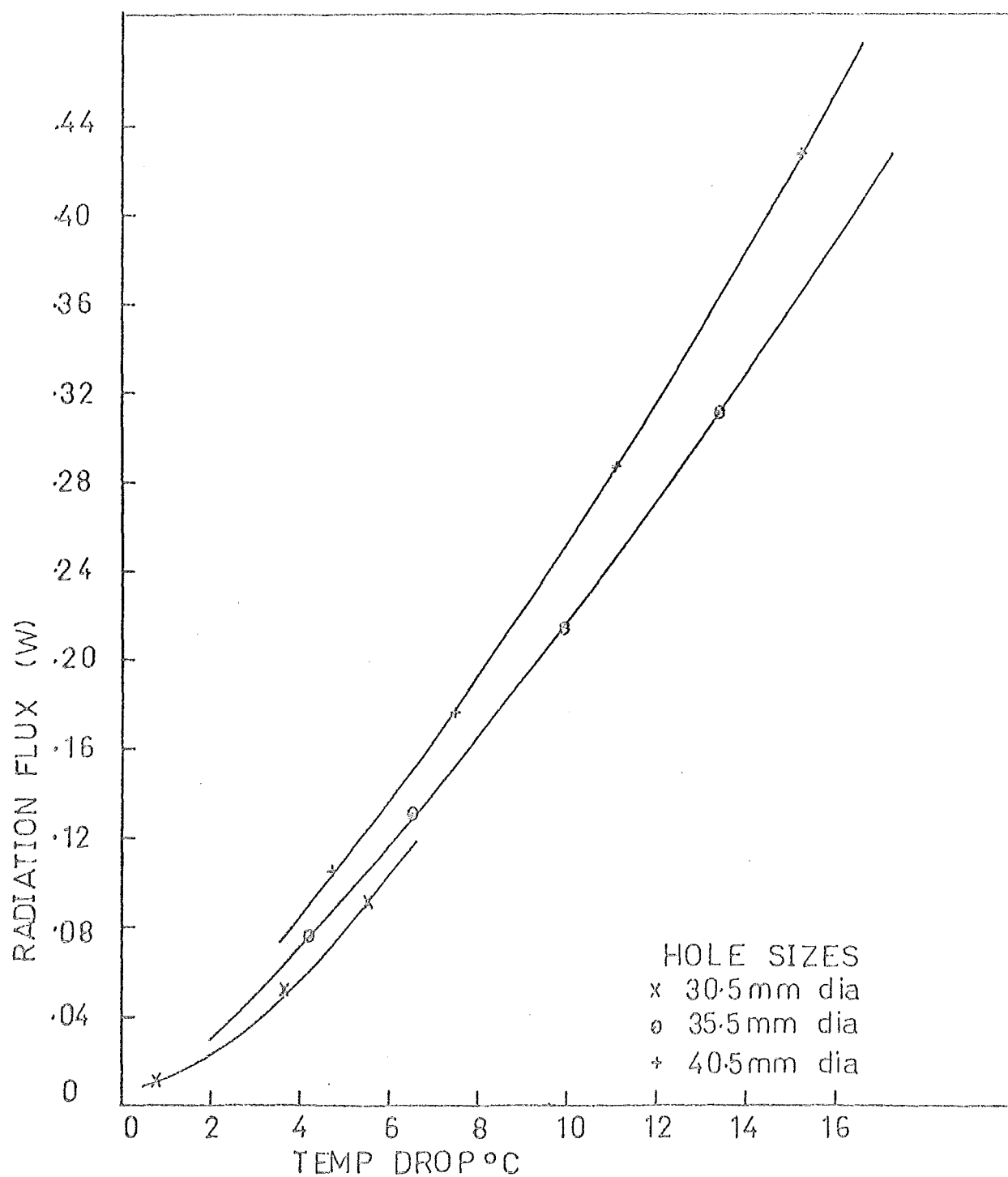


FIGURE 4-9 RADIATIVE TRANSFER Vs TEMP DROP FOR VARIOUS
HOLE SIZES (11mm thick pmma with $E_v = 0.11$)
Al



(1) Figure 4-10: Using the results of the durotherm runs with an aluminium emissivity of 0.11, the heat flows are plotted against the temperature differences.

(2) Figure 4-11: Similar to Figure 4-10, but with 11mm thick perspex plates with 35.5mm holes used instead of durotherm plates.

(3) Figure 4-12: Using the results of 11mm thick perspex plates (run 576), the heat transferred is plotted against the emissivity.

4.3 COMPARISON OF EXPERIMENTAL AND THEORETICAL RESULTS

As previously mentioned (Chapter 1), to analyse the cavity problem fully, experimental measurements of gas conduction, solid conduction and radiation are required. The experimental procedure used did not measure any of these quantities individually. Consequently, the comparison with theoretical results is given in terms of the total heat transferred.

Table 4-13 compares the total heat transferred from the experimental runs with that computed from the numerical simulations using the four values of the emissivity of aluminium. The results obtained using 11mm thick perspex with 40.5mm holes are also shown graphically in Figure 4-13.

DISCREPANCIES BETWEEN THE THEORETICAL AND EXPERIMENTAL RESULTS

The difference between the theoretical and the experimental results is presented in Table 4-14 as an error percentage.

$$\text{error percentage} = \frac{(Q_{\text{experimental}} - Q_{\text{theoretical}})}{Q_{\text{experimental}}} \times 100$$

(4-1)

FIGURE 4-10 THE CONTRIBUTION OF EACH MECHANISM OF HEAT TRANSFER (durotherm)

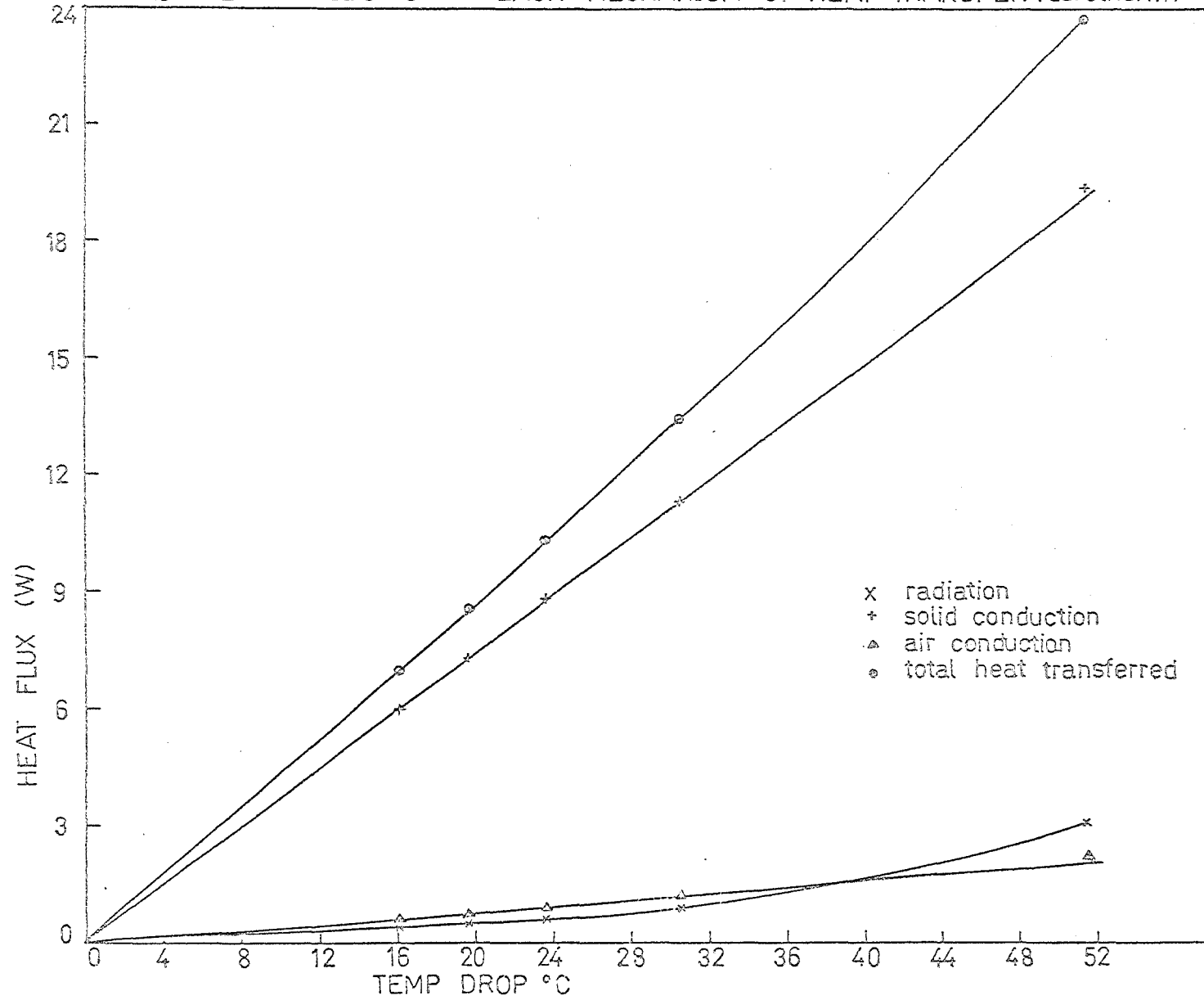


FIGURE 4-11 THE CONTRIBUTION OF EACH MECHANISM OF
HEAT TRANSFER IN PMMA WITH 35.5mm HOLES
($E_{Al} = 0.11$)

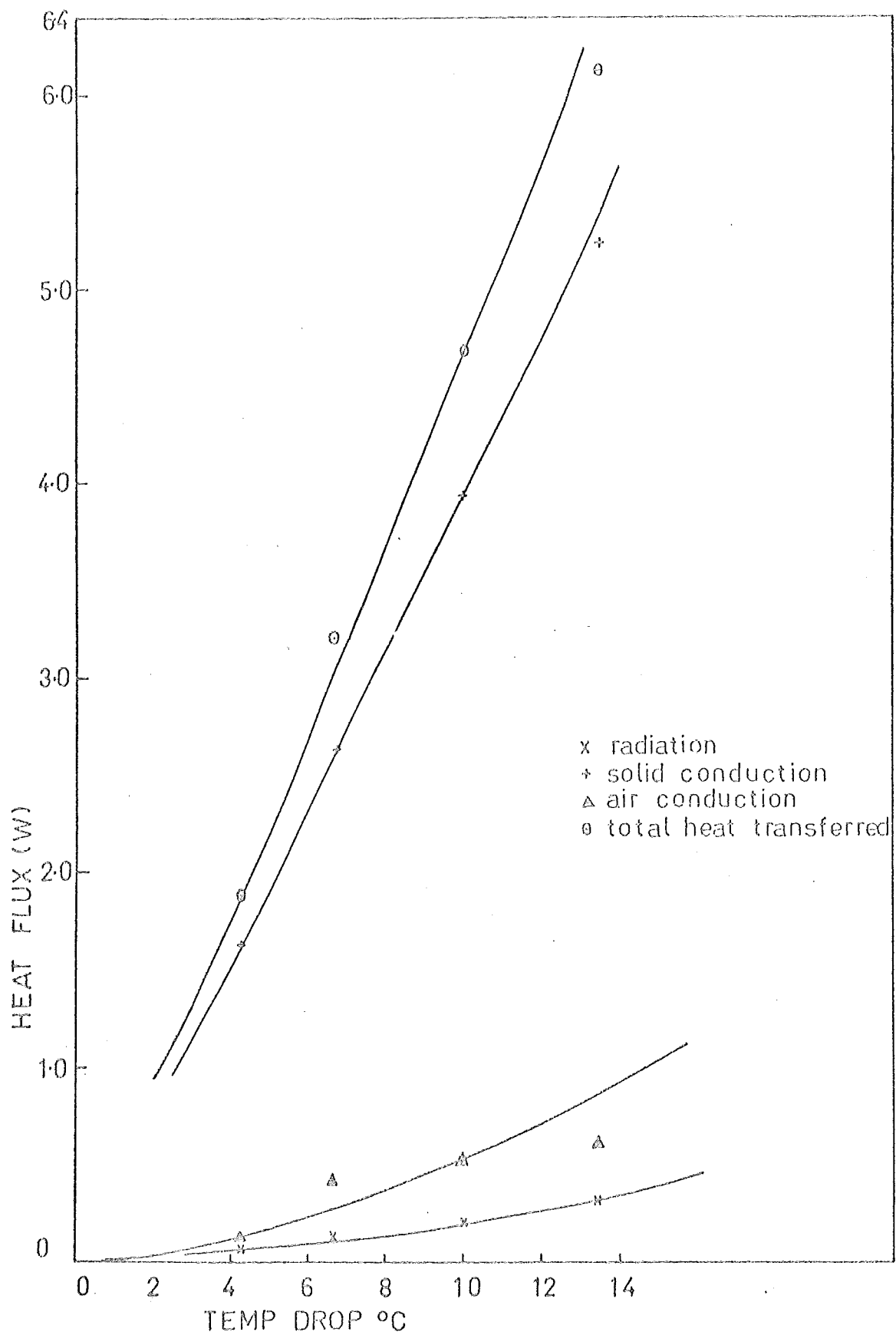


FIGURE 4-12 THE EFFECT OF EMISSIVITY (pmma with 35.5mm holes)

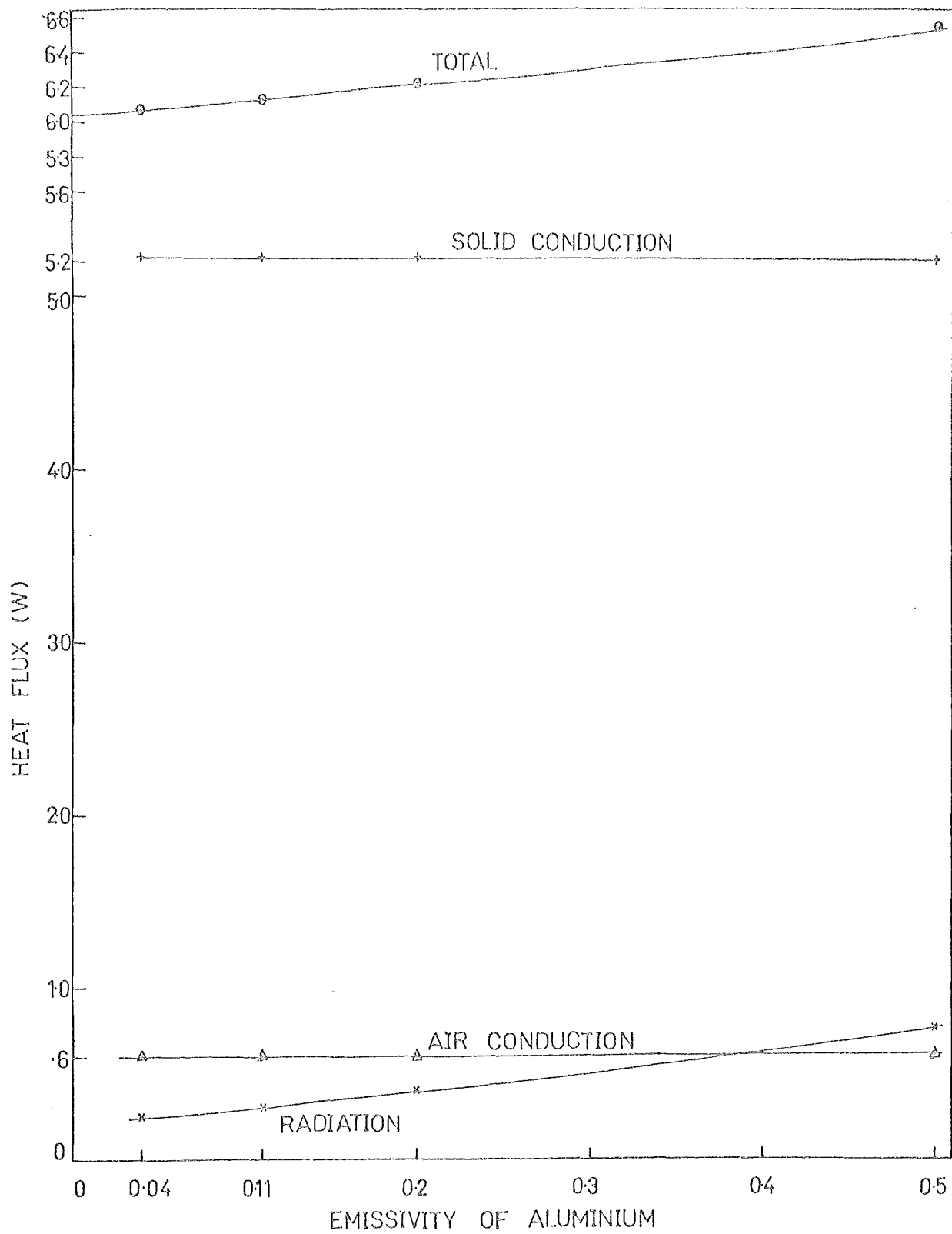


TABLE 4-13
The Total Heat Transferred - Experimental and Theoretical
For Various Values Of Aluminium Emissivity

Run	Total Heat Transferred (Watts)					Comments
	Experimental	Computed From Numerical Simulations For Emissivities Of Aluminium Of:				
		0.04	0.11	0.2	0.5	
159	2.294	1.981	1.991	2.005	2.059	11mm thick perspex plates with 30.5mm holes
172	0.526	0.413	0.415	0.418	0.429	
186	3.62	2.825	2.842	2.865	2.995	
201	2.301	1.989	1.999	2.014	2.070	As above with perspex plates swapped
315	2.289	2.053	2.060	2.070	2.108	5.6mm thick perspex plates with 30.5mm holes
331	0.528	0.507	0.508	0.510	0.519	
341	3.63	3.185	3.197	3.214	3.280	
549	2.292	1.867	1.883	1.906	1.993	11mm thick perspex plates with 35.5mm holes
556	3.65	3.175	3.202	3.239	3.383	
568	5.548	4.641	4.685	4.746	4.985	
576	7.518	6.071	6.134	6.221	6.563	
605	7.691	6.883	6.954	7.050	7.429	12mm thick durotherm plates with 34.925mm holes
611	11.528	10.223	10.340	10.500	11.128	
617	14.928	13.245	13.410	13.636	14.530	
624	27.069	23.350	23.718	24.230	26.272	
629	9.226	8.457	8.548	8.673	9.164	
679	2.272	1.690	1.715	1.749	1.880	11mm thick perspex plates with 40.5mm holes
686	3.633	3.247	3.288	3.343	3.563	
692	5.432	4.589	4.654	4.743	5.098	
698	7.6	5.991	6.087	6.220	6.747	

FIGURE 4.13 TOTAL HEAT TRANSFERRED--EXPERIMENTAL
Vs THEORETICAL (11 mm thick pmma with 40.5 mm holes)

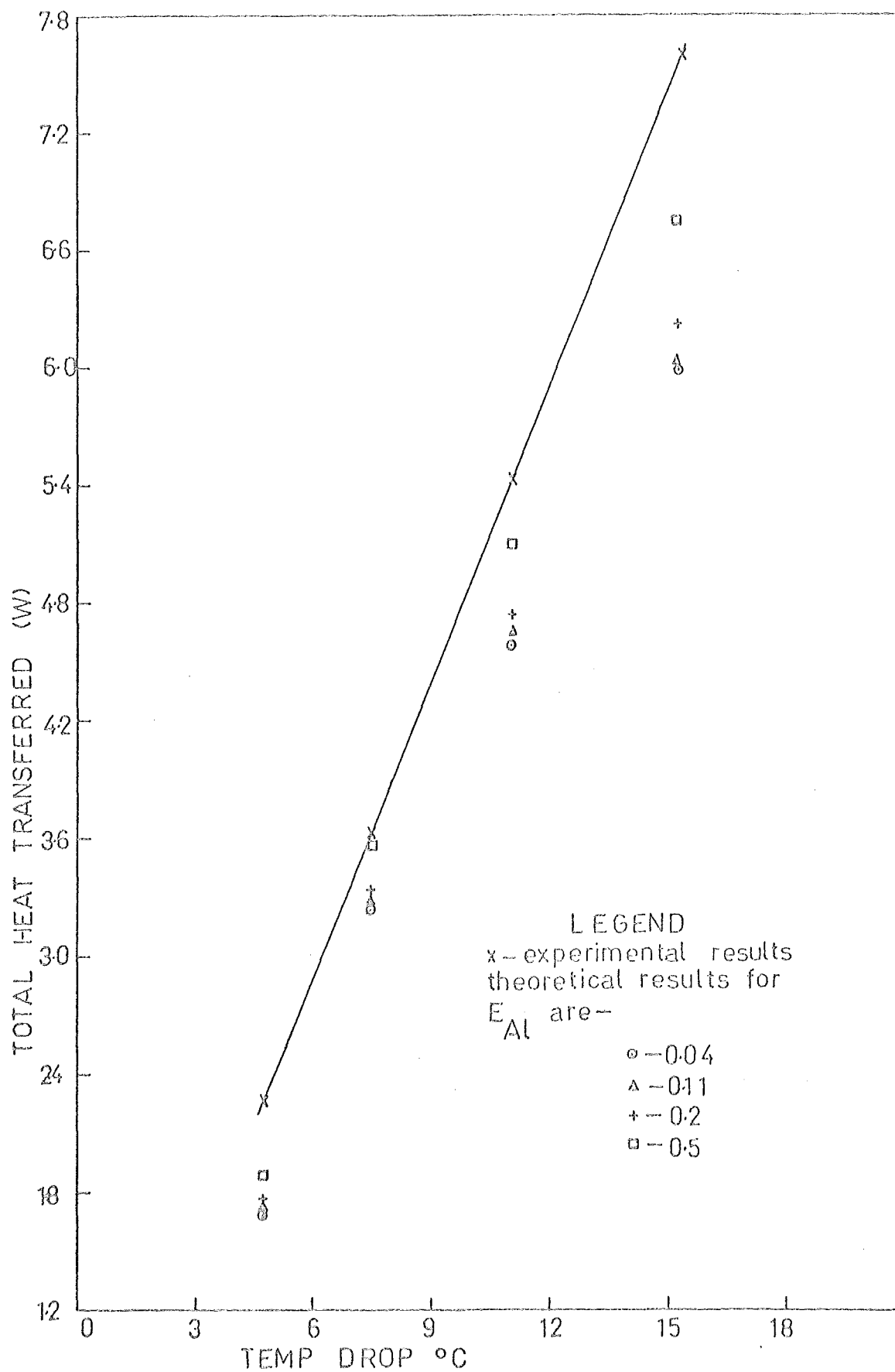


TABLE 4-14

The Discrepancies Between The Theoretical
And The Experimental Results

Run	Error Percentage Between Theoretical And Experimental Total Heat Flows				Comments
	Emissivity Of Aluminium				
	0.04	0.11	0.2	0.5	
159	13.64	13.21	12.60	10.24	11mm thick perspex plates with 30.5mm holes
172	21.48	21.10	20.53	18.44	
186	21.96	21.49	20.86	18.37	
201	13.56	13.12	12.47	10.04	
315	10.31	10.00	9.57	7.90	5.6mm thick perspex plates with 30.5mm holes
331	3.98	3.78	3.41	1.70	
341	12.60	11.93	11.46	9.64	
549	18.54	17.84	16.84	13.05	11mm thick perspex plates with 35.5mm holes
556	13.01	12.27	11.26	7.32	
568	16.35	15.56	14.46	10.15	
576	19.25	18.41	17.25	12.70	
605	10.51	9.58	8.33	3.41	12mm thick durotherm plates with 34.925mm holes
611	11.32	10.31	8.92	3.47	
617	11.27	10.17	8.65	2.67	
624	13.74	12.38	10.49	2.94	
629	8.34	7.35	5.99	0.67	
679	25.62	24.52	23.02	17.25	11mm thick perspex plates with 40.5mm holes
686	10.62	9.50	7.98	1.93	
692	15.52	14.32	12.68	6.15	
698	21.17	19.91	18.16	11.22	

CHAPTER 5DISCUSSION

5.1	<u>DISCUSSION OF THE APPARATUS</u>	186
5.1.1	REFERENCE MATERIALS	186
5.1.2	GUARDED HOT PLATE	187
5.1.3	MEASURING INSTRUMENTS	192
5.2	<u>DISCUSSION OF EXPERIMENTAL RESULTS</u>	193
5.2.1	DISCUSSION OF THERMAL CONDUCTIVITY RESULTS	193
5.2.2	DISCUSSION OF THERMAL CONDUCTANCE RESULTS	194
5.3	<u>DISCUSSION OF THEORETICAL RESULTS</u>	197
5.3.1	CREDIBILITY OF THE COMPUTED RESULTS	197
5.3.1.1	Fidelity of the Computer Program	197
5.3.1.2	Accuracy of the Results	197
5.3.1.3	Convergence	198
5.3.1.4	Experimental Verification of Computer Solutions	198
5.3.2	TEMPERATURE AND HEAT FLUX PROFILES	199
5.3.3	EFFECT OF MATERIAL THICKNESS	200
5.3.4	EFFECT OF HOLE SIZE	200
5.3.5	THE EFFECT OF EMISSIVITY	201
5.3.6	THE EFFECT OF RADIATION AND GAS CONDUCTION	202
5.4	<u>DISCUSSION OF APPARATUS PERFORMANCE AND THEORETICAL ANALYSIS</u>	202
5.4.1	PERSPEX RESULTS	203
5.4.2	DUROTHERM RESULTS	203
5.5	<u>CHARACTERISTICS OF THEORETICAL RESULTS</u>	204
5.6	<u>DISCUSSION CLOSURE</u>	207

CHAPTER 5

DISCUSSION

5.1 DISCUSSION OF THE APPARATUS

It has not been possible with the equipment (designed and built) to do full justice to the cavity problem. For example, gas conduction, solid conduction and radiation have not been measured experimentally. The cavity problem encompasses many materials in a wide range of practical conditions (for example temperatures and thicknesses). Many factors (section 1.3) can influence both the material and the results obtained.

5.1.1 REFERENCE MATERIALS

In work devoted to thermal conductivity (and/or conductance) measurements, some guide to the accuracy of the method can be obtained by the comparison of results obtained on reference materials. One of the difficulties for the case of the guarded hot plate method concerns the absence of suitable materials. The only ones which can be regarded as true reference materials are a pure gum rubber, a cork board, and a fibrous glass material of two different densities (6). All these have a limited temperature range of use. Rubber was used in trial runs (Chapter 3), but was found to be unsuitable due to the uncertainties in its thickness, homogeneity and thermal creep behaviour (143). Cork board was also used and rejected as its structure was not stable - (a) the moisture content varied with temperature, (b) the glue used to hold the wood particles together decomposed on heating, and (c) cork board is not homogeneous.

A suitable material to be used with the equipment designed in this work needs to be:

(a) an opaque insulator with a thermal conductivity of about $0.03 \text{ W/M}^{\circ}\text{C}$

(b) machineable

(c) homogeneous

Perspex was used in this work because it is:

- homogeneous
- machineable
- available locally in varying thicknesses

Perspex has a limited temperature range (maximum service temperature is 80°C). It is also partially transparent to radiation in the wavelength range 0.3 to 1.6 microns. The radiation transfer in this range was checked approximately (Appendix) and found to be negligible. Durotherm, which is opaque, was also used to check the validity of the developed experimental and numerical methods (at temperatures higher than 80°C , up to 160°C).

Other materials considered were:

- teflon which is very expensive (\$1500 for the specimen sizes used in this work)
- phenol formaldehyde (bakelite) which is not available locally
- Triton's kaowool and ICI's saffil aluminium fibre will become available next year

5.1.2 GUARDED HOT PLATE

The apparatus built in this work is the low temperature guarded hot plate. The maximum operating temperature is 600°K . Provided a suitable material can be found, it is possible to operate the apparatus at temperatures greater than 473°K

(where radiation is significant (47,48,60)).

From the nine thermocouple wires on each isothermal aluminium plate, the one dimensional heat flow assumption was ^{No} verified. The standard deviation of the thermocouple outputs on any plate was less than 0.001 millivolts. This corresponds to a probable error percentage of 0.02.

The power into the guarded hot plate was evaluated from the product of the voltage and current. The voltage and the current were measured to a high degree of accuracy (0.005%). The actual power dissipated through the specimens was assumed to be half the electrical power since two specimens were present (Chapter 1). There was no way of checking this assumption experimentally other than by comparing the temperatures of the two cold aluminium plates (and also the two hot aluminium plates). Other workers (30,44) used cooling coils in the cold aluminium plates and measured the heat gained by the cooling water. The use of cooling coils in the cold aluminium plates makes the guarded hot plate bulky and not so easy to dismantle and assemble. However, in order that the heat transferred by the specimens be known accurately, cooling coils are essential (Chapter 7).

The enclosure surrounding the guarded hot plate is important (49). The results of experimental runs Series 'A' (when plastic bags were used to enclose the apparatus) verify this. Steady-state was attained in three hours or less. With the stainless steel enclosure (Series 'B'), steady-state was attained after thirty six hours. From Table E1 (Series 'A' results), the temperature drop across perspex specimen 'CA' is 1.6°C , whereas that across specimen 'CB' is 1.67°C . The

difference between these two temperature drops is 0.07°C (a systematic error percentage of 4.3). For a typical Series 'B' experimental run, the mean temperature drop across perspex plate 1 is 1.66°C , and that across perspex plate 2 is 1.78°C . The difference between these two temperature drops is 0.12°C (a systematic error percentage of 7). Hence, although the perspex plates ('CA' and 'CB') of Series 'A' experiments were unmachined, they still gave better results than Series 'B' experiments (with the machined perspex plates). It seems likely that Series 'A' experiments gave better results because of the absence of the insulation resistance in the region of the cold aluminium plates because plastic bags were used instead of the stainless enclosure (see below). The hydrostatic pressure forced all the air out of the plastic bags and the aluminium plates were surrounded by the constant temperature water. In the stainless steel enclosure (used in Series 'B' experiments), insulation was put inside (Figure 2-5) and the thermocouple wire outlet tube blocked by cotton wool. A substantial amount of air remained in the box. Consequently, the insulation resistance in the stainless box contributed to the accuracy of the results obtained. As previously mentioned (Chapter 3), plastic bags were not used in Series 'B' experiments because they tore easily and hence leaked during runs.

The importance of the insulation used in the stainless box is illustrated by some of the durotherm runs. In runs 635 to 664, the guarded hot plate was completely surrounded by fibreglass insulation. Using the same temperature drops (voltage settings) as in runs 605 to 634, the thermal conductances were measured. Consider for example the results

of runs 611 and 647 (the former run used the polystyrene-air insulation system of Figure 2-5, while the latter run used fibreglass insulation).

(A) Run 611 - The thermal conductance of durotherm plate 19 = $0.147 \text{ W/M}^{\circ}\text{C}$ at a temperature drop of 23.66°C . The conductance of plate 20 = $0.138 \text{ W/M}^{\circ}\text{C}$ at a temperature drop of 25.22°C .

(B) Run 647 - The thermal conductance of durotherm plate 19 = $0.169 \text{ W/M}^{\circ}\text{C}$ at a temperature drop of 21°C and the conductance of plate 20 = $0.145 \text{ W/M}^{\circ}\text{C}$ at a temperature drop of 24.65°C .

Assuming that the discrepancy between the 'temperature-drops' across the specimens on either side of the heater is due to different heat flows through each specimen, the mean temperature drop should be used to work out the conductance. The causes of this discrepancy were discussed preliminarily in Chapter 2 in the description of the 'positioning arrangement' experiments. It was observed that the temperature of cold plate 11a was always greater than that of cold plate 11b. This statement is true for runs I to VI in Chapter 2, however, in general it is not true. In runs 432 to 444, the reverse is true. For example, in run 432, the temperature of cold plate 11a is 49.1°C , whereas that of aluminium cold plate 11b is 49.21°C . Similarly, in runs 289 to 314, the temperature of cold aluminium plate 11b is greater than that of cold aluminium plate 11a. Various other series of runs in the range 1 to 738 can be found in which the temperature of plate 11b is greater than that of plate 11a. From these observations and those outlined in Chapter 2, the difference in the

'temperature-drops' across the specimens was termed the systematic error of the experiment (with a magnitude of 10% (Appendix)). The causes of the systematic error were:

(a) Arrangement of the guarded hot plate in the box - since the insulation inside the box contributed substantially to the heat transfer, any slight changes in the exact positioning of the apparatus caused one cold aluminium plate to have a different external resistance from that of the other side. Orr (49) found it necessary to control the ambient temperature in the box by stirring the air with a large diameter fan at low speed and keeping the box close to the mean specimen temperature.

(b) Arrangement of the plates - in assembling the guarded hot plate, it was practically impossible to align the plates in exactly the same positions relative to one another. Set squares and right-angled steel sections were used in trying to align the plates in the same positions.

GENERAL REMARKS - GUARDED HOT PLATE:

(1) Fluctuations in the power supply could not be eliminated despite the use of two stage voltage regulation (Figure 2-2). The resulting process error was 0.04% (Appendix).

(2) The constant pressure on the plates (for good thermal contact) was implemented by the use of stainless steel studs and 'cross-bar' supports (Figure 2-3).

(3) The emissivity of the aluminium surfaces in the apparatus was not known accurately.*

5.1.3 MEASURING INSTRUMENTS

(1) Thermocouple outputs - these were measured using a potentiometer. The uncertainty in the potentiometer readings was 2 microvolts. The monitoring of the millivolt signals was a slow process (and very demanding in human endurance). More readings would have been obtained had an accurate digital potentiometer been available (for example, Honeywell, Model 40011-20). The uncertainty in the calibration of thermocouple wires was 0.04°C (Chapter 2). Considering a surface temperature of 45°C , the uncertainty in the indicated temperature was 0.02°C (Chapter 1).

(2) Power input - due to the accuracy of the digital multimeters used, the uncertainty in the product of the voltage and the current was 0.01%.

(3) Waterbath - the thermostatic bath was kept at $31.0 \pm 0.1^{\circ}\text{C}$.

(4) Plates - the aluminium plates and all the specimens were machined to $\pm 0.03\text{mm}$. Considering perspex plate 5 for example, the error due to its non-flatness was 0.3%.

* Preliminary measurements were made by Dr J.B. Stott of the Chemical Engineering Department, University of Canterbury. The radiation emitted by a plane aluminium surface similar to those used in the conductance experiments was compared with the radiation from a similar soot blackened surface using a 'Moll' thermopile over the temperature range 25° to 90°C . These experiments gave an emissivity of 0.08.

5.2 DISCUSSION OF EXPERIMENTAL RESULTS

The curves and tables of Chapter 4 and the Appendix summarise the results of the experimental investigations reported in this work.

5.2.1 DISCUSSION OF THERMAL CONDUCTIVITY RESULTS

The basis of the thermal conductivity evaluations is the Fourier equation (1-1). The uncertainties in the variables q , A , dT and dx all contribute to the uncertainty in the value of K . As previously discussed, the largest source of error is the systematic error (difference in the temperature drops across the specimens) (systematic error is equal to 10%). The other variables (A , q , dx -- process and measurement errors) contribute 2% to the experimental error (Appendix) making the total experimental error 12%.

The reliability of the apparatus is in its ability to reproduce the thermal conductivity of a given material at the same settings. The A.S.T.M. Standard (5) requires that the thermal conductivity be reproduced to within 1% from four consecutive readings every half hour. From Table 4-2, the thermal conductivities of 5.6mm and 11mm thick perspex plates are reproduced to within 1%. (For example, in runs 1 to 14, the mean thermal conductivity of plate 1 was $.1934 \text{ W/M}^{\circ}\text{C}$, with a standard deviation of $.002$.) The exceptions were runs performed at mean specimen temperatures of 36°C . The thermal conductivities for these runs were reproduced to within 9% (for example, runs 29 to 42). This large discrepancy was caused by the small temperature drops across the perspex specimens. For example, in run 30, the temperature drop across perspex plate number 4 was 0.5°C .

In the Appendix, Table F2 shows the mean thermal conductivities of the perspex plates 1 to 8, that is, the means of the temperature drops on both sides of heater have been used. For example, considering plate 1, the thermal conductivity was evaluated as the mean of results of runs 1 to 14, and those of runs 69 to 80. The value obtained was $0.194 \text{ W/M}^{\circ}\text{C}$ with a standard deviation of 0.0008. An estimate of the discrepancy in the determined thermal conductivity was 0.41%. For 11mm thick perspex plate 5, the discrepancy was found to be 3.5% (this was the worst discrepancy - Table F2). The determined thermal conductivities of perspex are in agreement with the literature values - $0.188 \text{ W/M}^{\circ}\text{C}$ (145) and (146).

The observations mentioned above also apply to the other materials used in this work. For example, the thermal conductivity of durotherm plate number 19 at 66°C is $0.2075 \text{ W/M}^{\circ}\text{C}$ with a standard deviation of 0.0006. Hence, the thermal conductivity of durotherm was determined to within 1%. The results of the thermal conductivities of 19mm thick perspex, particle board, syndanyo board, polystyrene and durotherm are in Table 4-3. Syndanyo board results show a large discrepancy at high temperatures (thermal conductivity of plate 15 is $0.80 \text{ W/M}^{\circ}\text{C}$, while that of plate 16 is $0.69 \text{ W/M}^{\circ}\text{C}$ at 110°C). Consequently, syndanyo board was not used in the experiments with holes drilled.

5.2.2 DISCUSSION OF THERMAL CONDUCTANCE RESULTS

The difference in the 'temperature-drops' across the specimens is evident in most results. For example, from Table 4-4, run 159, the temperature drop across perspex plate 5 is 3.65°C , while that across perspex plate 6 is 4.04°C . The

discrepancy between these two readings is 10%. Tables 4-4 to 4-8 show the temperature drops across the various specimens with different hole sizes.

Figure 4-1 shows the variation of total heat transferred with specimen thickness. Using the results of 5.6mm and 11mm thick perspex specimens with 30.5mm holes, the heat transferred is plotted against the temperature drop. As expected, for the same temperature drop, the thicker specimen transfers more heat than the thinner one. Also shown in the Figure are the curves of heat flux versus temperature drop for solid specimens. Again, as expected, the introduction of 30.5mm holes lowers the thermal conductances in both cases. Figure 4-3 shows the same results as described above, but using durotherm. It is significant that the plot of heat flux versus temperature difference across the specimen passes through the origin in all cases which have been plotted.

For the same material, the effect of hole size is shown in Figure 4-2. Using the results of 11mm thick perspex plate 5, the heat transferred is plotted against the temperature drop for the three holes used (30.5, 35.5 and 40.5mm). For the same heat flux, the temperature drop across the specimen increases significantly with hole diameter. For example, with a hole diameter of 30.5mm and the total heat transferred equal to 3.7 watts, the temperature drop is 5.5°C . At the same heat flux but with a hole diameter of 40.5mm, the temperature drop across the specimen is 7.5°C which is a 36% increase.

The importance of radiation transfer was assessed by putting aluminium foil in the holes (Chapter 3). Using perspex plates numbered 1 to 8, the results shown in Table 4-5 were

obtained. Since the holes in the specimens were 30.5mm in diameter, the temperature drops (voltage settings) used were similar to those used in the results shown in Table 4-4. The temperature drops obtained for runs with aluminium foil in the holes were not significantly different from those obtained without aluminium foil in the holes. For example, from Tables 4-4 and 4-5 (runs 159 and 237):

(a) Plate 5 -

temperature drop without aluminium foil	= 3.65°C
temperature drop with aluminium foil	= 3.68°C
increase in temperature drop	= 0.03°C

(b) Plate 6 -

temperature drop without aluminium foil	= 4.04°C
temperature drop with aluminium foil	= 4.12°C
increase in temperature drop	= 0.08°C

These results appeared to show that radiation transfer was not significant at the temperatures at which the perspex runs were being performed. Approximate calculations of radiation transfer using Series 'A' results and the assumption that heat transfer was between infinitely parallel plates, the amount of radiation was found to be about 5% of the total heat transferred (147). Durotherm was used in later experimental runs since it was able to be heated to temperatures above 80°C. However, later results from the computer calculations appear to show that radiation is quite significant.

The Rayleigh and Grashof numbers for the experimental runs (used in the numerical simulations) are presented in Table 4-9. For all the perspex runs, the Rayleigh numbers are below

the critical value of 1709 and similarly the Grashof numbers are below 2200. For the durotherm runs (runs 605 to 629), only runs 605 and 629 are below the critical limits. Runs 617 and 624 were carried out to determine the effect of convection in the transition region, while run 611 was on the transition-conduction boundary. As Figure 4-3 shows, there is no significant convection. Consequently, all the durotherm runs were used in the numerical simulations.

5.3 DISCUSSION OF THEORETICAL RESULTS

5.3.1 CREDIBILITY OF THE COMPUTED RESULTS

The validity of the computed results reported in this work can be judged from the following principal factors:

- (a) fidelity of the computer program
- (b) reliability of heat balances
- (c) convergence of the solution
- (d) comparison with experimental data

5.3.1.1 Fidelity of the Computer Program

This factor presents no small problem. Numerous simulation runs (not all described here) were devised to attest the fidelity of the computer program. These included solving the problem for various geometrical arrangements, relaxing the radiation temperatures, ignoring air conduction in the hole and solving the problem by using various radiation transfer approximations.

5.3.1.2 Accuracy of the Results

The basis of the computer program is attaining heat balances. The error percentage in all the heat balances was less than 0.03% (for every nodal point and in all the

simulation runs).

5.3.1.3 Convergence

The solutions converged for:

(a) Different grid sizes - the different hole diameters (30.5, 34.925, 35.5 and 40.5mm) and the different specimen thicknesses meant that the distances between the nodal points varied

(b) Different boundary and initial conditions (temperatures)

(c) Different emissivities - the emissivities of aluminium used were 0.04, 0.11, 0.2 and 0.5

(d) Different problem data - thermal conductivities of air, perspex and durotherm

The temperatures converged to within $\pm 0.00001^{\circ}\text{C}$.

However, when the temperatures of the hot and cold aluminium plates were increased to about 1000 and 800°K respectively (using exactly the same linear problem dimensions as used in the low temperature simulations), convergence did not occur. This point requires further work.

5.3.1.4 Experimental Verification of Computer Solutions

The ultimate test of validity of the computer results rests with comparison with experimental results. From Tables 4-13 and 4-14, the computer results were always less than the experimental results. Using the computed results with an aluminium emissivity of 0.04, the discrepancy between the experimental and the theoretical results varies between 4 and 26%.

5.3.2 TEMPERATURE AND HEAT FLUX PROFILES

Figures 4-4 and 4-5 show the temperature profile of simulation run 692A. The hot boundary temperature is 66.76°C and the cold boundary temperature is 55.63°C . The temperature gradients in the Z-X plane are small. For example, in the conduction region C2, the temperature varies between 62.92°C (for nodal point 198) and 63.05°C (for nodal points 222, 236 and 237). The large temperature gradients occur in the Y-direction; the direction of the hot aluminium plate to the cold aluminium plate. Consider for example nodal point 188 (in the C2 region); its temperature is 63.02°C . The corresponding point in the C3 region is nodal point 314 with a temperature of 59.34°C .

Figures 4-6 and 4-7 show some of the heat flows of simulation run 692A. In the solid, most of the heat flows in the Y-direction. Consider point 216; the flow of heat in the Y-direction is 0.67×10^{-3} watts, whereas in the Z and X directions it is in the order of magnitude 10^{-5} watts. For some surface points, the radiation flow is significant. Consider point 158 for example; the solid conduction in the Y-direction is 0.11×10^{-2} watts. Radiation flow away from surface point 158 is 0.18×10^{-3} watts (this is about 16% of the conduction flow). Similarly, for surface point 132, the radiation flow is 0.91×10^{-4} watts, while the conduction flow in the Y-direction is 0.62×10^{-3} watts. Hence the approximate ratio of radiation flow to conduction flow at this node is 1:15. Air conduction is often of the same order of magnitude as radiation. Consider nodal point 129; the heat flow in the Y-direction is 0.36×10^{-3} watts (radiation away from the surface point 158 is $.18 \times 10^{-3}$ watts).

Table 5-1 shows the computed major heat flows entering and leaving the cavity and solid material in the direction perpendicular to the hot and cold plates (Y-direction) for the runs simulating 12mm thick durotherm and perspex with 35.5mm holes. The heat flows apply to one eighth of the block of material (Figure B1). For most of the results shown (Table 5-1), the proportions of heat travelling through the solid as conduction, through the cavity as air conduction and through the cavity as radiation can be seen to be roughly 1, 0.11 and 0.05.

5.3.3 EFFECT OF MATERIAL THICKNESS

Run 341A used 5.6mm thick perspex with 30.5mm holes. The temperature drop across the specimen was 3.4°C . The computed total heat transfer was 3.185 watts.

Run 159A used 11mm thick perspex with 30.5mm holes. The temperature drop across the specimen was 3.65°C . The computed total heat transfer was 1.981 watts.

From runs 341A and 159A, it is observed that for about the same temperature drop, the thinner specimen transfers proportionately more heat than the thicker one. This is in agreement with the experimental results shown in Figure 4-1.

5.3.4 EFFECT OF HOLE SIZE

For the same specimen and at the same temperature drops, the total heat transferred decreases with increases in hole diameter (size). The results of 11mm thick perspex plates with 30.5, 35.5 and 40.5mm holes show this trend (runs 159, 549 and 679 respectively). From Table 4-13, the total heat transferred for runs 159A, 549A and 679A is 1.981, 1.867 and 1.69 watts respectively.

However, the radiation contribution to the total heat transferred increases with increase in the hole size (Figure 4-9). For the same temperature drop, the perspex plates with 40.5mm holes transmit more heat by radiation than those with 35.5mm and 30.5mm holes.

5.3.5 THE EFFECT OF EMISSIVITY

For a fixed hole size, the effects of (aluminium) emissivity are:

(a) The heat transferred by solid conduction is practically constant for all values of emissivity (Figure 4-12 and Table 4-10). For example, in run 576, for emissivity values of 0.04, 0.11, 0.2 and 0.5, the solid conduction heat transfer is 5.222, 5.218, 5.213 and 5.196 watts respectively.

(b) Similarly, the heat transferred by gaseous conduction is virtually constant. In run 576, for example, for the same emissivity values mentioned above, the heat transferred by gaseous conduction is 0.607, 0.607, 0.606 and 0.606 watts respectively.

(c) Radiation transfer increases substantially with emissivity as expected. In run 576, for example, the heat transferred by radiation is 0.242, 0.31, 0.402 and 0.761 watts respectively for the four emissivity values 0.04, 0.11, 0.20 and 0.5. Figure 4-8 and Table 4-12 show this trend.

(d) From (c), the total heat transferred increases with emissivity. Figure 4-12 shows this trend. In run 576, for example, the total heat transferred is 6.071, 6.134, 6.221 and 6.563 watts respectively for the four aluminium emissivities.

As a result, the emissivity of the aluminium plates used in the guarded hot plate needs to be known accurately.

5.3.6 THE EFFECT OF RADIATION AND GAS CONDUCTION

Solid conduction is the dominant mode of heat transfer. In run 159A for example, the total heat transferred is 1.981 watts; solid conduction is 1.761 watts (which is 89% of the total). With increases in hole diameter and operating temperature, the solid conduction percentage drops. In run 698D, the total heat transferred is 6.747 watts, with a solid conduction contribution of 4.638 watts (68%). As a result, the contributions of radiation transfer and gaseous conduction vary between about 10 and 30% of the total heat transferred.

In run 159A for example, the radiation contribution is 0.046 watts (2% of the total heat transferred), whereas the air conduction contribution is 0.175 watts (9%).

In run 698D, the radiation contribution is 0.993 watts (15%) and the air contribution is 1.116 watts (17%).

Figures 4-10 and 4-11 show the contributions of each of the mechanisms of heat transfer, using durotherm and perspex results respectively. The trends mentioned above are verified.

5.4 DISCUSSION OF APPARATUS PERFORMANCE AND THEORETICAL ANALYSIS

In all the runs, the total heat transferred by experiment is greater than that transferred by theoretical analysis (Table 4-13). For example, in run 159, the total

heat transferred by experiment is 2.294 watts. From the numerical simulations, the total heat transferred is 1.981, 1.991, 2.005 and 2.059 watts (for the four aluminium emissivities). Table 4-14 shows that the discrepancy between the experimental and the theoretical results varies between 2 and 26%. As expected (section 5.3), the results with the aluminium emissivity of 0.5 show the lowest discrepancy percentages. However, from the literature (1, 148) the emissivity of oxidised aluminium is expected to be between 0.04 and 0.2. The measured emissivity quoted earlier agrees with these figures.

In Figure 4-13, the total heat transferred is plotted against the temperature drop for both the experimental and theoretical results. The trends mentioned above are shown.

5.4.1 PERSPEX RESULTS

Considering the results with aluminium emissivities of 0.04, 0.11 and 0.2, about half of the results have discrepancies greater than 12%.

Swann (47,48) measured the total heat transferred across honeycomb-core sandwiches experimentally using a guarded hot plate. He performed a theoretical analysis as well. The discrepancy between his experimental and theoretical results was about 30%. Consequently, the discrepancies found in this work were not totally unexpected or unreasonably high.

5.4.2 DUROTHERM RESULTS

For all the durotherm results, the discrepancies between the experimental and the theoretical results are less than 12%. The exception is run 624A where the discrepancy is 13.7%. Possible reasons why the durotherm runs gave better

results than the perspex runs were:

(a) Durotherm was heated to higher temperatures (from 77°C to 162°C) while perspex was heated only up to 76°C . As a result, the durotherm experimental temperature drops were higher in the range 16 to 50°C , whereas the perspex results were in the range 0.8 to 15°C . If this reasoning is correct, it implies a large undiscovered error in the experimental measurements which needs further investigation.

(b) Durotherm is opaque while perspex is partially transparent. The thermal conductivity of durotherm determined was the true thermal conductivity. That determined for perspex was the apparent one due to the contribution of radiation. Although approximate calculations showed that radiation was not significant in the perspex, the suspicion remains that some radiant transmission may have affected the results. Since the aim of this work was to establish an easy method of determining heat transfer in the cavity problem, it was unfortunate that the only material available locally was the partially transparent perspex. If significant transmission can be shown to be taking place, the net radiation method would have to be modified so as to take account of the partially transparent perspex walls (53,149,150).

5.5 CHARACTERISTICS OF THEORETICAL RESULTS

The computed behaviour of the various heat transfer modes through the durotherm follows closely what would be expected. All transfers increase smoothly with temperature and the radiation transfer tends to increase with temperature at a rate somewhat greater than the conduction transfers (Figure 4-10).

However, the computed behaviour of the air conduction in the perspex cavities is disquietening, see Figure 4-11. The sudden rise in the air conduction with the first increase in temperature drop across the specimen is followed by a much smaller rise in heat flow as the temperature drop is increased. This effect has been emphasised by the line drawn through the points along what would have been the expected trend.

The reason for this behaviour has not been found. Although the air conduction is quite a small part of the total heat transfer, it might be affected substantially by small errors in the various heat balances. In fact, the heat balance at all nodes was correct to 0.03% of the net heat flow through the node. With this degree of accuracy, the deviation noted in air conduction would not be expected to arise from this cause.

The effect can be seen in more detail in Table 5-1 in the columns describing air conduction.

It also seems unlikely that the deviations, if they are deviations, occur because of incipient instability in the convergence. As mentioned earlier, convergence was not obtained at temperatures around 900°K, but the durotherm calculations were carried out at temperatures about 50°C higher than those used for perspex, and the durotherm results appear perfectly stable. Great care was taken to ensure that no 'rogue' (wrong) data had been used in the computer program during these calculations (none could be found). Further work needs to be carried out to find the cause of the behaviour of air conduction as shown in Figure 4-11.

TABLE 5-1

Major Computed Heat Flows (In Watts)

(PMMA With 35.5mm Holes Runs 549 to 576 and Durotherm Runs 605 to 629)

Run Number	Solid Conduction			Air Conduction			Radiation	
	Solid Conduction Regions			Air Conduction Regions			Radiation Regions	
	C2 Entering	C3 Mid-Plane	C4 Leaving	C2 Entering	C3 Mid-Plane	C4 Leaving	1 and 2 Entering	5 and 6 Leaving
549B	0.0125	0.0123	0.0125	0.0013	0.0013	0.0013	0.0005	0.0005
556B	0.0196	0.0191	0.0192	0.0031	0.0019	0.0012	0.0009	0.0008
568B	0.0297	0.0291	0.0297	0.0040	0.0020	0.0036	0.0014	0.0014
576B	0.0395	0.0388	0.0393	0.0047	0.0047	0.0037	0.0020	0.0020
605B	0.0452	0.0443	0.0452	0.0047	0.0045	0.0047	0.0024	0.0024
611B	0.0663	0.0649	0.0664	0.0072	0.0069	0.0072	0.0041	0.0039
617B	0.0849	0.0830	0.0852	0.0095	0.0090	0.0095	0.0059	0.0056
624B	0.1445	0.1405	0.1454	0.0175	0.0165	0.0176	0.0137	0.0127
629B	0.0552	0.0541	0.0553	0.0059	0.0056	0.0059	0.0032	0.0031

5.6 DISCUSSION CLOSURE

No other work was found in the literature which solved the cavity problem. However, the work of Swann (47,48) and Stroud (60) on honeycomb-core sandwich panels was used to check the heat transfer results obtained (147). The radiation transfer results obtained in this work were of the same order of magnitude as those obtained using the 'Swann-Stroud' equations, despite the fact that in honeycomb-core structures, solid conduction is negligible.

CHAPTER 6CONCLUSION

CHAPTER 6

CONCLUSION

The aim of this work was to develop simple experimental and theoretical methods of solving the equations which describe the heat transfer processes in a cavity, and thereby to investigate the assumptions and mechanisms significant to the cavity problem.

The equations describing the heat transfer processes have been solved computationally. Experimental verification of the results has also been carried out. Using durotherm specimens, the theoretical results were in agreement with the experimental results within the limits of the experimental error. For perspex specimens however, the discrepancy between the experimental and the theoretical results varied between 2 and 26%.

For various geometries, orientations and materials, the developed computer program gives the following:

- (a) solid conduction heat flows
- (b) gaseous conduction heat flows in the holes
- (c) radiation flows between the surfaces in the holes
- (d) temperature profiles

Without too many modifications, the effects of convection transfer can be incorporated in the program. The program uses simple heat transfer theory and is not too mathematical, consequently, the computing time is small (typically, 30 seconds Central Processing Unit time - Burroughs 6700).

The experiments have shown the lack of:

- (a) reference materials with which the experimental results obtained in this work could have been compared with
- (b) suitable materials - although durotherm gave satisfactory results, it is not a good material to work with because it is carcinogenic
- (c) suitable experimental methods of measuring radiation transfer and solid conduction separately

The experimental results have shown that (in the cavity problem) at atmospheric pressure, it is not possible to get large temperature drops across the holes without natural convection starting to occur. In the durotherm runs with temperature drops greater than 16°C , the Rayleigh numbers were greater than Ra_c . In order that the cavity problem be studied experimentally at high temperatures (600°K) where radiation is the dominant mode of heat transfer, the apparatus needs to be evacuated.

The problems associated with different temperature drops across the specimens can to a large extent be overcome by having reference materials and suitable specimens to work with. Using suitable specimens, the enclosure containing the guarded hot plate could be filled with insulation of one type, for example, fibreglass. In this work, a polystyrene-air insulation system was used so that reasonable temperature drops across the perspex specimens could be obtained. With insulation of one type in the box, the uncertainty of the external resistance could be overcome.

CHAPTER 7

RECOMMENDATIONS FOR FUTURE WORK

CHAPTER 7

RECOMMENDATIONS FOR FUTURE WORK

7.1. EXPERIMENTAL WORK

The number and nature of the experiments undertaken in this work were limited by:

- (a) the operating temperature
- (b) the materials available - initially perspex and later durotherm
- (c) temperature measuring equipment - the lack of a digital potentiometer meant that few millivolt readings were taken
- (d) the lack of methods of measuring the contributions of gaseous conduction, solid conduction and radiation transfer separately

In future experimental studies using the apparatus built in this work, the author considers that the above four points need to be studied closely. By finding a suitable material to work with, for example, insulation material of the type MIN-K (6), the apparatus could be operated at higher temperatures and consequently the radiation contribution effects studied at temperatures at which they are significant. At high temperatures however, natural convection becomes significant. If it is required to suppress it, evacuating the apparatus would achieve this. However, if it is not required to suppress natural convection, its importance could be assessed by using a Mach-Zehnder Interferometer.

There is a need for research into experimental methods of measuring solid conduction in the presence of radiation. No work was found in the literature which experimentally

measured solid conduction (or radiation) separately in the presence of radiation (or solid conduction). By introducing pressure as a variable in the apparatus built, the effect of gaseous conduction can be assessed.

In order that the total heat transferred be known accurately, metered cooling coils need to be put in the cold aluminium plates.

7.2 THEORETICAL WORK

The potential importance of finite element and finite difference methods for the solution of enclosed heat transfer problems warrants more theoretical investigations. In three dimensions especially, very little work was found. Considerable work remains regarding irregular boundary conditions.

Theoretical studies of natural and forced convection in conjunction with the radiation-conduction studies of this work need to be done, especially natural convection which has a myriad of correlations.

The techniques used to ensure convergence between the radiation and conduction calculations also need further study. A more sophisticated attempt to take account of radiation changes during the solution of the heat balance equations is needed especially at high temperatures (1000°K).

In conjunction with the experiments, the emissivity of aluminium needs to be known accurately.

7.3 CONCLUDING REMARKS

Future work on the cavity problem should also be concerned with transient state problems.

The cavity problem needs to be studied both experimentally and theoretically for typical large scale configurations, that is, a scale up of the linear dimensions and conditions used in this work.

NOMENCLATURE

This consists of two sections:

- (a) Part I - the symbols used in the text (the thesis)
- (b) Part II - the main variables used in the computer program (cavity problem computer program)

PART I

- A cross sectional area perpendicular to the direction of heat flow (M^2)
- B angle between 'conduction-rods' Figure B3 (degrees)
- C_p specific heat at constant pressure ($kJ/kg^{\circ}K$)
- CXY, CYX, and CZX conductances ($W/^{\circ}C$) see part II of this section
- D diameter (M)
- dQ_r/dT change in radiant flux as the temperature being relaxed is changed in the heat balance equations ($W/^{\circ}K$)
- dT temperature drop ($^{\circ}C$)
- E emissive power of a radiating body (W/M^2)
- e emf in millivolts
- F configuration (shape) factor - see part II
- g acceleration due to gravity (M/s^2)
- Gr Grashof number based on a characteristic dimension for example L in Figure 1-1

$$= g\beta(T_h - T_c)L^3\rho^2/\mu^2$$
- K thermal conductance ($W/^{\circ}C$)
- k thermal conductivity ($W/M^{\circ}C$)
- L, l length (M)
- N number of surfaces in enclosure

Nu	Nusselt number for natural convective heat transfer across an air layer
	$= q \times L / (k \times \Delta T)$
PMMA, pmma	Polymethyl methacrylate - perspex
Pr	Prandtl number $= C_p \mu / k$
Q	heat transfer rate (W)
q	energy flux, energy per unit area and time (W/M^2)
Q_{r3}	radiation heat flow in equation (1-12)
QXY, QYX, and QZX	solid conduction heat flows (W) - see part II
R	radius (M)
Ra	Rayleigh number $= Gr \times Pr$ based on L it is
	$= g \beta \rho^2 (T_h - T_c) L^3 C_p / (\mu k)$
r_i	inside radius (M)
r_o	outside radius (M)
Stark number	the conduction-radiation parameter based on the j th temperature defined by
	$N_j = ka / 4\sigma T_j^3$
	where 'a' is the absorption coefficient
T	temperature ($^{\circ}C$, $^{\circ}K$)
V	voltage in electrical analogy (W/M^2)
α	absorptivity
β	coefficient of thermal expansion
δ	Kronecker delta
ϵ	emissivity
λ	wavelength in microns
ρ	reflectivity
ρ	density (kg/M^3)
σ	Stefan-Boltzmann constant
μ	fluid viscosity (Ns/M^2)

SUBSCRIPTS

a	apparent
b	blackbody property
c	critical, that is, at the onset of convection
gc	gaseous conduction
i	incoming
i	initial
j,k	property of surface j or k
o	outgoing
r	radiative
sc	solid conduction
λ	spectrally (wavelength) dependent

UNITS

$^{\circ}\text{C}$	degrees Celsius
$^{\circ}\text{K}$	degrees Kelvin
M	metres
mV	millivolts
W	watts

PART II

The main program variables in the approximate order found in the program are:

NPITER	number of program iterations
NX	number of points in the X-direction (in the grid Figures B2 to B5, NX = 14)
NY	number of points in the Y-direction (number of constant temperature regions in Y direction - Figure B1, NY = 4)

NZ number of points in the Z-direction (Figures B2 to B5, NZ = 9)

E(I) emissivity of surface 'I'

TKAIR thermal conductivity of air. (W/M⁰C)

R radius of the cavity hole (M)

AA surface area of surface points (M²)

AR(I) area of radiation region 'I' (M²)

TR(I) temperature of radiation region 'I' (⁰K)

T(J) temperature of nodal point 'J' (⁰C)

QO(I) radiosity of region 'I' (W/M²)

QRADTO(I) net radiative loss from surface 'I' resulting from radiation in the enclosure (M²)

QRAD(I,J) radiation heat flow to surface point as defined in Appendix B (W)

DQDT(I,J) the change in radiant flux as the temperature being relaxed is changed (see equation 1-17)

F(I,J) radiation shape factor, that is, the fraction of diffusely distributed radiation leaving a surface 'I' that reaches surface 'J'

CXY(J) conductance in X-direction between nodal points 'J' and 'J + 1' (W/⁰C) - for example, in Figure B3, CXY(201) is the conductance between nodal points 201 and 202

CYX(J) conductance in Y-direction between nodal points 'J' and 'J - (NX * NZ)' (W/⁰C) - for example, in Figures B3 and B4, CYX(272) is the conductance between nodal points 272 and 146

CZX(J) conductance in Z-direction between nodal points 'J' and 'J + NX' (W/⁰C) - for example, in Figure B3, CZX(187) is the conductance between nodal points 187 and 201

TKP thermal conductivity of specimen ($\text{W/M}^{\circ}\text{C}$)

DELTAY thickness of specimen divided by 3 - see Figures B1 and B9 (M)

HC, AC, and DC coefficients used in evaluating conductances - see subroutine conduc

R1, R2, R3, and R4 radii used in air conductances evaluations (see Figure B8 and subroutine conduc)

CRAD(I) constant value in relaxation equation - it is equal to zero when considering interior points - for surface points it is equal to QRAD(I,J) (W)

RES(I) temperature residual of equation B-23 ($^{\circ}\text{C}$)

QXY(J) heat flow in the X-direction from nodal point 'J' towards nodal point 'J + 1' (W) - for example, in Figure B4, QXY(300) is the heat flow from nodal point 300 towards nodal point 301

QYX(J) heat flow in the Y-direction from nodal point 'J' towards nodal point 'J - (NX * NZ)' (W) - for example, in Figure B4, QYX(325) is the heat flow from nodal point 325 towards nodal point 199

QZX(J) heat flow in the Z-direction from nodal point 'J' towards nodal point '(J + NX)' (W) - for example, in Figure B4, QZX(333) is the heat flow from nodal point 333 towards nodal point 347

HEATIN net heat flow into a nodal point (W)

HEATOUT(HITOUT) net heat flow from a nodal point (W)

TOTFLO the difference between the HEATIN and the HITOUT (W)

PECERR the 'out-of-balance' error percentage, that is, TOTFLO divided by the mean of HEATIN and HITOUT (%)

SUMQXY net solid heat flow in X-direction (W)

SUMQYX net solid heat flow in Y-direction (W)

SUMQZX net solid heat flow in Z-direction (W)
QXYAIR net air conduction heat flow in X-direction (W)
QYXAIR net air conduction heat flow in Y-direction (W)
QZXAIR net air conduction heat flow in Z-direction (W)

REFERENCES

1. Kreith F., 'Principles of Heat Transfer', 2nd Edn, Int. Textbook Co., (1958)
2. Gilbo C.F., 'The Use of Envelope Type Cold Plates in Thermal Conductivity Apparatus', ASTM Special Technical Publication, No 217, pg 18-31, (1957)
3. Noble J.J., 'The Effect of Radiative Transfer on Natural Convection in Enclosures: A Numerical Investigation' PhD Thesis, Massachusetts Institute of Technology, Cambridge, Mass., April 1968
4. Siegel R., Perlmutter M., Int. J. Heat Mass Transfer, 5, 639, 1962
5. 'Method of Test for Thermal Conductivity of Materials by Means of the Guarded Hot Plate' (C177-71), Book of ASTM Standards, Part 14, pg 15, (1973)
6. Tye R.P., 'Thermal Conductivity', Vol I, Academic Press, N.Y., (1969)
7. Sparrow E.M., Cess R.D., 'Radiation Heat Transfer', Brooks/Cole Publ. Co., Belmont, Calif., (1966)
8. Probert S.D., 'Heat Transfer Across Rectangular Cavities' Chem & Process Engng Heat Transfer Survey, 42, 35-40, August 1970
9. De Graaf J.G.A., Van Der Held E.F.M., 'The Radiation Between the Heat Transfer and the Convection Phenomena in Enclosed Plane Air Layers', Applied Scientific Research, Section A, 3, 393-410, 1953
10. Elenbaas E., 'Dissipation of Heat by Free Convection', Parts I & II, Philips Research Report 3, N.V., Philips Gloeilampenfabrieken, Eindhoven, Netherlands 338-360 & 450-465, 1948

11. Probert S.D., Dixon M., 'Heat Transfer Regimes in Vertical Plane-walled Air-filled Cavities', Int. J. Heat Mass Transfer, 18, 709-710, May 1975
12. Churchill S.W., Ozoe H. et al., 'Three Dimensional Numerical Analysis of Laminar Natural Convection in a Confined Fluid Heated From Below', Trans. ASME, 98, 202, May 1976
13. Glaser P.E. et al, 'Thermal Insulation Systems', NASA, SP5027, (1967)
- * 14. Siegal R., Howell J.R., 'Thermal Radiation Heat Transfer' McGraw-Hill Book Co., N.Y., (1972)
15. McAdams W.H., 'Heat Transmission', McGraw-Hill, (1954)
16. Tabor H., 'Radiation, Convection and Conduction Coefficients in Solar Collectors', Bull. Res. Council of Israel, 6C, 155, 1958
17. Stott J.B., Garrod C.W., 'A Method of Applying Electrical Analogues to Calculation of Radiative Heat Transfer' Proceedings of Chemeca '70, Australian Academy of Science, Melbourne, 1970
18. Buchberg H., Edwards D.K., 'Natural Convection in Enclosed Spaces - A Review of Application To Solar Energy Collection', Trans. ASME, 98, 182, May 1976
19. Mull W., Reiher H., 'Der Wärmeschutz von Luftschichten', Reihe 1, Gesundh-Ing. Beihefte, Heft No 28, Munich and Berline, Germany, 1930
20. Jakob M., 'Free Heat Convection Through Enclosed Plane Gas Layers', Trans. ASME, 68, 189, 1946
21. Jakob M., 'Heat Transfer', 1st Edn, Vols 1 & 2, Wiley N.Y., (1949)
22. Peck R.E. et al, Trans. ASME, 73, 281, 1951

23. Kent A.C., 'Thermal Convection by Air in Small Cells Heated From Below', Ind. & Engng Chem. (Fundamentals), 11, 319, August 1972
24. Robinson H.E. et al, 'The Thermal Insulating Value of Airspaces', Housing Research Paper no 32, Housing and Home Finance Agency, Washington D.C., April 1954
25. Eckert E.R.G., Carlson W.O., 'Natural Convection in an Air Layer Enclosed Between Two Vertical Plates With Different Temperatures', Int. J. Heat Mass Transfer, 2, 106, 1961
26. Thomson J., Proc. Glasgow Phil. Soc., 13, 469, 1882
27. Benard H., Rev. Gen. Sci. Pur. Appl., 11, 1261 and 1309, 1900
28. Schmidt R.J., Saunders O.A., Proc. Roy. Soc. A165, 216, 1938
29. Sadhu D., 'Thermal Insulation Provided by Vertical, Annular, Air-Filled Cavities', Mech. Engng Science, 15, 11-16, February 1973
30. Edwards R.M., 'Heat Transfer Through Cavity Walls', M.Sc. Thesis, University College of Swansea, Glamorgan, November 1968
31. Churchill S.W., 'Natural Convection in an Inclined Square Channel', Int. J. Heat Mass Transfer, 17, 401, March 1974
32. Churchill S.W., Chu, 'Correlating Equations for Laminar and Turbulent Free Convection From a Vertical Plate' Int. J. Heat Mass Transfer, 18, 1323, November 1975
33. Probert S.D., 'Heat Transfers Across Cavities', Int. J. Heat Mass Transfer, 12, 527, April 1969
34. Probert S.D., 'Heat Transfer Through Rarefied Fluids', Int. J. Heat Mass Transfer, 10, 135, 1967

35. Probert S.D., 'An Interferometric Study of Heat Transfer Across a Rectangular Cavity', Mech. Engng Sci., 14, n2, 1972
36. Sparrow E.M., Gregg J.L., 'Radiant Interchange Between Circular Discs Having Arbitrarily Different Temperatures', Trans. ASME, J. Heat Transfer, 83, 494, November 1961
37. Ostrach S., 'Laminar Natural Convection Flow and Heat Transfer of Fluids With and Without Heat Sources in Channels With Constant Wall Temperatures', NACA, TN 2863, 1952
38. Ostrach S., 'Natural Convection in Enclosures', Advances in Heat Transfer, 8, 161, 1972
39. Drake E.M., 'Transient Natural Convection of Fluids Within Vertical Cylinders', ScD. Thesis, Dept of Chem. Engng, M.I.T. Cambridge, 1966
40. Allcut E.A., 'Analysis of Heat Transfer Through Thermal Insulating Materials - Proceedings General Discussion on Heat Transfer', Inst. Mech. Engrs, London, 1951
41. Verschoor J.D., Greebler R., 'Heat Transfer by Gas Conduction and Radiation in Fibrous Insulation', Trans. ASME, 74, 961, 1952
42. Mischke C.R., 'An Accurate Method for the Determination of Thermal Conductivity of Insulating Solids', Report No5, Engineering Expt Station, University of Wisconsin, (1956)
43. Woodside W., Wilson A.G., 'Unbalance Errors in Guarded Hot Plate Measurements', ASTM Special Technical Publication No 217, pp 32-46, (1957)

44. Richardson P.C., 'The Difference Equation Method for Solving the Dirichlet Problem', Phil. Trans. Roy. Soc., London, 210A, 307, 1910
45. ASTM, STP 411, 'Thermal Conductivity Measurements of Insulating Materials at Cryogenic Temperatures', March 1967
46. Bratis J.C., 'Radiation Interaction in Real Gases', AIAA Prog. Astronautics and Aeronautics, 31, 329, 1973
47. Swann R.T., Pittman C.M., 'Analysis of Effective Thermal Conductivities of Honeycomb-Core and Corrugated-Core Sandwich Panels', NASA TN D-714, April 1961
48. Swann R.T., 'Calculated Effective Thermal Conductivities of Honeycomb Sandwich Panels', NASA TN D-171, December 1959
49. 7th Conference on Thermal Conductivity, NBS, Special Publication 302, 1967
50. Schneider P.J., 'Conduction of Heat Transfer', Addison Wesley Publishing Co., 2nd Edn, 1955
51. Rohsenow W.M., Hartnett J.P., 'Handbook of Heat Transfer' McGraw-Hill, N.Y., 1973
52. Cess R.D., 'The Interaction of Thermal Radiation With Conduction and Convection Heat Transfer', Advances in Heat Transfer, Vol I, Academic Press N.Y., 1964
53. Hussain N.A., Siegal R., 'Radiation Exchange for a System With Partially Transmitting Wall', Letters in Heat Mass Transfer, 2, 105-114, March-April 1975
54. England W.G., Emery A.F., 'Thermal Radiation Effects on the Laminar Free Convection Boundary of an Absorbing Gas', Trans. ASME, J. Heat Transfer, 91, 37, 1969
55. Schimmel W.P., 'Interferometric Study of Radiation-

- Conduction Interaction', Proceedings of the 4th Int. Heat Transfer Conference, paper R2.1, Elsevier, Amsterdam, (1970)
56. Novotny J.L., 'The Influence of a Non-absorbing Gas in Radiation-Conduction Interaction', AIAA Prog. Astronautics Aeronautics, 24, 410, 1971
 57. Gille J., 'Convection in a Radiating Gas', J. Fluid Mechanics, 20, 47, 1964
 58. Novotny J.L., 'Radiation Interaction in Non-gray Boundary Layers', Int. J. Heat Mass Transfer, 11, 1823, 1968
 59. Strong H.M., Bundy F.P., 'Radiation Effects in Fibrous Materials', J. Appl. Phys., 31, 39, 1960
 60. Stroud C.W., 'Experimental Verification of an Analytical Determination of Overall Thermal Conductivity of Honeycomb-Core Panels', NASA TN D-2866, 1965
 61. Hollands K.G.T., 'Natural Convection in Horizontal Thin-walled Honeycomb Panels', Trans. ASME, J. Heat Transfer, 95, 439, November 1973
 62. Carslaw H.S., Jaeger J.C., 'Conduction of Heat in Solids', 2nd Edn, Oxford Univ. Press, (1959)
 63. Ozisik M.N., 'Boundary Value Problems of Heat Conduction' International Textbook Co., Scranton, Pa, (1968)
 64. Oppenheim A.K., 'Radiation Analysis by Network Method', Trans. ASME, 78, 725, 1956
 65. Poljak G., 'Analysis of Heat Interchange by Radiation Between Diffuse Surfaces', Tech. Phys. USSR, Vol I, nos 5, 6, 555-590, 1935
 66. Gebhart B., 'Unified Treatment for Thermal Radiation Transfer Processes - Gray, Diffuse Radiators and

- Absorbers', Paper no 57-A-34, ASME, December 1957
67. Sparrow E.M., 'On the Calculation of Radiant Interchange Between Surfaces', Warren Ibele (Ed.) - Modern Developments in Heat Transfer, pp 181-212, Academic Press Inc. N.Y., 1963
 68. Bevans J.T., 'Radiant Interchange Within an Enclosure', Trans. ASME, J. Heat Transfer, 82, 457, 1960
 69. Stott J.B., Garrod C.W., 'Calculation of Radiative and Convective Heat Transfer in Combustion Chambers', J. Inst. Fuel, pp 115-123, September 1975
 70. Eckert E.R.G., Drake R.M., 'Analysis of Heat and Mass Transfer', McGraw-Hill, (1972)
 71. Fourier J.B.J., 'Theorie Analytique de la Chaleur', Paris 1822, translated by A. Freeman, Stechart, N.Y., 1878
 72. Arpaci V.S., 'Conduction Heat Transfer', Addison-Wesley, Reading, Mass., (1966)
 73. Bayley F.J., 'Heat Transfer', Thomas Nelson & Sons Ltd, London, (1972)
 74. Myers G.E., 'Analytical Methods in Conduction Heat Transfer', McGraw-Hill Book Co., (1971)
 75. Fox L., 'Numerical Solution of Ordinary and Partial Differential Equations', Pergamon Press, Oxford, (1962)
 76. Smith G.D., 'Numerical Solution of Partial Differential Equations', Oxford Univ. Press, London, (1965)
 77. Ames W.F., 'Numerical Methods for Partial Differential Equations', Nelson, London, (1969)
 78. Forsythe G.E., Wasow W.R., 'Finite Difference Methods for Partial Differential Equations', John Wiley, N.Y., (1960)

79. Richtmyer R.D., Morton K.W., 'Difference Methods for Initial Value Problems', Interscience Publishers, N.Y., (1967)
80. Dusanberre G.M., 'Heat Transfer Calculations by Finite Differences', International Textbook Co., (1961)
81. Emmons H.W., 'The Numerical Solution of Heat Conduction Problems', Trans. ASME, 65, 607, 1943
82. Carnahan B., Luther H.A., Wilkes J.D., 'Applied Numerical Methods', John Wiley & Sons, N.Y., (1969)
83. Southwell R.V., 'Relaxation Methods in Theoretical Physics', Oxford University Press, London, (1946)
84. Southwell R.V., Christopherson D.G., Proc. Roy. Soc., Ser. A, 168, 317, 1938
85. Zienkiewicz O.C., Cheung Y.K., 'Finite Elements in the Solution of Field Problems', The Engineer, 507, September 24, 1965
86. Zienkiewicz O.C., Cheung Y.K., 'The Finite Element Method in Structural and Continuum Mechanics', McGraw-Hill, N.Y., (1967)
87. Reid J.K., Turner A.B., 'Fortran Subroutines for the Solution of Laplace's Equation Over a General Region in Two Dimensions', U.K.A.E.A., Rept T.P. 422, September 1970
88. Zienkiewicz et al, 'Solution of Three Dimensional Field Problems by the Finite Element Method', The Engineer, 547, (October 27) 1967
89. Zienkiewicz O.C., Anderson, 'Spontaneous Ignition - Finite Element Solutions for Steady and Transient Conditions', Trans. ASME, J. Heat Transfer, 96, 398-404, August 1974

90. Emery A.F., Carson W.W., 'An Evaluation of the Use of the Finite Element Method in the Computation of Temperature', *ibid*, 93, 136-145, May 1971
91. Walker M., 'The Schwarz-Christoffel Transformation and Its Application - A Simple Exposition', Dover Publications Inc., (1964)
92. Churchill R.V., 'Introduction to Complex Variables and Applications', McGraw-Hill, N.Y., (1948)
93. Allen D.N.de G., 'Relaxation Methods Applied to Conformal Transformations', *Quart. J. Mech. & Appl. Maths*, 15, 35, 1962
94. Douglas J.Jnr, 'A Survey of Numerical Methods for Parabolic Differential Equations', *Advances in Computers*, 2:1, Academic Press, (1961)
95. Emery E.F., 'Free Convection Through Vertical Plane Layers - Moderate and High Prandtl Number Fluids', *Trans. ASME, J. Heat Transfer*, 91, 391, Aug. 1969
96. Emery A.F., 'Heat Transfer Across Vertical Layers', *Trans. ASME, J. Heat Transfer*, 87, 110, Feb. 1965
97. Newell M.E., 'Heat Transfer by Laminar Natural Convection Within Rectangular Enclosures', *Trans. ASME, J. Heat Transfer*, 92, 159, February 1970
98. Landis F., Yanowitz H., 'Transient Natural Convection in a Narrow Vertical Cell', *Proceedings of the Third International Heat Transfer Conference, A.I.Ch.E.*, 2, 139-151, N.Y., (1966)
99. Batchelor G.K., 'Heat Transfer by Free Convection Across a Closed Cavity Between Vertical Boundaries at Different Temperatures', *Quarterly of Applied Mathematics*, 12, 209, 1954

100. Poots G., Quart. J. Mech. Appl. Maths, 11, 257, 1958
101. Mynett J.A., M.Sc. Thesis, Bristol University, 1960
102. Elder J.W., 'Laminar Free Convection in a Vertical Slot', J. Fluid Mech., 23, 77, 1965
103. Elder J.W., 'Numerical Experiments With Free Convection in a Vertical Slot', J. Fluid Mech., 24, 823, 1966
104. de Vahl D.G., 'Laminar Natural Convection in an Enclosed Rectangular Cavity', Int. J. Heat Mass Transfer, 11, 1675, November 1968
105. de Vahl D.G., 'Natural Convection in an Enclosed Rectangular Cavity', Trans. Inst. Engrs Australia Mechanical & Chemical Engng Trans., 1, 43, 1965
106. Lord Rayleigh, Phil. Mag. J. Sci., 32, (192), 529, 1916
107. Jeffreys H., Phil. Mag., 2, 833, 1926
108. Jeffreys H., Proc. Roy. Soc., A118, 195, 1928
109. Low A.R., Proc. Roy. Soc., A125, 180, 1929
110. Churchill, Chu, 'The Effect of Heater Size, Location, Aspect Ratio, and Boundary Conditions in Two Dimensional Laminar, Natural Convection in Rectangular Channels', Trans. ASME, J. Heat Transfer, 98, 194, May 1976
111. Catton I., 'The Effect of Insulating Vertical Walls on the Onset of Motion in a Fluid Heated from Below', Int. J. Heat Mass Transfer, 15, 665, 1972
112. Heitz W.L., Westwater J.W., 'Critical Rayleigh Numbers for Natural Convection of Water Confined in Square Cells with L/D from 0.5 to 8"', Trans. ASME J. Heat Transfer, 93, 188, 1971
113. Catton I. et al, 'Natural Convection Flow in a Finite Rectangular Slot Arbitrarily Oriented With Respect

- to the Gravity Vector', Int. J. Heat Mass Transfer, 17, 173, February 1974
114. Hollands K.G.T., 'Free Convective Heat Transfer Across Inclined Air Layers', Trans. ASME, J. Heat Transfer, 98, 189, May 1976
115. Eckert E.R.G., Goldstein R.J., 'Measurements Techniques in Heat Transfer', Technivision Services, Slough, England, (1970)
116. Hottel H.C., Sarofim A.F., 'Radiative Transfer', McGraw-Hill Book Co., N.Y., (1967)
117. Macneal R.H., 'An Asymmetric Finite Difference Network', Quart. Appl. Math., 2, 295, 1953
118. 'Temperature, Its Measurements and Control in Science and Industry', vol 3, Part 2, Reinhold, N.Y., (1962)
119. Boelter L.M.K. et al, 'An Investigation of Aircraft Heaters XXCIII - Equations for Steady State Temperature Distribution Caused by Thermal Sources in Flat Plates Applied to Calculation of Thermocouple Errors, Heat Meter Corrections, and Heat Transfer by Pin-fin Plates', TN1452, NACA, 1944
120. Fitts R.L., 'Study of Temperature Distribution in a Finned Nuclear Fuel Sheath by Electrical Analogue and Mathematic Analysis (revision)', R65CAP1, Canadian General Electric, Peterborough, Ontario, 19 January 1965
121. Singh B.S., 'Error in Temperature Measurements due to Conduction Along the Sensor Leads', Trans. ASME, J. Heat Transfer, 98, 491, August 1976
122. Chan K.S., 'The Simulation of Boundary Conditions in Heat Conduction Problems in a Resistance-Capacitance

- Electrical Analogue', J. Sci. Instruments, 41,
n9, 535, September 1964
123. Brindley J.H., 'Calibration of Surface-attached
Thermocouples on a Flat Plate Fuel Element by
Electrical Analogue and Analytical Techniques',
Trans. of the American Nuclear Soc., 6, n2, 333,
November 1963
124. Powell W.B., Price T.W., 'A Method for the Determination
of Local Heat Flux from Transient Temperature
Measurements', Trans. Instr. Soc. Amer., 3, n3,
246, July 1964
125. Boelter L.M.K., 'Thermocouple Conduction Error Observed
in Measuring Surface Temperatures', TN2427,
NACA, 1946
126. Stoll A.M., 'Direct Experimental Comparison of Several
Surface Temperature Measuring Devices', Rev.
Sci. Instr., 20, n9, 678, September 1949
127. Oetken E.R., 'Evaluation of Surface-attached Thermo-
couples during Forced Convection Heat Transfer',
IDO-16889, OTS, Dept of Commerce, Washington D.C.
128. Sudar S., 'Calibration of OMRE Fuel-element Surface
Thermocouple Assembly', NAA-SR-Memo 3671, 1959
129. Baker H.D., 'Temperature Measurement in Engineering'
Vols 1 & 2, John Wiley & Sons Inc., 1961
130. Cetinkale T.N., Fishenden M., 'Thermal Conductance of
Metal Surfaces in Contact', General discussion on
Heat Transfer - Conference of Institute of Mech.
Eng. and ASME, pp 271-5, (1951)
131. Fried E., Costello F.A., 'Interface Thermal Contact
Resistance Problem In Space Vehicles', ARS Journal
32, 237-243, (1962)

132. Fenech H., 'Prediction of Thermal Conductance of
Metallic Surfaces in Contact', Trans. ASME, J.
Heat Transfer, 85, 15-24, (1963)
133. Mikic B.B., 'Thermal Contact Conductances', Int. J.
Heat Mass Transfer, 12, 279, 1969
134. Mikic B.B., 'Thermal Contact Resistance in a Non-ideal
Joint', Tech. Rep. No 71821-77, H.T. Laboratory,
M.I.T., Cambridge, Mass., November 1971
135. Tye R.P., Thermal Conductivity Vol 2, Academic Press,
N.Y., (1969)
136. Wiebelt J.A., 'Engineering Radiation Heat Transfer',
Holt, Rinehart & Winston Inc., 1966
137. Keshock E.G., Siegal R., Trans. ASME, J. Heat Transfer,
86, 341, 1964
138. U.S. National Bureau of Standards, Circular 590,
'Methods of Testing Thermocouples and Thermocouple
Materials', 6 February 1958
139. Hall J.A., 'Calibration of Temperature Measuring
Instruments', National Physical Laboratories,
Notes on Applied Science, No 12, HMSO, (1964)
140. Billing B.F., 'Thermocouples, Their Instrumentation,
Selection and Use', Royal Aircraft Establishment,
(1964)
141. U.S. National Bureau of Standards-Monograph 40,
'Thermocouple Materials', March 1962
142. ASTM Special Technical Publication 470A, Manual on
the Use of Thermocouples in Temperature Measurement'
143. Espie A.A., 'Heat Transfer Through Composite Bodies',
B.E. Project Report, Dept of Chem. Eng., University
of Canterbury, 1973

144. Dunkle R.V., Private Communications, Chief Research Scientist, CSIRO, Melbourne, Australia, (1975)
145. Imperial Chemical Industries Ltd, 'Perspex - Acrylic Sheet' Technical Service Note PX122, (1973)
146. Touloukian Y.S. (Editor), 'Thermophysical Properties of Matter', Vols 1-10, IFI/Plenum Data Corp. N.Y., (1970-1974)
147. Lishomwa L., Private Communications, (1975)
148. Gubareff G.G., Jansen J.E., Torberg R.H., 'Thermal Radiation Properties Survey', 2nd Edn - Honeywell Research Center, Minneapolis, 1960
- × 149. Siegal R., 'Net Radiation Method for Enclosure Systems Involving Partially Transparent Walls', NASA TN D-7384, August 1973
150. Anderson E.E., 'Heat Transfer in Semi-transparent Solids', Advances in Heat Transfer, 11, 317-441, 1975
151. Ogorkiewicz R.M., 'Engineering Properties of Thermoplastics', John Wiley & Sons, London, (1970)
152. Imperial Chemical Industries Ltd - Plastics Division Sheet Group, 'Engineering Design Data for Perspex Acrylic Sheet'
153. Roff W.J., 'Fibers, Films, Plastics and Rubbers - A Handbook of Common Polymers', Butterworths, London, (1971)
154. Wyatt O., 'Metals, Ceramics and Polymers', Cambridge University Press, London, (1974)
155. Jenkins A.D., 'Polymer Science', A Materials Science Handbook Vols 1 & 2, Published by North-Holland Publishing Co., Amsterdam, (1972)

156. Clark M., 'Insulating Materials for Design and Engineering Practice', John Wiley & Sons Inc., N.Y., (1962)
157. Ciba-Geigy Co. Publication No 35736/e 'Araldite'
158. Column Research Committee of Japan, 'Handbook of Structural Stability', Tokyo, Corona, (1971)
159. Bowen L.P., 'Structural Design in Aluminium', Publishers - Hutchinson & Co., 1966
160. High Duty Alloys Ltd, 'Standard Extruded Sections in Hiduminium'
161. Northern Aluminium Co. Ltd, 'Structural Aluminium', 1st Edn, Banbury, England, (1956)
162. Aluminium Co. of America, 'Alcoa - Structural Handbook - A Design Manual for Aluminium', 1960
163. Reynolds Metals Co., 'Structural Aluminium Design by Karl Angermayer', (1967)
164. Aluminium Co. of Canada Ltd, 'Handbook of Aluminium', Montreal, 1957
165. Leuenberger H., 'Compilation of Radiation Shape Factors for Cylindrical Assemblies', ASME paper no 56-A-144, July 1956
166. Pivovonsky M., Nagel M.R., 'Tables of Blackbody Radiation Functions', Macmillan Co., N.Y., (1961)
167. U.S. National Bureau of Standards, Circular 564, 'Tables of Thermal Properties of Gases'
168. Watson J.T.R., 'Viscosity of Gases in Metric Units', Dept of Trade and Industry, National Engng Laboratory HMSO, 1972

APPENDIX A
MISCELLANEOUS DATA

A1	<u>THICKNESSES OF THE SPECIMENS</u>	237
A2	<u>PROPERTIES OF PERSPEX</u>	238
A3	<u>PROPERTIES OF ALUMINIUM AND ARALDITE</u>	241

A1 THICKNESSES OF THE SPECIMENS

The thicknesses of the various materials (specimens) used in the guarded hot plate are:

TABLE A1
Thicknesses of the Specimens

Specimen Plate Number	Material	Nominal Thickness (inches)	Average Thickness (millimetres)
1	Perspex	1/4	5.69
2	Perspex	1/4	5.54
3	Perspex	1/4	5.66
4	Perspex	1/4	5.64
5	Perspex	1/2	11.15
6	Perspex	1/2	11.20
7	Perspex	1/2	11.21
8	Perspex	1/2	11.17
9	Perspex	3/4	19.03
10	Perspex	3/4	19.08
11	Perspex	3/4	19.08
12	Perspex	3/4	19.05
13	Particle Board	3/4	19.70
14	Particle Board	3/4	19.71
15	Syndanyo Board	3/8	9.70
16	Syndanyo Board	3/8	9.74
17	Polystyrene	1/2	12.70
18	Polystyrene	1/2	12.70
19	Durotherm	1/2	12.07
20	Durotherm	1/2	12.12
21	Tufnol Spacers	1/2	11.25
22	Tufnol Spacers	1/2	11.25

A2 PROPERTIES OF PERSPEX

The mechanical, thermal, optical, and electrical properties of perspex are given in the I.C.I. publication - 'Properties and Perspex' (145). Other publications with properties of perspex are:

- (a) Ogorkiewicz (151)
- (b) Imperial Chemical Industries Ltd (152)
- (c) Roff (153)
- (d) Wyatt (154)
- (e) Thermophysical Properties of Matter (146)
- (f) Jenkins (155)
- (g) Clark (156)

The thermal properties from the I.C.I. publication (145) are:

TABLE A2

Thermal Properties of Perspex

Property	Units	Mean Value
1/10 Vicat softening point	$^{\circ}\text{C}$	100
Temperature of deflection under load (in accordance with BS 2782, Part 1, method 102G at a fibre-stress of 18.5 kgf/cm ²)	$^{\circ}\text{C}$	100
Demoulding temperature	$^{\circ}\text{C}$	87
Maximum service temperature	$^{\circ}\text{C}$	80
Thermal conductivity at 20 $^{\circ}\text{C}$	W/M $^{\circ}\text{C}$	0.188
Coefficient of thermal expansion at 20 $^{\circ}\text{C}$:		
volume	/ $^{\circ}\text{C}$	2.2×10^{-4}
linear	/ $^{\circ}\text{C}$	7.3×10^{-5}

A2.1 RADIATIVE PROPERTIES OF PERSPEX

Reflectance, absorptance and transmittance data is available in the thermophysical properties books (146). The emissivity of perspex could not be found in the literature.

PREDICTION OF THE EMISSIVITY OF PERSPEX

Using classical electromagnetic theory, the emissivity of perspex was calculated as follows:

(i) Assumptions:

- perspex is a dielectric (Dielectrics are materials which are insulators, that is, have direct current resistivities greater than 10^8 ohm-cm. Clark (156) gives the resistance of PMMA as 10^{15} ohm-cm.)
- perspex is isotropic -That is, electrical and internal optical properties are independent of direction.
- the magnetic permeability of perspex is equal to that of a vacuum
- no accumulation of static electrical charge
- no externally produced electrical conduction currents present

(ii) Mathematical Formulation:

The normal emissivity is computed from the formula

$$\epsilon_n = 1 - \left(\frac{n-1}{n+1}\right)^2 \quad (A-1)$$

where ϵ_n = the normal emissivity

n = the refractive index of perspex

The refractive index of perspex does not vary appreciably with wavelength (151). $n = 1.59$ was chosen.

Therefore,

$$\begin{aligned}\epsilon_n &= 1 - \frac{(1.59 - 1)}{(1.59 + 1)} \\ &= \underline{0.95}\end{aligned}$$

The relationship of the normal emissivity to the hemispherical emissivity is well known (Graphical representation in Siegal's book (14)).

At a normal emissivity of 0.95, the ratio of the hemispherical emissivity (ϵ) to the normal emissivity is equal to 0.935, that is,

$$\epsilon/\epsilon_n = 0.935$$

hence, $\epsilon = 0.935 \times 0.95$

$$= \underline{0.9}$$

THE MEASURED EMISSIVITY OF PERSPEX

The emittance of perspex was measured at the Commonwealth Scientific and Industrial Research Organisation in Australia using the Gier-Dunkle Scanning Infra-Red Reflectometer.

The emittance of machined perspex was found to be 0.905. That of clear (unmachined) perspex was found to be 0.916. As the specimens used in the experiments were machined, the former figure was applicable.

A3 MISCELLANEOUS DATA

A3.1 ARALDITE

Araldite is a trade name of CIBA-GEIGY for an epoxy resin based adhesive. The epoxy resin system used in this work has the designations of Araldite AW106 and Hardener

HV953U. The general properties of araldite are outlined in the CIBA-GEIGY pamphlet (157).

TABLE A3
Properties of Araldite

	Araldite AW106	Hardener HV953U
Physical form	viscous epoxy resin	treacle-like, slightly alkaline liquid
Colour	cream	yellow
Viscosity at 25°C cP	30,000 - 50,000	25,000 - 40,000
Specific gravity at 25°C gm/c.c.	1.15 - 1.25	0.9 - 1.0
Flash Point °C (Pensky-Martens)	greater than 200	50 - 55

The thermal conductivity at a mean temperature of 28°C is given as 0.282 W/M°C (157).

A3.2 ALUMINIUM

In the design of the aluminium plates, the following references were used - 158, 159, 160, 161 and 162. Structural and other physical properties of aluminium are outlined in references 163 and 164.

For 99.95% pure commercial aluminium, the properties outlined in reference 164 are:

TABLE A4
Properties of Aluminium

Property	Units
Density at 20°C	0.0975 psi
Melting Point	1220°F (660°C)
Young's Modulus	10 ⁷ psi
Modulus of Rigidity (shear)	3.79 x 10 ⁶ psi
Poisson's Ratio	0.33

The thermal conductivity of aluminium is well documented in the literature (1,146).

Numerous values of the emissivity of aluminium (different surface conditions) are available in the literature. The Thermophysical Properties book (146) presents forty four curves of the emissivity versus temperature. Gubareef (148) presents a thorough review of the emissivity values of aluminium and other radiative properties of various materials.

Since the aluminium plates were oxidised, from the above two references, values of emissivity were chosen. The chosen values were 0.04, 0.11, 0.2 and 0.5.

APPENDIX BCAVITY PROBLEM THEORETICAL DERIVATIONS

B1	<u>PHYSICAL FORMULATIONS</u>	245
B2	<u>CHOICE OF ZONES</u>	245
B3	<u>NET RADIATION METHOD</u>	255
B4	<u>SHAPE FACTORS</u>	261
B5	<u>THERMAL CONDUCTANCES</u>	264
B6	<u>NODAL EQUATIONS</u>	266
B7	<u>NOTES ON SPECIMENS USED</u>	268

APPENDIX BCAVITY PROBLEM THEORETICAL DERIVATIONSB1 PHYSICAL FORMULATIONS

As previously mentioned (Chapter 2 - Figure 2-12), the specimens used in the experiments had holes drilled in them in a regular pattern (square pitch). From the linear dimensions of each specimen, the block of material used in the numerical analysis is 47.66mm x 47.66mm x thickness of the specimen. The hole of chosen diameter is in the centre of this block of material (specimen). The leading dimensions of the cavity problem are shown in Figure B1. The diameters used for the perspex simulation runs were 30.5mm, 35.5mm and 40.5mm. For the durotherm simulation runs, only one diameter was used, 34.925mm (1 3/8").

From Figure B1, it is apparent that the cavity problem is symmetrical. Consequently, only 1/8th of the block of material was required to be analysed. For example, for solid conduction, the regions C1, C2, C3 and C4 in Figure B1.

B2 CHOICE OF ZONES

Three zoning systems were used.

B2.1 SOLID CONDUCTION ZONES

These are regions C1, C2, C3 and C4 in Figure B1. Each of these conduction regions had 58 nodal points. Figures B2 to B5.

B2.2 RADIATION REGIONS

Figure B6 shows the radiation regions. There are six radiation regions. Regions 1 and 6 are the two end discs

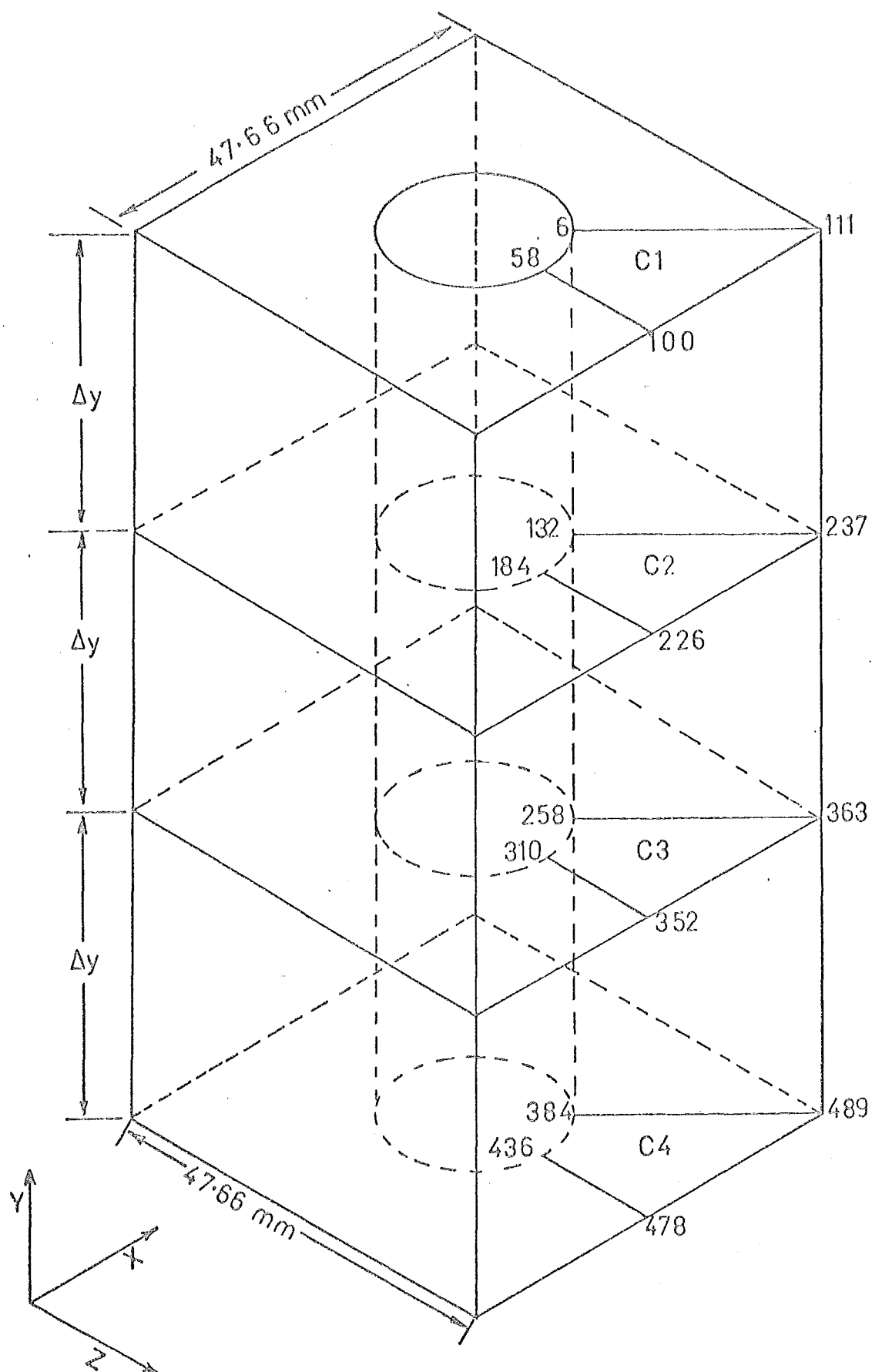


FIGURE B1 THE CAVITY PROBLEM PHYSICAL FORMULATION

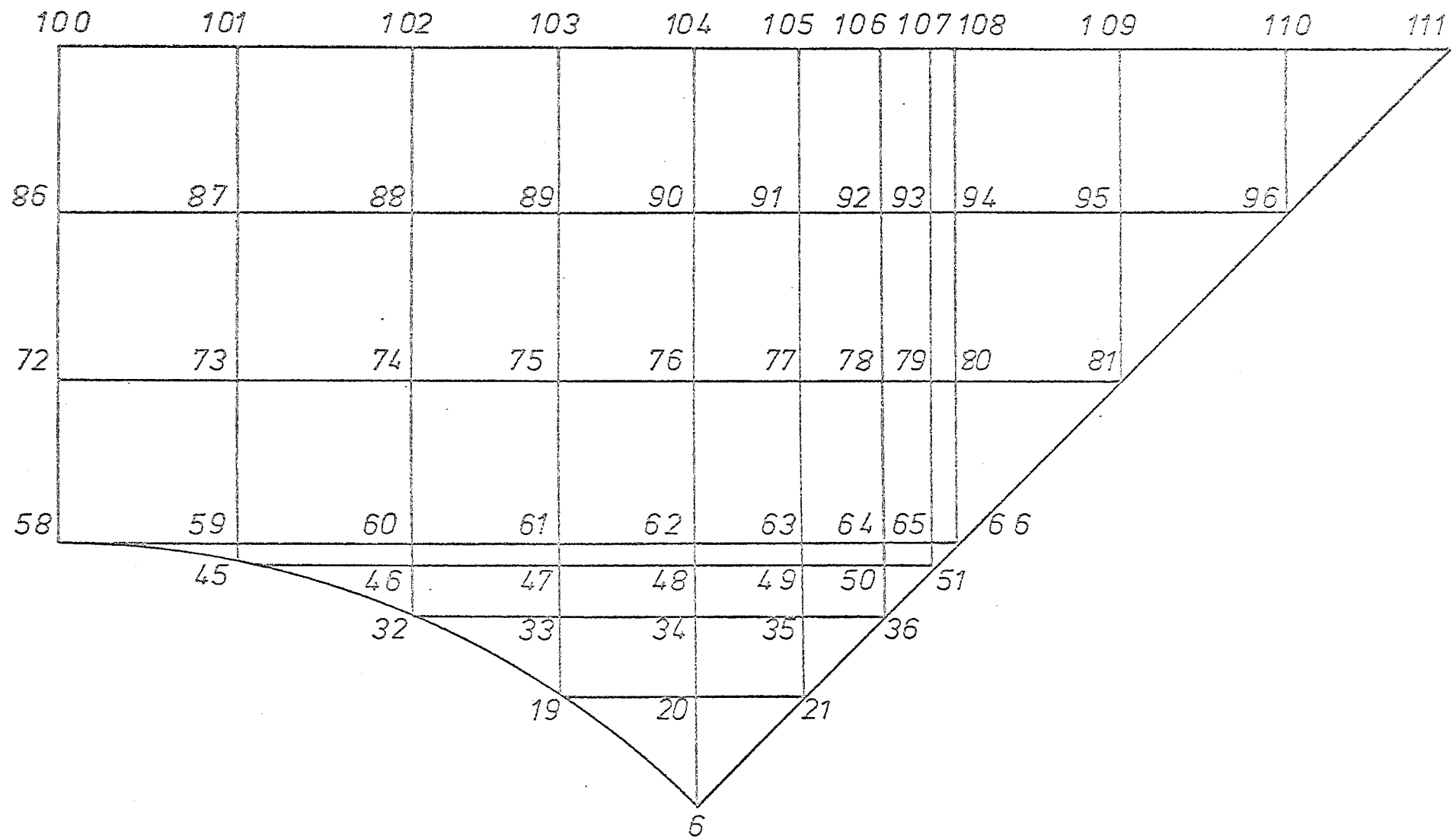


FIGURE B2 SOLID CONDUCTION ZONE C1-PLAN VIEW

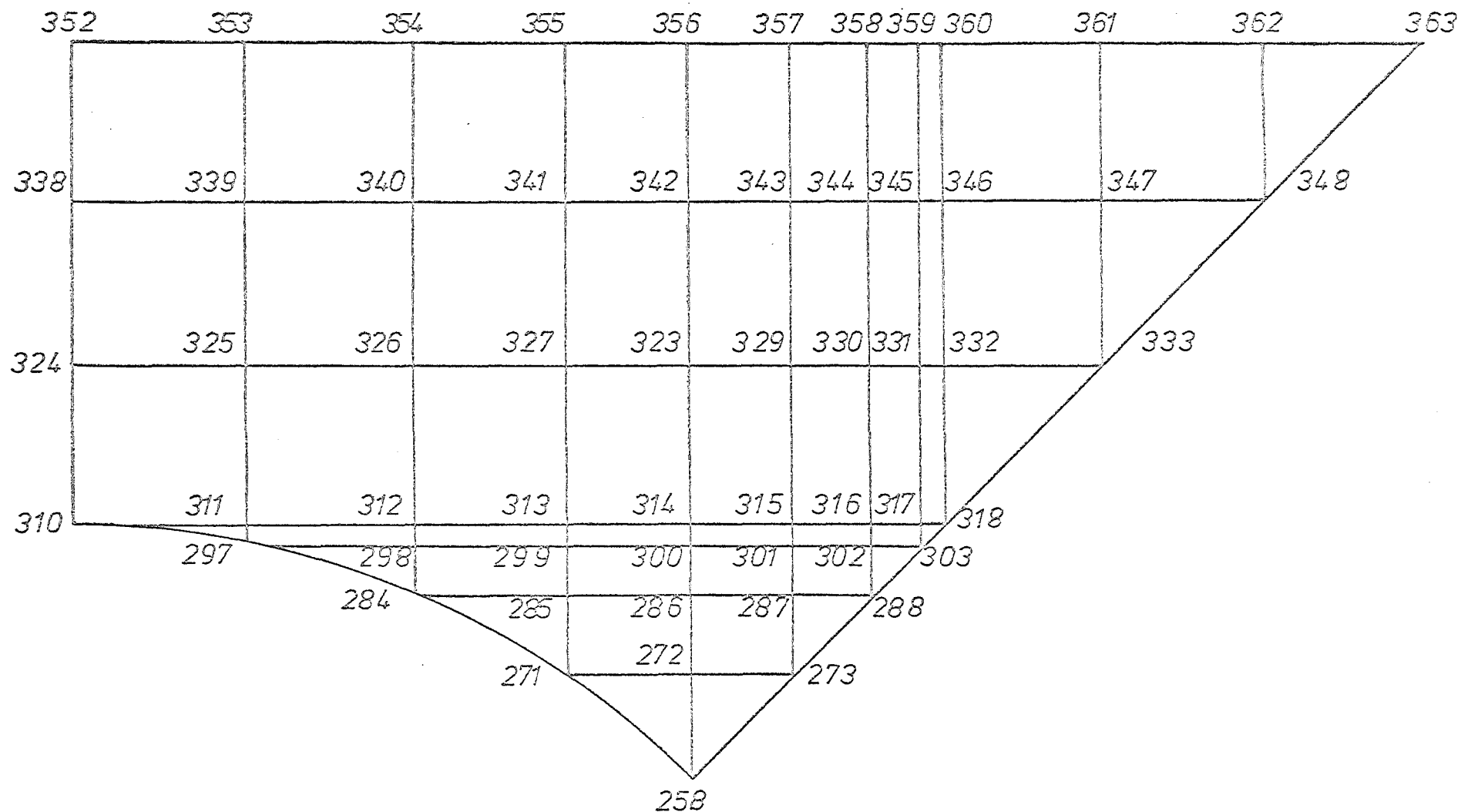


FIGURE B4 SOLID CONDUCTION ZONE C3-PLAN VIEW

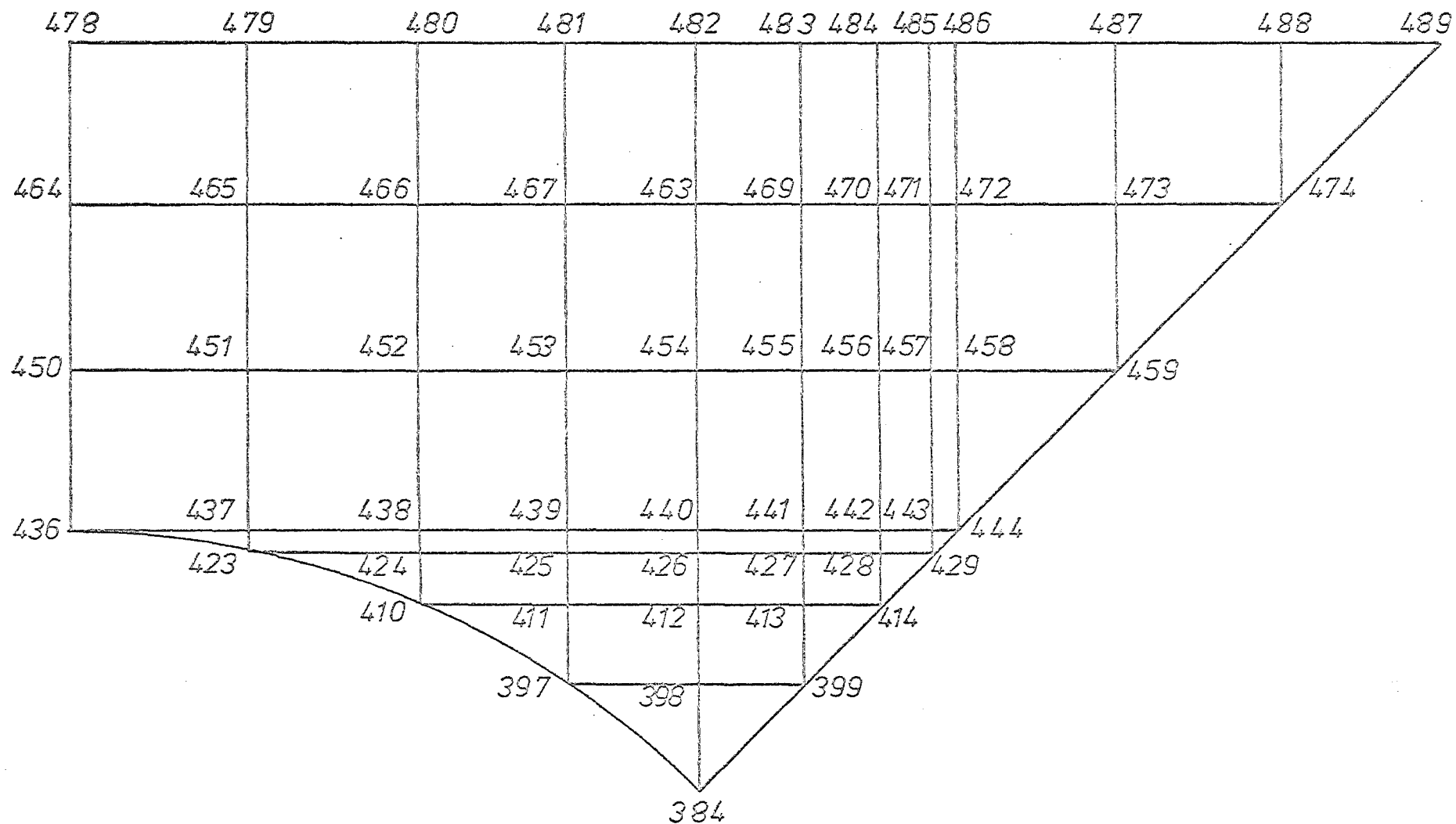


FIGURE B5 SOLID CONDUCTION ZONE C4-PLAN VIEW

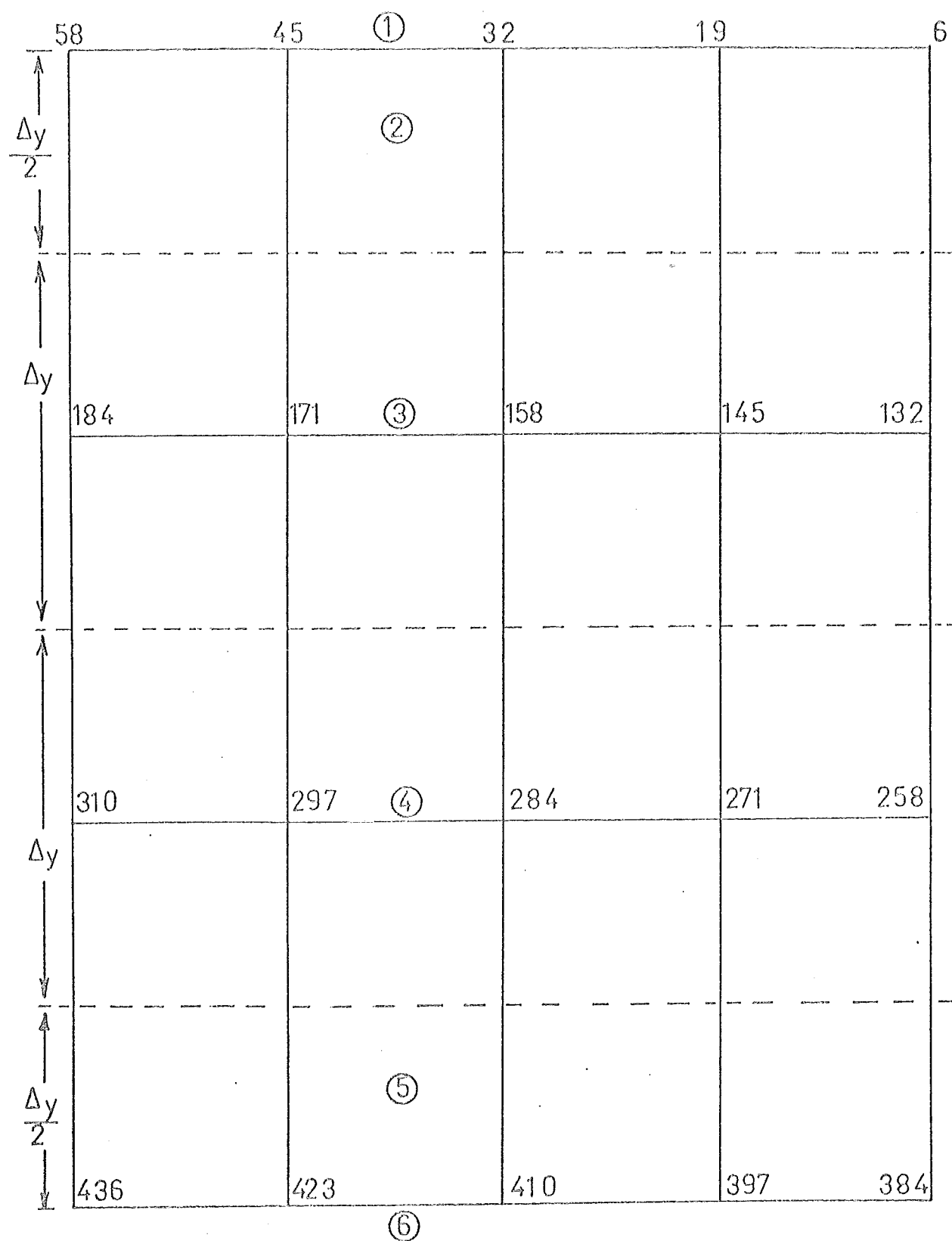


FIGURE B6 RADIATION REGIONS AND SURFACE POINTS

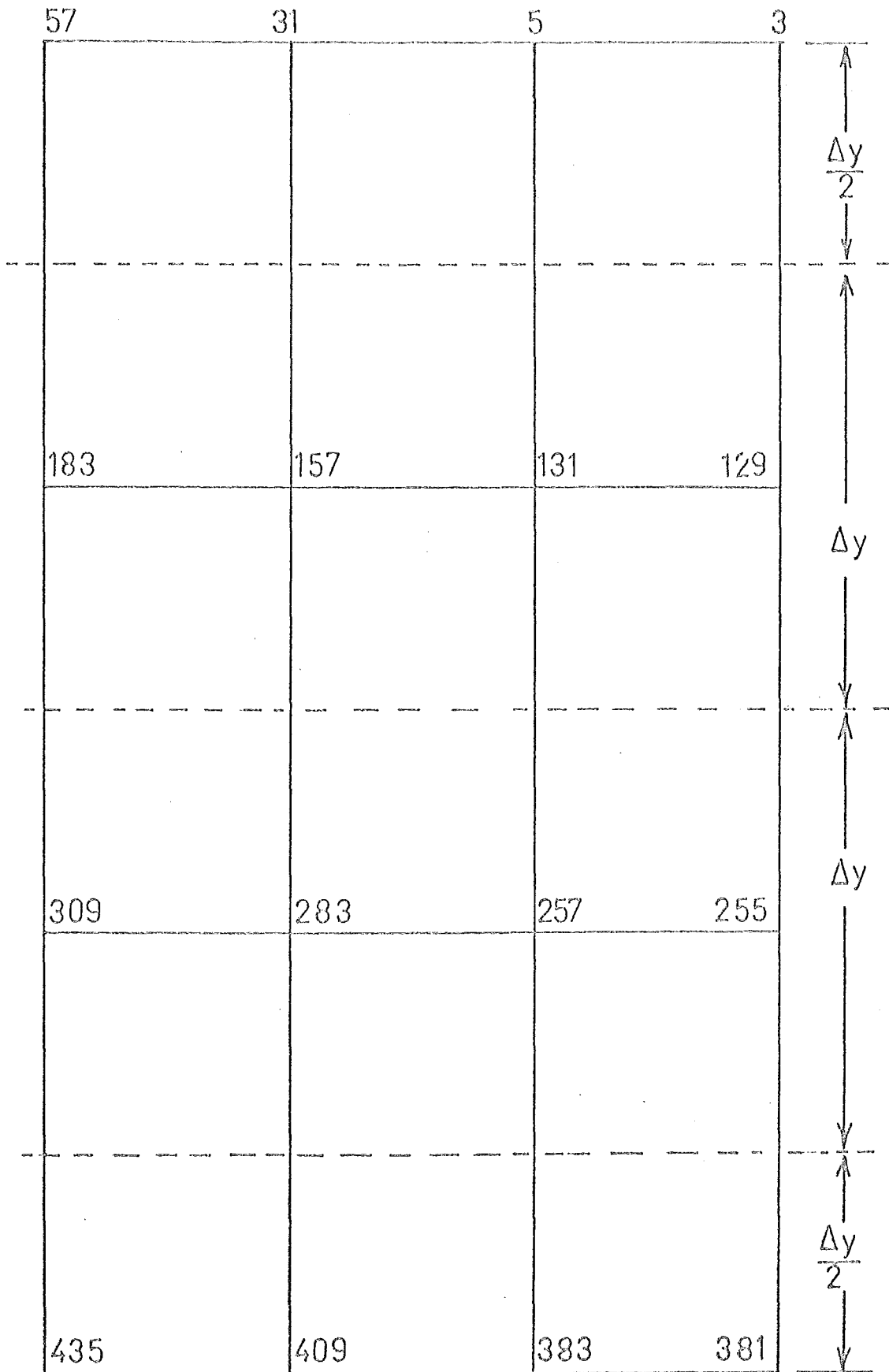


FIGURE B7 AIR CONDUCTION REGIONS

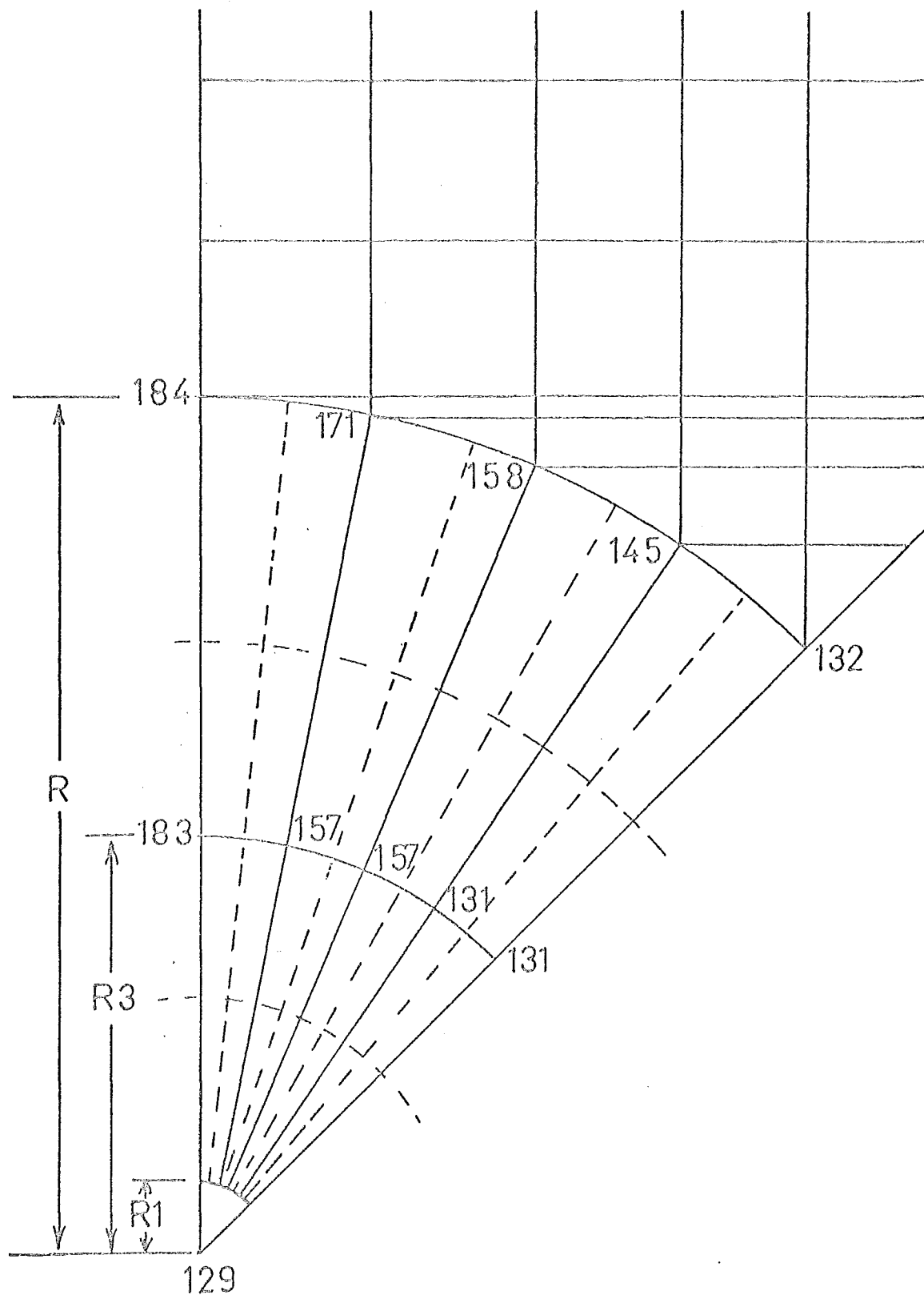


FIGURE B8 PLAN VIEW OF AIR CONDUCTION
REGIONS

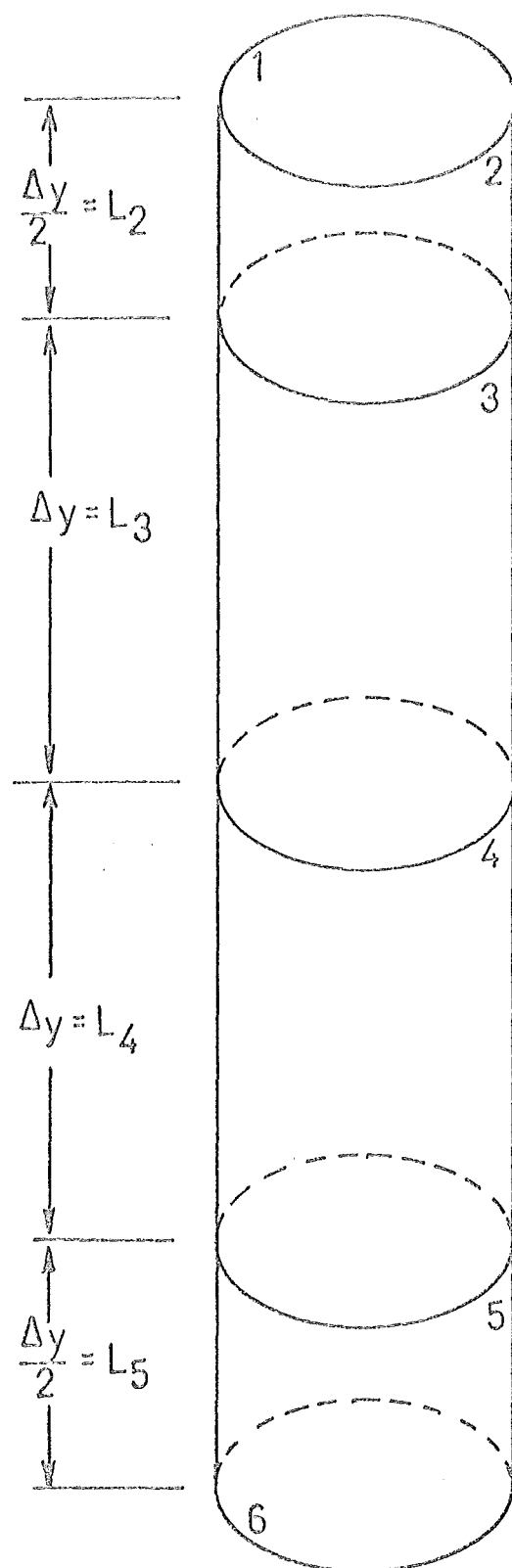


FIGURE B9 HOLE DRILLED IN BLOCK OF SPECIMEN
SHOWING RADIATION REGIONS

(aluminium cold and hot plates). The rest of the regions are ring regions (Figure B9). Each radiation region has a 'radiation-region' temperature ($TR(I)$) associated with it. The surface nodal points in each radiation region are shown in Figure B6.

The radiation flow to each surface point is $Q_{RAD}(I,J)$, where J is the radiation region number

I is the surface point counter

That is:

(a) for surface points 6, 19, 32, 45 and 58: $J = 2$, whereas $I = 1, 2, 3, 4$ and 5 respectively

(b) for surface points 132, 145, 158, 171 and 184: $J = 3$, whereas $I = 1, 2, 3, 4$ and 5 respectively

(c) similarly, for surface points in regions 4 and 5, $J = 4$ and 5 respectively

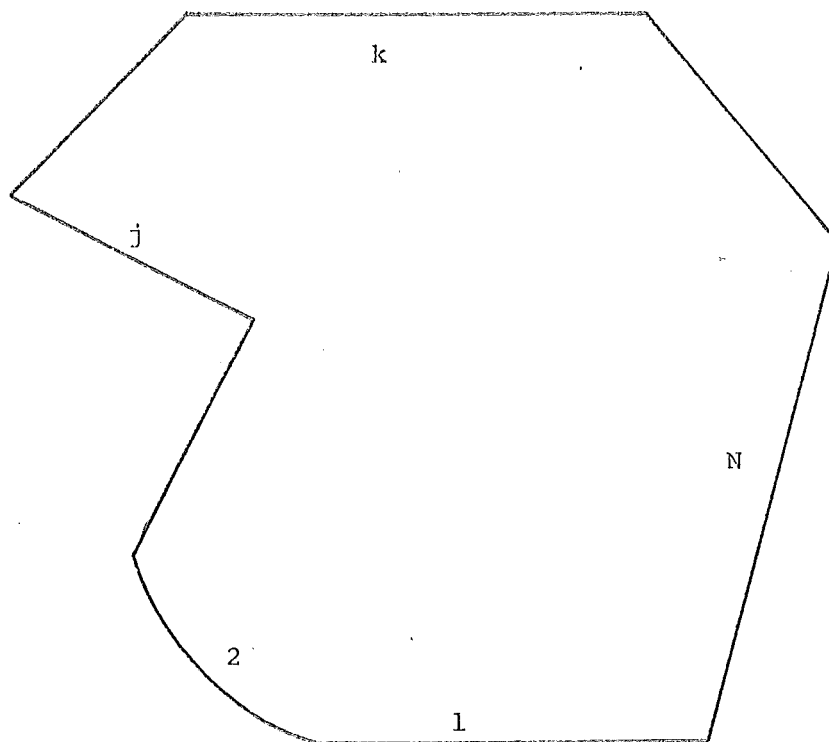
B2.3 AIR CONDUCTION ZONES

In the hole, the air contained within was divided into isothermal regions. Figure B8 shows the 2mm diameter constant temperature air core in the centre of the hole, and the two radial air regions - one at surface point temperatures and the other at intermediate temperatures between the air core temperature and the surface temperatures. In the y-direction, the air regions corresponded exactly to the solid conduction regions (Figure B7).

B3 NET RADIATION METHOD

Consider an enclosure composed of N discrete surface areas as shown in Figure B10. The objective of the analysis is to analyse the radiation exchange between the surface areas.

- (A) Enclosure Composed Of N Discrete Surface Areas
With Typical Surfaces j and k



- (B) Energy Quantities Incident Upon And Leaving
Typical Surface Of Enclosure

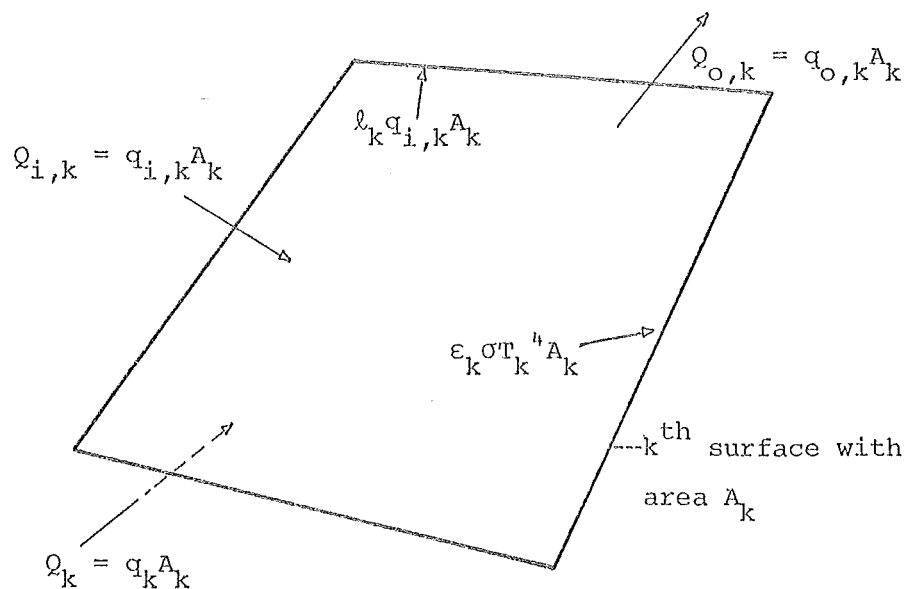


FIGURE B10 RADIATION BETWEEN FINITE AREAS

Two types of boundary conditions can be used with this method.

(a) the required energy supplied to a surface is to be determined when the surface temperature is specified

(b) the temperature that a surface will achieve is to be found when a known heat input is imposed

In this work, boundary conditions of type 'a' were used.

Consider the k th inside surface area A_k of the enclosure shown in Figure B10. The quantities q_i and q_o are the rates of incoming and outgoing radiant energy per unit area, respectively. The quantity q is the energy flux supplied by some external means to the surface to make up for the net radiative loss and thereby maintain the specified surface temperature. A heat balance at the surface provides the relation:

$$Q_k = q_k A_k = (q_{o,k} - q_{i,k}) A_k \quad (B-1)$$

A second equation results from the fact that the energy flux leaving the surface is composed of directly emitted plus reflected energy. This gives:

$$\begin{aligned} q_{o,k} &= \epsilon_k \sigma T_k^4 + \ell_k q_{i,k} \\ &= \epsilon_k \sigma T_k^4 + (1 - \epsilon_k) q_{i,k} \end{aligned} \quad (B-2)$$

where $\ell_k = 1 - \alpha_k = 1 - \epsilon_k$ (assuming opaque gray surfaces)

q_o is the radiosity

The incident flux $q_{i,k}$ is derived from the portions of the energy leaving the surfaces in the enclosure that arrive at the k th surface. The incident flux is equal to:

$$\begin{aligned}
A_k q_{i,k} = & A_1 q_{O,1} F_{1-k} + A_2 q_{O,2} F_{2-k} + \dots + \dots \\
& \dots + A_j q_{O,j} F_{j-k} + \dots + A_k q_{O,k} F_{k-k} + \dots \\
& + A_N q_{O,N} F_{N-k}
\end{aligned} \tag{B-3}$$

From the configuration-factor reciprocity relation,

$$A_1 F_{1-k} = A_k F_{k-1}$$

$$A_2 F_{2-k} = A_k F_{k-2}$$

$$\vdots \quad \quad \quad \vdots$$

$$A_N F_{N-k} = A_k F_{k-N} \tag{B-4}$$

Then equation B-3 can be written so that the only area appearing is A_k .

$$\begin{aligned}
A_k q_{i,k} = & A_k F_{k-1} q_{O,1} + A_k F_{k-2} q_{O,2} + \dots + A_k F_{k-j} q_{O,j} + \\
& \dots + \dots + A_k F_{k-k} q_{O,k} + \dots + \\
& A_k F_{k-N} q_{O,N}
\end{aligned} \tag{B-5}$$

$$\text{or} \quad q_{i,k} = \sum_{j=1}^N F_{k-j} q_{O,j} \tag{B-6}$$

Equations B-2 and B-6 provide two different expressions for $q_{i,k}$. These are each substituted into equation B-1 to eliminate $q_{i,k}$ and provide two basic heat balance equations for Q_k in terms of $q_{O,k}$.

$$Q_k = \frac{A_k \epsilon_k}{(1-\epsilon_k)} (\sigma T_k^4 - q_{O,k}) \tag{B-7}$$

$$Q_k = A_k (q_{O,k} - \sum_{j=1}^N F_{k-j} q_{O,j}) \tag{B-8}$$

where Q_k can be regarded as either the energy supplied to the surface k by external means or the net radiative loss from surface k resulting from radiation in the enclosure.

Equations B-7 and B-8 can be written for each of the N surfaces in the enclosure. This provides $2N$ equations for $2N$ unknowns. The q 's are N of the unknowns. The remaining unknowns consist of the Q 's.

B3.1 SOLUTION METHOD

Computing the radiative exchange within an enclosure involves first solving for q_o for each surface and then computing the Q 's.

When the surface temperatures are all specified, the set of simultaneous equations for q_o 's is obtained by eliminating Q_k 's from B-7 and B-8. This yields the following equation for the k th surface.

$$q_{o,k} - (1-\epsilon_k) \sum_{j=1}^N F_{k-j} q_{o,j} = \epsilon_k \sigma T_k^4 \quad (B-9)$$

an alternate form of this equation is:

$$\sum_{j=1}^N \{\delta_{kj} - (1-\epsilon_k) F_{k-j}\} q_{o,j} = \epsilon_k \sigma T_k^4 \quad (B-10)$$

where δ_{kj} is the Kronecker delta symbol:

$$\begin{aligned} \delta_{kj} &= 0 && \text{when } k \neq j \\ &= 1 && \text{when } k = j \end{aligned}$$

With the T 's known, the q_o 's can be found from B-10.

Equation B-7 is then used to compute the Q 's.

B3.2 METHOD OF SOLUTION (USED IN THIS WORK)

From Figure B9, $N = 6$. The matrix of outgoing radiative flux (q_o) is derived from equation B-10.

Matrix Of The Radiosities - Equation B-11

$$\{1-(1-\epsilon_1)F_{1-1}\}q_{O,1}-(1-\epsilon_1)F_{1-2}q_{O,2}-(1-\epsilon_1)F_{1-3}q_{O,3}-(1-\epsilon_1)F_{1-4}q_{O,4}-(1-\epsilon_1)F_{1-5}q_{O,5}-(1-\epsilon_1)F_{1-6}q_{O,6} = \epsilon_1 \sigma T_{r1}^4$$

$$-(1-\epsilon_1)F_{2-1}q_{O,1}+\{1-(1-\epsilon_2)F_{2-2}\}q_{O,2}-(1-\epsilon_2)F_{2-3}q_{O,3}-(1-\epsilon_2)F_{2-4}q_{O,4}-(1-\epsilon_2)F_{2-5}q_{O,5}-(1-\epsilon_2)F_{2-6}q_{O,6} = \epsilon_2 \sigma T_{r2}^4$$

$$-(1-\epsilon_3)F_{3-1}q_{O,1}-(1-\epsilon_3)F_{3-2}q_{O,2}+\{1-(1-\epsilon_3)F_{3-3}\}q_{O,3}-(1-\epsilon_3)F_{3-4}q_{O,4}-(1-\epsilon_3)F_{3-5}q_{O,5}-(1-\epsilon_3)F_{3-6}q_{O,6} = \epsilon_3 \sigma T_{r3}^4$$

$$-(1-\epsilon_4)F_{4-1}q_{O,1}-(1-\epsilon_4)F_{4-2}q_{O,2}-(1-\epsilon_4)F_{4-3}q_{O,3}+\{1-(1-\epsilon_4)F_{4-4}\}q_{O,4}-(1-\epsilon_4)F_{4-5}q_{O,5}-(1-\epsilon_4)F_{4-6}q_{O,6} = \epsilon_4 \sigma T_{r4}^4$$

$$-(1-\epsilon_5)F_{5-1}q_{O,1}-(1-\epsilon_5)F_{5-2}q_{O,2}-(1-\epsilon_5)F_{5-3}q_{O,3}-(1-\epsilon_5)F_{5-4}q_{O,4}+\{1-(1-\epsilon_5)F_{5-5}\}q_{O,5}-(1-\epsilon_5)F_{5-6}q_{O,6} = \epsilon_5 \sigma T_{r5}^4$$

$$-(1-\epsilon_6)F_{6-1}q_{O,1}-(1-\epsilon_6)F_{6-2}q_{O,2}-(1-\epsilon_6)F_{6-3}q_{O,3}-(1-\epsilon_6)F_{6-4}q_{O,4}-(1-\epsilon_6)F_{6-5}q_{O,5}+\{1-(1-\epsilon_6)F_{6-6}\}q_{O,6} = \epsilon_6 \sigma T_{r6}^4$$

B4 SHAPE FACTORS

For a cylinder divided into rings and discs, shape factors are of three basic configurations (Figure B9).

- (a) from any ring to another e.g. F_{2-3}
- (b) from any ring to any disc e.g. F_{3-1}
- (c) from any disc to another disc e.g. F_{1-6}

Leuenberger (165) developed shape factors for cylindrical assemblies encompassing the above three configurations. By using flux algebra and Leuenberger's formulas, 'statement functions' were set up in Fortran IV to evaluate the shape factors for the various linear dimensions of the cavity problem simulations. The basic expressions used are given below (all referring to Figure B9).

B4.1 SHAPE FACTORS OF RING TO RING

The general formula for the shape factor of one ring surface 'a' to another 'b' is:

$$F_{a-b} = \frac{L_b}{2R} + \frac{1}{4} \left\{ \left(\sqrt{4 + \frac{L^2 b}{R^2}} \right) + \frac{L_b}{L_a} \left(\sqrt{4 + \frac{L^2 b}{R^2}} \right) - \left(\frac{L_a + L_b}{L_a} \right) \right. \\ \left. \left(\sqrt{4 + \left(\frac{L_a + L_b}{R} \right)^2} \right) \right\} \quad (B-12)$$

where R is the radius of the cylinder.

(1) Computing F_{2-3}

$$F_{2-3} = F_{5-4}$$

$$\text{Put } L_a = L_2$$

$$L_b = L_3 \text{ and then substitute into B-12}$$

(2) Computing F_{2-4}

$$F_{2-4} = F_{5-3}$$

First compute $F_{2-(3+4)}$, that is,

$$\text{Put } L_a = L_2$$

$$L_b = L_3 + L_4$$

$$\text{But } F_{2-(3+4)} = F_{2-3} + F_{2-4}$$

Since F_{2-3} is known from (1)

$$\text{Then } F_{2-4} = F_{2-(3+4)} - F_{2-3}$$

(3) Computing F_{2-5}

Again compute $F_{2-(3+4+5)}$ first

$$\text{That is, put } L_a = L_2$$

$$L_b = L_3 + L_4 + L_5$$

$$\text{Since } F_{2-(3+4+5)} = F_{2-3} + F_{2-4} + F_{2-5}$$

Then F_{2-5} is known

(4) Computing F_{3-4}

$$F_{3-4} = F_{4-3}$$

$$\text{Put } L_a = L_3 \text{ and } L_b = L_4$$

Substitute into B-12

B4.2 SHAPE FACTORS OF DISC TO RING

Starting with the top disc, that is, region 1, the shape factors of a disc surface to a ring surface are F_{1-2} , F_{1-3} , F_{1-4} , and F_{1-5} . By symmetry, these are equal to those from region 6, that is, F_{6-5} , F_{6-4} , F_{6-3} , and F_{6-2} respectively.

The general expression for the shape factor of a disc surface 'a' to a ring surface 'b' is:

$$F_{a-b} = \frac{1}{2} \left(\frac{L_b}{R} \left(\sqrt{4 + \frac{L_b^2}{R^2}} - \frac{L_b^2}{R^2} \right) \right) \quad (B-13)$$

(1) Computing F_{1-2}

Put $L_b = L_2$ and substitute into B-13

(2) Computing F_{1-3}

Put $L_b = L_2 + L_3$ and hence compute $F_{1-(2+3)}$

$$F_{1-(2+3)} = F_{1-2} + F_{1-3}$$

Since F_{1-2} is known from (1), then F_{1-3} can be found

(3) Computing F_{1-4}

Put $L_b = L_2 + L_3 + L_4$ and hence compute $F_{1-(2+3+4)}$

From (1), (2) and flux algebra,

$$F_{1-4} = F_{1-(2+3+4)} - F_{1-2} - F_{1-3}$$

(4) Computing F_{1-5}

Put $L_b = L_2 + L_3 + L_4 + L_5$

$$\text{Hence } F_{1-5} = F_{1-(2+3+4+5)} - F_{1-2} - F_{1-3} - F_{1-4}$$

B4.3 SHAPE FACTORS OF DISC TO DISC

The equation used for the shape factors of a disc surface ('1') to another ('6') is:

$$F_{1-6} = F_{6-1} = 1 - \frac{1}{2} \left(\frac{L}{R} \sqrt{4 + \frac{L^2}{R^2}} - \frac{L^2}{R^2} \right) \quad (B-14)$$

where $L = L_2 + L_3 + L_4 + L_5$ (thickness of specimen)

B4.4 SHAPE FACTORS OF SURFACE k TO SURFACE k

If the kth surface can view itself (is concave), it will intercept a portion of its own emitted energy. The configuration factor F_{k-k} is evaluated from equation B-15 after all the other factors are known.

$$F_{k-1} + F_{k-2} + F_{k-3} + \dots + F_{k-k} + \dots + F_{k-N} = 1 \quad (B-15)$$

B5 THERMAL CONDUCTANCES

The thermal conductances are calculated using the basic formula:

$$K_{ij} = k \frac{A_{ij}}{L_{ij}} \quad (B-16)$$

where k = thermal conductivity

A_{ij} = average surface area perpendicular to the
direction of heat flow

L_{ij} = distance between the nodes

B5.1 SOLID CONDUCTION REGION (INTERIOR)

In Figure B3, consider nodal point 201 (diameter of hole = 35.5mm).

$$CXY(201) = \frac{k \times 2.027 \times \Delta y}{2.690} \quad (B-17)$$

where CXY = conductance in the x-direction

Δy = depth of zone of constant temperature Figure B1

2.027×10^{-3} metres = width of the zone associated with
point 201

2.690×10^{-3} metres = distance between nodal points 201
and 202

Similarly, if considering the conductance in the y-direction

$$CYX(201) = \frac{k \times 2.879 \times 2.027}{\Delta y} \quad (B-18)$$

with Δy as the distance between nodal points 201 and 75

In the z-direction, the conductance associated with point 201 is:

$$CZX(201) = \frac{k \times 3.404 \times \Delta y}{2.027} \quad (B-19)$$

with 2.027×10^{-3} metres as the distance between nodal points 201 and 215

B5.2 SOLID CONDUCTION REGION (BOUNDARY NODES)

For irregular boundaries, the rectangular network formulas used for the interior nodes are not applicable. The irregular boundaries occurred at the air-solid interface, points such as 132, 145, 158, 171 and 184 in Figure B3. The thermal conductances associated with these points were evaluated using the unified method due to Macneal (117).

In Figure B3, the conductance between nodal points 132 and 146 is:

$$CZX(132) = \frac{k(\cot B_1 + \cot B_2)\Delta y}{2} \quad (B-20)$$

This type of equation was used for all the other surface points. For example,

$$CZX(284) = k \left(\frac{3.30}{1.10} + \frac{3.068}{1.01} \right) \frac{\Delta y}{2} \quad (B-21)$$

Before accepting Macneal's method, a geometrical proof of the validity of the method was done.

B5.3 AIR CONDUCTANCES

The conductances between the various air nodal points in the hole (Figure B8) were evaluated using equation B-22.

$$K_{ij} = 2\pi k L_{ij} / \ln (r_o / r_i) \quad (B-22)$$

B6 NODAL EQUATIONS

For the nodal points shown in Figures B3 and B4, one general relaxation equation was derived. This equation (B-23) was derived by considering the heat balance of a general point. The numbering system used refers to the nodal points shown in Figures B2 to B5.

For surface points, some of the conductances are used for storing the convergence variable, that is, dQ_r/dT .

For example,

$$CXY(132) = -DQDT(1,3)$$

$$CXY(144) = -DQDT(2,3)$$

$$CZX(144) = -DQDT(3,3)$$

See the computer listing for more details.

$$\frac{\text{CRAD}(I) + (\text{CXY}(I-1)T(I-1)) + (\text{CXY}(I)T(I+1)) + (\text{CYX}(I+126)T(I+126)) + (\text{CYX}(I)T(I-126)) + (\text{CZX}(I-14)T(I-14)) + (\text{CZX}(I)T(I+14))}{(\text{CXY}(I-1) + \text{CXY}(I) + \text{CYX}(I+126) + \text{CYX}(I) + \text{CZX}(I-14) + \text{CZX}(I))} - T(I) = \text{RES}(I)$$

(B-23)

where CRAD(I) = radiation heat flow for surface points

(points like 132, 145, 297, 284)

= 0 for interior points (solid conduction points)

T = the temperature in degrees Celsius

CXY, CYX, CZX = the conductances

RES(I) = residual of the equation which is evaluated until

it becomes negligible in magnitude e.g. 10^{-5}

B7 NOTES ON SPECIMENS USED

Durotherm (asbestos cement board) is opaque. Perspex, however, has a transmittance of 92% in the wavelength range 0.335 microns to 1.6 microns (146). No data was found in the wavelength range 2 to 20 microns. In the range 20 to 100 microns, the transmittance is about 20%.

Assuming that perspex transmits 92% of the incident radiation in the wavelength range 0.335 to 1.6 microns, and is opaque at shorter and longer wavelengths, the percentage of incident radiation from a blackbody at a specified temperature which perspex will transmit can be estimated.

(i) Specimen temperature of 44°C - from radiation functions tables (166) (and also a computer program evaluating radiation function polynomials), the percentage of the total radiant energy incident upon perspex was:

$$\{(0.166 \times 10^{-8})\% - (0.615 \times 10^{-53})\% \} \times 0.92 = 0\%$$

(ii) Specimen temperature of 60°C

$$\lambda T_{\text{lower}} = 0.335 \times 600 = 201 \text{ (microns, } ^{\circ}\text{R)}$$

$$\lambda T_{\text{upper}} = 1.59 \times 600 = 954 \text{ (microns, } ^{\circ}\text{R)}$$

From the computer program (which is not given in this work)

$$\frac{\int_{0.335}^{\infty} E_{b\lambda} d\lambda}{\int_0^{\infty} E_{b\lambda} d\lambda} = 0.37 \times 10^{-50}\%$$

and

$$\frac{\int_{1.59}^{\infty} E_{b\lambda} d\lambda}{\int_0^{\infty} E_{b\lambda} d\lambda} = 0.5578 \times 10^{-8}\%$$

The amount of energy transmitted is:

$$((0.56 \times 10^{-8}) - (0.37 \times 10^{-50})) \times .92 = 0\%$$

The transmittance data used in the above calculations was for 3.2mm thick lucite. Plexiglas plate 4.93mm thick gave a transmittance of 0% in the wavelength range 20 to 100 microns (146). Since all the specimens used in this work were 5.6mm thick or more, it was assumed that all incident radiation in the perspex specimens was absorbed. With a scattering coefficient of less than 0.01cm^{-1} (151), the scattering of radiation in the perspex specimens was also ignored. Note that a scattering coefficient of 0.01cm^{-1} implies that the mean free path before scattering starts is equal to 100cm.

CONCLUDING REMARKS - The perspex specimens used are of sufficient thickness to ensure that all the incident radiation is absorbed and they can be considered to be opaque.

APPENDIX C
SURFACE TEMPERATURE SIMULATIONS

C1	<u>EVALUATION OF CONDUCTANCES</u>	271
C2	<u>GENERAL GRID SYSTEM</u>	273
C3	<u>TEMPERATURE PROFILES OF SIMULATION RUNS 1 TO 10</u>	275
C4	<u>CONDUCTANCES OF SIMULATION RUN 16</u>	286
C5	<u>HEAT FLOWS OF SIMULATION RUN 16</u>	292
C6	<u>COMPUTER LISTING OF THE SURFACE TEMPERATURE SIMULATION PROGRAM</u>	306

C1 EVALUATION OF CONDUCTANCES

The formulae used in Appendix B are applicable. Due to the presence of the three different materials (perspex, araldite and aluminium), composite media formulae had to be applied. The total conductances between isothermal faces were obtained by adding the individual parallel conductances. When conductances were in series, the total conductance was set equal to the sum of the reciprocal of the individual conductances. Consider for example, the structure shown in Figure C1.

The faces AB and CD are at constant temperatures; therefore, they can be represented by two nodes, say 1 and 2. Consider the auxiliary nodes a, b, c, d, e and f. The total conductance between nodes 1 and 2 is:

$$K_{1,2} = K_{a,b} + K_{c,d} + K_{e,f} \quad (C-1)$$

$$\text{where } \frac{1}{K_{a,b}} = \frac{L_1}{\ell_1 k_1} + \frac{L_2}{\ell_1 k_2} \quad (C-2)$$

$$K_{c,d} = \frac{k_1 \ell_2}{\frac{L_1}{k_1} + L_2} \quad (C-3)$$

$$K_{e,f} = \frac{k_3 \ell_3}{\frac{L_1}{k_3} + L_2} \quad (C-4)$$

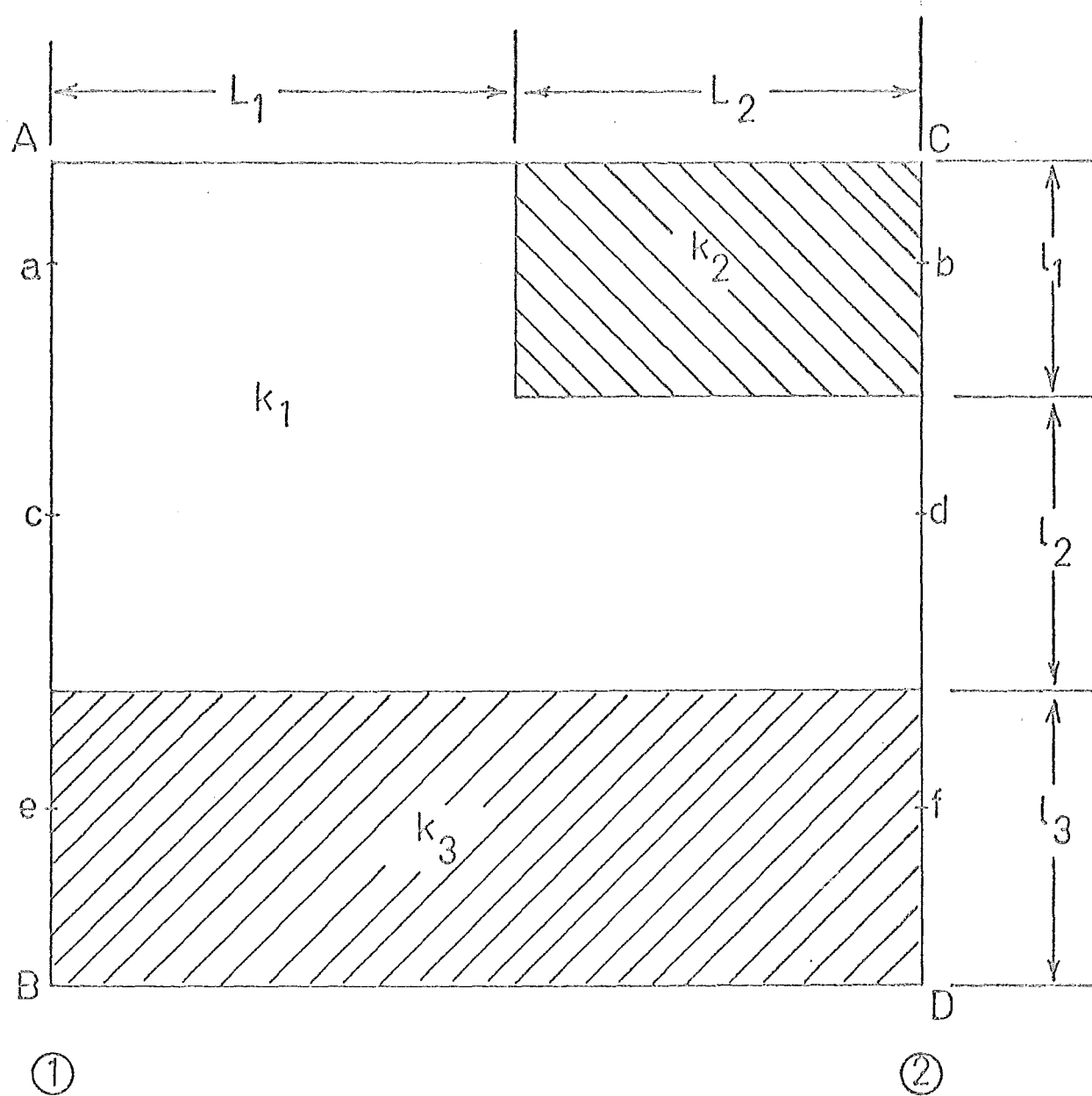


FIGURE C1—COMPOSITE SYSTEM

C2 GENERAL GRID SYSTEM

Figure C2 shows a general grid system. The three thermocouple grooves are expanded in size to show the nodal points. Since aluminium has a much higher thermal conductivity than araldite, despite their size, the thermocouple grooves always had more nodal points. Similarly, in the specimen region, nodal points were more numerous than in the aluminium region.

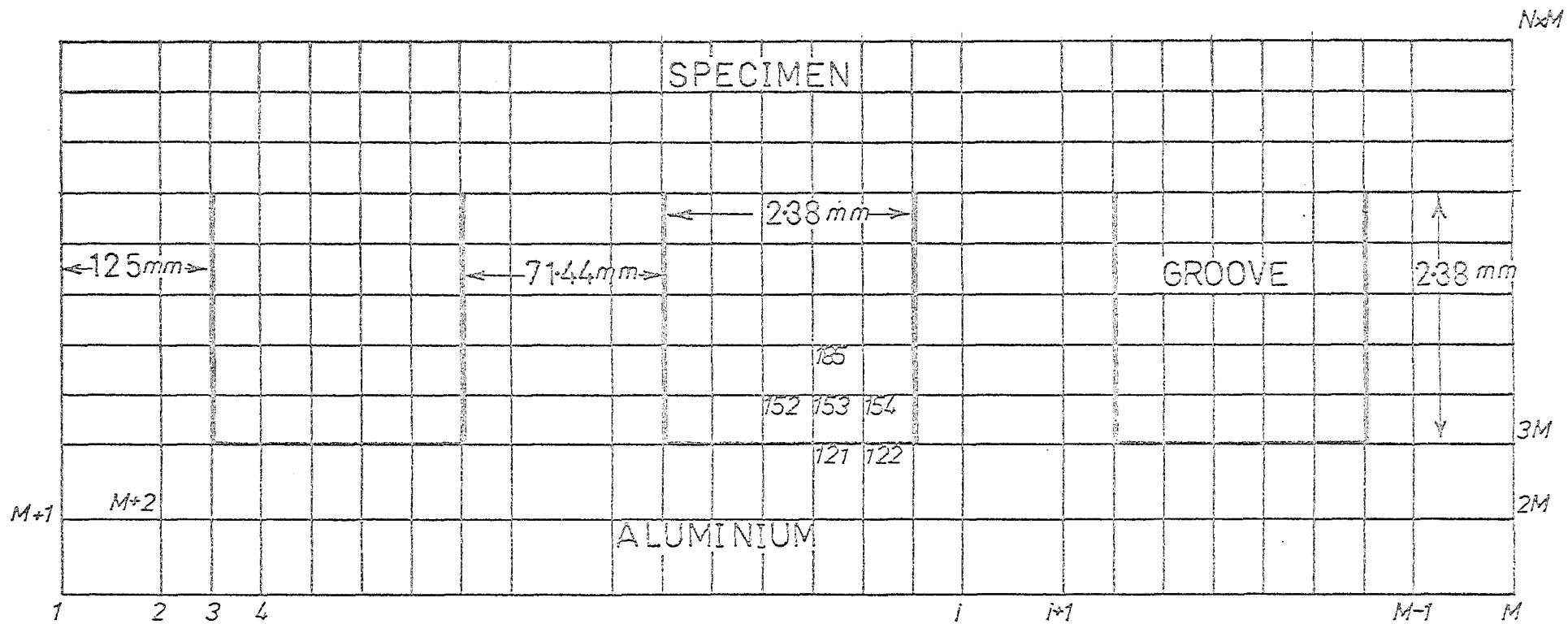


FIGURE C2-A TYPICAL NODAL SYSTEM — SURFACE TEMPERATURE SIMULATIONS ²⁷⁴

C3 TEMPERATURE PROFILES OF SIMULATION RUNS 1 TO 10

The temperature profiles of the surface temperature simulation runs described in Chapter 1 are shown in Tables C1 to C10.

TABLE C1
Temperature profile of surface temperature
simulation run 1 showing the 1 groove configuration
with a 3mm x 4mm aluminium insert in the groove

10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000
9905	9985	9985	9985	9986	9986	9987	9989	9991	9992	9992	9991	9989	9987	9986	9986	9985	9985	9985	9985
9971	9971	9971	9971	9971	9972	9974	9977	9982	9984	9984	9982	9977	9974	9972	9971	9971	9971	9971	9971
9956	9956	9956	9956	9956	9957	9959	9965	9975	9979	9979	9975	9965	9959	9957	9956	9956	9956	9956	9956
9941	9941	9941	9941	9941	9941	9941	9940	9125	9120	9120	9124	9940	9940	9940	9941	9941	9941	9941	9941
9927	9927	9926	9926	9925	9924	9922	9920	9117	9115	9114	9117	9920	9922	9924	9925	9926	9926	9927	9927
9912	9912	9912	9911	9910	9908	9905	9902	9108	9106	9106	9106	9902	9905	9908	9910	9911	9912	9912	9912
9898	9898	9898	9897	9895	9892	9888	9883	9097	9096	9096	9097	9883	9888	9892	9895	9897	9898	9898	9898
9885	9885	9884	9883	9881	9878	9872	9861	9083	9084	9084	9082	9861	9872	9878	9881	9883	9884	9885	9885
7256	7256	7255	7253	7247	7235	7203	7115	6859	6785	6785	6859	7115	7202	7235	7247	7253	7255	7256	7256
4628	4628	4627	4625	4621	4611	4588	4539	4453	4413	4413	4453	4539	4588	4611	4621	4625	4627	4628	4628
2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000

TABLE C2
Temperature profile of surface temperature
simulation run 2 showing the 1 groove configuration
with a 4.99mm x 4mm aluminium insert in the groove

10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000	10000
9985	9985	9985	9985	9985	9985	9986	9988	9991	9992	9992	9991	9988	9986	9985	9985	9985	9985	9985	9985
9969	9969	9969	9969	9970	9970	9972	9976	9982	9986	9986	9982	9976	9972	9970	9970	9969	9969	9969	9969
9954	9954	9954	9954	9954	9954	9955	9961	9977	9983	9983	9977	9961	9955	9954	9954	9954	9954	9954	9954
9939	9939	9939	9938	9938	9936	9934	9928	9900	9893	9893	9900	9928	9934	9936	9938	9938	9939	9939	9939
9924	9924	9924	9923	9922	9920	9917	9911	9894	9889	9889	9894	9911	9917	9920	9922	9923	9924	9924	9924
9910	9910	9909	9908	9907	9904	9901	9896	9884	9881	9881	9884	9896	9901	9904	9907	9908	9909	9910	9910
9896	9896	9895	9894	9892	9890	9886	9882	9871	9869	9869	9871	9882	9886	9890	9892	9894	9895	9896	9896
9882	9882	9882	9881	9879	9876	9873	9868	9853	9855	9855	9853	9868	9873	9876	9879	9881	9882	9882	9882
7255	7255	7254	7253	7252	7250	7248	7244	7239	7238	7238	7239	7244	7248	7250	7252	7253	7254	7255	7255
4627	4627	4627	4627	4626	4625	4624	4622	4620	4619	4619	4620	4622	4624	4625	4626	4627	4627	4627	4627
2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000	2000

TABLE C3

Temperature profile of surface temperature
simulation run 3 showing the 1 groove configuration

4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514
4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514
4514	4514	4513	4513	4513	4513	4513	4513	4514	4514	4514	4514	4513	4513	4513	4513	4513	4513	4514	4514
4513	4513	4513	4513	4513	4513	4513	4513	4513	4514	4514	4513	4513	4513	4513	4513	4513	4513	4513	4513
4513	4513	4513	4512	4512	4512	4512	4512	4511	4510	4510	4511	4512	4512	4512	4512	4512	4513	4513	4513
4512	4512	4512	4511	4511	4512	4512	4512	4508	4506	4506	4508	4512	4512	4512	4511	4511	4512	4512	4512
4511	4511	4510	4510	4511	4511	4511	4511	4504	4499	4499	4504	4511	4511	4511	4511	4510	4510	4511	4511
4507	4507	4508	4509	4510	4511	4511	4511	4496	4488	4488	4496	4511	4511	4511	4510	4509	4508	4507	4507
4496	4496	4505	4508	4510	4510	4511	4511	4481	4470	4470	4481	4511	4511	4510	4510	4508	4505	4496	4496
4442	4442	4454	4459	4461	4462	4461	4458	4447	4441	4441	4447	4458	4461	4462	4461	4459	4454	4442	4442
4403	4403	4409	4413	4414	4414	4414	4412	4408	4406	4406	4408	4412	4414	4414	4414	4413	4409	4403	4403
4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368

TABLE C4
Temperature profile of surface temperature
simulation run 4 showing the 1 groove configuration
using constant temperature boundary conditions

4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514
4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514
4514	4514	4513	4513	4513	4513	4513	4513	4514	4514	4514	4514	4513	4513	4513	4513	4513	4513	4514	4514
4513	4513	4513	4513	4513	4513	4513	4513	4513	4514	4514	4513	4513	4513	4513	4513	4513	4513	4513	4513
4513	4513	4513	4512	4512	4512	4512	4512	4511	4511	4511	4511	4512	4512	4512	4512	4512	4513	4513	4513
4512	4512	4512	4511	4511	4512	4512	4512	4509	4507	4507	4509	4512	4512	4512	4511	4511	4512	4512	4512
4511	4511	4510	4510	4511	4511	4511	4511	4506	4502	4502	4506	4511	4511	4511	4511	4510	4510	4511	4511
4507	4507	4508	4509	4510	4511	4511	4511	4500	4494	4494	4500	4511	4511	4511	4510	4509	4508	4507	4507
4496	4496	4505	4508	4510	4510	4511	4511	4489	4481	4481	4489	4511	4511	4510	4510	4508	4505	4496	4496
4442	4442	4454	4459	4461	4462	4461	4459	4451	4447	4447	4451	4459	4461	4462	4461	4459	4454	4442	4442
4403	4403	4409	4413	4414	4415	4414	4413	4410	4408	4408	4410	4413	4414	4415	4414	4413	4409	4403	4403
4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368	4368

TABLE C7

Temperature profile of surface temperature
simulation run 7 showing the 1 deep narrow
groove configuration

4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514
4504	4504	4504	4504	4504	4504	4505	4505	4505	4506	4506	4505	4505	4505	4504	4504	4504	4504	4504	4504
4493	4493	4493	4493	4494	4494	4495	4496	4498	4498	4498	4498	4496	4495	4494	4494	4493	4493	4493	4493
4482	4482	4482	4483	4483	4484	4485	4488	4492	4494	4494	4492	4488	4485	4484	4483	4483	4482	4482	4482
4472	4472	4472	4472	4472	4472	4472	4473	4475	4475	4475	4475	4473	4472	4472	4472	4472	4472	4472	4472
4461	4461	4461	4461	4461	4461	4461	4461	4461	4462	4462	4461	4461	4461	4461	4461	4461	4461	4461	4461
4451	4451	4451	4451	4451	4450	4450	4450	4450	4450	4450	4450	4450	4450	4450	4451	4451	4451	4451	4451
4442	4442	4442	4442	4441	4441	4441	4441	4441	4441	4441	4441	4441	4441	4441	4441	4442	4442	4442	4442
4435	4435	4434	4434	4434	4433	4433	4433	4433	4432	4432	4433	4433	4433	4433	4434	4434	4434	4435	4435
4428	4428	4428	4427	4427	4427	4426	4426	4426	4426	4426	4426	4426	4426	4427	4427	4427	4427	4428	4428
4423	4423	4423	4422	4422	4422	4421	4421	4421	4420	4420	4421	4421	4421	4422	4422	4422	4422	4423	4423
4419	4419	4419	4419	4418	4418	4418	4417	4417	4416	4416	4417	4417	4418	4418	4418	4419	4419	4419	4419
4417	4417	4417	4417	4416	4416	4415	4415	4414	4413	4413	4414	4415	4415	4416	4416	4417	4417	4417	4417
4417	4417	4416	4416	4416	4415	4415	4415	4411	4409	4409	4411	4415	4415	4415	4416	4416	4417	4417	4417
4400	4400	4400	4399	4399	4398	4398	4397	4396	4395	4395	4396	4397	4398	4398	4399	4399	4400	4400	4400
4385	4385	4384	4384	4384	4383	4383	4382	4382	4381	4381	4382	4382	4383	4383	4384	4384	4384	4385	4385
4371	4371	4371	4371	4370	4370	4369	4369	4368	4368	4368	4368	4369	4369	4370	4370	4371	4371	4371	4371
4359	4359	4359	4359	4358	4358	4358	4357	4357	4357	4357	4357	4357	4358	4358	4358	4359	4359	4359	4359
4349	4349	4349	4348	4348	4348	4347	4347	4347	4346	4346	4347	4347	4347	4348	4348	4348	4349	4349	4349
4340	4340	4339	4339	4339	4339	4338	4338	4338	4337	4337	4338	4338	4338	4339	4339	4339	4339	4340	4340
4332	4332	4332	4331	4331	4331	4330	4330	4330	4330	4330	4330	4330	4330	4331	4331	4331	4332	4332	4332
4325	4325	4325	4324	4324	4324	4324	4324	4323	4323	4323	4323	4324	4324	4324	4324	4324	4325	4325	4325
4319	4319	4319	4318	4318	4318	4318	4318	4318	4317	4317	4318	4318	4318	4318	4318	4318	4319	4319	4319
4314	4314	4313	4313	4313	4313	4313	4313	4313	4312	4312	4313	4313	4313	4313	4313	4313	4313	4314	4314
4309	4309	4309	4309	4308	4308	4308	4308	4308	4308	4308	4308	4308	4308	4308	4308	4309	4309	4309	4309
4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304	4304
4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300

TABLE C8

Temperature profile of surface temperature
simulation run: 8 showing the
1 narrow groove configuration

4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514	4514
4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504	4504
4495	4495	4495	4494	4494	4494	4494	4494	4494	4494	4494	4494	4494	4494	4494	4494	4495	4495	4495
4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485	4485
4477	4477	4477	4476	4476	4476	4476	4476	4476	4476	4476	4476	4476	4476	4476	4476	4477	4477	4477
4469	4469	4469	4468	4468	4468	4468	4468	4468	4468	4468	4468	4468	4468	4468	4468	4469	4469	4469
4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461	4461
4455	4455	4454	4454	4454	4455	4455	4455	4455	4456	4456	4456	4456	4455	4455	4455	4454	4454	4455
4449	4449	4448	4448	4448	4449	4449	4450	4453	4454	4454	4453	4450	4449	4449	4448	4448	4448	4449
4443	4443	4443	4443	4443	4443	4443	4443	4444	4444	4444	4444	4443	4443	4443	4443	4443	4443	4443
4439	4439	4439	4438	4438	4438	4438	4438	4438	4438	4438	4438	4438	4438	4438	4438	4439	4439	4439
4436	4436	4436	4435	4435	4435	4435	4434	4434	4433	4433	4434	4434	4435	4435	4435	4435	4436	4436
4434	4434	4434	4433	4433	4433	4433	4432	4431	4430	4430	4431	4432	4433	4433	4433	4433	4434	4434
4434	4434	4433	4433	4433	4432	4432	4432	4428	4426	4426	4428	4432	4432	4432	4433	4433	4434	4434
4416	4416	4416	4416	4415	4415	4414	4413	4412	4412	4412	4412	4413	4414	4415	4415	4416	4416	4416
4440	4440	4440	4440	4399	4399	4398	4398	4397	4397	4397	4397	4398	4398	4399	4399	4400	4400	4400
4386	4386	4386	4385	4385	4384	4384	4384	4383	4383	4383	4383	4384	4384	4384	4385	4385	4386	4386
4373	4373	4373	4372	4372	4371	4371	4371	4370	4370	4370	4370	4371	4371	4371	4372	4372	4373	4373
4361	4361	4361	4361	4360	4360	4360	4359	4359	4359	4359	4359	4359	4360	4360	4360	4361	4361	4361
4351	4351	4350	4350	4350	4350	4349	4349	4349	4349	4349	4349	4349	4349	4350	4350	4350	4351	4351
4341	4341	4341	4341	4341	4340	4340	4340	4340	4340	4340	4340	4340	4340	4340	4341	4341	4341	4341
4333	4333	4333	4333	4332	4332	4332	4332	4332	4332	4331	4331	4332	4332	4332	4332	4333	4333	4333
4325	4325	4325	4325	4325	4325	4325	4324	4324	4324	4324	4324	4324	4325	4325	4325	4325	4325	4325
4319	4319	4318	4318	4318	4318	4318	4318	4318	4318	4318	4318	4318	4318	4318	4318	4318	4319	4319
4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312	4312
4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306	4306
4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300	4300

TABLE C9
Temperature profile of surface temperature
simulation run 9 showing the 3 groove configuration

514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514
514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514
514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514
514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514
514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514	514
514	514	514	514	514	514	513	513	514	514	514	514	514	514	513	513	514	514	514	514	514	514	514	514	514	514	514	514	514
514	514	514	514	514	513	512	512	513	514	514	514	514	513	512	512	513	514	514	514	514	514	513	512	512	513	514	514	514
514	514	514	514	514	512	511	511	512	514	514	514	514	512	511	511	512	514	514	514	514	514	512	511	511	512	514	514	514
514	514	514	514	514	511	509	509	511	514	514	514	514	511	509	509	511	514	514	514	514	514	511	509	509	511	514	514	514
514	514	514	514	514	507	505	505	507	514	514	514	514	507	505	505	507	514	514	514	514	514	507	505	505	507	514	514	514
471	471	471	471	471	469	469	469	469	471	471	471	471	469	469	469	469	471	471	471	471	471	469	469	469	469	471	471	471
425	425	425	425	425	428	428	428	428	428	428	428	428	428	427	427	428	428	428	428	428	428	428	428	428	428	428	428	428
386	386	386	386	385	385	385	385	385	385	386	386	386	385	385	385	385	385	386	386	386	385	385	385	385	385	386	386	386
343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343	343
300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300	300

TABLE C10
Temperature profile of surface temperature
simulation run 10 showing the
ideal temperature profile

[illegible]

C4 CONDUCTANCES OF SIMULATION RUN 16

Table C11 shows the conductances of simulation run 16. The conductances are in watts per degree Celsius.

Notation:

CA(I) - conductance in X-direction between nodal points 'I' and 'I + 1'

CU(I) - conductance in Y-direction between nodal points 'I' and 'I + M'

TABLE C11 - Conductances Of Surface Temperature Simulation Run 16

M= 32

N= 17

THE CONDUCTANCES IN WATTS PER DEGREE KELVIN ARE

CA(33)=	0.000000	CA(34)=	10.060708	CA(35)=	10.060708	CA(36)=	10.060708	CA(37)=	662.611765	CA(38)=	662.611765
CA(39)=	662.611765	CA(40)=	662.611765	CA(41)=	662.611765	CA(42)=	17.659754	CA(43)=	17.659754	CA(44)=	17.659754
CA(45)=	17.659754	CA(46)=	662.611765	CA(47)=	662.611765	CA(48)=	662.611765	CA(49)=	662.611765	CA(50)=	662.611765
CA(51)=	17.659754	CA(52)=	17.659754	CA(53)=	17.659754	CA(54)=	17.659754	CA(55)=	662.611765	CA(56)=	662.611765
CA(57)=	662.611765	CA(58)=	662.611765	CA(59)=	662.611765	CA(60)=	10.060708	CA(61)=	10.060708	CA(62)=	10.060708
CA(63)=	0.000000	CA(64)=	0.000000	CA(65)=	0.000000	CA(66)=	10.060708	CA(67)=	10.060708	CA(68)=	10.060708
CA(69)=	662.611765	CA(70)=	662.611765	CA(71)=	662.611765	CA(72)=	662.611765	CA(73)=	662.611765	CA(74)=	17.659754
CA(75)=	17.659754	CA(76)=	17.659754	CA(77)=	17.659754	CA(78)=	662.611765	CA(79)=	662.611765	CA(80)=	662.611765
CA(81)=	662.611765	CA(82)=	662.611765	CA(83)=	17.659754	CA(84)=	17.659754	CA(85)=	17.659754	CA(86)=	17.659754
CA(87)=	662.611765	CA(88)=	662.611765	CA(89)=	662.611765	CA(90)=	662.611765	CA(91)=	662.611765	CA(92)=	10.060708
CA(93)=	10.060708	CA(94)=	10.060708	CA(95)=	0.000000	CA(96)=	0.000000	CA(97)=	0.000000	CA(98)=	0.000000
CA(99)=	6.840000	CA(100)=	6.840000	CA(101)=	331.450000	CA(102)=	331.450000	CA(103)=	331.450000	CA(104)=	331.450000
CA(105)=	331.450000	CA(106)=	12.000000	CA(107)=	12.000000	CA(108)=	12.000000	CA(109)=	12.000000	CA(110)=	331.450000
CA(111)=	331.450000	CA(112)=	331.450000	CA(113)=	331.450000	CA(114)=	331.450000	CA(115)=	12.000000	CA(116)=	12.000000
CA(117)=	12.000000	CA(118)=	12.000000	CA(119)=	331.450000	CA(120)=	331.450000	CA(121)=	331.450000	CA(122)=	331.450000
CA(123)=	331.450000	CA(124)=	6.840000	CA(125)=	6.840000	CA(126)=	6.840000	CA(127)=	0.000000	CA(128)=	0.000000
CA(129)=	0.000000	CA(130)=	3.619726	CA(131)=	3.619726	CA(132)=	3.619726	CA(133)=	0.282000	CA(134)=	0.282000
CA(135)=	0.282000	CA(136)=	0.282000	CA(137)=	0.282000	CA(138)=	6.353774	CA(139)=	6.353774	CA(140)=	6.353774
CA(141)=	6.353774	CA(142)=	0.282000	CA(143)=	0.282000	CA(144)=	0.282000	CA(145)=	0.282000	CA(146)=	0.282000
CA(147)=	6.353774	CA(148)=	6.353774	CA(149)=	6.353774	CA(150)=	6.353774	CA(151)=	0.282000	CA(152)=	0.282000
CA(153)=	0.282000	CA(154)=	0.282000	CA(155)=	0.282000	CA(156)=	3.619726	CA(157)=	3.619726	CA(158)=	3.619726
CA(159)=	0.000000	CA(160)=	0.000000	CA(161)=	0.000000	CA(162)=	3.619726	CA(163)=	3.619726	CA(164)=	3.619726
CA(165)=	0.282000	CA(166)=	0.282000	CA(167)=	0.282000	CA(168)=	0.282000	CA(169)=	0.282000	CA(170)=	6.353774
CA(171)=	6.353774	CA(172)=	6.353774	CA(173)=	6.353774	CA(174)=	0.282000	CA(175)=	0.282000	CA(176)=	0.282000
CA(177)=	0.282000	CA(178)=	0.282000	CA(179)=	6.353774	CA(180)=	6.353774	CA(181)=	6.353774	CA(182)=	6.353774
CA(183)=	0.282000	CA(184)=	0.282000	CA(185)=	0.282000	CA(186)=	0.282000	CA(187)=	0.282000	CA(188)=	3.619726
CA(189)=	3.619726	CA(190)=	3.619726	CA(191)=	0.000000	CA(192)=	0.000000	CA(193)=	0.000000	CA(194)=	3.619726
CA(195)=	3.619726	CA(196)=	3.619726	CA(197)=	0.282000	CA(198)=	0.282000	CA(199)=	0.282000	CA(200)=	0.282000
CA(201)=	0.282000	CA(202)=	6.353774	CA(203)=	6.353774	CA(204)=	6.353774	CA(205)=	6.353774	CA(206)=	0.282000
CA(207)=	0.282000	CA(208)=	0.282000	CA(209)=	0.282000	CA(210)=	0.282000	CA(211)=	6.353774	CA(212)=	6.353774
CA(213)=	6.353774	CA(214)=	6.353774	CA(215)=	0.282000	CA(216)=	0.282000	CA(217)=	0.282000	CA(218)=	0.282000
CA(219)=	0.282000	CA(220)=	3.619726	CA(221)=	3.619726	CA(222)=	3.619726	CA(223)=	0.000000	CA(224)=	0.000000
CA(225)=	0.000000	CA(226)=	3.619726	CA(227)=	3.619726	CA(228)=	3.619726	CA(229)=	0.282000	CA(230)=	0.282000

TABLE C11 (continued)

CA(231)=	0.282000	CA(232)=	0.282000	CA(233)=	0.282000	CA(234)=	0.353774	CA(235)=	0.353774	CA(236)=	0.353774
CA(237)=	0.353774	CA(238)=	0.282000	CA(239)=	0.282000	CA(240)=	0.282000	CA(241)=	0.282000	CA(242)=	0.282000
CA(243)=	0.353774	CA(244)=	0.353774	CA(245)=	0.353774	CA(246)=	0.353774	CA(247)=	0.282000	CA(248)=	0.282000
CA(249)=	0.282000	CA(250)=	0.282000	CA(251)=	0.282000	CA(252)=	3.619726	CA(253)=	3.619726	CA(254)=	3.619726
CA(255)=	0.000000	CA(256)=	0.000000	CA(257)=	0.000000	CA(258)=	1.811000	CA(259)=	1.811000	CA(260)=	1.811000
CA(261)=	0.215200	CA(262)=	0.215200	CA(263)=	0.215200	CA(264)=	0.215200	CA(265)=	0.215200	CA(266)=	0.180000
CA(267)=	3.180000	CA(268)=	3.180000	CA(269)=	3.180000	CA(270)=	0.215200	CA(271)=	0.215200	CA(272)=	0.215200
CA(273)=	0.215200	CA(274)=	0.215200	CA(275)=	3.180000	CA(276)=	3.180000	CA(277)=	3.180000	CA(278)=	3.180000
CA(279)=	0.215200	CA(280)=	0.215200	CA(281)=	0.215200	CA(282)=	0.215200	CA(283)=	0.215200	CA(284)=	1.811000
CA(285)=	1.811000	CA(286)=	1.811000	CA(287)=	0.000000	CA(288)=	0.000000	CA(289)=	0.000000	CA(290)=	0.002253
CA(291)=	0.002253	CA(292)=	0.002253	CA(293)=	0.148405	CA(294)=	0.148405	CA(295)=	0.148405	CA(296)=	0.148405
CA(297)=	0.148405	CA(298)=	0.003955	CA(299)=	0.003955	CA(300)=	0.003955	CA(301)=	0.003955	CA(302)=	0.148405
CA(303)=	0.148405	CA(304)=	0.148405	CA(305)=	0.148405	CA(306)=	0.148405	CA(307)=	0.003955	CA(308)=	0.003955
CA(309)=	0.003955	CA(310)=	0.003955	CA(311)=	0.148405	CA(312)=	0.148405	CA(313)=	0.148405	CA(314)=	0.148405
CA(315)=	0.148405	CA(316)=	0.002253	CA(317)=	0.002253	CA(318)=	0.002253	CA(319)=	0.000000	CA(320)=	0.000000
CA(321)=	0.000000	CA(322)=	0.002253	CA(323)=	0.002253	CA(324)=	0.002253	CA(325)=	0.148405	CA(326)=	0.148405
CA(327)=	0.148405	CA(328)=	0.148405	CA(329)=	0.148405	CA(330)=	0.003955	CA(331)=	0.003955	CA(332)=	0.003955
CA(333)=	0.003955	CA(334)=	0.148405	CA(335)=	0.148405	CA(336)=	0.148405	CA(337)=	0.148405	CA(338)=	0.148405
CA(339)=	0.003955	CA(340)=	0.003955	CA(341)=	0.003955	CA(342)=	0.003955	CA(343)=	0.148405	CA(344)=	0.148405
CA(345)=	0.148405	CA(346)=	0.148405	CA(347)=	0.148405	CA(348)=	0.002253	CA(349)=	0.002253	CA(350)=	0.002253
CA(351)=	0.000000	CA(352)=	0.000000	CA(353)=	0.000000	CA(354)=	0.002253	CA(355)=	0.002253	CA(356)=	0.002253
CA(357)=	0.148405	CA(358)=	0.148405	CA(359)=	0.148405	CA(360)=	0.148405	CA(361)=	0.148405	CA(362)=	0.003955
CA(363)=	0.003955	CA(364)=	0.003955	CA(365)=	0.003955	CA(366)=	0.148405	CA(367)=	0.148405	CA(368)=	0.148405
CA(369)=	0.148405	CA(370)=	0.148405	CA(371)=	0.003955	CA(372)=	0.003955	CA(373)=	0.003955	CA(374)=	0.003955
CA(375)=	0.148405	CA(376)=	0.148405	CA(377)=	0.148405	CA(378)=	0.148405	CA(379)=	0.148405	CA(380)=	0.002253
CA(381)=	0.002253	CA(382)=	0.002253	CA(383)=	0.000000	CA(384)=	0.000000	CA(385)=	0.000000	CA(386)=	0.002253
CA(387)=	0.002253	CA(388)=	0.002253	CA(389)=	0.148405	CA(390)=	0.148405	CA(391)=	0.148405	CA(392)=	0.148405
CA(393)=	0.148405	CA(394)=	0.003955	CA(395)=	0.003955	CA(396)=	0.003955	CA(397)=	0.003955	CA(398)=	0.148405
CA(399)=	0.148405	CA(400)=	0.148405	CA(401)=	0.148405	CA(402)=	0.148405	CA(403)=	0.003955	CA(404)=	0.003955
CA(405)=	0.003955	CA(406)=	0.003955	CA(407)=	0.148405	CA(408)=	0.148405	CA(409)=	0.148405	CA(410)=	0.148405
CA(411)=	0.148405	CA(412)=	0.002253	CA(413)=	0.002253	CA(414)=	0.002253	CA(415)=	0.000000	CA(416)=	0.000000
CA(417)=	0.000000	CA(418)=	0.002253	CA(419)=	0.002253	CA(420)=	0.002253	CA(421)=	0.148405	CA(422)=	0.148405
CA(423)=	0.148405	CA(424)=	0.148405	CA(425)=	0.148405	CA(426)=	0.003955	CA(427)=	0.003955	CA(428)=	0.003955
CA(429)=	0.003955	CA(430)=	0.148405	CA(431)=	0.148405	CA(432)=	0.148405	CA(433)=	0.148405	CA(434)=	0.148405
CA(435)=	0.003955	CA(436)=	0.003955	CA(437)=	0.003955	CA(438)=	0.003955	CA(439)=	0.148405	CA(440)=	0.148405
CA(441)=	0.148405	CA(442)=	0.148405	CA(443)=	0.148405	CA(444)=	0.002253	CA(445)=	0.002253	CA(446)=	0.002253
CA(447)=	0.000000	CA(448)=	0.000000	CA(449)=	0.000000	CA(450)=	0.004500	CA(451)=	0.004500	CA(452)=	0.004500
CA(453)=	0.297000	CA(454)=	0.297000	CA(455)=	0.297000	CA(456)=	0.297000	CA(457)=	0.297000	CA(458)=	0.297000

TABLE C11 (continued)

CA(454)=	0.007918	CA(460)=	0.007918	CA(461)=	0.007918	CA(462)=	0.297000	CA(463)=	0.297000	CA(464)=	0.297000
CA(465)=	0.297000	CA(466)=	0.297000	CA(467)=	0.007918	CA(468)=	0.007918	CA(469)=	0.007918	CA(470)=	0.007918
CA(471)=	0.297000	CA(472)=	0.297000	CA(473)=	0.297000	CA(474)=	0.297000	CA(475)=	0.297000	CA(476)=	0.004500
CA(477)=	0.004500	CA(478)=	0.004500	CA(479)=	0.000000	CA(480)=	0.000000	CA(481)=	0.000000	CA(482)=	0.006765
CA(483)=	0.006765	CA(484)=	0.006765	CA(485)=	0.445567	CA(486)=	0.445567	CA(487)=	0.445567	CA(488)=	0.445567
CA(489)=	0.445567	CA(490)=	0.011875	CA(491)=	0.011875	CA(492)=	0.011875	CA(493)=	0.011875	CA(494)=	0.445567
CA(495)=	0.445567	CA(496)=	0.445567	CA(497)=	0.445567	CA(498)=	0.445567	CA(499)=	0.011875	CA(500)=	0.011875
CA(501)=	0.011875	CA(502)=	0.011875	CA(503)=	0.445567	CA(504)=	0.445567	CA(505)=	0.445567	CA(506)=	0.445567
CA(507)=	0.445567	CA(508)=	0.006765	CA(509)=	0.006765	CA(510)=	0.006765	CA(511)=	0.000000	CA(512)=	0.000000
CA(513)=	0.000000	CA(514)=	0.006765	CA(515)=	0.006765	CA(516)=	0.006765	CA(517)=	0.445567	CA(518)=	0.445567
CA(519)=	0.445567	CA(520)=	0.445567	CA(521)=	0.445567	CA(522)=	0.011875	CA(523)=	0.011875	CA(524)=	0.011875
CA(525)=	0.011875	CA(526)=	0.445567	CA(527)=	0.445567	CA(528)=	0.445567	CA(529)=	0.445567	CA(530)=	0.445567
CA(531)=	0.011875	CA(532)=	0.011875	CA(533)=	0.011875	CA(534)=	0.011875	CA(535)=	0.445567	CA(536)=	0.445567
CA(537)=	0.445567	CA(538)=	0.445567	CA(539)=	0.445567	CA(540)=	0.006765	CA(541)=	0.006765	CA(542)=	0.006765
CA(543)=	0.000000	CA(

CUC 1)=	0.000000	CUC 2)=	56491.609977	CUC 3)=	56491.609977	CUC 4)=	56491.609977	CUC 5)=	2867.470000	CUC 6)=	85.773545
CUC 7)=	85.773545	CUC 8)=	85.773545	CUC 9)=	85.773545	CUC 10)=	1652.040000	CUC 11)=	3218.309902	CUC 12)=	3218.309902
CUC 13)=	3218.309902	CUC 14)=	1652.040000	CUC 15)=	85.773545	CUC 16)=	85.773545	CUC 17)=	85.773545	CUC 18)=	85.773545
CUC 19)=	1652.040000	CUC 20)=	3218.309902	CUC 21)=	3218.309902	CUC 22)=	3218.309902	CUC 23)=	1652.040000	CUC 24)=	85.773545
CUC 25)=	85.773545	CUC 26)=	85.773545	CUC 27)=	85.773545	CUC 28)=	2867.470000	CUC 29)=	56491.609977	CUC 30)=	56491.609977
CUC 31)=	56491.609977	CUC 32)=	0.000000	CUC 33)=	0.000000	CUC 34)=	56491.609977	CUC 35)=	56491.609977	CUC 36)=	56491.609977
CUC 37)=	2867.470000	CUC 38)=	85.773545	CUC 39)=	85.773545	CUC 40)=	85.773545	CUC 41)=	85.773545	CUC 42)=	1652.040000
CUC 43)=	3218.309902	CUC 44)=	3218.309902	CUC 45)=	3218.309902	CUC 46)=	1652.040000	CUC 47)=	85.773545	CUC 48)=	85.773545
CUC 49)=	85.773545	CUC 50)=	85.773545	CUC 51)=	1652.040000	CUC 52)=	3218.309902	CUC 53)=	3218.309902	CUC 54)=	3218.309902
CUC 55)=	1652.040000	CUC 56)=	85.773545	CUC 57)=	85.773545	CUC 58)=	85.773545	CUC 59)=	85.773545	CUC 60)=	2867.470000
CUC 61)=	56491.609977	CUC 62)=	56491.609977	CUC 63)=	56491.609977	CUC 64)=	0.000000	CUC 65)=	0.000000	CUC 66)=	56491.609977
CUC 67)=	56491.609977	CUC 68)=	56491.609977	CUC 69)=	2867.470000	CUC 70)=	85.773545	CUC 71)=	85.773545	CUC 72)=	85.773545
CUC 73)=	85.773545	CUC 74)=	1652.040000	CUC 75)=	3218.309902	CUC 76)=	3218.309902	CUC 77)=	3218.309902	CUC 78)=	1652.040000
CUC 79)=	85.773545	CUC 80)=	85.773545	CUC 81)=	85.773545	CUC 82)=	85.773545	CUC 83)=	1652.040000	CUC 84)=	3218.309902
CUC 85)=	3218.309902	CUC 86)=	3218.309902	CUC 87)=	1652.040000	CUC 88)=	85.773545	CUC 89)=	85.773545	CUC 90)=	85.773545
CUC 91)=	85.773545	CUC 92)=	2867.470000	CUC 93)=	56491.609977	CUC 94)=	56491.609977	CUC 95)=	56491.609977	CUC 96)=	0.000000
CUC 97)=	0.000000	CUC 98)=	15701.344538	CUC 99)=	15701.344538	CUC(100)=	15701.344538	CUC(101)=	7850.810000	CUC(102)=	0.282000
CUC(103)=	0.282000	CUC(104)=	0.282000	CUC(105)=	0.282000	CUC(106)=	4472.650000	CUC(107)=	8945.008403	CUC(108)=	8945.008403
CUC(109)=	8945.008403	CUC(110)=	4472.650000	CUC(111)=	0.282000	CUC(112)=	0.282000	CUC(113)=	0.282000	CUC(114)=	0.282000
CUC(115)=	4472.650000	CUC(116)=	8945.008403	CUC(117)=	8945.008403	CUC(118)=	8945.008403	CUC(119)=	4472.650000	CUC(120)=	0.282000
CUC(121)=	0.282000	CUC(122)=	0.282000	CUC(123)=	0.282000	CUC(124)=	7850.810000	CUC(125)=	15701.344538	CUC(126)=	15701.344538
CUC(127)=	15701.344538	CUC(128)=	0.000000	CUC(129)=	0.000000	CUC(130)=	15701.344538	CUC(131)=	15701.344538	CUC(132)=	15701.344538

TABLE C11 (continued)

CU(133)= 7850.810000	CU(134)= 0.282000	CU(135)= 0.282000	CU(136)= 0.282000	CU(137)= 0.282000	CU(138)= 4472.650000
CU(139)= 8945.008403	CU(140)= 8945.008403	CU(141)= 8945.008403	CU(142)= 4472.650000	CU(143)= 0.282000	CU(144)= 0.282000
CU(145)= 0.282000	CU(146)= 0.282000	CU(147)= 4472.650000	CU(148)= 8945.008403	CU(149)= 8945.008403	CU(150)= 8945.008403
CU(151)= 4472.650000	CU(152)= 0.282000	CU(153)= 0.282000	CU(154)= 0.282000	CU(155)= 0.282000	CU(156)= 7850.810000
CU(157)=15701.344538	CU(158)=15701.344538	CU(159)=15701.344538	CU(160)= 0.000000	CU(161)= 0.000000	CU(162)=15701.344538
CU(163)=15701.344538	CU(164)=15701.344538	CU(165)= 7850.810000	CU(166)= 0.282000	CU(167)= 0.282000	CU(168)= 0.282000
CU(169)= 0.282000	CU(170)= 4472.650000	CU(171)= 8945.008403	CU(172)= 8945.008403	CU(173)= 8945.008403	CU(174)= 4472.650000
CU(175)= 0.282000	CU(176)= 0.282000	CU(177)= 0.282000	CU(178)= 0.282000	CU(179)= 4472.650000	CU(180)= 8945.008403
CU(181)= 8945.008403	CU(182)= 8945.008403	CU(183)= 4472.650000	CU(184)= 0.282000	CU(185)= 0.282000	CU(186)= 0.282000
CU(187)= 0.282000	CU(188)= 7850.810000	CU(189)=15701.344538	CU(190)=15701.344538	CU(191)=15701.344538	CU(192)= 0.000000
CU(193)= 0.000000	CU(194)=15701.344538	CU(195)=15701.344538	CU(196)=15701.344538	CU(197)= 7850.810000	CU(198)= 0.282000
CU(199)= 0.282000	CU(200)= 0.282000	CU(201)= 0.282000	CU(202)= 4472.650000	CU(203)= 8945.008403	CU(204)= 8945.008403
CU(205)= 8945.008403	CU(206)= 4472.650000	CU(207)= 0.282000	CU(208)= 0.282000	CU(209)= 0.282000	CU(210)= 0.282000
CU(211)= 4472.650000	CU(212)= 8945.008403	CU(213)= 8945.008403	CU(214)= 8945.008403	CU(215)= 4472.650000	CU(216)= 0.282000
CU(217)= 0.282000	CU(218)= 0.282000	CU(219)= 0.282000	CU(220)= 7850.810000	CU(221)=15701.344538	CU(222)=15701.344538
CU(223)=15701.344538	CU(224)= 0.000000	CU(225)= 0.000000	CU(226)=15701.344538	CU(227)=15701.344538	CU(228)=15701.344538
CU(229)= 7850.810000	CU(230)= 0.282000	CU(231)= 0.282000	CU(232)= 0.282000	CU(233)= 0.282000	CU(234)= 4472.650000
CU(235)= 8945.008403	CU(236)= 8945.008403	CU(237)= 8945.008403	CU(238)= 4472.650000	CU(239)= 0.282000	CU(240)= 0.282000
CU(241)= 0.282000	CU(242)= 0.282000	CU(243)= 4472.650000	CU(244)= 8945.008403	CU(245)= 8945.008403	CU(246)= 8945.008403
CU(247)= 4472.650000	CU(248)= 0.282000	CU(249)= 0.282000	CU(250)= 0.282000	CU(251)= 0.282000	CU(252)= 7850.810000
CU(253)=15701.344538	CU(254)=15701.344538	CU(255)=15701.344538	CU(256)= 0.000000	CU(257)= 0.000000	CU(258)= 12.376950
CU(259)= 12.376950	CU(260)= 12.376950	CU(261)= 6.282000	CU(262)= 0.187924	CU(263)= 0.187924	CU(264)= 0.187924
CU(265)= 0.187924	CU(266)= 3.620000	CU(267)= 7.051111	CU(268)= 7.051111	CU(269)= 7.051111	CU(270)= 3.620000
CU(271)= 0.187924	CU(272)= 0.187924	CU(273)= 0.187924	CU(274)= 0.187924	CU(275)= 3.620000	CU(276)= 7.051111
CU(277)= 7.051111	CU(278)= 7.051111	CU(279)= 3.620000	CU(280)= 0.187924	CU(281)= 0.187924	CU(282)= 0.187924
CU(283)= 0.187924	CU(284)= 6.282000	CU(285)= 12.376950	CU(286)= 12.376950	CU(287)= 12.376950	CU(288)= 6.282000
CU(289)= 0.000000	CU(290)= 12.376950	CU(291)= 12.376950	CU(292)= 12.376950	CU(293)= 6.282000	CU(294)= 0.187924
CU(295)= 0.187924	CU(296)= 0.187924	CU(297)= 0.187924	CU(298)= 3.620000	CU(299)= 7.051111	CU(300)= 7.051111
CU(301)= 7.051111	CU(302)= 3.620000	CU(303)= 0.187924	CU(304)= 0.187924	CU(305)= 0.187924	CU(306)= 0.187924
CU(307)= 3.620000	CU(308)= 7.051111	CU(309)= 7.051111	CU(310)= 7.051111	CU(311)= 3.620000	CU(312)= 0.187924
CU(313)= 0.187924	CU(314)= 0.187924	CU(315)= 0.187924	CU(316)= 6.282000	CU(317)= 12.376950	CU(318)= 12.376950
CU(319)= 12.376950	CU(320)= 0.000000	CU(321)= 0.000000	CU(322)= 12.376950	CU(323)= 12.376950	CU(324)= 12.376950
CU(325)= 6.282000	CU(326)= 0.187924	CU(327)= 0.187924	CU(328)= 0.187924	CU(329)= 0.187924	CU(330)= 3.620000
CU(331)= 7.051111	CU(332)= 7.051111	CU(333)= 7.051111	CU(334)= 3.620000	CU(335)= 0.187924	CU(336)= 0.187924
CU(337)= 0.187924	CU(338)= 0.187924	CU(339)= 3.620000	CU(340)= 7.051111	CU(341)= 7.051111	CU(342)= 7.051111
CU(343)= 3.620000	CU(344)= 0.187924	CU(345)= 0.187924	CU(346)= 0.187924	CU(347)= 0.187924	CU(348)= 6.282000
CU(349)= 12.376950	CU(350)= 12.376950	CU(351)= 12.376950	CU(352)= 0.000000	CU(353)= 0.000000	CU(354)= 12.376950
CU(355)= 12.376950	CU(356)= 12.376950	CU(357)= 6.282000	CU(358)= 0.187924	CU(359)= 0.187924	CU(360)= 0.187924
CU(361)= 0.187924	CU(362)= 3.620000	CU(363)= 7.051111	CU(364)= 7.051111	CU(365)= 7.051111	CU(366)= 3.620000

TABLE C11 (continued)

CU(167)=	0.187924	CU(366)=	0.187924	CU(369)=	0.187924	CU(370)=	0.187924	CU(371)=	3.620000	CU(372)=	7.051111
CU(373)=	7.051111	CU(374)=	7.051111	CU(375)=	3.620000	CU(376)=	0.187924	CU(377)=	0.187924	CU(378)=	0.187924
CU(379)=	0.187924	CU(380)=	8.282000	CU(381)=	12.376950	CU(382)=	12.376950	CU(383)=	12.376950	CU(384)=	0.000000
CU(385)=	0.000000	CU(386)=	12.376950	CU(387)=	12.376950	CU(388)=	12.376950	CU(389)=	8.282000	CU(390)=	0.187924
CU(391)=	0.187924	CU(392)=	0.187924	CU(393)=	0.187924	CU(394)=	3.620000	CU(395)=	7.051111	CU(396)=	7.051111
CU(397)=	7.051111	CU(398)=	3.620000	CU(399)=	0.187924	CU(400)=	0.187924	CU(401)=	0.187924	CU(402)=	0.187924
CU(403)=	3.620000	CU(404)=	7.051111	CU(405)=	7.051111	CU(406)=	7.051111	CU(407)=	3.620000	CU(408)=	0.187924
CU(409)=	0.187924	CU(410)=	0.187924	CU(411)=	0.187924	CU(412)=	8.282000	CU(413)=	12.376950	CU(414)=	12.376950
CU(415)=	12.376950	CU(416)=	0.000000	CU(417)=	0.000000	CU(418)=	12.376950	CU(419)=	12.376950	CU(420)=	12.376950
CU(421)=	8.282000	CU(422)=	0.187924	CU(423)=	0.187924	CU(424)=	0.187924	CU(425)=	0.187924	CU(426)=	3.620000
CU(427)=	7.051111	CU(428)=	7.051111	CU(429)=	7.051111	CU(430)=	3.620000	CU(431)=	0.187924	CU(432)=	0.187924
CU(433)=	0.187924	CU(434)=	0.187924	CU(435)=	3.620000	CU(436)=	7.051111	CU(437)=	7.051111	CU(438)=	7.051111
CU(439)=	3.620000	CU(440)=	0.187924	CU(441)=	0.187924	CU(442)=	0.187924	CU(443)=	0.187924	CU(444)=	8.282000
CU(445)=	12.376950	CU(446)=	12.376950	CU(447)=	12.376950	CU(448)=	0.000000	CU(449)=	0.000000	CU(450)=	4.122402
CU(451)=	4.122402	CU(452)=	4.122402	CU(453)=	2.092000	CU(454)=	0.062592	CU(455)=	0.062592	CU(456)=	0.062592
CU(457)=	0.062592	CU(458)=	1.206000	CU(459)=	2.348520	CU(460)=	2.348520	CU(461)=	2.348520	CU(462)=	1.206000
CU(463)=	0.062592	CU(464)=	0.062592	CU(465)=	0.062592	CU(466)=	0.062592	CU(467)=	1.206000	CU(468)=	2.348520
CU(469)=	2.348520	CU(470)=	2.348520	CU(471)=	1.206000	CU(472)=	0.062592	CU(473)=	0.062592	CU(474)=	0.062592
CU(475)=	0.062592	CU(476)=	2.092000	CU(477)=	4.122402	CU(478)=	4.122402	CU(479)=	4.122402	CU(480)=	0.000000
CU(481)=	0.000000	CU(482)=	4.122402	CU(483)=	4.122402	CU(484)=	4.122402	CU(485)=	2.092000	CU(486)=	0.062592
CU(487)=	0.062592	CU(488)=	0.062592	CU(489)=	0.062592	CU(490)=	1.206000	CU(491)=	2.348520	CU(492)=	2.348520
CU(493)=	2.348520	CU(494)=	1.206000	CU(495)=	0.062592	CU(496)=	0.062592	CU(497)=	0.062592	CU(498)=	0.062592
CU(499)=	1.206000	CU(500)=	2.348520	CU(501)=	2.348520	CU(502)=	2.348520	CU(503)=	1.206000	CU(504)=	0.062592
CU(505)=	0.062592	CU(506)=	0.062592	CU(507)=	0.062592	CU(508)=	2.092000	CU(509)=	4.122402	CU(510)=	4.122402
CU(511)=	4.122402	CU(512)=	0.000000	CU(513)=	0.000000	CU(514)=	4.122402	CU(515)=	4.122402	CU(516)=	4.122402
CU(517)=	2.092000	CU(518)=	0.062592	CU(519)=	0.062592	CU(520)=	0.062592	CU(521)=	0.062592	CU(522)=	1.206000
CU(523)=	2.348520	CU(524)=	2.348520	CU(525)=	2.348520	CU(526)=	1.206000	CU(527)=	0.062592	CU(528)=	0.062592
CU(529)=	0.062592	CU(530)=	0.062592	CU(531)=	1.206000	CU(532)=	2.348520	CU(533)=	2.348520	CU(534)=	2.348520
CU(535)=	1.206000	CU(536)=	0.062592	CU(537)=	0.062592	CU(538)=	0.062592	CU(539)=	0.062592	CU(540)=	2.092000
CU(541)=	4.122402	CU(542)=	4.122402	CU(543)=	4.122402	CU(544)=	0.000000				

C5 HEAT FLOWS OF SIMULATION RUN 16

Table C12 shows the heat flows between nodal points in watts for the surface temperature simulation run number 16.

Notation:

QA(I) - heat flow in X-direction from nodal point
'I' towards nodal point 'I + 1'

QU(I) - heat flow in Y-direction from nodal point
'I' towards nodal point 'I + M'

TABLE C12 -- Heat Flows

QA(33) =	0.0000	QU(2) =	1.7644
QA(34) =	0.0000	QU(3) =	1.7644
QA(35) =	0.0000	QU(4) =	1.7720
QA(36) =	0.0027	QU(5) =	0.8723
QA(37) =	0.0016	QU(6) =	0.0259
QA(38) =	0.0007	QU(7) =	0.0253
QA(39) =	0.0007	QU(8) =	0.0259
QA(40) =	0.0022	QU(9) =	0.0262
QA(41) =	0.0030	QU(10) =	0.5115
QA(42) =	0.0001	QU(11) =	1.0003
QA(43) =	0.0000	QU(12) =	1.0077
QA(44) =	0.0000	QU(13) =	1.0007
QA(45) =	0.0000	QU(14) =	0.5146
QA(46) =	0.0024	QU(15) =	0.0264
QA(47) =	0.0015	QU(16) =	0.0262
QA(48) =	0.0000	QU(17) =	0.0262
QA(49) =	0.0015	QU(18) =	0.0264
QA(50) =	0.0024	QU(19) =	0.5146
QA(51) =	0.0000	QU(20) =	1.0090
QA(52) =	0.0000	QU(21) =	1.0001
QA(53) =	0.0000	QU(22) =	1.0087
QA(54) =	0.0001	QU(23) =	0.5115
QA(55) =	0.0030	QU(24) =	0.0262
QA(56) =	0.0022	QU(25) =	0.0259
QA(57) =	0.0007	QU(26) =	0.0258
QA(58) =	0.0007	QU(27) =	0.0259
QA(59) =	0.0016	QU(28) =	0.8722
QA(60) =	0.0027	QU(29) =	1.7720
QA(61) =	0.0000	QU(30) =	1.7644
QA(62) =	0.0000	QU(31) =	1.7644
QA(63) =	0.0000	QU(32) =	0.0000
QA(64) =	0.0000	QU(33) =	1.7644
QA(65) =	0.0000	QU(34) =	1.7645
QA(66) =	0.0000	QU(35) =	1.7692
QA(67) =	0.0000	QU(36) =	0.8765
QA(68) =	0.0055	QU(37) =	0.0250
QA(69) =	0.0111	QU(38) =	0.0243
QA(70) =	0.0059	QU(39) =	0.0244
QA(71) =	0.0015	QU(40) =	0.0253
QA(72) =	0.0008	QU(41) =	0.5144
QA(73) =	0.0140	QU(42) =	1.0002
QA(74) =	0.0001	QU(43) =	1.0075
QA(75) =	0.0000	QU(44) =	1.0086
QA(76) =	0.0000	QU(45) =	0.5169
QA(77) =	0.0000	QU(46) =	0.0255
QA(78) =	0.0127	QU(47) =	0.0247
QA(79) =	0.0075	QU(48) =	0.0247
QA(80) =	0.0000	QU(49) =	0.0255
QA(81) =	0.0074	QU(50) =	0.5168
QA(82) =	0.0127	QU(51) =	1.0089
QA(83) =	0.0000	QU(52) =	

TABLE C12 (continued)

QA(84)=	=0.0000	QU(53)=	1.0079
QA(85)=	0.0000	QU(54)=	1.0086
QA(86)=	=0.0001	QU(55)=	0.5144
QA(87)=	=0.0140	QU(56)=	0.0253
QA(88)=	=0.0089	QU(57)=	0.0244
QA(89)=	=0.0015	QU(58)=	0.0243
QA(90)=	0.0059	QU(59)=	0.0250
QA(91)=	0.0111	QU(60)=	0.8764
QA(92)=	=0.0055	QU(61)=	1.7092
QA(93)=	=0.0000	QU(62)=	1.7645
QA(94)=	=0.0000	QU(63)=	1.7644
QA(95)=	=0.0000	QU(64)=	0.0000
QA(97)=	=0.0000	QU(66)=	1.7644
QA(98)=	0.0000	QU(67)=	1.7645
QA(99)=	0.0000	QU(68)=	1.7638
QA(100)=	0.0057	QU(69)=	0.8930
QA(101)=	=0.0324	QU(70)=	0.0190
QA(102)=	=0.0138	QU(71)=	0.0170
QA(103)=	0.0012	QU(72)=	0.0171
QA(104)=	0.0163	QU(73)=	0.0201
QA(105)=	0.0352	QU(74)=	0.5282
QA(106)=	=0.0000	QU(75)=	1.0082
QA(107)=	=0.0000	QU(76)=	1.0073
QA(108)=	0.0000	QU(77)=	1.0085
QA(109)=	0.0001	QU(78)=	0.5294
QA(110)=	=0.0343	QU(79)=	0.0203
QA(111)=	=0.0153	QU(80)=	0.0173
QA(112)=	=0.0000	QU(81)=	0.0173
QA(113)=	0.0153	QU(82)=	0.0203
QA(114)=	0.0343	QU(83)=	0.5294
QA(115)=	=0.0001	QU(84)=	1.0087
QA(116)=	=0.0000	QU(85)=	1.0077
QA(117)=	0.0000	QU(86)=	1.0085
QA(118)=	0.0000	QU(87)=	0.5283
QA(119)=	=0.0352	QU(88)=	0.0201
QA(120)=	=0.0163	QU(89)=	0.0171
QA(121)=	=0.0012	QU(90)=	0.0170
QA(122)=	0.0138	QU(91)=	0.0190

TABLE C12 (continued)

QA(123)=	0.0324	QU(92)=	0.8929
QA(124)=	0.0057	QU(93)=	1.7037
QA(125)=	0.0000	QU(94)=	1.7645
QA(126)=	0.0000	QU(95)=	1.7644
QA(127)=	0.0000	QU(96)=	0.0000
QA(129)=	0.0000	QU(98)=	1.7644
QA(130)=	0.0000	QU(99)=	1.7645
QA(131)=	0.0000	QU(100)=	1.7781
QA(132)=	0.0030	QU(101)=	0.9307
QA(133)=	0.0012	QU(102)=	0.0012
QA(134)=	0.0007	QU(103)=	0.0019
QA(135)=	0.0000	QU(104)=	0.0019
QA(136)=	0.0007	QU(105)=	0.0012
QA(137)=	0.0012	QU(106)=	0.5632
QA(138)=	0.0001	QU(107)=	1.0076
QA(139)=	0.0000	QU(108)=	1.0067
QA(140)=	0.0000	QU(109)=	1.0076
QA(141)=	0.0001	QU(110)=	0.5635
QA(142)=	0.0012	QU(111)=	0.0012
QA(143)=	0.0007	QU(112)=	0.0020
QA(144)=	0.0000	QU(113)=	0.0020
QA(145)=	0.0007	QU(114)=	0.0012
QA(146)=	0.0012	QU(115)=	0.5635
QA(147)=	0.0001	QU(116)=	1.0080
QA(148)=	0.0000	QU(117)=	1.0070
QA(149)=	0.0000	QU(118)=	1.0079
QA(150)=	0.0001	QU(119)=	0.5632
QA(151)=	0.0012	QU(120)=	0.0012
QA(152)=	0.0007	QU(121)=	0.0019
QA(153)=	0.0000	QU(122)=	0.0019
QA(154)=	0.0007	QU(123)=	0.0012
QA(155)=	0.0012	QU(124)=	0.9307
QA(156)=	0.0030	QU(125)=	1.7781
QA(157)=	0.0000	QU(126)=	1.7645
QA(158)=	0.0000	QU(127)=	1.7644
QA(159)=	0.0000	QU(128)=	0.0000
QA(161)=	0.0000	QU(130)=	1.7644
QA(162)=	0.0000	QU(131)=	1.7645
QA(163)=	0.0000	QU(132)=	1.7751

TABLE C12 (continued)

QA(164)=	0.0030	QU(133)=	0.9323
QA(165)=	0.0028	QU(134)=	0.0017
QA(166)=	0.0017	QU(135)=	0.0027
QA(167)=	0.0000	QU(136)=	0.0027
QA(168)=	-0.0017	QU(137)=	0.0017
QA(169)=	-0.0028	QU(138)=	0.5619
QA(170)=	-0.0002	QU(139)=	1.0071
QA(171)=	-0.0000	QU(140)=	1.0062
QA(172)=	0.0000	QU(141)=	1.0072
QA(173)=	0.0002	QU(142)=	0.5623
QA(174)=	0.0028	QU(143)=	0.0017
QA(175)=	0.0017	QU(144)=	0.0027
QA(176)=	-0.0000	QU(145)=	0.0027
QA(177)=	-0.0017	QU(146)=	0.0017
QA(178)=	-0.0028	QU(147)=	0.5623
QA(179)=	-0.0002	QU(148)=	1.0074
QA(180)=	-0.0000	QU(149)=	1.0064
QA(181)=	0.0000	QU(150)=	1.0073
QA(182)=	0.0002	QU(151)=	0.5620
QA(183)=	0.0028	QU(152)=	0.0017
QA(184)=	0.0017	QU(153)=	0.0027
QA(185)=	-0.0000	QU(154)=	0.0027
QA(186)=	-0.0017	QU(155)=	0.0017
QA(187)=	-0.0028	QU(156)=	0.9323
QA(188)=	-0.0030	QU(157)=	1.7751
QA(189)=	-0.0000	QU(158)=	1.7645
QA(190)=	-0.0000	QU(159)=	1.7644
QA(191)=	0.0000	QU(160)=	0.0000
QA(193)=	-0.0000	QU(162)=	1.7644
QA(194)=	0.0000	QU(163)=	1.7644
QA(195)=	0.0000	QU(164)=	1.7721
QA(196)=	0.0031	QU(165)=	0.9323
QA(197)=	0.0056	QU(166)=	0.0028
QA(198)=	0.0032	QU(167)=	0.0043
QA(199)=	0.0000	QU(168)=	0.0043
QA(200)=	-0.0032	QU(169)=	0.0028
QA(201)=	-0.0056	QU(170)=	0.5591
QA(202)=	-0.0003	QU(171)=	1.0064

TABLE C12 (continued)

QA(203)=	-0.0000	QU(172)=	1.0057
QA(204)=	0.0000	QU(173)=	1.0065
QA(205)=	0.0003	QU(174)=	0.5594
QA(206)=	0.0056	QU(175)=	0.0028
QA(207)=	0.0032	QU(176)=	0.0043
QA(208)=	-0.0000	QU(177)=	0.0043
QA(209)=	-0.0032	QU(178)=	0.0028
QA(210)=	-0.0056	QU(179)=	0.5594
QA(211)=	-0.0003	QU(180)=	1.0066
QA(212)=	-0.0000	QU(181)=	1.0058
QA(213)=	0.0000	QU(182)=	1.0065
QA(214)=	0.0003	QU(183)=	0.5592
QA(215)=	0.0056	QU(184)=	0.0028
QA(216)=	0.0032	QU(185)=	0.0043
QA(217)=	-0.0000	QU(186)=	0.0043
QA(218)=	-0.0032	QU(187)=	0.0028
QA(219)=	-0.0056	QU(188)=	0.9322
QA(220)=	-0.0031	QU(189)=	1.7721
QA(221)=	-0.0000	QU(190)=	1.7644
QA(222)=	-0.0000	QU(191)=	1.7644
QA(223)=	0.0000	QU(192)=	0.0000
QA(225)=	-0.0000	QU(194)=	1.7644
QA(226)=	0.0000	QU(195)=	1.7644
QA(227)=	0.0000	QU(196)=	1.7691
QA(228)=	0.0031	QU(197)=	0.9295
QA(229)=	0.0108	QU(198)=	0.0052
QA(230)=	0.0055	QU(199)=	0.0075
QA(231)=	0.0000	QU(200)=	0.0075
QA(232)=	-0.0055	QU(201)=	0.0052
QA(233)=	-0.0108	QU(202)=	0.5536
QA(234)=	-0.0003	QU(203)=	1.0057
QA(235)=	-0.0000	QU(204)=	1.0051
QA(236)=	0.0000	QU(205)=	1.0058
QA(237)=	0.0003	QU(206)=	0.5539
QA(238)=	0.0108	QU(207)=	0.0052
QA(239)=	0.0055	QU(208)=	0.0075
QA(240)=	-0.0000	QU(209)=	0.0075
QA(241)=	-0.0055	QU(210)=	0.0052
QA(242)=	-0.0108	QU(211)=	0.5539

TABLE C12 (continued)

QA(243)=	0.0003	QU(212)=	1.0058
QA(244)=	0.0000	QU(213)=	1.0052
QA(245)=	0.0000	QU(214)=	1.0057
QA(246)=	0.0003	QU(215)=	0.5536
QA(247)=	0.0108	QU(216)=	0.0052
QA(248)=	0.0055	QU(217)=	0.0075
QA(249)=	0.0000	QU(218)=	0.0075
QA(250)=	0.0055	QU(219)=	0.0052
QA(251)=	0.0108	QU(220)=	0.9295
QA(252)=	0.0031	QU(221)=	1.7690
QA(253)=	0.0000	QU(222)=	1.7644
QA(254)=	0.0000	QU(223)=	1.7644
QA(255)=	0.0000	QU(224)=	0.0000
QA(257)=	0.0000	QU(226)=	1.7644
QA(258)=	0.0000	QU(227)=	1.7644
QA(259)=	0.0000	QU(228)=	1.7660
QA(260)=	0.0015	QU(229)=	0.9215
QA(261)=	0.0162	QU(230)=	0.0105
QA(262)=	0.0061	QU(231)=	0.0130
QA(263)=	0.0000	QU(232)=	0.0130
QA(264)=	0.0061	QU(233)=	0.0105
QA(265)=	0.0163	QU(234)=	0.5430
QA(266)=	0.0002	QU(235)=	1.0049
QA(267)=	0.0000	QU(236)=	1.0046
QA(268)=	0.0000	QU(237)=	1.0049
QA(269)=	0.0002	QU(238)=	0.5432
QA(270)=	0.0163	QU(239)=	0.0105
QA(271)=	0.0061	QU(240)=	0.0131
QA(272)=	0.0000	QU(241)=	0.0131
QA(273)=	0.0061	QU(242)=	0.0105
QA(274)=	0.0163	QU(243)=	0.5432
QA(275)=	0.0002	QU(244)=	1.0049
QA(276)=	0.0000	QU(245)=	1.0046
QA(277)=	0.0000	QU(246)=	1.0049
QA(278)=	0.0002	QU(247)=	0.5430
QA(279)=	0.0163	QU(248)=	0.0105
QA(280)=	0.0061	QU(249)=	0.0130
QA(281)=	0.0000	QU(250)=	0.0130

TABLE C12 (continued)

QA(282)=	0.0061	QU(251)=	0.0105
QA(283)=	0.0162	QU(252)=	0.9215
QA(284)=	0.0015	QU(253)=	1.7660
QA(285)=	0.0000	QU(254)=	1.7644
QA(286)=	0.0000	QU(255)=	1.7644
QA(287)=	0.0000	QU(256)=	0.0000
QA(289)=	0.0000	QU(258)=	1.7644
QA(290)=	0.0000	QU(259)=	1.7644
QA(291)=	0.0000	QU(260)=	1.7644
QA(292)=	0.0000	QU(261)=	0.9069
QA(293)=	0.0060	QU(262)=	0.0206
QA(294)=	0.0031	QU(263)=	0.0191
QA(295)=	0.0000	QU(264)=	0.0191
QA(296)=	0.0030	QU(265)=	0.0207
QA(297)=	0.0059	QU(266)=	0.5270
QA(298)=	0.0000	QU(267)=	1.0049
QA(299)=	0.0000	QU(268)=	1.0048
QA(300)=	0.0000	QU(269)=	1.0049
QA(301)=	0.0000	QU(270)=	0.5272
QA(302)=	0.0060	QU(271)=	0.0207
QA(303)=	0.0030	QU(272)=	0.0192
QA(304)=	0.0000	QU(273)=	0.0192
QA(305)=	0.0030	QU(274)=	0.0207
QA(306)=	0.0060	QU(275)=	0.5272
QA(307)=	0.0000	QU(276)=	1.0049
QA(308)=	0.0000	QU(277)=	1.0048
QA(309)=	0.0000	QU(278)=	1.0049
QA(310)=	0.0000	QU(279)=	0.5270
QA(311)=	0.0059	QU(280)=	0.0207
QA(312)=	0.0030	QU(281)=	0.0191
QA(313)=	0.0000	QU(282)=	0.0191
QA(314)=	0.0031	QU(283)=	0.0206
QA(315)=	0.0060	QU(284)=	0.9069
QA(316)=	0.0000	QU(285)=	1.7644
QA(317)=	0.0000	QU(286)=	1.7644
QA(318)=	0.0000	QU(287)=	1.7644
QA(319)=	0.0000	QU(288)=	0.0000
QA(321)=	0.0000	QU(290)=	1.7644

TABLE C12 (continued)

QA(323)=	0.0000	QU(292)=	1.7644
QA(324)=	0.0000	QU(293)=	0.9009
QA(325)=	0.0034	QU(294)=	0.0236
QA(326)=	0.0019	QU(295)=	0.0222
QA(327)=	0.0000	QU(296)=	0.0222
QA(328)=	-0.0018	QU(297)=	0.0236
QA(329)=	-0.0032	QU(298)=	0.5211
QA(330)=	-0.0000	QU(299)=	1.0049
QA(331)=	-0.0000	QU(300)=	1.0048
QA(332)=	0.0000	QU(301)=	1.0049
QA(333)=	0.0000	QU(302)=	0.5213
QA(334)=	0.0033	QU(303)=	0.0237
QA(335)=	0.0019	QU(304)=	0.0222
QA(336)=	-0.0000	QU(305)=	0.0222
QA(337)=	-0.0019	QU(306)=	0.0237
QA(338)=	-0.0033	QU(307)=	0.5213
QA(339)=	-0.0000	QU(308)=	1.0049
QA(340)=	-0.0000	QU(309)=	1.0048
QA(341)=	0.0000	QU(310)=	1.0049
QA(342)=	0.0000	QU(311)=	0.5211
QA(343)=	0.0032	QU(312)=	0.0236
QA(344)=	0.0018	QU(313)=	0.0222
QA(345)=	-0.0000	QU(314)=	0.0222
QA(346)=	-0.0019	QU(315)=	0.0236
QA(347)=	-0.0034	QU(316)=	0.9009
QA(348)=	-0.0000	QU(317)=	1.7644
QA(349)=	-0.0000	QU(318)=	1.7644
QA(350)=	-0.0000	QU(319)=	1.7644
QA(351)=	0.0000	QU(320)=	0.0000
QA(353)=	-0.0000	QU(322)=	1.7644
QA(354)=	0.0000	QU(323)=	1.7644
QA(355)=	0.0000	QU(324)=	1.7644
QA(356)=	0.0000	QU(325)=	0.8975
QA(357)=	0.0019	QU(326)=	0.0250
QA(358)=	0.0012	QU(327)=	0.0240
QA(359)=	0.0001	QU(328)=	0.0241
QA(360)=	-0.0011	QU(329)=	0.0250
QA(361)=	-0.0018	QU(330)=	0.5178

TABLE C1.2 (continued)

QA(362)=	~0.0000	QU(331)=	1.0049
QA(363)=	~0.0000	QU(332)=	1.0048
QA(364)=	0.0000	QU(333)=	1.0049
QA(365)=	0.0000	QU(334)=	0.5180
QA(366)=	0.0018	QU(335)=	0.0251
QA(367)=	0.0011	QU(336)=	0.0241
QA(368)=	~0.0000	QU(337)=	0.0241
QA(369)=	~0.0011	QU(338)=	0.0251
QA(370)=	~0.0018	QU(339)=	0.5180
QA(371)=	~0.0000	QU(340)=	1.0049
QA(372)=	~0.0000	QU(341)=	1.0048
QA(373)=	0.0000	QU(342)=	1.0049
QA(374)=	0.0000	QU(343)=	0.5178
QA(375)=	0.0018	QU(344)=	0.0250
QA(376)=	0.0011	QU(345)=	0.0241
QA(377)=	~0.0001	QU(346)=	0.0240
QA(378)=	~0.0012	QU(347)=	0.0250
QA(379)=	~0.0019	QU(348)=	0.8975
QA(380)=	~0.0000	QU(349)=	1.7644
QA(381)=	~0.0000	QU(350)=	1.7644
QA(382)=	~0.0000	QU(351)=	1.7644
QA(383)=	0.0000	QU(352)=	0.0000
QA(385)=	~0.0000	QU(354)=	1.7644
QA(386)=	0.0000	QU(355)=	1.7644
QA(387)=	0.0000	QU(356)=	1.7644
QA(388)=	0.0000	QU(357)=	0.8956
QA(389)=	0.0011	QU(358)=	0.0250
QA(390)=	0.0007	QU(359)=	0.0252
QA(391)=	0.0001	QU(360)=	0.0252
QA(392)=	~0.0006	QU(361)=	0.0258
QA(393)=	~0.0010	QU(362)=	0.5161
QA(394)=	~0.0000	QU(363)=	1.0048
QA(395)=	~0.0000	QU(364)=	1.0048
QA(396)=	0.0000	QU(365)=	1.0048
QA(397)=	0.0000	QU(366)=	0.5162
QA(398)=	0.0010	QU(367)=	0.0258
QA(399)=	0.0006	QU(368)=	0.0252
QA(400)=	~0.0000	QU(369)=	0.0252

TABLE C12 (continued)

QA(402)=	0.0010	QU(371)=	0.5162
QA(403)=	0.0000	QU(372)=	1.0048
QA(404)=	0.0000	QU(373)=	1.0048
QA(405)=	0.0000	QU(374)=	1.0048
QA(406)=	0.0000	QU(375)=	0.5161
QA(407)=	0.0010	QU(376)=	0.0258
QA(408)=	0.0006	QU(377)=	0.0252
QA(409)=	0.0001	QU(378)=	0.0252
QA(410)=	0.0007	QU(379)=	0.0258
QA(411)=	0.0011	QU(380)=	0.0956
QA(412)=	0.0000	QU(381)=	1.7644
QA(413)=	0.0000	QU(382)=	1.7644
QA(414)=	0.0000	QU(383)=	1.7644
QA(415)=	0.0000	QU(384)=	0.0000
QA(417)=	0.0000	QU(385)=	1.7644
QA(418)=	0.0000	QU(387)=	1.7644
QA(419)=	0.0000	QU(388)=	1.7644
QA(420)=	0.0000	QU(389)=	0.8945
QA(421)=	0.0006	QU(390)=	0.0262
QA(422)=	0.0004	QU(391)=	0.0258
QA(423)=	0.0001	QU(392)=	0.0258
QA(424)=	0.0003	QU(393)=	0.0262
QA(425)=	0.0005	QU(394)=	0.5151
QA(426)=	0.0000	QU(395)=	1.0048
QA(427)=	0.0000	QU(396)=	1.0048
QA(428)=	0.0000	QU(397)=	1.0048
QA(429)=	0.0000	QU(398)=	0.5152
QA(430)=	0.0006	QU(399)=	0.0262
QA(431)=	0.0004	QU(400)=	0.0258
QA(432)=	0.0000	QU(401)=	0.0258
QA(433)=	0.0004	QU(402)=	0.0262
QA(434)=	0.0006	QU(403)=	0.5152
QA(435)=	0.0000	QU(404)=	1.0048
QA(436)=	0.0000	QU(405)=	1.0048
QA(437)=	0.0000	QU(406)=	1.0048
QA(438)=	0.0000	QU(407)=	0.5151
QA(439)=	0.0005	QU(408)=	0.0262
QA(440)=	0.0003	QU(409)=	0.0258

TABLE C12 (continued)

QA(441)=	0.0001	QU(410)=	0.0250
QA(442)=	0.0004	QU(411)=	0.0262
QA(443)=	0.0006	QU(412)=	0.0245
QA(444)=	0.0000	QU(413)=	1.7644
QA(445)=	0.0000	QU(414)=	1.7644
QA(446)=	0.0000	QU(415)=	1.7644
QA(447)=	0.0000	QU(416)=	0.0000
QA(449)=	0.0000	QU(418)=	1.7644
QA(450)=	0.0000	QU(419)=	1.7644
QA(451)=	0.0000	QU(420)=	1.7644
QA(452)=	0.0000	QU(421)=	0.8939
QA(453)=	0.0007	QU(422)=	0.0264
QA(454)=	0.0005	QU(423)=	0.0262
QA(455)=	0.0001	QU(424)=	0.0262
QA(456)=	0.0003	QU(425)=	0.0264
QA(457)=	0.0005	QU(426)=	0.5146
QA(458)=	0.0000	QU(427)=	1.0048
QA(459)=	0.0000	QU(428)=	1.0048
QA(460)=	0.0000	QU(429)=	1.0048
QA(461)=	0.0000	QU(430)=	0.5147
QA(462)=	0.0006	QU(431)=	0.0264
QA(463)=	0.0004	QU(432)=	0.0262
QA(464)=	0.0000	QU(433)=	0.0262
QA(465)=	0.0004	QU(434)=	0.0264
QA(466)=	0.0006	QU(435)=	0.5147
QA(467)=	0.0000	QU(436)=	1.0048
QA(468)=	0.0000	QU(437)=	1.0048
QA(469)=	0.0000	QU(438)=	1.0048
QA(470)=	0.0000	QU(439)=	0.5146
QA(471)=	0.0005	QU(440)=	0.0264
QA(472)=	0.0003	QU(441)=	0.0262
QA(473)=	0.0001	QU(442)=	0.0262
QA(474)=	0.0005	QU(443)=	0.0264
QA(475)=	0.0007	QU(444)=	0.8939
QA(476)=	0.0000	QU(445)=	1.7644
QA(477)=	0.0000	QU(446)=	1.7644
QA(478)=	0.0000	QU(447)=	1.7644
QA(479)=	0.0000	QU(448)=	0.0000
QA(481)=	0.0000	QU(450)=	1.7644

TABLE C12 (continued)

QA(482)E	0.0000	QU(451)E	1.7644
QA(483)E	0.0000	QU(452)E	1.7644
QA(484)E	0.0000	QU(453)E	0.8932
QA(485)E	0.0003	QU(454)E	0.0266
QA(486)E	0.0002	QU(455)E	0.0265
QA(487)E	0.0001	QU(456)E	0.0265
QA(488)E	0.0000	QU(457)E	0.0266
QA(489)E	0.0001	QU(458)E	0.5141
QA(490)E	0.0000	QU(459)E	1.0048
QA(491)E	0.0000	QU(460)E	1.0048
QA(492)E	0.0000	QU(461)E	1.0048
QA(493)E	0.0000	QU(462)E	0.5141
QA(494)E	0.0002	QU(463)E	0.0266
QA(495)E	0.0001	QU(464)E	0.0265
QA(496)E	0.0000	QU(465)E	0.0265
QA(497)E	0.0001	QU(466)E	0.0266
QA(498)E	0.0002	QU(467)E	0.5141
QA(499)E	0.0000	QU(468)E	1.0048
QA(500)E	0.0000	QU(469)E	1.0048
QA(501)E	0.0000	QU(470)E	1.0048
QA(502)E	0.0000	QU(471)E	0.5141
QA(503)E	0.0001	QU(472)E	0.0266
QA(504)E	0.0000	QU(473)E	0.0265
QA(505)E	0.0001	QU(474)E	0.0265
QA(506)E	0.0002	QU(475)E	0.0266
QA(507)E	0.0003	QU(476)E	0.8932
QA(508)E	0.0000	QU(477)E	1.7644
QA(509)E	0.0000	QU(478)E	1.7644
QA(510)E	0.0000	QU(479)E	1.7644
QA(511)E	0.0000	QU(480)E	0.0000
QA(513)E	0.0000	QU(482)E	1.7644
QA(514)E	0.0000	QU(483)E	1.7644
QA(515)E	0.0000	QU(484)E	1.7644
QA(516)E	0.0000	QU(485)E	0.8929
QA(517)E	0.0001	QU(486)E	0.0267
QA(518)E	0.0001	QU(487)E	0.0267
QA(519)E	0.0000	QU(488)E	0.0267
QA(520)E	0.0000	QU(489)E	0.0267

TABLE C12 (continued)

QA(521)=	0.0000	QU(490)=	0.5141
QA(522)=	0.0000	QU(491)=	1.0047
QA(523)=	0.0000	QU(492)=	1.0048
QA(524)=	0.0000	QU(493)=	1.0047
QA(525)=	0.0000	QU(494)=	0.5140
QA(526)=	0.0000	QU(495)=	0.0267
QA(527)=	0.0000	QU(496)=	0.0266
QA(528)=	0.0000	QU(497)=	0.0266
QA(529)=	0.0000	QU(498)=	0.0267
QA(530)=	0.0000	QU(499)=	0.5140
QA(531)=	0.0000	QU(500)=	1.0047
QA(532)=	0.0000	QU(501)=	1.0048
QA(533)=	0.0000	QU(502)=	1.0047
QA(534)=	0.0000	QU(503)=	0.5141
QA(535)=	0.0000	QU(504)=	0.0267
QA(536)=	0.0000	QU(505)=	0.0267
QA(537)=	0.0000	QU(506)=	0.0267
QA(538)=	0.0001	QU(507)=	0.0267
QA(539)=	0.0001	QU(508)=	0.8929
QA(540)=	0.0000	QU(509)=	1.7644
QA(541)=	0.0000	QU(510)=	1.7644
QA(542)=	0.0000	QU(511)=	1.7644
QA(543)=	0.0000	QU(512)=	0.0000
QU(514)=	1.7644		
QU(515)=	1.7644		
QU(516)=	1.7644	QU(530)=	0.0267
QU(517)=	0.8929	QU(531)=	0.5139
QU(518)=	0.0267	QU(532)=	1.0047
QU(519)=	0.0267	QU(533)=	1.0048
QU(520)=	0.0267	QU(534)=	1.0047
QU(521)=	0.0267	QU(535)=	0.5141
QU(522)=	0.5141	QU(536)=	0.0267
QU(523)=	1.0047	QU(537)=	0.0267
QU(524)=	1.0048	QU(538)=	0.0267
QU(525)=	1.0047	QU(539)=	0.0267
QU(526)=	0.5139	QU(540)=	0.8929
QU(527)=	0.0267	QU(541)=	1.7644
QU(528)=	0.0267	QU(542)=	1.7644
QU(529)=	0.0267	QU(543)=	1.7644

C6 COMPUTER LISTING

Table C13 shows the basic computer listing of the program used in the surface temperature simulations.

Subroutine conduc was altered for each simulation run - due to the different grid sizes and hence conductances used. For the interested readers, the conductances were evaluated using two different algorithms: (a) as outlined at the start of the program, that is, reading in numerous data cards and/or (b) reading in a few data cards and equating the equal conductances as shown in subroutine conduc.

TABLE C13

Computer Listing Of Surface Temperature Simulation Program

B6700/B7700 F D R I R A N C O M P I L A T I O N M A R K 2.7.300

DIMENSION CA(576),CU(576),QA(576),QU(576),T(576),RES(576)
 DIMENSION TT(576)

RELAXATION OF A RECTANGULAR GRID OF POINTS IN TWO
 DIMENSIONS CONSIDERING ONLY CONVECTIVE AND CONDUCTIVE HEAT
 TRANSFER

IF CONVECTIVE HEAT TRANSFER IS BEING CONSIDERED, THEN
 H=CONVECTIVE HEAT TRANSFER COEFFICIENT
 A=SURFACE AREA OF HEAT TRANSFER
 D=1

IF CONDUCTIVE HEAT TRANSFER IS BEING CONSIDERED, THEN
 K=THE THERMAL CONDUCTIVITY
 A=CROSS-SECTIONAL AREA OF HEAT TRANSFER
 D=LENGTH OVER WHICH HEAT IS BEING TRANSFERRED

CONDUCTANCE=C=H*A/D IN WATTS PER DEGREE KELVIN

ARRANGING THE DATA CARDS
 THE FIRST CARD HAS THE VALUES OF M AND N ON IT.

THE NEXT SET OF CARDS HAS THE CONDUCTANCE VALUES
 AT THE END OF THE CONDUCTANCE CARDS, PUT IN A DUMMY CARD
 IN THE SAME FORMAT AS THE OTHER CONDUCTANCE CARDS

THE GUESSED TEMPERATURES CONSTITUTE THE NEXT SET OF
 DATA CARDS PARTICULAR ATTENTION TO BOUNDARY CONDITIONS MUST BE
 PAID

CONSIDER FOR EXAMPLE THE NETWORK SHOWN BELOW
 WITH N=4 AND M=6

```

T19*****T20*****T21*****T22*****T23*****T24
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
T13*****T14*****T15*****T16*****T17*****T18
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
T7*****T8*****T9*****T10*****T11*****T12
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
*          *          *          *          *          *
T1*****T2*****T3*****T4*****T5*****T6

```

THE CONDUCTANCES ARE READ IN, IN THE FOLLOWING ORDER
 CA(1),CU(2),CA(8),CU(3),CA(9),ETC,ETC,CA(10),CU(5),AND CA(11)
 THE NEXT LINE BEING CA(13),CU(8),CA(14),CU(9)ETC.
 HAVING READ IN CA(24),THEN READ IN, THE UPPER BOUNDARY CONDITIONS

TABLE C13 (continued)

```

C      NAMELY, CU(20), CU(21), CU(22), CU(23)
C
C      THE GUESSED TEMPERATURES BEING READ IN ACCORDING
C      TO THE FORMAT OF STATEMENT 41, FROM T1 UP TO T30
C      NR=NUMBER OF ROW BEING COMPUTED
C      K=TEMPERATURE COUNTER
C
C      M=NUMBER OF GRID POINTS IN THE X DIRECTION
C      N=NUMBER OF GRID POINTS IN THE Y DIRECTION
C
C      READ(5,19)M,N
19  FORMAT(2I3)
    M1=(N+1)*M
    WRITE(6,42)M,N
42  FORMAT(/,11X,'M=',I3,10X,'N=',I3)
    EVALUATION OF CONDUCTANCES
    CA=CONDUCTANCE ACROSS THE GRID IN X-DIRECTION
    CU=CONDUCTANCE UP IN THE GRID IN Y-DIRECTION
    WRITE(6,34)
34  FORMAT(/,11X,'THE CONDUCTANCES IN WATTS PER DEGREE KELVIN ARE')
    CALL CONDOC(CA,CU)
    WRITE(6,48)
48  FORMAT(/,11X,'THE GUESSED TEMPERATURES FOR THE POINTS ARE')
    READ(5,41)(T(I),I=1,MN1)
    WRITE(6,47)(T(I),I=1,MN1)
47  FORMAT(/,1X,8(2X,'T(',I3,'): ',F6,2)))
    EVALUATING THE TEMP. AND GRID POINTS
    CALL RELAXT(CA,CU,RES,M,N)
41  FORMAT(16F5,2)
    EVALUATING THE HEAT FLOW BETWEEN GRID POINTS
    WRITE(6,36)
36  FORMAT(/,11X,'THE HEAT FLUX PROFILE IS!')
    CALL HEATFL(T,CA,CU,QA,QU,M,N)
    CONTINUE
    STOP
    END

```

TABLE C13 (continued)

```

SUBROUTINE CONDOC(CA, CU)
DIMENSION CA(576), CU(576)
C   SETTING BOUNDARY CONDITIONS FOR ZERO HEAT FLUX
C   READ(5,11)H,A,D
11  FORMAT(3F12,7)
    CA(33)=H*A/D
    CA(63)=CA(33)
    DO 121=33,461,32
    CA(1+32)=CA(1)
12  CA(1+62)=CA(1)

C   EVALUATING BOUNDARY CONDITIONS BETWEEN VARIOUS REGIONS
C   C   READING CONDUCTANCES BTWN REGIONS A+B AND ALSO B+C
C   READ(5,13)HAB,AAB,DAB,HBC,ABC,DBC
13  FORMAT(6F12,7)
    CU(5)=HAB*AAB/DAB
    CU(28)=CU(5)
    CU(10)=HBC*ABC/DBC
    CU(14)=CU(10)
    CU(19)=CU(10)
    CU(23)=CU(10)
    DO 141=5,37,32
    CU(1+32)=CU(1)
14  CU(1+55)=CU(1)
    DO 151=10,42,32
    CU(1+32)=CU(1)
    CU(1+36)=CU(1)
    CU(1+41)=CU(1)
15  CU(1+45)=CU(1)
C   READING CONDUCTANCES BTWN REGIONS A+I AND ALSO B+E
C   READ(5,13)HAI,AAI,DAI,HBE,ABE,DBE
    CA(98)=HAI*AAI/DAI
    CA(126)=CA(98)
    CA(101)=HBE*ABE/DBE
    CA(114)=CA(101)
    CA(123)=CA(101)
    DO 161=98,99,1
    CA(1+1)=CA(1)
16  CA(1+26)=CA(1)
    DO 171=101,104
    CA(1+1)=CA(1)
    CA(1+9)=CA(1)
17  CA(1+10)=CA(1)
C   READING CONDUCTANCES BTWN REGIONS C+D AND ALSO I+E
C   READ(5,13)HCD,ACD,DCD,HIE,AIE,DIE
    CA(106)=HCD*ACD/DCD
    CA(118)=CA(106)
    DO 181=106,108,1
    CA(1+1)=CA(1)
18  CA(1+9)=CA(1)
    CU(101)=HIE*AIE/DIE
    CU(252)=CU(101)
    DO 191=101,197,32
    CU(1+32)=CU(1)
19  CU(1+23)=CU(1)
C   READING CONDUCTANCES BTWN REGIONS E+D AND ALSO I+J
C   READ(5,13)HED,AED,DED,HIJ,AIJ,DIJ
    CU(106)=HED*AED/DED
    CU(238)=CU(106)
    CU(243)=CU(106)
    CU(247)=CU(106)
    DO 201=106,202,32
    CU(1+32)=CU(1)
    CU(1+4)=CU(1)
    CU(1+9)=CU(1)
20  CU(1+13)=CU(1)
    CA(258)=HIJ*AIJ/DIJ
    CA(286)=CA(258)
    DO 211=258,259,1
    CA(1+1)=CA(1)
21  CA(1+26)=CA(1)
C   READING CONDUCTANCES BTWN REGIONS E+K AND ALSO D+L
C   READ(5,13)HEK,AEK,DEK,HDL,ADL,DDL
    CA(261)=HEK*AEK/DEK
    CA(274)=CA(261)

```

TABLE C13 (continued)

```

CA(283)=CA(261)
DO 221=261,264,1
CA(1+1)=CA(1)
CA(1+9)=CA(1)
22 CA(1+18)=CA(1)
   CA(266)=HDL*ADL/DDL
   CA(278)=CA(266)
   DO 231=266,268,1
   CA(1+1)=CA(1)
23 CA(1+9)=CA(1)
C  READING CONDUCTANCES BTWN J+K AND K+L.
   READ(5,13)HJK,AJK,DJK,HKL,AKL,DKL
   CU(261)=HJK*AJK/DJK
   CU(444)=CU(261)
   DO 241=261,389,32
   CU(1+32)=CU(1)
24 CU(1+23)=CU(1)
   CU(266)=HKL*AKL/DKL
   CU(430)=CU(266)
   CU(435)=CU(266)
   CU(439)=CU(266)
   DO 251=266,394,32
   CU(1+32)=CU(1)
   CU(1+4)=CU(1)
   CU(1+9)=CU(1)
25 CU(1+13)=CU(1)
C  READING CONDUCTANCES BTWN REGIONS J+F AND ALSO K+G
   READ(5,13)HJF,AJF,DJF,HKG,AKG,DKG
   CA(450)=HJF*AJF/DJF
   CA(478)=CA(450)
   DO 261=450,451,1
   CA(1+1)=CA(1)
26 CA(1+26)=CA(1)
   CA(453)=HKG*AKG/DKG
   CA(486)=CA(453)
   CA(475)=CA(453)
   DO 271=453,456,1
   CA(1+1)=CA(1)
   CA(1+9)=CA(1)
27 CA(1+18)=CA(1)
C  READING CONDUCTANCES BTWN REGIONS L+H AND ALSO F+G
   READ(5,13)HLH,ALH,DLH,HFG,AFG,DFG
   CA(450)=HLH*ALH/DLH
   CA(470)=CA(458)
   DO 281=458,460,1
   CA(1+1)=CA(1)
28 CA(1+9)=CA(1)
   CU(453)=HFG*AFG/DFG
   CU(540)=CU(453)
   DO 291=453,485,32
   CU(1+32)=CU(1)
29 CU(1+23)=CU(1)
C  READING CONDUCTANCES BTWN REGIONS G+H
   READ(5,30)HGH,AGH,DGH
30 FORMAT(3F12.7)
   CU(458)=HGH*AGH/DGH
   CU(526)=CU(458)
   CU(531)=CU(458)
   CU(535)=CU(458)
   DO 311=458,490,32
   CU(1+32)=CU(1)
   CU(1+4)=CU(1)
   CU(1+9)=CU(1)
31 CU(1+13)=CU(1)
C
C
C
C
C  NOW THAT ALL THE BOUNDARY CONDITIONS HAVE BEEN READ IN,
  THE HORIZONTAL AND VERTICAL CONDUCTANCES FOR EACH REGION
  ARE EVALUATED AS SHOWN BELOW
  READING CONDUCTANCES OF REGION A-CA AND CU
  READ(5,13)HAA,AAA,DAA,HAU,AAU,DAU
  CA(34)=HAA*AAA/DAA
  CA(62)=CA(34)
  CA(68)=CA(34)
  CA(94)=CA(34)
  CU(2)=HAU*AAU/DAU
  DO 321=34,35,1

```

TABLE C13 (continued)

	CA(1+1)=CA(1)
	CA(1+32)=CA(1)
	CA(1+26)=CA(1)
32	CA(1+58)=CA(1)
	CU(36)=CU(2)
	CU(68)=CU(2)
	CU(31)=CU(2)
	CU(63)=CU(2)
	CU(95)=CU(2)
	DO 331=2,3,1
	CU(1+1)=CU(1)
	CU(1+32)=CU(1)
	CU(1+64)=CU(1)
	CU(1+27)=CU(1)
	CU(1+59)=CU(1)
33	CU(1+91)=CU(1)
C	READING CONDUCTANCES OF REGION C-CA AND CU
	READ(5,13)HBA,ABA,DBA,HBU,ABU,DBU
	CA(37)=HBA*ABA/DBA
	CA(73)=CA(37)
	CA(56)=CA(37)
	CA(62)=CA(37)
	CA(59)=CA(37)
	CA(91)=CA(37)
	DO 341=37,40,1
	CA(1+1)=CA(1)
	CA(1+32)=CA(1)
	CA(1+9)=CA(1)
	CA(1+41)=CA(1)
	CA(1+18)=CA(1)
34	CA(1+50)=CA(1)
	CU(6)=HBU*ABU/DBU
	CU(41)=CU(6)
	CU(73)=CU(6)
	CU(18)=CU(6)
	CU(50)=CU(6)
	CU(42)=CU(6)
	CU(27)=CU(6)
	CU(59)=CU(6)
	CU(91)=CU(6)
	DO 351=6,9,1
	CU(1+1)=CU(1)
	CU(1+32)=CU(1)
	CU(1+64)=CU(1)
	CU(1+9)=CU(1)
	CU(1+41)=CU(1)
	CU(1+73)=CU(1)
	CU(1+18)=CU(1)
	CU(1+50)=CU(1)
35	CU(1+82)=CU(1)
C	READING CONDUCTANCES OF REGION C-CA AND CU
	READ(5,13)HCA,ACA,DCA,HCU,ACU,DCU
	CA(42)=HCA*ACA/DCA
	CA(77)=CA(42)
	CA(46)=CA(42)
	CA(54)=CA(42)
	DO 361=42,44,1
	CA(1+1)=CA(1)
	CA(1+32)=CA(1)
	CA(1+9)=CA(1)
	CA(1+41)=CA(1)
36	CU(11)=HCU*ACU/DCU
	CU(45)=CU(11)
	CU(77)=CU(11)
	CU(22)=CU(11)
	CU(54)=CU(11)
	CU(86)=CU(11)
	DO 371=11,12,1
	CU(1+1)=CU(1)
	CU(1+32)=CU(1)
	CU(1+64)=CU(1)
	CU(1+9)=CU(1)
	CU(1+41)=CU(1)
	CU(1+73)=CU(1)
37	CU(1+73)=CU(1)
C	READING CONDUCTANCES OF REGION I-CA AND CU
	READ(5,13)HIA,AIA,DIA,HIU,AIU,DIU
	CA(130)=HIA*AIA/DIA

TABLE C13 (continued)

CU(98)*HIU*AIU/DIU
 DD 381=130,131,1
 CA(1+1)=CA(1)
 CA(1+32)=CA(1)
 CA(1+64)=CA(1)
 CA(1+96)=CA(1)
 CA(1+28)=CA(1)
 CA(1+53)=CA(1)
 CA(1+90)=CA(1)
 38 CA(1+122)=CA(1)
 CA(164)=CA(130)
 CA(196)=CA(130)
 CA(220)=CA(130)
 CA(158)=CA(130)
 CA(190)=CA(130)
 CA(222)=CA(130)
 CA(256)=CA(130)
 DD 391=98,99,1
 CU(1+1)=CU(1)
 CU(1+32)=CU(1)
 CU(1+64)=CU(1)
 CU(1+96)=CU(1)
 CU(1+128)=CU(1)
 CU(1+27)=CU(1)
 CU(1+59)=CU(1)
 CU(1+91)=CU(1)
 CU(1+123)=CU(1)
 39 CU(1+165)=CU(1)
 CU(132)=CU(98)
 CU(164)=CU(98)
 CU(196)=CU(98)
 CU(226)=CU(98)
 CU(157)=CU(98)
 CU(159)=CU(98)
 CU(191)=CU(98)
 CU(223)=CU(98)
 CU(255)=CU(98)
 C READING CONDUCTANCES OF REGIONE* CA AND CU
 READ(5,13)HEA,AEA,DFA,HEU,AEU,DEU
 CA(133)=HEA*AEA/DEA
 CA(169)=CA(133)
 CA(201)=CA(133)
 CA(233)=CA(133)
 CA(166)=CA(133)
 CA(178)=CA(133)
 CA(210)=CA(133)
 CA(242)=CA(133)
 CA(155)=CA(133)
 CA(187)=CA(133)
 CA(219)=CA(133)
 CA(251)=CA(133)
 DD 401=133,136,1
 CA(1+1)=CA(1)
 CA(1+32)=CA(1)
 CA(1+64)=CA(1)
 CA(1+96)=CA(1)
 CA(1+9)=CA(1)
 CA(1+41)=CA(1)
 CA(1+73)=CA(1)
 CA(1+105)=CA(1)
 CA(1+18)=CA(1)
 CA(1+50)=CA(1)
 CA(1+82)=CA(1)
 40 CA(1+114)=CA(1)
 CU(102)=HEU*AEU/DEU
 CU(137)=CU(102)
 CU(169)=CU(102)
 CU(201)=CU(102)
 CU(233)=CU(102)
 CU(114)=CU(102)
 CU(166)=CU(102)
 CU(178)=CU(102)
 CU(210)=CU(102)
 CU(242)=CU(102)
 CU(123)=CU(102)
 CU(155)=CU(102)
 CU(187)=CU(102)

TABLE C13 (continued)

```

CU(219)=CU(102)
CU(251)=CU(102)
DO 411=102,104,1
CU(1+1)=CU(1)
CU(1+32)=CU(1)
CU(1+64)=CU(1)
CU(1+96)=CU(1)
CU(1+128)=CU(1)
CU(1+9)=CU(1)
CU(1+41)=CU(1)
CU(1+73)=CU(1)
CU(1+105)=CU(1)
CU(1+137)=CU(1)
CU(1+18)=CU(1)
CU(1+50)=CU(1)
CU(1+82)=CU(1)
CU(1+114)=CU(1)
CU(1+146)=CU(1)
C 41 READING CONDUCTANCES OF REGION D-CA AND CU
READ(5,13)HDA,ADA,DUA,HDU,ADU,DOU
CA(138)=HDA*ADA/DDA
CA(173)=CA(138)
CA(205)=CA(138)
CA(237)=CA(138)
CA(150)=CA(138)
CA(182)=CA(138)
CA(214)=CA(138)
CA(246)=CA(138)
DO 421=138,140,1
CA(1+1)=CA(1)
CA(1+32)=CA(1)
CA(1+64)=CA(1)
CA(1+96)=CA(1)
CA(1+9)=CA(1)
CA(1+41)=CA(1)
CA(1+73)=CA(1)
C 42 CA(1+105)=CA(1)
CU(107)=HDO*ADU/DDU
CU(141)=CU(107)
CU(173)=CU(107)
CU(205)=CU(107)
CU(237)=CU(107)
CU(118)=CU(107)
CU(150)=CU(107)
CU(182)=CU(107)
CU(214)=CU(107)
CU(246)=CU(107)
DO 431=107,108,1
CU(1+1)=CU(1)
CU(1+32)=CU(1)
CU(1+64)=CU(1)
CU(1+96)=CU(1)
CU(1+128)=CU(1)
CU(1+9)=CU(1)
CU(1+41)=CU(1)
CU(1+73)=CU(1)
CU(1+105)=CU(1)
C 43 CU(1+137)=CU(1)
READING CONDUCTANCES OF REGION J-CA AND CU
READ(5,13)HJA,AJA,DJA,HJU,AJU,DUJ
CA(290)=HJA*AJA/DJA
CA(318)=CA(290)
DO 441=318,414,32
C 44 CA(1+32)=CA(1)
DO 451=290,291,1
CA(1+1)=CA(1)
CA(1+32)=CA(1)
CA(1+64)=CA(1)
CA(1+96)=CA(1)
CA(1+128)=CA(1)
CA(1+26)=CA(1)
CA(1+58)=CA(1)
CA(1+90)=CA(1)
CA(1+122)=CA(1)
C 45 CA(1+154)=CA(1)
DO 461=292,388,32
C 46 CA(1+32)=CA(1)

```

TABLE C13 (continued)

```

CU(250)=HJU*AJU/DJU
CU(257)=CU(250)
DO 47 I=250,259,1
CU(I+1)=CU(I)
CU(I+32)=CU(I)
CU(I+64)=CU(I)
CU(I+96)=CU(I)
CU(I+128)=CU(I)
CU(I+160)=CU(I)
CU(I+27)=CU(I)
CU(I+59)=CU(I)
CU(I+91)=CU(I)
CU(I+123)=CU(I)
CU(I+155)=CU(I)
47 CU(I+187)=CU(I)
DO 48 I=260,385,32
CU(I+32)=CU(I)
CU(I+59)=CU(I)
C 40 READING CONDUCTANCES OF REGION K*CA AND CU
READ(5,13)HKA,AKA,DKA,HKU,AKU,DKU
CA(293)=HKA*AKA/DKA
CA(306)=CA(293)
CA(319)=CA(293)
DO 49 I=293,296,1
CA(I+1)=CA(I)
CA(I+32)=CA(I)
CA(I+64)=CA(I)
CA(I+96)=CA(I)
CA(I+128)=CA(I)
CA(I+5)=CA(I)
CA(I+91)=CA(I)
CA(I+73)=CA(I)
CA(I+105)=CA(I)
CA(I+137)=CA(I)
CA(I+18)=CA(I)
CA(I+50)=CA(I)
CA(I+82)=CA(I)
49 CA(I+114)=CA(I)
CA(I+146)=CA(I)
DO 50 I=297,393,32
CA(I+32)=CA(I)
CA(I+64)=CA(I)
50 CA(I+50)=CA(I)
CU(262)=HKU*AKU/DKU
CU(274)=CU(262)
CU(283)=CU(262)
DO 51 I=282,284,1
CU(I+1)=CU(I)
CU(I+32)=CU(I)
CU(I+64)=CU(I)
CU(I+96)=CU(I)
CU(I+128)=CU(I)
CU(I+160)=CU(I)
CU(I+5)=CU(I)
CU(I+91)=CU(I)
CU(I+73)=CU(I)
CU(I+105)=CU(I)
CU(I+137)=CU(I)
CU(I+169)=CU(I)
CU(I+18)=CU(I)
CU(I+50)=CU(I)
CU(I+82)=CU(I)
CU(I+114)=CU(I)
CU(I+146)=CU(I)
51 CU(I+178)=CU(I)
DO 52 I=265,393,32
CU(I+32)=CU(I)
CU(I+91)=CU(I)
52 CU(I+50)=CU(I)
C READING CONDUCTANCES OF REGION L*CA AND CU
READ(5,13)HLA,ALA,DLA,HLU,ALU,DLU
CA(298)=HLA*ALA/DLA
CA(310)=CA(298)
DO 53 I=298,300,1
CA(I+1)=CA(I)
CA(I+32)=CA(I)
CA(I+64)=CA(I)

```


TABLE C13 (continued)

```

CA(1+96)=CA(1)
CA(1+128)=CA(1)
CA(1+9)=CA(1)
CA(1+91)=CA(1)
CA(1+73)=CA(1)
CA(1+105)=CA(1)
53 CA(1+137)=CA(1)
DO 54 I=301,397,32
CA(1+32)=CA(1)
54 CA(1+41)=CA(1)
CU(267)=HLU*ALU/OLU
CU(278)=CU(267)
DO 55 I=267,268,1
CU(1+1)=CU(1)
CU(1+32)=CU(1)
CU(1+64)=CU(1)
CU(1+96)=CU(1)
CU(1+128)=CU(1)
CU(1+160)=CU(1)
CU(1+9)=CU(1)
CU(1+41)=CU(1)
CU(1+73)=CU(1)
CU(1+105)=CU(1)
CU(1+137)=CU(1)
55 CU(1+169)=CU(1)
DO 56 I=269,397,32
CU(1+32)=CU(1)
56 CU(1+41)=CU(1)
C READING CONDUCTANCES OF REGION F=CA AND CU
READ(5,13)HFA,AFU,DFA,HFU,AFU,DFU
CA(482)=HFA*AFU/DFU
CA(516)=CA(482)
CA(510)=CA(482)
CA(542)=CA(482)
DO 57 I=482,483,1
CA(1+1)=CA(1)
CA(1+32)=CA(1)
CA(1+26)=CA(1)
57 CA(1+58)=CA(1)
CU(450)=HFU*AFU/DFU
CU(464)=CU(450)
CU(516)=CU(450)
CU(479)=CU(450)
CU(511)=CU(450)
CU(543)=CU(450)
DO 58 I=450,451,1
CU(1+1)=CU(1)
CU(1+32)=CU(1)
CU(1+64)=CU(1)
CU(1+27)=CU(1)
CU(1+59)=CU(1)
58 CU(1+91)=CU(1)
C READING CONDUCTANCES OF REGION G=CA AND CU
READ(5,13)HGA,AGA,DGA,HGU,AGU,DGU
CA(485)=HGA*AGA/DGA
CA(521)=CA(485)
CA(490)=CA(485)
CA(530)=CA(485)
CA(507)=CA(485)
CA(539)=CA(485)
DO 59 I=485,488,1
CA(1+1)=CA(1)
CA(1+32)=CA(1)
CA(1+9)=CA(1)
CA(1+41)=CA(1)
CA(1+18)=CA(1)
59 CA(1+50)=CA(1)
CU(454)=HGU*AGU/DGU
CU(530)=CU(454)
CU(537)=CU(454)
DO 60 I=454,456,1
CU(1+1)=CU(1)
CU(1+32)=CU(1)
CU(1+64)=CU(1)
CU(1+9)=CU(1)
CU(1+41)=CU(1)
CU(1+73)=CU(1)

```

TABLE C13 (continued)

```

      CU(1+18)=CU(1)
      CU(1+50)=CU(1)
60    CU(1+82)=CU(1)
      DO 61 I=457,489,32
      CU(1+32)=CU(1)
      CU(1+9)=CU(1)
C 61    CU(1+18)=CU(1)
      READING CONDUCTANCES OF REGION HCCA AND CU
      READ(5,13)HHA,APA,DHA,HHU,AHU,DHU
      CA(490)=HHA*AHA/DHA
      CA(525)=CA(490)
      CA(502)=CA(490)
      CA(534)=CA(490)
      DO 62 I=490,492,1
      CA(1+1)=CA(1)
      CA(1+32)=CA(1)
      CA(1+9)=CA(1)
62    CA(1+41)=CA(1)
      CU(459)=HHU*AHU/DHU
      CU(534)=CU(459)
      DO 63 I=459,460,1
      CU(1+1)=CU(1)
      CU(1+32)=CU(1)
      CU(1+64)=CU(1)
      CU(1+9)=CU(1)
      CU(1+41)=CU(1)
63    CU(1+73)=CU(1)
      DO 64 I=461,493,32
      CU(1+32)=CU(1)
      CU(1+9)=CU(1)
C 64    WRITING THE CONDUCTANCES=FIRSTLY CA AND THEN CU
      WRITE(6,65)(I,CA(I),I=33,543)
65    FORMAT(///,(1X,/,1X,6('CA(',13,')= ',F12.6,2X)))
      WRITE(6,66)(I,CU(I),I=1,504)
66    FORMAT(///,(1X,/,1X,6('CU(',13,')= ',F12.6,2X)))
      RETURN
      END

```

TABLE C13 (continued)

```

SUBROUTINE RELAX(T,CA,CU,RES,H,N)
DIMENSION T(576),CA(576),CU(576),RES(576)
DIMENSION TI(576)
H=1.26
C  H IS THE RELAXATION FACTOR
KI=1
C  KI IS THE COUNTER OF THE NUMBER OF RESIDUAL ITERATIONS
M1=M-1
M2=M+1
M3=2*M
LL=1
L=0
C  LL AND L ARE COUNTERS FOR WRITING THE TEMP PROFILE
C  EVERY 3 ITERATIONS
TOL=0.005
24 NR=1
TOLM=1.E-02
K=2
NR=(NR+H)*1
21 CONTINUE
IF(K.GT.NR)GO TO 20
KM1=K+M1
KM2=K+M2
KM3=K+M3
DEN=(CA(KM1)*T(KM1))+(CA(KM)*T(KM2))+(CU(K)*T(K))+(CU(KM)*T(KM3))
DENM=DEN/(CA(KM1)+CA(KM)+CU(K)+CU(KM))
RES(KM)=DENM-T(KM)
T(KM)=T(KM)+(H*RES(KM))
K=K+1
GO TO 21
20 K=K+2
NR=NR+1
NR=NR+H
IF(NR.EQ.N)GO TO 22
GO TO 21
22 CONTINUE
C  THE FIRST ESTIMATE OF TEMPS HAS BEEN OBTAINED
C  RESIDUALS ITERATING STARTS HERE
NR=1
K=2
KM=K+H
NR=(NR+H)*1
28 CONTINUE
IF(K.GT.NR)GO TO 26
IF(ABS(RES(KM)).GT.TOLM)GO TO 25
K=K+1
KM=K+H
GO TO 28
25 TOLM=RES(KM)
K=K+1
KM=K+H
GO TO 28
26 K=K+2
NR=NR+1
NR=NR+H
IF(NR.EQ.N)GO TO 27
GO TO 28
27 IF(ABS(TOLM).LE.TOL)GO TO 29
IF(KI.GT.400)GO TO 29
IF(KI.EQ.L)GO TO 52
KI=KI+1
GO TO 24
52 WRITE(6,46)KI
46 FORMAT(///,1X,'THE NUMBER OF RESIDUAL ITERATIONS FOR THE TEMPERAT
    URE PROFILE SHOWN BELOW',I3)
DO 71 J=1,545,32
NR=J+15
71 WRITE(6,70)(T(I),I=J,NH+1)
70 FORMAT(1X,16(F6.3,2X))
54 FORMAT(///,1X,32(I3,1X))
KI=KI+1
LL=LL+1
L=L+3
GO TO 24
29 CONTINUE

```

TABLE C13 (continued)

```

WRITE(6,72)
72  FORMAT(///,1X,'THE TEMPERATURE PROFILE FOR THE WHOLE NETWORK IS:')
    WRITE(6,46)NI
    WRITE(6,75)
75  FORMAT(///,1X,'THE TEMP PROFILE FOR L.H.S. OF NETWORK:')
    DO 73 J=1,543,32
        NH=J*15
73  WRITE(6,70)(T(I),I=J,NH,1)
        WRITE(6,76)
76  FORMAT(///,1X,'THE TEMP. PROFILE FOR R.H.S. OF NETWORK:')
        DO 74 J=17,561,32
            NH2=J*15
74  WRITE(6,70)(T(I),I=J,NH2,1)
        WRITE(6,46)NI
        NH1=(NH+1)*M
        SF=1.0
        DO 65 I=1,MH1
            TI(I)=T(I)*SF
65  TI(I)=TI(I)+4000.
        WRITE(6,54)(TI(I),I=1,MH1,1)
        RETURN
    END

```

TABLE C13 (continued)

```

SUBROUTINE HEATFL(T,CA,CU,QA,QU,H,N)
DIMENSION T(576),CA(576),CU(576),QA(576),QU(576)
NR=1
K=2
M1=H-1
NR=(NR+H)-1
33 CONTINUE
IF(K,GT,MR)GO TO 31
KH=K+H
KM1=K-1
QA(KM1)=CA(KM1)*(T(KM1)-T(KH))
QU(K)=CU(K)*(T(K)-T(KH))
WRITE(6,50)KM1,QA(KM1),K,QU(K)
50 FORMAT(/,20X,'QA(',13,')=',F12.4,'QU(',13,')=',F12.4)
K=K+1
GO TO 33
31 CONTINUE
KH=K+H
KM1=K-1
QA(KM1)=CA(KM1)*(T(KM1)-T(KH))
WRITE(6,50)KM1,QA(KM1),K,QU(K)
K=K+2
NR=NR+1
MR=MR+H
IF(MR,EQ,N)GO TO 32
GO TO 33
32 CONTINUE
IF(K,GT,MR)GO TO 37
KH=K+H
QU(K)=CU(K)*(T(K)-T(KH))
WRITE(6,51)K,QU(K)
51 FORMAT(/,20X,'QU(',13,')=',F12.4)
K=K+1
GO TO 32
37 CONTINUE
RETURN
END

```

APPENDIX D
CALIBRATION OF THERMOCOUPLES

D1	<u>WORKING STANDARD</u>	321
D2	<u>THE COMPARISON BRIDGE</u>	321
D3	<u>THERMOCOUPLE CALIBRATION DATA</u>	323
D4	<u>THERMOCOUPLE EQUATIONS</u>	323
D5	<u>THERMOCOUPLE TABLES</u>	325

D1 WORKING STANDARD

The platinum resistance thermometer was calibrated by the National Physical Laboratory, Teddington, England. The results of the calibration were given in tabular form; resistance ratio (W) versus temperature.

$W = \frac{R(T)}{R(273.15^{\circ}\text{K})}$ over the temperature range from 273°K to 90°K and $W = \frac{R(t)}{R(0^{\circ}\text{C})}$ over the temperature range from 0°C to 500°C , $T = t + 273.15$ and R is the resistance of the platinum resistor.

The heating effect of a measuring current of 1 milli-ampere when the thermometer was immersed in unstirred water was 0.00013 ohms.

The value of $R(0^{\circ}\text{C})$ after the stability test was 25.4899 ohms; the final value being 25.4893 ohms.

Table D1 gives the resistance ratio (W) of the platinum resistance thermometer in the temperature range used in the thermocouple calibrations.

The standard resistor used in the thermocouple calibrations was a 25.5 ohms H. Tinsley and Co. class S standard resistor number 188.092. The National Physical Laboratory measured its resistance at 20°C : 25.4999 ± 0.0001 ohms.

D2 THE COMPARISON BRIDGE

The Rosemount Engineering Company precision comparison bridge model VLF 51A is specifically designed for precision measurements in resistance thermometry. The precise ratio of currents flowing through two resistances being compared is obtained from accurate tapped current transformers. The

TABLE D1

Platinum Resistance Thermometer NPL Calibrations

W	t (°C)
1.00	0.0000
1.01	2.5101
1.02	5.0222
1.03	7.5363
1.04	10.0522
1.05	12.5702
1.06	15.0900
1.07	17.6119
1.08	20.1356
1.09	22.6614
1.10	25.1891
1.11	27.7187
1.12	30.2504
1.13	32.7840
1.14	35.3195
1.15	37.8571
1.16	40.3966
1.17	42.9381
1.18	45.4816
1.19	48.0271
1.20	50.5745
1.21	53.1240
1.22	55.6754
1.23	58.2289

bridge uses four-terminal connections and a low working frequency 5 c/s. The bridge has resistance ratio ranges of 0 to 1.111110 and 0 to 11.11110 with comparison accuracy of 1 in 10^5 and a resolution of 1 in 10^6 .

D3 THERMOCOUPLE CALIBRATION DATA

The temperatures of the aluminium calibration block as indicated by

- (i) the platinum resistance thermometer
 - (ii) the four thermocouple wires (numbers 5, 23, 33 and 35)
- are shown in Table D2.

The temperatures of the water bath as indicated by the mercury-in-glass thermometer are also presented.

D4 THERMOCOUPLE EQUATIONS

Using non-linear regression (least squares parabolic fit), the quadratic equations relating the emf to the temperature were obtained.

- (a) for thermocouple wires 5 and 23

$$e = 0.02785736 + 0.03741623T + 0.00004287T^2 \quad (D-1)$$

- (b) for thermocouple wires 33 and 35

$$e = -0.00726804 + 0.03904908T + 0.00004037T^2 \quad (D-2)$$

TABLE D2

Thermocouple Calibration - Raw Experimental Data

Run	Room Temp. °C	Hg-in-glass Thermometer Bath Temp. °C	Thermocouple Wires Millivolt Readings				Water Bath Temperature By Platinum Resistance Thermometer			
			5 mV	23 mV	33 mV	35 mV	Resistance Ratios R1/R2	Resistance Ratios R2/R1	Mean Resistance Ratio	Water Bath Temperature °C
1	22.2	25.47	1.031	1.031	1.017	1.017	1.101140	.908191	1.101115	25.5837
2	22.0	25.47	1.017	1.017	1.021	1.021	1.101348	.908004	1.101332	25.6386
3	21.8	25.65	1.023	1.023	1.028	1.028	1.102199	.907327	1.102169	25.8504
4	21.7	25.67	1.024	1.024	1.029	1.029	1.102281	.907274	1.102242	25.8669
5	22.0	27.8	1.109	1.109	1.117	1.117	1.110726	.900362	1.110695	28.0083
6	22.6	27.8	1.109	1.109	1.117	1.117	1.110709	.900376	1.110678	28.0040
7	21.6	28.65	1.14	1.14	1.153	1.153	1.11395	.897953	1.113859	28.8096
8	21.8	28.68	1.14	1.14	1.153	1.153	1.11412	.897667	1.114059	28.8603
9	21.7	29.9	1.192	1.192	1.204	1.204	1.11884	.893896	1.118769	30.0532
10	22.1	29.9	1.192	1.192	1.204	1.204	1.11887	.893860	1.118807	30.0628
11	21.4	31.2	1.247	1.247	1.261	1.26	1.12426	.889567	1.124201	31.4299
12	21.6	31.2	1.247	1.247	1.261	1.261	1.12430	.889541	1.124238	31.4392
13	22.8	33.05	1.323	1.323	1.337	1.337	1.13140	.883967	1.131332	33.2376
14	22.8	33.05	1.322	1.322	1.337	1.337	1.13144	.883930	1.131376	33.2488
15	20.9	35.95	1.435	1.434	1.457	1.456	1.14290	.875063	1.142837	36.1566
16	21.5	35.95	1.437	1.437	1.458	1.458	1.14294	.875024	1.142883	36.1623
17	22.2	38.02	1.522	1.522	1.546	1.546	1.15116	.868820	1.151073	38.2477
18	21.9	38.02	1.521	1.521	1.545	1.545	1.15121	.868772	1.15113	38.2622
19	22.8	40.1	1.611	1.611	1.637	1.637	1.15958	.862504	1.159497	40.3878
20	23.0	40.1	1.612	1.611	1.637	1.637	1.15962	.862468	1.159542	40.3993
21	22.1	40.9	1.638	1.637	1.667	1.667	1.16276	.86014	1.162681	41.1974
22	22.4	40.9	1.639	1.638	1.667	1.667	1.16267	.86022	1.162582	41.1722
23	21.0	42	1.688	1.688	1.718	1.718	1.16712	.856934	1.167036	42.3046
24	22.1	42	1.690	1.689	1.718	1.718	1.16715	.856894	1.167078	42.3153
25	22.2	43	1.730	1.73	1.761	1.761	1.17119	.853935	1.17112	43.3433
26	22.3	43.02	1.729	1.728	1.759	1.759	1.17119	.853943	1.171114	43.3418
27	22.3	44	1.770	1.769	1.802	1.803	1.17503	.851149	1.174956	44.3194
28	22.3	44	1.770	1.769	1.802	1.802	1.17502	.851166	1.174939	44.3151
29	22.3	44.9	1.813	1.811	1.846	1.846	1.17885	.848429	1.178750	45.2848
30	22.8	44.9	1.813	1.812	1.845	1.845	1.17883	.848421	1.178745	45.2835
31	22.8	46.1	1.857	1.855	1.890	1.891	1.18307	.845338	1.183014	46.3705
32	22.7	46.05	1.855	1.854	1.889	1.889	1.18307	.845372	1.182991	46.3646
33	22.3	49.95	2.016	2.016	2.058	2.058	1.19859	.834434	1.198504	50.3158
34	22.0	50	2.019	2.018	2.058	2.058	1.19858	.834467	1.198475	50.3094
35	23.0	54.9	2.228	2.225	2.274	2.274	1.21787	.821208	1.217794	55.2381
36	22.9	54.9	2.227	2.225	2.274	2.274	1.21786	.821213	1.217785	55.2358

D5 THERMOCOUPLE TABLES

APPENDIX ESERIES 'A' - EXPERIMENTAL RESULTS

E1	<u>THERMAL CONDUCTIVITY DETERMINATION</u>	331
E2	<u>SPECIMENS WITH HOLES DRILLED</u>	331

E1 THERMAL CONDUCTIVITY DETERMINATION

E1.1 POSITIONING OF SPECIMENS

During the experimental runs using clear perspex plates, the clear perspex plate marked 'CA' was held between aluminium plates 11a and 13a in Figure 2-5. The perspex plate labelled 'CB' was held between the aluminium plates 11b and 13b. Similarly, during white perspex experimental runs, the perspex plate marked 'WA' was held between the aluminium plates 11a and 13a, while that marked 'WB' was held between the plates 11b and 13b.

The thicknesses of the perspex plates were:

(i) Clear perspex:

plate 'CA' = 5.94mm

plate 'CB' = 5.74mm

(ii) White perspex:

plate 'WA' = 6.21mm

plate 'WB' = 6.29mm

E1.2 THERMAL CONDUCTIVITIES OF THE SPECIMENS

Table E1 shows the thermal conductivities of the clear and white perspex specimens.

E2 SPECIMENS WITH HOLES DRILLED

The clear perspex plates 'CA' and 'CB' had 30.5mm holes drilled (in a square pitch pattern). The resulting temperature drops across the specimens were of interest (since in Table E1, the temperature drops across the specimens were small). Table E2 shows the resulting temperature drops.

TABLE E1
Thermal Conductivities (Clear and White Perspex)

Run	Specimen Plate Number	Temperature of Specimen Surface		Temperature Drop Across Specimen C	Mean Specimen Temperature C	Thermal Conductivity W/M°C
		Hot °C	Cold °C			
1	CA	38.29	37.29	1	37.79	0.179
	CB	38.26	37.25	1.01	37.76	0.172
2	CA	38.89	37.83	1.06	38.36	0.169
	CB	38.82	37.71	1.11	38.27	0.155
3	CA	42.93	41.33	1.6	42.13	0.181
	CB	42.84	41.17	1.67	42.01	0.163
4	CA	45.24	43.29	1.95	44.27	0.172
	CB	45.08	43.06	2.02	44.07	0.16
5	CA	45.47	43.43	2.04	44.45	0.165
	CB	45.25	43.24	2.01	44.25	0.161
6	CA	45.81	43.76	2.05	44.79	0.164
	CB	45.52	43.57	1.95	44.55	0.167
7	CA	45.14	43.19	1.95	44.17	0.171
	CB	44.97	42.94	2.03	43.96	0.159
8	CA	45.02	43.06	1.96	44.04	0.172
	CB	44.83	42.81	2.02	43.82	0.162
9	WA	39.26	37.40	1.86	38.33	0.188
	WB	39.13	37.19	1.94	38.16	0.184
10	WA	34.97	33.35	1.62	34.16	0.217
	WB	34.97	33.55	1.62	34.16	0.22
11	WA	34.56	33.10	1.46	33.83	0.244
	WB	34.53	33.12	1.41	33.83	0.251

TABLE E2

Temperature Drops Across Clear Perspex Plates
With 30.5mm Holes

Run	Specimen Plate Number	Temperature of Specimen Surface		Temperature Drop Across Specimen °C	Electrical Power Into Specimen (W)
		Hot °C	Cold °C		
1	CA	50.83	48.6	2.23	2.285
	CB	50.48	47.8	2.68	2.285
2	CA	50.88	48.7	2.18	2.285
	CB	50.64	48.07	2.57	2.285
3	CA	50.98	48.86	2.12	2.285
	CB	50.74	48.14	2.6	2.285
4	CA	51.72	49.6	2.12	2.284
	CB	51.28	48.79	2.49	2.284
5	CA	51.58	49.56	2.02	2.284
	CB	51.38	48.6	2.73	2.284
6	CA	51.58	49.58	2.0	2.285
	CB	51.35	48.64	2.71	2.285

APPENDIX FSERIES 'B' - RAW EXPERIMENTAL DATA AND RESULTS

F1	<u>CONDUCTIVITY (CONDUCTANCE) SAMPLE CALCULATION</u>	336
F2	<u>RAW EXPERIMENTAL DATA AND CALCULATED RESULTS</u>	338
F3	<u>CALCULATIONS OF RAYLEIGH AND GRASHOF NUMBERS</u>	339
F4	<u>MEAN THERMAL CONDUCTIVITIES OF PERSPEX</u>	339

LIST OF TABLES

<u>Number</u>	<u>Title</u>	<u>Page</u>
F1	Rayleigh and Grashof Numbers	340
F2	The Thermal Conductivities of 5.6mm and 11mm Thick Perspex Plates	341
F3	Raw Experimental Data - Thermocouple Wires Numbers 1 to 9	342
F4	Mean Millivolts (Temperatures) of Thermo- couple Wires Numbers 1 to 9	352
F5	Raw Experimental Data - Thermocouple Wires Numbers 10 to 18	356
F6	Mean Millivolts (Temperatures) of Thermo- couple Wires Numbers 10 to 18	366
F7	Raw Experimental Data - Thermocouple Wires Numbers 19 to 27	370
F8	Mean Millivolts (Temperatures) of Thermo- couple Wires Numbers 19 to 27	380
F9	Raw Experimental Data - Thermocouple Wires Numbers 28 to 32	384
F10	Mean Millivolts (Temperatures) of Thermo- couple Wires Numbers 28 to 32	394
F11	Raw Experimental Data - Current and Voltage	398
F12	Power Input into the Specimens (watts)	418
F13	Thermal Conductivities and Conductances - Runs 1 to 738	419
F14	Mean Thermal Conductivities and Conductances - Runs 1 to 738	429

F1 CONDUCTIVITY (CONDUCTANCE) SAMPLE CALCULATION

The thermal conductivity (or conductance for specimens with holes in them) was calculated using equation 1-1.

$$q = kA \frac{dT}{dx} \quad (1-1)$$

Consider for example, run 1. The measured millivolts for the cold aluminium plate 11a (thermocouple wires 1 to 9) were: 1.977, 1.979, 1.977, 1.980, 1.980, 1.979, 1.978, 1.979 and 1.979.

Hence, the mean = 1.979mV with a standard deviation of 0.001. From the thermocouple equation D-1, this corresponds to a temperature of 49.348°C.

For the hot aluminium plate 13a (thermocouple wires 10 to 18), the millivolts measured were: 2.048, 2.049, 2.047, 2.049, 2.049, 2.048, 2.050, 2.051 and 2.049.

The mean = 2.049mV with a standard deviation of 0.001. The temperature = 51.031°C.

Since perspex plate number 1 was used in this run,

$$dx = 5.69 \times 10^{-3} \text{ metres}$$

The area perpendicular to the direction of heat flow 'A' is 0.04m² (Figure 2-7).

The heat input is the product of the current and the voltage.

$$\begin{aligned} Q &= \left(\frac{0.5187 + 0.5189}{2} \right) \text{ amps} \times \left(\frac{35.42 + 35.43}{2} \right) \text{ volts} \\ &= 18.378 \text{ watts} \end{aligned}$$

The power into the metered section of the guarded hot plate is 18.378/4 watts. Since the two specimens exist, the power into the central section of each specimen = 18.378/4/2.

$$q = 2.297 \text{ watts}$$

Substituting the above values into equation 1-1,

$$2.297 = \frac{k \times 0.04 \times (51.031 - 49.348)}{5.69 \times 10^{-3}}$$

Hence,

$$k = 0.194 \text{ W/M}^{\circ}\text{C}$$

The above calculation of the thermal conductivity of 5.6mm perspex was for the specimen held between aluminium plates 11a and 13a. In the computer program used to evaluate the thermal conductivities and conductances, it is designated the 'top specimen'. The 'bottom specimen (plate)' refers to the specimen held between aluminium plates 11b and 13b. The millivolts of the bottom plate are those indicated by thermocouple wires numbered 19 to 27 and 28 to 32. Although thermocouple readings of wires numbered 33 to 36 were taken, they are not shown in the raw data presented (recall these thermocouple wires used 39 gauge constantan instead of 36 gauge due to the lack of thermocouple wire in New Zealand).

For specimens with holes in them, the above procedure was repeated, but the evaluated k was termed 'the thermal conductance' - in the computer printout presented below, they were still called thermal conductivities rather than thermal conductances.

F2 COMPUTER PRINTOUTS OF RAW EXPERIMENTAL DATA AND
CALCULATED RESULTS

Tables F3 to F14 present the raw experimental data and the calculated results for Series 'B' experiments (runs 1 to 738).

Notation:

K	run number counter
XBAR	mean of the millivolt readings (mV)
STD	standard deviation of the millivolt readings
TEMP	the temperature corresponding to XBAR millivolts ($^{\circ}\text{C}$)
AMPS1 (VOLTS1)	Current (voltage) indicated by multimeter before millivolts were recorded
AMPS2 (VOLTS2)	Current (voltage) after all the millivolt readings had been taken
DTE TOP	temperature drop across top specimen ($^{\circ}\text{C}$)
DTE BOT	temperature drop across bottom specimen ($^{\circ}\text{C}$)
THI TOP	thickness of top specimen (metres)
THI BOT	thickness of bottom specimen (metres)
WATTAGE	heat input into the metered area of each specimen (watts)
CODCTO	conductivity (conductance) of top specimen ($\text{W}/\text{M}^{\circ}\text{C}$)
CODCBO	conductivity (conductance) of bottom specimen ($\text{W}/\text{M}^{\circ}\text{C}$)
AVT TOP	mean (average) temperature of top specimen ($^{\circ}\text{C}$)
AVT BOT	mean temperature of bottom specimen

F3 CALCULATIONS OF RAYLEIGH AND GRASHOF NUMBERS

$$Gr = \frac{\beta g \rho^2 (T_h - T_c) L^3}{\mu^2} \quad (F-1)$$

$$Pr = \frac{C_p \mu}{k} \quad (F-2)$$

$$Ra = Gr \times Pr \quad (F-3)$$

The fluid (air) properties are obtained from references 146, 167 and 168. They are evaluated at the mean temperature. The calculated Rayleigh number is based on the height of air cavity (thickness of specimen).

For experimental runs used in the numerical simulations, the Rayleigh and Grashof numbers computed are presented in Table F1.

F4 MEAN THERMAL CONDUCTIVITIES OF PERSPEX

The mean thermal conductivities of 5.6mm and 11mm thick perspex plates are summarised in Table 4-2. In runs 1 to 158 (range covered by Table 4-2), the perspex plates 1 to 8 had their thermal conductivities determined for various positionings of the perspex plates (specimens) in the guarded hot plate. In Table F2, the means of various configurations are tabulated. For example, the (mean of the mean) thermal conductivity of perspex plate 1 is $(0.1934 + 0.1946)/2 = 0.1940 \text{ W/M}^{\circ}\text{C}$ with a standard deviation of $0.0008 \text{ W/M}^{\circ}\text{C}$. The error in the determination of the thermal conductivity of plate 1 = standard deviation/mean thermal conductivity.

$$= \frac{0.0008}{0.194} \times 100$$

$$= 0.41\%$$

TABLE F1
Rayleigh and Grashof Numbers

Run	T _h	T _c	Mean Temperature		Viscosity	Density	Gr	Pr	Ra
			°C	°K	×10 ⁻⁶ Ns/m ²	kg/m ³			
159	52.32	48.68	50.5	323.5	19.65	1.0915	465.3	0.7	325.7
172	36.48	35.67	36.08	309.08	19	1.1389	126.2	0.7	88.3
186	61.76	56.25	58.99	331.99	20.06	1.0634	625.1	0.7	437.6
201	51.99	48.25	50.11	323.11	19.64	1.0928	480.3	0.7	336.2
315	50.89	48.73	49.82	322.82	19.62	1.0938	37	0.7	35.9
331	36.36	35.82	36.08	309.08	19	1.1389	11	0.7	7.8
341	61.78	58.37	60.08	333.08	20.11	1.06	50.7	0.7	35.5
549	47.67	43.41	45.54	318.54	19.42	1.1084	583.9	0.7	408.7
556	56.27	49.64	52.95	325.95	19.77	1.0833	818.5	0.7	573.0
568	66.2	56.1	61.15	334.15	20.16	1.0566	1112.8	0.7	779
576	76.68	63.25	69.97	342.97	20.58	1.0294	1313	0.7	919
605	77.07	60.94	69.00	342	20.53	1.0323	2052.3	0.7	1436.6
611	96.09	72.43	84.26	357.26	21.23	0.9882	2469.6	0.7	1728.7
617	112.57	82.26	97.42	370.42	21.82	0.9539	2691.5	0.7	1884
624	162.77	111.23	137.01	410.01	23.57	0.8608	2885.7	0.7	2020
629	86.21	66.51	76.35	349.35	20.87	1.0105	2275	0.7	1593
679	47.34	42.59	44.96	317.96	19.39	1.1105	656.7	0.7	459.7
686	55.94	48.42	52.17	325.17	19.73	1.0859	938.9	0.7	657.2
692	66.76	55.63	61.19	334.19	20.16	1.0565	1226	0.7	858
698	78.36	63.14	70.74	343.74	20.61	1.0271	1474	0.7	1032

TABLE F2

The (Mean of the Mean) Thermal Conductivities of
5.6mm and 11mm Thick Perspex Plates

Plate	Thermal Conductivity in W/M ^o C		
	Mean	Std Deviation	Error%
1	0.1940	.0008	0.41
2	0.1795	.0025	1.39
3	0.1911	.0077	4.03
4	0.1795	.0042	2.34
5	0.2003	.0071	3.54
6	0.2194	.0001	0.05
7	0.2088	.0049	2.35
8	0.2074	.0055	2.65

TABLE F3

Raw Experimental Data

Thermocouple Wires Numbers 1 to 9

	MILLIVOLTS READ IN FOR POSITIONS 1 TO 9 ARE								
1	1.977	1.979	1.977	1.980	1.980	1.979	1.978	1.979	1.979
2	1.979	1.983	1.980	1.983	1.984	1.983	1.982	1.983	1.983
3	1.981	1.983	1.981	1.984	1.985	1.984	1.984	1.985	1.984
4	1.984	1.986	1.984	1.986	1.987	1.986	1.986	1.987	1.986
5	1.984	1.987	1.984	1.987	1.988	1.987	1.986	1.988	1.987
6	1.986	1.987	1.985	1.988	1.989	1.988	1.987	1.988	1.988
7	1.986	1.988	1.985	1.988	1.989	1.988	1.987	1.989	1.989
8	1.989	1.992	1.989	1.992	1.993	1.993	1.991	1.993	1.993
9	1.988	1.990	1.987	1.989	1.990	1.989	1.989	1.990	1.989
10	1.989	1.990	1.987	1.989	1.990	1.989	1.988	1.990	1.988
11	1.989	1.990	1.989	1.991	1.992	1.990	1.989	1.991	1.990
12	1.989	1.991	1.988	1.991	1.993	1.991	1.990	1.991	1.990
13	1.989	1.990	1.988	1.992	1.993	1.991	1.990	1.992	1.992
14	1.988	1.990	1.988	1.991	1.993	1.991	1.990	1.991	1.991
15	1.988	1.989	1.988	1.990	1.991	1.990	1.989	1.991	1.990
16	1.988	1.989	1.987	1.989	1.992	1.991	1.989	1.991	1.990
17	1.988	1.989	1.988	1.990	1.991	1.990	1.989	1.991	1.991
18	1.989	1.991	1.989	1.991	1.992	1.992	1.989	1.991	1.990
19	1.989	1.991	1.989	1.991	1.992	1.991	1.989	1.991	1.991
20	1.988	1.990	1.987	1.990	1.990	1.990	1.988	1.990	1.990
21	1.988	1.989	1.988	1.990	1.992	1.990	1.989	1.991	1.990
22	1.989	1.993	1.990	1.991	1.993	1.992	1.990	1.993	1.991
23	1.992	1.994	1.992	1.993	1.994	1.994	1.991	1.993	1.993
24	1.992	1.993	1.992	1.994	1.995	1.994	1.993	1.994	1.994
25	1.991	1.993	1.991	1.993	1.995	1.994	1.993	1.994	1.994
26	1.991	1.993	1.991	1.993	1.994	1.993	1.992	1.994	1.993
27	1.991	1.994	1.991	1.994	1.995	1.993	1.991	1.994	1.993
28	1.991	1.993	1.991	1.993	1.994	1.993	1.991	1.993	1.993
29	1.462	1.463	1.463	1.463	1.463	1.464	1.464	1.464	1.464
30	1.459	1.459	1.459	1.460	1.460	1.460	1.460	1.460	1.460
31	1.451	1.452	1.452	1.453	1.454	1.454	1.454	1.455	1.455
32	1.450	1.448	1.448	1.448	1.448	1.448	1.448	1.448	1.449
33	1.448	1.448	1.447	1.448	1.448	1.448	1.448	1.448	1.448
34	1.434	1.436	1.435	1.436	1.436	1.436	1.436	1.436	1.436
35	1.436	1.438	1.438	1.438	1.438	1.438	1.438	1.438	1.438
36	1.438	1.438	1.438	1.438	1.438	1.438	1.438	1.438	1.438
37	1.438	1.439	1.439	1.439	1.439	1.439	1.439	1.439	1.439
38	1.439	1.439	1.439	1.440	1.440	1.440	1.440	1.440	1.440
39	1.440	1.441	1.441	1.441	1.441	1.441	1.441	1.441	1.441
40	1.440	1.441	1.441	1.441	1.441	1.441	1.441	1.441	1.441
41	1.441	1.441	1.441	1.441	1.441	1.441	1.441	1.441	1.441
42	1.442	1.443	1.443	1.443	1.443	1.443	1.443	1.443	1.443
43	2.388	2.389	2.386	2.389	2.390	2.389	2.388	2.389	2.388
44	2.386	2.388	2.388	2.388	2.389	2.388	2.387	2.389	2.388
45	2.386	2.388	2.385	2.388	2.389	2.389	2.387	2.388	2.388
46	2.386	2.388	2.385	2.388	2.389	2.388	2.387	2.389	2.388
47	2.386	2.388	2.384	2.389	2.389	2.388	2.387	2.389	2.389
48	2.386	2.389	2.384	2.389	2.389	2.389	2.387	2.389	2.387
49	2.385	2.386	2.383	2.388	2.389	2.389	2.385	2.386	2.387
50	2.391	2.393	2.390	2.394	2.395	2.394	2.392	2.394	2.394
51	2.389	2.391	2.389	2.393	2.394	2.393	2.391	2.393	2.391
52	2.389	2.392	2.389	2.391	2.393	2.393	2.390	2.393	2.391
53	2.389	2.390	2.387	2.391	2.391	2.390	2.389	2.391	2.390
54	2.387	2.389	2.386	2.389	2.390	2.389	2.388	2.389	2.389
55	2.387	2.389	2.387	2.389	2.390	2.389	2.389	2.389	2.389
56	2.029	2.030	2.028	2.030	2.031	2.030	2.029	2.030	2.030
57	2.024	2.026	2.024	2.026	2.027	2.026	2.025	2.027	2.025
58	2.020	2.021	2.019	2.022	2.023	2.023	2.020	2.022	2.020
59	2.017	2.019	2.017	2.019	2.020	2.020	2.019	2.020	2.019
60	2.016	2.017	2.015	2.018	2.018	2.018	2.017	2.018	2.017
61	2.038	2.039	2.037	2.040	2.040	2.039	2.039	2.040	2.039
62	2.032	2.034	2.032	2.035	2.036	2.034	2.033	2.034	2.034
63	2.029	2.030	2.029	2.031	2.032	2.031	2.030	2.031	2.030
64	2.028	2.029	2.028	2.029	2.031	2.029	2.029	2.030	2.029
65	2.027	2.029	2.026	2.029	2.029	2.029	2.028	2.029	2.029
66	2.023	2.024	2.022	2.025	2.026	2.025	2.024	2.026	2.024
67	2.023	2.023	2.021	2.023	2.025	2.024	2.023	2.024	2.024
68	2.021	2.022	2.021	2.023	2.024	2.024	2.023	2.024	2.022
69	2.018	2.019	2.017	2.018	2.019	2.018	2.017	2.018	2.017
70	2.015	2.017	2.014	2.017	2.018	2.017	2.016	2.017	2.016
71	2.013	2.014	2.013	2.015	2.016	2.015	2.014	2.015	2.014
72	2.011	2.013	2.011	2.014	2.014	2.013	2.013	2.014	2.013

TABLE F3 (continued)

73	2.010	2.012	2.011	2.013	2.014	2.013	2.013	2.013	2.013
74	2.009	2.010	2.009	2.010	2.011	2.010	2.010	2.010	2.010
75	2.006	2.007	2.004	2.007	2.008	2.006	2.005	2.006	2.006
76	2.006	2.007	2.004	2.006	2.008	2.007	2.007	2.007	2.007
77	2.006	2.007	2.005	2.008	2.008	2.007	2.006	2.007	2.006
78	2.000	2.000	1.998	2.001	2.001	2.001	2.000	2.000	2.000
79	2.000	2.002	2.001	2.003	2.004	2.003	2.002	2.003	2.002
80	2.001	2.003	2.001	2.004	2.004	2.003	2.002	2.002	2.002
81	1.959	1.961	1.959	1.961	1.961	1.961	1.959	1.960	1.959
82	1.945	1.947	1.945	1.946	1.948	1.946	1.946	1.948	1.947
83	1.952	1.954	1.952	1.955	1.956	1.954	1.952	1.954	1.953
84	1.950	1.952	1.949	1.951	1.952	1.951	1.950	1.951	1.950
85	1.945	1.947	1.945	1.947	1.948	1.946	1.945	1.947	1.945
86	1.944	1.946	1.943	1.946	1.948	1.946	1.945	1.946	1.945
87	1.944	1.946	1.943	1.947	1.948	1.946	1.944	1.946	1.946
88	1.962	1.967	1.964	1.966	1.968	1.966	1.964	1.967	1.965
89	1.957	1.959	1.950	1.959	1.960	1.959	1.958	1.959	1.958
90	1.950	1.952	1.950	1.952	1.953	1.952	1.951	1.952	1.952
91	1.949	1.951	1.949	1.951	1.952	1.951	1.949	1.951	1.950
92	1.949	1.950	1.949	1.950	1.951	1.950	1.949	1.950	1.950
93	1.953	1.955	1.952	1.955	1.956	1.955	1.953	1.955	1.955
94	1.430	1.431	1.430	1.430	1.430	1.430	1.430	1.430	1.430
95	1.434	1.435	1.434	1.436	1.436	1.436	1.435	1.435	1.435
96	1.433	1.434	1.434	1.434	1.435	1.435	1.435	1.435	1.435
97	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440
98	1.439	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440
99	1.438	1.439	1.439	1.439	1.439	1.440	1.440	1.440	1.440
100	1.438	1.439	1.439	1.439	1.439	1.439	1.439	1.439	1.439
101	1.430	1.431	1.431	1.431	1.431	1.431	1.430	1.431	1.431
102	1.435	1.437	1.437	1.437	1.437	1.437	1.437	1.437	1.437
103	1.435	1.438	1.438	1.438	1.438	1.438	1.438	1.438	1.438
104	1.435	1.437	1.437	1.438	1.438	1.438	1.438	1.438	1.438
105	1.434	1.437	1.437	1.437	1.438	1.438	1.438	1.438	1.438
106	1.434	1.434	1.434	1.435	1.435	1.435	1.435	1.435	1.435
107	2.327	2.329	2.327	2.329	2.330	2.329	2.327	2.329	2.329
108	2.321	2.325	2.321	2.324	2.326	2.324	2.324	2.324	2.323
109	2.316	2.319	2.314	2.319	2.320	2.319	2.316	2.319	2.316
110	2.330	2.332	2.330	2.332	2.334	2.333	2.330	2.332	2.331
111	2.322	2.327	2.321	2.325	2.328	2.327	2.323	2.326	2.323
112	2.317	2.320	2.316	2.319	2.320	2.320	2.318	2.319	2.319
113	2.311	2.314	2.310	2.313	2.316	2.314	2.311	2.314	2.312
114	2.308	2.309	2.307	2.309	2.310	2.309	2.308	2.309	2.309
115	2.308	2.307	2.302	2.306	2.309	2.307	2.303	2.307	2.304
116	2.300	2.303	2.300	2.302	2.304	2.303	2.300	2.303	2.302
117	2.298	2.300	2.299	2.300	2.301	2.300	2.299	2.300	2.299
118	2.291	2.294	2.290	2.293	2.295	2.294	2.291	2.294	2.293
119	2.290	2.293	2.289	2.292	2.294	2.293	2.290	2.292	2.291
120	1.993	1.995	1.992	1.995	1.996	1.996	1.993	1.995	1.994
121	1.989	1.991	1.990	1.991	1.992	1.991	1.990	1.991	1.991
122	1.984	1.987	1.983	1.988	1.988	1.987	1.985	1.988	1.986
123	1.980	1.981	1.980	1.981	1.981	1.981	1.981	1.981	1.980
124	1.974	1.976	1.973	1.976	1.977	1.977	1.974	1.976	1.975
125	1.971	1.972	1.970	1.972	1.973	1.972	1.971	1.972	1.971
126	1.969	1.970	1.969	1.970	1.971	1.970	1.970	1.970	1.970
127	1.970	1.971	1.969	1.971	1.971	1.971	1.970	1.971	1.971
128	1.990	1.991	1.989	1.991	1.991	1.991	1.990	1.991	1.990
129	1.988	1.989	1.987	1.989	1.990	1.989	1.989	1.989	1.989
130	1.983	1.987	1.983	1.987	1.988	1.987	1.986	1.987	1.986
131	1.980	1.981	1.980	1.981	1.982	1.981	1.980	1.981	1.981
132	1.974	1.975	1.972	1.976	1.977	1.976	1.973	1.976	1.975
133	1.977	1.978	1.975	1.979	1.979	1.978	1.978	1.979	1.978
134	1.973	1.974	1.971	1.975	1.977	1.974	1.974	1.975	1.974
135	1.970	1.971	1.970	1.972	1.972	1.972	1.971	1.972	1.971
136	1.977	1.979	1.975	1.979	1.979	1.979	1.978	1.979	1.978
137	1.971	1.973	1.970	1.973	1.974	1.973	1.971	1.973	1.972
138	1.955	1.958	1.954	1.958	1.959	1.959	1.958	1.959	1.959
139	1.978	1.979	1.977	1.979	1.980	1.979	1.979	1.979	1.979
140	1.974	1.976	1.973	1.977	1.978	1.976	1.976	1.977	1.975
141	1.969	1.970	1.969	1.970	1.970	1.970	1.970	1.970	1.970
142	1.964	1.965	1.963	1.967	1.968	1.966	1.965	1.967	1.965
143	1.959	1.960	1.959	1.960	1.961	1.960	1.960	1.961	1.960
144	1.955	1.956	1.953	1.958	1.958	1.957	1.955	1.958	1.957
145	1.953	1.954	1.952	1.956	1.957	1.955	1.955	1.956	1.955
146	1.954	1.957	1.954	1.956	1.958	1.957	1.954	1.957	1.956
147	1.951	1.954	1.952	1.953	1.957	1.955	1.953	1.955	1.953
148	1.948	1.949	1.948	1.949	1.950	1.949	1.949	1.950	1.950
149	1.947	1.949	1.948	1.949	1.950	1.950	1.949	1.950	1.950

TABLE F3 (continued)

150	1.945	1.949	1.946	1.948	1.949	1.948	1.947	1.948	1.949
151	1.945	1.947	1.944	1.947	1.949	1.948	1.946	1.948	1.948
152	1.942	1.945	1.944	1.945	1.947	1.947	1.945	1.947	1.947
153	1.941	1.944	1.942	1.945	1.946	1.945	1.943	1.946	1.945
154	1.940	1.942	1.941	1.942	1.944	1.942	1.941	1.943	1.942
155	1.941	1.943	1.941	1.942	1.944	1.944	1.942	1.943	1.943
156	1.941	1.942	1.941	1.942	1.943	1.942	1.941	1.943	1.942
157	1.955	1.958	1.956	1.958	1.959	1.955	1.957	1.956	1.958
158	1.951	1.953	1.951	1.953	1.955	1.954	1.952	1.953	1.953
159	1.950	1.952	1.949	1.951	1.952	1.951	1.949	1.951	1.950
160	1.947	1.948	1.946	1.948	1.949	1.948	1.947	1.948	1.948
161	1.942	1.944	1.942	1.943	1.944	1.943	1.942	1.943	1.943
162	1.939	1.939	1.937	1.939	1.940	1.939	1.938	1.939	1.939
163	1.937	1.939	1.936	1.938	1.939	1.938	1.936	1.938	1.938
164	1.933	1.934	1.932	1.934	1.936	1.934	1.931	1.934	1.933
165	1.930	1.931	1.930	1.931	1.931	1.931	1.930	1.931	1.930
166	1.925	1.927	1.924	1.926	1.928	1.925	1.924	1.926	1.925
167	1.924	1.925	1.922	1.926	1.927	1.925	1.923	1.924	1.923
168	1.920	1.921	1.919	1.921	1.921	1.921	1.919	1.921	1.920
169	1.920	1.921	1.919	1.920	1.921	1.920	1.920	1.921	1.920
170	1.922	1.924	1.921	1.923	1.925	1.923	1.921	1.923	1.922
171	1.922	1.924	1.921	1.924	1.924	1.924	1.922	1.923	1.923
172	1.416	1.417	1.418	1.417	1.418	1.418	1.417	1.417	1.417
173	1.413	1.414	1.413	1.413	1.414	1.413	1.414	1.414	1.414
174	1.410	1.410	1.410	1.410	1.410	1.410	1.410	1.410	1.410
175	1.409	1.409	1.409	1.409	1.409	1.409	1.409	1.409	1.409
176	1.408	1.408	1.408	1.408	1.409	1.409	1.409	1.409	1.408
177	1.406	1.407	1.407	1.407	1.407	1.407	1.407	1.407	1.407
178	1.406	1.407	1.407	1.407	1.407	1.407	1.407	1.407	1.407
179	1.407	1.408	1.406	1.406	1.407	1.407	1.407	1.407	1.407
180	1.406	1.407	1.407	1.407	1.407	1.407	1.407	1.407	1.407
181	1.406	1.409	1.408	1.408	1.408	1.408	1.408	1.408	1.408
182	1.407	1.407	1.408	1.408	1.408	1.408	1.408	1.408	1.408
183	1.407	1.408	1.408	1.408	1.408	1.408	1.408	1.408	1.408
184	1.403	1.408	1.408	1.408	1.408	1.408	1.408	1.408	1.408
185	2.261	2.263	2.259	2.261	2.262	2.261	2.259	2.261	2.261
186	2.267	2.269	2.264	2.268	2.269	2.268	2.266	2.269	2.268
187	2.265	2.268	2.263	2.268	2.269	2.267	2.264	2.268	2.266
188	2.288	2.289	2.285	2.288	2.289	2.288	2.287	2.289	2.288
189	2.271	2.274	2.270	2.273	2.274	2.273	2.270	2.273	2.272
190	2.309	2.311	2.308	2.310	2.312	2.311	2.308	2.310	2.310
191	2.300	2.302	2.299	2.302	2.303	2.301	2.299	2.301	2.300
192	2.293	2.295	2.291	2.294	2.297	2.294	2.292	2.294	2.293
193	2.276	2.279	2.274	2.278	2.279	2.277	2.274	2.278	2.276
194	2.271	2.273	2.270	2.271	2.273	2.272	2.270	2.272	2.271
195	2.268	2.269	2.265	2.269	2.270	2.269	2.267	2.269	2.268
196	2.265	2.266	2.263	2.268	2.268	2.268	2.264	2.268	2.267
197	2.267	2.269	2.264	2.268	2.269	2.268	2.265	2.268	2.268
198	1.940	1.942	1.940	1.941	1.943	1.941	1.940	1.942	1.942
199	1.938	1.940	1.938	1.939	1.940	1.939	1.938	1.939	1.939
200	1.934	1.938	1.934	1.937	1.938	1.937	1.934	1.938	1.937
201	1.932	1.934	1.931	1.932	1.934	1.934	1.931	1.934	1.933
202	1.930	1.931	1.930	1.931	1.932	1.931	1.930	1.932	1.931
203	1.928	1.930	1.928	1.929	1.930	1.930	1.929	1.930	1.929
204	1.929	1.929	1.927	1.929	1.930	1.929	1.929	1.929	1.929
205	1.927	1.928	1.926	1.928	1.929	1.929	1.927	1.929	1.929
206	1.926	1.928	1.925	1.927	1.928	1.928	1.925	1.928	1.928
207	1.924	1.926	1.923	1.925	1.927	1.925	1.923	1.925	1.925
208	1.923	1.926	1.923	1.924	1.926	1.925	1.923	1.925	1.924
209	1.922	1.925	1.922	1.923	1.925	1.924	1.922	1.924	1.924
210	1.919	1.920	1.919	1.920	1.920	1.920	1.919	1.920	1.920
211	1.925	1.927	1.924	1.927	1.928	1.926	1.925	1.927	1.927
212	1.928	1.929	1.926	1.929	1.929	1.928	1.928	1.928	1.928
213	1.927	1.928	1.925	1.928	1.928	1.927	1.926	1.927	1.927
214	1.927	1.928	1.925	1.928	1.928	1.927	1.926	1.927	1.927
215	1.927	1.928	1.925	1.928	1.928	1.927	1.926	1.927	1.928
216	1.948	1.949	1.947	1.948	1.949	1.948	1.948	1.948	1.948
217	1.942	1.944	1.942	1.943	1.944	1.943	1.942	1.944	1.943
218	1.940	1.941	1.939	1.941	1.942	1.941	1.940	1.941	1.940
219	1.937	1.939	1.938	1.939	1.939	1.939	1.938	1.939	1.939
220	1.933	1.935	1.932	1.934	1.936	1.934	1.932	1.934	1.934
221	1.932	1.933	1.932	1.934	1.934	1.934	1.932	1.933	1.933
222	1.930	1.931	1.930	1.931	1.932	1.930	1.930	1.931	1.931
223	1.928	1.929	1.927	1.928	1.929	1.928	1.927	1.929	1.928
224	1.921	1.923	1.921	1.922	1.923	1.921	1.922	1.923	1.922
225	1.922	1.923	1.921	1.922	1.923	1.922	1.921	1.922	1.922
226	1.920	1.921	1.919	1.920	1.921	1.920	1.920	1.921	1.920

TABLE F3 (continued)

227	1.922	1.923	1.921	1.922	1.923	1.922	1.921	1.922	1.922
228	1.922	1.923	1.921	1.922	1.923	1.923	1.922	1.922	1.922
229	1.918	1.919	1.916	1.918	1.919	1.918	1.917	1.916	1.918
230	1.919	1.919	1.918	1.919	1.920	1.919	1.919	1.919	1.919
231	1.918	1.920	1.918	1.920	1.920	1.919	1.919	1.919	1.919
232	1.922	1.923	1.922	1.923	1.924	1.923	1.922	1.923	1.923
233	1.923	1.924	1.923	1.924	1.925	1.924	1.923	1.925	1.924
234	1.924	1.926	1.923	1.926	1.927	1.926	1.924	1.925	1.925
235	1.923	1.925	1.922	1.924	1.925	1.924	1.924	1.924	1.924
236	1.925	1.925	1.924	1.927	1.927	1.926	1.924	1.927	1.927
237	1.919	1.920	1.918	1.920	1.920	1.920	1.919	1.920	1.919
238	1.914	1.915	1.912	1.916	1.917	1.916	1.914	1.916	1.915
239	1.911	1.912	1.910	1.912	1.913	1.912	1.911	1.912	1.911
240	1.910	1.911	1.909	1.911	1.911	1.910	1.910	1.910	1.910
241	1.918	1.919	1.917	1.919	1.919	1.918	1.918	1.918	1.918
242	1.918	1.919	1.917	1.919	1.920	1.919	1.918	1.919	1.918
243	1.917	1.918	1.917	1.919	1.920	1.919	1.918	1.919	1.918
244	1.918	1.919	1.917	1.919	1.919	1.918	1.917	1.919	1.918
245	1.918	1.919	1.918	1.919	1.920	1.919	1.918	1.919	1.919
246	1.919	1.919	1.917	1.919	1.920	1.920	1.919	1.919	1.919
247	1.918	1.919	1.917	1.919	1.920	1.919	1.919	1.919	1.919
248	1.919	1.920	1.918	1.920	1.920	1.920	1.919	1.919	1.919
249	1.919	1.920	1.918	1.920	1.920	1.920	1.919	1.920	1.919
250	1.407	1.409	1.407	1.407	1.407	1.408	1.408	1.408	1.408
251	1.407	1.408	1.408	1.408	1.408	1.408	1.408	1.408	1.408
252	1.407	1.408	1.407	1.407	1.407	1.407	1.407	1.407	1.407
253	1.407	1.407	1.406	1.406	1.407	1.407	1.407	1.407	1.407
254	1.405	1.406	1.405	1.407	1.407	1.407	1.407	1.407	1.407
255	1.404	1.404	1.403	1.404	1.404	1.404	1.404	1.404	1.404
256	1.404	1.404	1.403	1.404	1.404	1.404	1.404	1.404	1.404
257	1.403	1.404	1.403	1.403	1.403	1.403	1.403	1.403	1.403
258	1.403	1.404	1.403	1.403	1.403	1.403	1.403	1.403	1.403
259	1.401	1.402	1.401	1.401	1.402	1.402	1.401	1.401	1.401
260	1.401	1.402	1.402	1.402	1.402	1.402	1.402	1.402	1.402
261	1.401	1.402	1.402	1.402	1.402	1.402	1.402	1.402	1.402
262	1.401	1.402	1.402	1.402	1.402	1.402	1.402	1.402	1.402
263	2.260	2.262	2.260	2.262	2.263	2.262	2.261	2.262	2.261
264	2.262	2.264	2.260	2.263	2.265	2.263	2.262	2.263	2.262
265	2.267	2.269	2.264	2.268	2.269	2.268	2.267	2.268	2.268
266	2.267	2.269	2.266	2.269	2.270	2.269	2.267	2.269	2.268
267	2.268	2.270	2.267	2.270	2.270	2.269	2.268	2.269	2.268
268	2.269	2.270	2.269	2.270	2.271	2.270	2.268	2.270	2.269
269	2.269	2.270	2.267	2.270	2.271	2.270	2.268	2.269	2.269
270	2.270	2.271	2.269	2.271	2.272	2.270	2.270	2.271	2.270
271	2.270	2.272	2.269	2.271	2.272	2.271	2.270	2.271	2.270
272	2.270	2.272	2.269	2.272	2.273	2.271	2.270	2.271	2.270
273	2.270	2.273	2.269	2.272	2.273	2.272	2.270	2.271	2.270
274	2.269	2.271	2.268	2.270	2.272	2.270	2.269	2.270	2.269
275	2.269	2.270	2.268	2.270	2.271	2.270	2.269	2.270	2.269
276	1.956	1.958	1.955	1.958	1.959	1.958	1.956	1.958	1.957
277	1.954	1.957	1.954	1.957	1.957	1.957	1.954	1.955	1.955
278	1.953	1.956	1.953	1.956	1.957	1.956	1.954	1.956	1.954
279	1.952	1.953	1.951	1.953	1.954	1.952	1.953	1.953	1.952
280	1.950	1.952	1.950	1.952	1.952	1.952	1.951	1.952	1.952
281	1.950	1.950	1.949	1.950	1.951	1.950	1.949	1.950	1.950
282	1.948	1.949	1.948	1.949	1.950	1.949	1.949	1.949	1.949
283	1.942	1.944	1.941	1.943	1.944	1.943	1.942	1.943	1.943
284	1.943	1.944	1.942	1.944	1.945	1.944	1.943	1.944	1.943
285	1.943	1.944	1.942	1.943	1.944	1.943	1.942	1.943	1.942
286	1.943	1.946	1.944	1.947	1.947	1.946	1.945	1.946	1.945
287	1.945	1.948	1.944	1.948	1.948	1.948	1.946	1.947	1.947
288	1.946	1.948	1.945	1.948	1.948	1.948	1.947	1.947	1.947
289	1.932	1.933	1.931	1.933	1.933	1.932	1.931	1.932	1.932
290	1.932	1.935	1.931	1.934	1.935	1.934	1.933	1.934	1.933
291	1.932	1.933	1.931	1.933	1.934	1.932	1.932	1.933	1.932
292	1.931	1.932	1.930	1.933	1.933	1.932	1.932	1.932	1.932
293	1.953	1.954	1.952	1.955	1.956	1.954	1.953	1.954	1.954
294	1.951	1.952	1.950	1.953	1.954	1.952	1.952	1.953	1.952
295	1.948	1.949	1.947	1.949	1.950	1.949	1.948	1.949	1.949
296	1.944	1.946	1.943	1.947	1.946	1.946	1.944	1.945	1.944
297	1.941	1.942	1.940	1.942	1.942	1.942	1.941	1.942	1.941
298	1.932	1.932	1.930	1.933	1.933	1.932	1.931	1.932	1.931
299	1.931	1.933	1.930	1.933	1.933	1.931	1.931	1.932	1.931
300	1.930	1.931	1.929	1.931	1.931	1.930	1.930	1.931	1.930
301	1.930	1.931	1.929	1.931	1.931	1.930	1.930	1.930	1.930
302	1.921	1.923	1.921	1.922	1.924	1.922	1.921	1.922	1.922
303	1.921	1.923	1.921	1.923	1.924	1.923	1.921	1.922	1.922

TABLE F3 (continued)

304	1.920	1.920	1.919	1.920	1.920	1.920	1.919	1.920	1.919
305	1.919	1.920	1.919	1.920	1.920	1.920	1.919	1.920	1.920
306	1.920	1.920	1.919	1.920	1.920	1.920	1.919	1.920	1.920
307	1.911	1.913	1.911	1.912	1.913	1.913	1.911	1.912	1.912
308	1.911	1.913	1.911	1.912	1.913	1.912	1.911	1.912	1.912
309	1.911	1.913	1.911	1.913	1.914	1.914	1.911	1.913	1.913
310	1.912	1.914	1.912	1.914	1.916	1.917	1.913	1.914	1.913
311	1.913	1.916	1.913	1.917	1.918	1.917	1.915	1.917	1.915
312	1.914	1.917	1.914	1.917	1.918	1.917	1.914	1.917	1.915
313	1.914	1.917	1.914	1.917	1.918	1.915	1.914	1.915	1.915
314	1.914	1.917	1.913	1.915	1.917	1.915	1.913	1.914	1.914
315	1.953	1.954	1.952	1.954	1.955	1.953	1.953	1.953	1.953
316	1.953	1.957	1.953	1.957	1.957	1.956	1.954	1.956	1.955
317	1.957	1.959	1.957	1.958	1.959	1.958	1.957	1.958	1.958
318	1.957	1.959	1.957	1.959	1.959	1.959	1.958	1.958	1.958
319	1.958	1.959	1.958	1.959	1.959	1.959	1.958	1.958	1.958
320	1.959	1.960	1.958	1.960	1.960	1.959	1.959	1.959	1.959
321	1.959	1.960	1.959	1.960	1.961	1.960	1.959	1.960	1.959
322	1.960	1.961	1.960	1.961	1.962	1.961	1.960	1.961	1.961
323	1.960	1.962	1.960	1.962	1.963	1.961	1.960	1.961	1.961
324	1.961	1.962	1.960	1.961	1.962	1.961	1.960	1.961	1.960
325	1.961	1.962	1.960	1.961	1.962	1.961	1.961	1.961	1.961
326	1.965	1.966	1.963	1.966	1.967	1.966	1.964	1.965	1.964
327	1.966	1.968	1.964	1.968	1.968	1.968	1.967	1.968	1.968
328	1.424	1.424	1.424	1.424	1.424	1.424	1.424	1.424	1.424
329	1.424	1.424	1.424	1.424	1.424	1.424	1.424	1.424	1.424
330	1.422	1.423	1.423	1.423	1.424	1.424	1.424	1.424	1.424
331	1.423	1.423	1.423	1.423	1.423	1.423	1.423	1.423	1.423
332	1.423	1.423	1.423	1.423	1.423	1.424	1.424	1.424	1.424
333	1.423	1.423	1.423	1.423	1.424	1.424	1.424	1.424	1.424
334	1.423	1.423	1.423	1.423	1.424	1.424	1.424	1.424	1.424
335	1.422	1.422	1.422	1.422	1.422	1.423	1.423	1.422	1.422
336	1.423	1.423	1.423	1.423	1.423	1.423	1.423	1.423	1.423
337	1.422	1.423	1.423	1.423	1.423	1.423	1.423	1.423	1.423
338	1.423	1.423	1.422	1.422	1.422	1.422	1.422	1.422	1.422
339	1.422	1.424	1.422	1.423	1.424	1.424	1.423	1.424	1.424
340	1.423	1.424	1.423	1.423	1.423	1.423	1.423	1.423	1.423
341	2.358	2.359	2.356	2.359	2.360	2.359	2.357	2.358	2.358
342	2.349	2.351	2.349	2.351	2.352	2.350	2.349	2.350	2.349
343	2.344	2.348	2.342	2.346	2.346	2.346	2.343	2.346	2.344
344	2.337	2.339	2.335	2.339	2.339	2.339	2.337	2.339	2.338
345	2.333	2.337	2.332	2.335	2.338	2.334	2.334	2.335	2.334
346	2.331	2.333	2.330	2.332	2.333	2.331	2.330	2.332	2.331
347	2.330	2.331	2.329	2.331	2.331	2.330	2.329	2.330	2.330
348	2.323	2.327	2.321	2.326	2.327	2.325	2.323	2.325	2.323
349	2.324	2.327	2.322	2.327	2.328	2.327	2.324	2.325	2.323
350	2.323	2.328	2.322	2.326	2.328	2.325	2.324	2.325	2.324
351	2.324	2.327	2.322	2.328	2.328	2.327	2.323	2.325	2.324
352	2.325	2.328	2.324	2.328	2.329	2.327	2.324	2.327	2.326
353	2.328	2.329	2.326	2.329	2.330	2.329	2.328	2.329	2.328
354	1.981	1.982	1.981	1.982	1.983	1.982	1.981	1.982	1.982
355	1.979	1.980	1.979	1.980	1.981	1.980	1.979	1.980	1.980
356	1.978	1.979	1.978	1.979	1.980	1.979	1.979	1.979	1.979
357	1.975	1.978	1.975	1.978	1.978	1.977	1.976	1.977	1.975
358	1.973	1.975	1.972	1.975	1.976	1.974	1.972	1.974	1.974
359	1.970	1.972	1.970	1.972	1.972	1.972	1.970	1.971	1.971
360	1.970	1.971	1.970	1.971	1.972	1.971	1.970	1.971	1.970
361	1.969	1.969	1.967	1.969	1.969	1.969	1.968	1.969	1.968
362	1.969	1.970	1.968	1.970	1.970	1.969	1.969	1.969	1.969
363	1.969	1.970	1.968	1.970	1.970	1.969	1.968	1.969	1.969
364	1.964	1.966	1.963	1.967	1.967	1.967	1.963	1.964	1.964
365	1.964	1.968	1.964	1.967	1.968	1.967	1.966	1.967	1.967
366	1.964	1.967	1.964	1.967	1.969	1.968	1.965	1.967	1.967
367	1.945	1.948	1.944	1.947	1.948	1.947	1.944	1.946	1.946
368	1.946	1.949	1.947	1.949	1.949	1.948	1.947	1.949	1.948
369	1.949	1.950	1.949	1.950	1.950	1.949	1.949	1.949	1.949
370	1.949	1.950	1.949	1.950	1.951	1.950	1.950	1.950	1.950
371	1.949	1.951	1.950	1.951	1.951	1.951	1.949	1.950	1.950
372	1.951	1.953	1.951	1.952	1.953	1.953	1.951	1.952	1.952
373	1.951	1.954	1.952	1.953	1.954	1.954	1.952	1.953	1.952
374	1.952	1.954	1.951	1.953	1.954	1.953	1.952	1.953	1.952
375	1.951	1.953	1.951	1.953	1.953	1.953	1.951	1.951	1.952
376	1.950	1.952	1.950	1.951	1.952	1.951	1.950	1.950	1.950
377	1.950	1.952	1.950	1.951	1.952	1.952	1.950	1.951	1.951
378	1.951	1.952	1.950	1.951	1.952	1.951	1.950	1.951	1.951
379	1.951	1.953	1.951	1.952	1.953	1.952	1.951	1.952	1.952
380	1.979	1.979	1.978	1.979	1.980	1.979	1.978	1.979	1.979

TABLE F3 (continued)

381	1.975	1.978	1.975	1.978	1.979	1.978	1.975	1.977	1.977
382	1.971	1.974	1.971	1.973	1.974	1.972	1.971	1.973	1.972
383	1.970	1.971	1.970	1.970	1.971	1.970	1.969	1.970	1.970
384	1.969	1.970	1.968	1.969	1.970	1.969	1.968	1.969	1.969
385	1.964	1.967	1.963	1.964	1.967	1.964	1.963	1.964	1.964
386	1.962	1.964	1.962	1.964	1.965	1.963	1.962	1.963	1.963
387	1.962	1.964	1.962	1.963	1.964	1.963	1.961	1.962	1.962
388	1.961	1.962	1.961	1.962	1.962	1.961	1.960	1.962	1.961
389	1.960	1.961	1.960	1.960	1.961	1.960	1.959	1.960	1.960
390	1.957	1.958	1.954	1.957	1.958	1.957	1.953	1.956	1.955
391	1.957	1.958	1.958	1.958	1.959	1.958	1.954	1.957	1.957
392	1.957	1.958	1.955	1.958	1.958	1.957	1.954	1.957	1.956
393	1.958	1.959	1.957	1.959	1.959	1.959	1.958	1.959	1.958
394	1.959	1.960	1.959	1.960	1.961	1.960	1.959	1.960	1.960
395	1.960	1.961	1.960	1.961	1.962	1.961	1.960	1.961	1.961
396	1.962	1.964	1.961	1.963	1.964	1.963	1.962	1.962	1.962
397	1.962	1.963	1.961	1.962	1.963	1.962	1.961	1.962	1.962
398	1.964	1.967	1.963	1.966	1.968	1.966	1.964	1.967	1.964
399	1.967	1.969	1.967	1.969	1.969	1.968	1.967	1.968	1.968
400	1.968	1.969	1.968	1.969	1.970	1.969	1.967	1.969	1.969
401	1.969	1.970	1.969	1.970	1.970	1.970	1.969	1.969	1.969
402	1.969	1.971	1.969	1.970	1.971	1.970	1.969	1.970	1.970
403	1.971	1.972	1.970	1.971	1.972	1.971	1.970	1.971	1.971
404	1.971	1.972	1.970	1.972	1.972	1.971	1.970	1.971	1.971
405	1.970	1.971	1.969	1.970	1.971	1.970	1.969	1.970	1.970
406	2.321	2.323	2.321	2.323	2.324	2.322	2.320	2.322	2.321
407	2.323	2.328	2.323	2.327	2.328	2.326	2.323	2.326	2.323
408	2.324	2.329	2.323	2.328	2.329	2.326	2.324	2.328	2.326
409	2.328	2.330	2.328	2.329	2.330	2.329	2.328	2.329	2.328
410	2.329	2.331	2.328	2.330	2.331	2.330	2.328	2.330	2.329
411	2.329	2.331	2.329	2.330	2.332	2.330	2.329	2.330	2.330
412	2.329	2.331	2.329	2.330	2.332	2.330	2.329	2.330	2.329
413	2.330	2.332	2.330	2.332	2.333	2.332	2.330	2.331	2.331
414	2.331	2.333	2.330	2.332	2.334	2.332	2.331	2.332	2.331
415	2.331	2.334	2.331	2.333	2.337	2.334	2.331	2.333	2.332
416	2.332	2.337	2.332	2.334	2.338	2.336	2.332	2.336	2.334
417	2.333	2.338	2.332	2.337	2.338	2.338	2.333	2.336	2.335
418	1.435	1.435	1.434	1.434	1.434	1.434	1.434	1.434	1.434
419	1.432	1.432	1.432	1.433	1.433	1.432	1.433	1.433	1.432
420	1.431	1.431	1.431	1.431	1.431	1.431	1.431	1.431	1.431
421	1.430	1.430	1.430	1.430	1.430	1.430	1.430	1.430	1.430
422	1.429	1.429	1.429	1.429	1.429	1.429	1.429	1.429	1.429
423	1.427	1.427	1.426	1.426	1.427	1.426	1.427	1.426	1.426
424	1.425	1.426	1.424	1.425	1.427	1.425	1.425	1.425	1.425
425	1.424	1.426	1.424	1.426	1.426	1.426	1.425	1.425	1.425
426	1.423	1.423	1.423	1.423	1.423	1.423	1.423	1.423	1.423
427	1.421	1.421	1.421	1.421	1.421	1.421	1.421	1.421	1.421
428	1.422	1.422	1.421	1.421	1.421	1.421	1.421	1.421	1.421
429	1.422	1.422	1.422	1.422	1.421	1.421	1.421	1.421	1.421
430	1.421	1.421	1.421	1.421	1.421	1.421	1.421	1.421	1.421
431	1.968	1.969	1.968	1.969	1.970	1.969	1.967	1.968	1.967
432	1.968	1.970	1.968	1.969	1.970	1.969	1.967	1.969	1.969
433	1.968	1.969	1.968	1.969	1.969	1.969	1.967	1.968	1.968
434	1.967	1.969	1.967	1.968	1.969	1.969	1.967	1.968	1.967
435	1.966	1.968	1.964	1.967	1.968	1.967	1.965	1.968	1.965
436	1.960	1.961	1.960	1.960	1.961	1.960	1.959	1.960	1.960
437	1.960	1.961	1.960	1.961	1.961	1.961	1.959	1.960	1.960
438	1.960	1.961	1.960	1.961	1.962	1.961	1.960	1.961	1.961
439	1.960	1.962	1.960	1.961	1.963	1.962	1.961	1.961	1.961
440	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
441	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
442	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
443	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
444	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
445	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
446	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
447	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
448	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
449	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
450	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
451	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
452	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
453	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
454	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
455	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
456	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961
457	1.961	1.962	1.961	1.961	1.963	1.962	1.961	1.961	1.961

TABLE F3 (continued)

458	1.953	1.958	1.953	1.958	1.959	1.958	1.953	1.957	1.956
459	1.954	1.959	1.954	1.957	1.959	1.958	1.954	1.958	1.958
460	1.955	1.959	1.953	1.958	1.959	1.959	1.954	1.958	1.958
461	1.954	1.958	1.953	1.958	1.960	1.960	1.954	1.958	1.957
462	1.954	1.958	1.953	1.958	1.960	1.960	1.954	1.958	1.958
463	1.956	1.959	1.956	1.959	1.960	1.960	1.956	1.958	1.958
464	1.958	1.959	1.957	1.959	1.960	1.960	1.958	1.958	1.959
465	1.957	1.959	1.954	1.959	1.960	1.960	1.956	1.959	1.959
466	1.958	1.959	1.957	1.958	1.960	1.960	1.958	1.959	1.959
467	1.957	1.959	1.957	1.959	1.960	1.960	1.957	1.959	1.959
468	1.958	1.959	1.956	1.959	1.960	1.960	1.955	1.959	1.959
469	1.958	1.959	1.955	1.956	1.960	1.960	1.955	1.959	1.958
470	1.954	1.958	1.952	1.955	1.958	1.958	1.952	1.957	1.955
471	1.993	1.997	1.992	1.995	1.997	1.994	1.991	1.994	1.993
472	1.991	1.994	1.990	1.992	1.994	1.992	1.990	1.992	1.991
473	1.989	1.990	1.988	1.989	1.990	1.989	1.985	1.989	1.986
474	1.988	1.989	1.985	1.988	1.990	1.988	1.985	1.988	1.987
475	1.987	1.989	1.984	1.988	1.989	1.987	1.984	1.988	1.987
476	1.985	1.988	1.984	1.988	1.988	1.987	1.983	1.986	1.987
477	1.984	1.988	1.982	1.986	1.988	1.984	1.982	1.985	1.983
478	1.982	1.987	1.981	1.984	1.986	1.984	1.981	1.984	1.983
479	1.982	1.986	1.982	1.983	1.987	1.984	1.981	1.984	1.983
480	1.973	1.978	1.972	1.975	1.978	1.974	1.972	1.975	1.973
481	1.973	1.977	1.971	1.975	1.977	1.975	1.971	1.975	1.974
482	1.973	1.978	1.972	1.975	1.978	1.975	1.972	1.975	1.974
483	1.973	1.978	1.972	1.974	1.977	1.975	1.972	1.975	1.974
484	2.021	2.024	2.021	2.023	2.026	2.024	2.021	2.024	2.023
485	2.022	2.024	2.021	2.024	2.027	2.024	2.021	2.024	2.022
486	2.021	2.024	2.021	2.023	2.026	2.024	2.021	2.024	2.023
487	2.021	2.024	2.021	2.023	2.025	2.023	2.021	2.023	2.022
488	2.020	2.023	2.020	2.022	2.025	2.023	2.020	2.023	2.022
489	2.020	2.022	2.020	2.021	2.023	2.022	2.019	2.021	2.021
490	2.020	2.022	2.019	2.021	2.023	2.022	2.019	2.021	2.021
491	2.019	2.021	2.019	2.020	2.023	2.021	2.019	2.021	2.020
492	2.019	2.021	2.019	2.020	2.023	2.021	2.019	2.021	2.019
493	2.018	2.020	2.018	2.019	2.021	2.020	2.017	2.019	2.019
494	2.018	2.019	2.017	2.019	2.021	2.020	2.016	2.019	2.019
495	2.018	2.020	2.017	2.019	2.021	2.020	2.017	2.019	2.019
496	2.017	2.018	2.015	2.018	2.020	2.019	2.015	2.019	2.018
497	1.669	1.670	1.668	1.669	1.670	1.670	1.668	1.669	1.669
498	1.668	1.669	1.668	1.668	1.669	1.669	1.667	1.669	1.669
499	1.667	1.669	1.668	1.668	1.669	1.668	1.667	1.669	1.668
500	1.668	1.669	1.667	1.668	1.669	1.668	1.665	1.668	1.667
501	1.667	1.668	1.666	1.668	1.668	1.668	1.665	1.668	1.667
502	1.665	1.668	1.666	1.668	1.668	1.668	1.665	1.668	1.668
503	1.663	1.664	1.662	1.663	1.664	1.663	1.661	1.663	1.661
504	1.663	1.664	1.662	1.663	1.664	1.664	1.662	1.664	1.663
505	1.662	1.665	1.662	1.664	1.666	1.664	1.662	1.664	1.664
506	1.662	1.664	1.663	1.664	1.666	1.665	1.663	1.664	1.664
507	1.662	1.664	1.662	1.664	1.666	1.664	1.663	1.664	1.664
508	1.662	1.664	1.663	1.664	1.665	1.664	1.662	1.664	1.664
509	1.662	1.664	1.662	1.664	1.665	1.665	1.662	1.664	1.664
510	2.029	2.031	2.030	2.031	2.032	2.031	2.029	2.031	2.030
511	2.029	2.031	2.029	2.031	2.033	2.031	2.029	2.031	2.030
512	2.030	2.032	2.030	2.031	2.033	2.031	2.029	2.031	2.031
513	2.030	2.031	2.030	2.031	2.033	2.032	2.029	2.031	2.031
514	2.030	2.031	2.030	2.031	2.033	2.032	2.029	2.031	2.031
515	2.030	2.032	2.030	2.031	2.033	2.032	2.029	2.031	2.031
516	2.030	2.032	2.030	2.031	2.033	2.031	2.029	2.031	2.031
517	2.029	2.031	2.029	2.031	2.032	2.031	2.029	2.031	2.030
518	2.029	2.031	2.029	2.030	2.032	2.031	2.029	2.031	2.031
519	2.030	2.032	2.030	2.031	2.034	2.033	2.030	2.031	2.031
520	2.030	2.032	2.030	2.031	2.033	2.032	2.030	2.031	2.031
521	2.030	2.032	2.030	2.031	2.034	2.033	2.030	2.031	2.031
522	2.030	2.032	2.030	2.031	2.034	2.033	2.030	2.031	2.031
523	1.948	1.949	1.947	1.947	1.949	1.948	1.946	1.949	1.949
524	1.948	1.949	1.947	1.948	1.949	1.948	1.947	1.949	1.949
525	1.947	1.949	1.947	1.948	1.950	1.948	1.946	1.949	1.949
526	1.945	1.947	1.944	1.945	1.948	1.945	1.943	1.948	1.948
527	1.945	1.948	1.944	1.946	1.948	1.945	1.943	1.947	1.947
528	1.944	1.948	1.944	1.945	1.948	1.945	1.943	1.946	1.946
529	1.943	1.947	1.943	1.944	1.948	1.944	1.942	1.946	1.946
530	1.943	1.947	1.943	1.944	1.948	1.944	1.942	1.946	1.946
531	1.942	1.947	1.943	1.944	1.946	1.945	1.942	1.947	1.946
532	1.941	1.943	1.941	1.942	1.944	1.942	1.940	1.943	1.943
533	1.941	1.943	1.941	1.942	1.944	1.942	1.940	1.943	1.943
534	1.941	1.943	1.941	1.941	1.944	1.942	1.940	1.943	1.943

TABLE F3 (continued)

535	1.941	1.943	1.941	1.942	1.944	1.943	1.940	1.942	1.942
536	2.084	2.089	2.087	2.087	2.090	2.089	2.084	2.089	2.087
537	2.084	2.089	2.085	2.088	2.090	2.089	2.084	2.089	2.087
538	2.084	2.089	2.085	2.087	2.090	2.089	2.084	2.083	2.087
539	2.083	2.088	2.085	2.087	2.090	2.089	2.082	2.083	2.086
540	2.083	2.089	2.086	2.087	2.089	2.089	2.083	2.088	2.089
541	2.084	2.089	2.087	2.088	2.090	2.089	2.083	2.089	2.087
542	2.084	2.089	2.087	2.088	2.090	2.090	2.083	2.089	2.088
543	2.084	2.089	2.087	2.089	2.090	2.090	2.086	2.089	2.083
544	4.413	4.460	4.467	4.434	4.474	4.477	4.410	4.459	4.462
545	4.420	4.468	4.471	4.441	4.480	4.482	4.417	4.467	4.469
546	4.423	4.471	4.474	4.446	4.485	4.489	4.421	4.470	4.473
547	4.426	4.473	4.479	4.449	4.489	4.490	4.423	4.472	4.477
548	4.423	4.470	4.473	4.443	4.484	4.486	4.419	4.470	4.473
549	1.731	1.734	1.732	1.733	1.735	1.734	1.732	1.734	1.733
550	1.732	1.736	1.734	1.734	1.737	1.736	1.734	1.736	1.736
551	1.733	1.737	1.736	1.737	1.739	1.739	1.734	1.737	1.737
552	1.737	1.739	1.739	1.739	1.740	1.739	1.738	1.739	1.739
553	1.739	1.740	1.739	1.740	1.740	1.740	1.739	1.740	1.740
554	1.739	1.740	1.740	1.740	1.741	1.740	1.739	1.740	1.740
555	1.740	1.741	1.740	1.740	1.742	1.741	1.740	1.741	1.741
556	1.989	1.991	1.989	1.991	1.992	1.992	1.989	1.991	1.991
557	1.989	1.992	1.990	1.991	1.994	1.993	1.989	1.992	1.992
558	1.990	1.994	1.992	1.992	1.994	1.994	1.990	1.993	1.993
559	1.990	1.994	1.992	1.994	1.997	1.994	1.991	1.994	1.994
560	1.990	1.995	1.992	1.994	1.997	1.996	1.992	1.994	1.994
561	1.990	1.995	1.993	1.994	1.997	1.997	1.991	1.995	1.994
562	1.991	1.995	1.993	1.994	1.997	1.997	1.991	1.994	1.993
563	1.689	1.689	1.688	1.689	1.690	1.690	1.689	1.690	1.689
564	1.689	1.690	1.689	1.690	1.691	1.690	1.689	1.690	1.690
565	1.689	1.690	1.689	1.690	1.691	1.690	1.689	1.691	1.691
566	1.689	1.691	1.690	1.691	1.692	1.691	1.690	1.691	1.690
567	1.690	1.692	1.690	1.692	1.692	1.691	1.690	1.692	1.692
568	2.261	2.268	2.262	2.264	2.268	2.267	2.261	2.266	2.265
569	2.267	2.271	2.268	2.269	2.272	2.270	2.267	2.270	2.270
570	2.269	2.273	2.269	2.270	2.273	2.273	2.269	2.272	2.272
571	2.272	2.277	2.271	2.273	2.276	2.274	2.270	2.275	2.275
572	2.272	2.278	2.274	2.277	2.279	2.276	2.273	2.278	2.278
573	2.275	2.280	2.278	2.279	2.282	2.280	2.276	2.280	2.280
574	2.278	2.281	2.278	2.280	2.283	2.282	2.278	2.281	2.281
575	2.278	2.283	2.279	2.280	2.284	2.281	2.278	2.281	2.281
576	2.562	2.569	2.562	2.565	2.570	2.568	2.562	2.568	2.568
577	2.563	2.570	2.564	2.567	2.572	2.569	2.562	2.569	2.569
578	2.563	2.570	2.566	2.568	2.572	2.570	2.563	2.570	2.570
579	2.565	2.571	2.567	2.569	2.572	2.570	2.563	2.570	2.570
580	2.565	2.572	2.567	2.569	2.573	2.571	2.565	2.571	2.571
581	2.567	2.573	2.568	2.570	2.572	2.572	2.567	2.572	2.572
582	2.568	2.573	2.569	2.572	2.577	2.572	2.568	2.573	2.573
583	2.569	2.575	2.569	2.572	2.578	2.574	2.568	2.573	2.573
584	2.469	2.473	2.470	2.466	2.470	2.468	2.463	2.467	2.468
585	2.464	2.470	2.467	2.463	2.468	2.466	2.461	2.463	2.464
586	2.463	2.470	2.467	2.463	2.467	2.464	2.461	2.463	2.463
587	2.461	2.469	2.462	2.460	2.462	2.460	2.458	2.460	2.460
588	2.460	2.468	2.461	2.459	2.462	2.460	2.458	2.460	2.459
589	3.386	3.394	3.387	3.378	3.384	3.380	3.373	3.379	3.379
590	3.383	3.392	3.384	3.376	3.381	3.379	3.373	3.378	3.378
591	3.380	3.390	3.383	3.374	3.380	3.378	3.370	3.375	3.377
592	3.380	3.389	3.381	3.373	3.379	3.376	3.370	3.374	3.374
593	3.379	3.389	3.380	3.372	3.379	3.376	3.370	3.373	3.373
594	3.378	3.388	3.380	3.371	3.378	3.374	3.369	3.373	3.373
595	4.708	4.720	4.716	4.693	4.709	4.703	4.690	4.700	4.702
596	4.707	4.729	4.714	4.694	4.709	4.702	4.689	4.698	4.701
597	4.704	4.724	4.713	4.692	4.705	4.702	4.688	4.698	4.700
598	4.704	4.724	4.713	4.691	4.705	4.701	4.687	4.697	4.699
599	2.954	2.963	2.959	2.949	2.955	2.954	2.948	2.951	2.953
600	2.956	2.964	2.960	2.950	2.958	2.956	2.949	2.952	2.954
601	2.957	2.964	2.960	2.951	2.958	2.956	2.950	2.954	2.957
602	2.957	2.966	2.961	2.953	2.959	2.958	2.951	2.956	2.958
603	2.960	2.970	2.964	2.957	2.962	2.961	2.954	2.957	2.960
604	2.961	2.971	2.967	2.958	2.963	2.962	2.956	2.960	2.961
605	2.463	2.471	2.468	2.465	2.471	2.469	2.461	2.467	2.469
606	2.464	2.471	2.468	2.467	2.471	2.470	2.463	2.469	2.470
607	2.466	2.472	2.470	2.467	2.473	2.470	2.464	2.470	2.470
608	2.467	2.472	2.469	2.468	2.473	2.471	2.464	2.470	2.471
609	2.467	2.473	2.470	2.468	2.473	2.470	2.464	2.470	2.471
610	2.467	2.472	2.470	2.468	2.472	2.470	2.464	2.470	2.470
611	2.959	2.969	2.962	2.960	2.969	2.963	2.956	2.964	2.964

TABLE F3 (continued)

612	2.960	2.970	2.963	2.960	2.970	2.965	2.958	2.967	2.965
613	2.960	2.970	2.964	2.961	2.971	2.966	2.959	2.968	2.969
614	2.961	2.971	2.965	2.962	2.972	2.966	2.959	2.968	2.969
615	2.962	2.972	2.967	2.963	2.972	2.967	2.960	2.969	2.969
616	2.963	2.973	2.969	2.964	2.973	2.970	2.960	2.969	2.970
617	3.390	3.402	3.398	3.390	3.403	3.399	3.398	3.398	3.400
618	3.390	3.403	3.398	3.391	3.403	3.399	3.398	3.399	3.400
619	3.392	3.404	3.399	3.392	3.405	3.400	3.399	3.400	3.402
620	3.392	3.406	3.399	3.393	3.407	3.401	3.390	3.401	3.402
621	3.394	3.408	3.401	3.397	3.409	3.403	3.392	3.403	3.402
622	3.397	3.409	3.402	3.398	3.410	3.405	3.393	3.403	3.407
623	4.699	4.722	4.717	4.705	4.726	4.717	4.696	4.720	4.723
624	4.709	4.732	4.722	4.705	4.732	4.723	4.702	4.725	4.730
625	4.711	4.734	4.723	4.707	4.734	4.724	4.704	4.729	4.732
626	4.713	4.739	4.728	4.711	4.738	4.726	4.709	4.730	4.734
627	4.716	4.739	4.728	4.713	4.739	4.726	4.709	4.731	4.736
628	4.720	4.742	4.732	4.717	4.741	4.731	4.712	4.734	4.740
629	2.700	2.709	2.706	2.701	2.710	2.709	2.699	2.708	2.709
630	2.700	2.710	2.708	2.701	2.711	2.709	2.700	2.709	2.709
631	2.701	2.711	2.709	2.703	2.712	2.710	2.701	2.709	2.710
632	2.702	2.711	2.709	2.702	2.713	2.710	2.701	2.710	2.710
633	2.703	2.713	2.710	2.705	2.714	2.711	2.702	2.710	2.712
634	2.704	2.714	2.710	2.705	2.714	2.712	2.704	2.711	2.712
635	2.894	2.901	2.898	2.898	2.901	2.899	2.895	2.899	2.899
636	2.898	2.903	2.899	2.899	2.903	2.901	2.898	2.900	2.900
637	2.898	2.903	2.900	2.899	2.903	2.901	2.898	2.901	2.901
638	2.899	2.903	2.899	2.899	2.903	2.901	2.898	2.901	2.901
639	2.899	2.904	2.900	2.900	2.906	2.901	2.898	2.902	2.902
640	2.900	2.906	2.902	2.901	2.907	2.903	2.899	2.902	2.902
641	3.192	3.199	3.193	3.193	3.199	3.196	3.190	3.196	3.196
642	3.193	3.200	3.195	3.195	3.200	3.197	3.192	3.197	3.198
643	3.194	3.200	3.195	3.195	3.201	3.196	3.192	3.196	3.198
644	3.194	3.200	3.196	3.196	3.201	3.196	3.192	3.196	3.198
645	3.195	3.201	3.197	3.196	3.201	3.199	3.193	3.199	3.198
646	3.196	3.201	3.197	3.196	3.201	3.199	3.193	3.199	3.199
647	3.663	3.672	3.664	3.664	3.671	3.666	3.660	3.667	3.667
648	3.664	3.672	3.665	3.664	3.672	3.666	3.661	3.668	3.668
649	3.664	3.673	3.667	3.664	3.673	3.666	3.661	3.668	3.668
650	3.664	3.672	3.667	3.665	3.672	3.666	3.661	3.668	3.668
651	3.666	3.673	3.668	3.666	3.673	3.669	3.663	3.669	3.669
652	3.666	3.674	3.668	3.666	3.673	3.669	3.663	3.669	3.669
653	4.219	4.227	4.220	4.219	4.228	4.220	4.213	4.221	4.221
654	4.219	4.229	4.220	4.219	4.228	4.221	4.214	4.222	4.223
655	4.220	4.230	4.221	4.220	4.229	4.222	4.218	4.222	4.223
656	4.220	4.230	4.221	4.220	4.229	4.222	4.216	4.223	4.224
657	4.220	4.230	4.221	4.220	4.230	4.223	4.217	4.223	4.224
658	4.221	4.230	4.222	4.220	4.230	4.223	4.218	4.223	4.224
659	6.102	6.119	6.107	6.092	6.113	6.102	6.092	6.109	6.110
660	6.103	6.120	6.108	6.093	6.113	6.103	6.093	6.109	6.112
661	6.103	6.120	6.109	6.096	6.115	6.104	6.094	6.109	6.112
662	6.103	6.121	6.110	6.095	6.114	6.107	6.096	6.110	6.113
663	6.105	6.121	6.110	6.096	6.116	6.107	6.097	6.110	6.113
664	6.109	6.124	6.112	6.099	6.120	6.109	6.099	6.112	6.118
665	1.574	1.579	1.579	1.574	1.579	1.579	1.574	1.578	1.579
666	1.577	1.580	1.580	1.576	1.580	1.580	1.576	1.578	1.580
667	1.578	1.581	1.580	1.577	1.580	1.580	1.576	1.579	1.580
668	1.579	1.581	1.581	1.579	1.582	1.581	1.579	1.580	1.581
669	1.580	1.584	1.583	1.579	1.582	1.582	1.579	1.580	1.582
670	1.722	1.729	1.728	1.721	1.729	1.729	1.720	1.723	1.727
671	1.722	1.729	1.729	1.723	1.729	1.729	1.721	1.726	1.728
672	1.724	1.731	1.731	1.723	1.730	1.730	1.722	1.727	1.729
673	1.724	1.731	1.730	1.723	1.730	1.730	1.723	1.725	1.729
674	1.726	1.732	1.731	1.724	1.731	1.731	1.723	1.729	1.730
675	2.092	2.106	2.103	2.089	2.102	2.102	2.087	2.096	2.100
676	2.094	2.106	2.106	2.090	2.103	2.103	2.089	2.097	2.101
677	2.096	2.109	2.107	2.091	2.105	2.104	2.089	2.098	2.102
678	2.098	2.110	2.109	2.093	2.107	2.107	2.090	2.099	2.103
679	1.699	1.700	1.700	1.698	1.699	1.700	1.698	1.699	1.700
680	1.699	1.700	1.700	1.698	1.700	1.700	1.698	1.699	1.700
681	1.699	1.701	1.700	1.699	1.701	1.701	1.699	1.701	1.701
682	1.699	1.701	1.701	1.699	1.701	1.701	1.699	1.701	1.702
683	1.699	1.702	1.702	1.699	1.702	1.702	1.700	1.701	1.702
684	1.700	1.702	1.702	1.700	1.702	1.702	1.700	1.701	1.702
685	1.936	1.940	1.940	1.937	1.940	1.940	1.937	1.939	1.940
686	1.939	1.941	1.941	1.938	1.941	1.942	1.938	1.940	1.941
687	1.939	1.942	1.943	1.939	1.942	1.942	1.940	1.941	1.943
688	1.939	1.943	1.942	1.939	1.942	1.942	1.940	1.942	1.943

TABLE F3 (continued)

689	1.939	1.943	1.943	1.940	1.944	1.943	1.941	1.942	1.944
690	1.940	1.944	1.944	1.941	1.944	1.944	1.942	1.944	1.945
691	2.238	2.243	2.241	2.237	2.242	2.241	2.246	2.241	2.242
692	2.239	2.244	2.243	2.239	2.244	2.243	2.240	2.242	2.244
693	2.240	2.246	2.245	2.240	2.246	2.246	2.241	2.244	2.247
694	2.241	2.247	2.246	2.240	2.247	2.245	2.241	2.244	2.247
695	2.240	2.246	2.245	2.240	2.246	2.245	2.240	2.244	2.247
696	2.241	2.247	2.244	2.240	2.245	2.244	2.240	2.243	2.247
697	2.556	2.562	2.561	2.553	2.561	2.560	2.554	2.559	2.562
698	2.557	2.563	2.563	2.555	2.563	2.563	2.557	2.561	2.564
699	2.559	2.567	2.565	2.558	2.568	2.566	2.559	2.563	2.567
700	2.560	2.567	2.567	2.559	2.568	2.566	2.560	2.565	2.568
701	2.561	2.569	2.568	2.560	2.569	2.568	2.561	2.566	2.569
702	2.561	2.569	2.568	2.560	2.569	2.568	2.561	2.566	2.570
703	1.679	1.680	1.680	1.680	1.681	1.681	1.680	1.680	1.681
704	1.681	1.683	1.683	1.683	1.684	1.684	1.682	1.683	1.683
705	1.682	1.683	1.683	1.683	1.683	1.684	1.683	1.683	1.683
706	1.683	1.684	1.684	1.683	1.684	1.685	1.683	1.683	1.685
707	1.683	1.686	1.685	1.684	1.686	1.687	1.684	1.687	1.687
708	1.685	1.687	1.687	1.686	1.688	1.688	1.686	1.688	1.688
709	1.908	1.910	1.910	1.909	1.910	1.911	1.908	1.910	1.910
710	1.909	1.911	1.911	1.910	1.912	1.912	1.910	1.912	1.912
711	1.909	1.912	1.912	1.911	1.913	1.913	1.911	1.913	1.913
712	1.909	1.913	1.913	1.911	1.913	1.913	1.911	1.913	1.913
713	1.910	1.912	1.913	1.911	1.914	1.914	1.911	1.913	1.913
714	1.910	1.913	1.913	1.912	1.914	1.914	1.912	1.913	1.914
715	2.231	2.237	2.234	2.232	2.238	2.237	2.232	2.237	2.237
716	2.231	2.237	2.237	2.233	2.249	2.248	2.233	2.248	2.246
717	2.232	2.238	2.237	2.234	2.239	2.239	2.234	2.238	2.239
718	2.233	2.239	2.238	2.234	2.239	2.239	2.235	2.238	2.239
719	2.233	2.239	2.238	2.235	2.240	2.240	2.236	2.240	2.240
720	2.234	2.239	2.239	2.236	2.240	2.240	2.237	2.240	2.240
721	1.685	1.688	1.688	1.688	1.689	1.689	1.686	1.689	1.689
722	1.686	1.689	1.689	1.688	1.689	1.689	1.688	1.689	1.689
723	1.688	1.690	1.690	1.689	1.690	1.690	1.689	1.690	1.690
724	1.689	1.690	1.690	1.690	1.691	1.691	1.690	1.691	1.691
725	1.689	1.690	1.690	1.690	1.692	1.691	1.691	1.691	1.691
726	1.690	1.692	1.692	1.692	1.694	1.693	1.692	1.693	1.692
727	1.910	1.912	1.912	1.912	1.913	1.913	1.911	1.913	1.914
728	1.911	1.914	1.913	1.913	1.917	1.916	1.913	1.916	1.916
729	1.912	1.916	1.914	1.914	1.918	1.917	1.915	1.918	1.916
730	1.913	1.917	1.917	1.917	1.919	1.918	1.916	1.919	1.919
731	1.913	1.918	1.917	1.916	1.920	1.919	1.918	1.920	1.920
732	1.914	1.919	1.917	1.918	1.920	1.920	1.919	1.920	1.920
733	2.231	2.235	2.233	2.234	2.239	2.237	2.233	2.239	2.238
734	2.231	2.236	2.234	2.234	2.239	2.237	2.234	2.238	2.238
735	2.231	2.237	2.235	2.235	2.239	2.239	2.235	2.239	2.239
736	2.232	2.239	2.236	2.236	2.240	2.239	2.237	2.240	2.240
737	2.233	2.239	2.237	2.237	2.241	2.240	2.237	2.240	2.240
738	2.234	2.240	2.239	2.238	2.242	2.240	2.239	2.241	2.241

TABLE F4

THE MEAN AND STD DEVIATION OF MILLIVOLT POSNS 1 TO 9											
K	XBAR	STD	TEMP	K	XBAR	STD	TEMP	K	XBAR	STD	TEMP
1	1.97867	0.00112	9.348	2	1.97867	0.00112	9.348	3	1.97867	0.00112	9.348
4	1.97867	0.00112	9.348	7	1.97867	0.00112	9.348	10	1.97867	0.00112	9.348
13	1.97867	0.00112	9.348	16	1.97867	0.00112	9.348	19	1.97867	0.00112	9.348
22	1.97867	0.00112	9.348	25	1.97867	0.00112	9.348	28	1.97867	0.00112	9.348
31	1.97867	0.00112	9.348	34	1.97867	0.00112	9.348	37	1.97867	0.00112	9.348
40	1.97867	0.00112	9.348	43	1.97867	0.00112	9.348	46	1.97867	0.00112	9.348
49	1.97867	0.00112	9.348	52	1.97867	0.00112	9.348	55	1.97867	0.00112	9.348
58	1.97867	0.00112	9.348	61	1.97867	0.00112	9.348	64	1.97867	0.00112	9.348
67	1.97867	0.00112	9.348	70	1.97867	0.00112	9.348	73	1.97867	0.00112	9.348
76	1.97867	0.00112	9.348	79	1.97867	0.00112	9.348	82	1.97867	0.00112	9.348
85	1.97867	0.00112	9.348	88	1.97867	0.00112	9.348	91	1.97867	0.00112	9.348
94	1.97867	0.00112	9.348	97	1.97867	0.00112	9.348	100	1.97867	0.00112	9.348

442	1.00100	0.00100	48.923	443	1.96144	0.00073	46.934	444	1.96133	0.00087	48.932
443	1.00100	0.00050	48.923	444	1.96144	0.00109	46.934	445	1.95467	0.00150	48.971
444	1.00100	0.00050	48.923	445	1.96144	0.00067	46.934	446	1.96260	0.00100	48.948
445	1.00100	0.00050	48.923	446	1.96144	0.00141	46.934	447	1.96776	0.00097	48.906
446	1.00100	0.00050	48.923	447	1.96144	0.00071	46.934	448	1.96969	0.00053	48.912
447	1.00100	0.00050	48.923	448	1.96144	0.00247	46.934	449	1.96676	0.00217	48.922
448	1.00100	0.00050	48.923	449	1.96144	0.00244	46.934	450	1.95700	0.00263	48.942
449	1.00100	0.00050	48.923	450	1.96144	0.00165	46.934	451	1.95833	0.00203	48.939
450	1.00100	0.00050	48.923	451	1.96144	0.00124	46.934	452	1.95833	0.00170	48.939
451	1.00100	0.00050	48.923	452	1.96144	0.00111	46.934	453	1.95833	0.00160	48.939
452	1.00100	0.00050	48.923	453	1.96144	0.00144	46.934	454	1.95833	0.00229	48.942
453	1.00100	0.00050	48.923	454	1.96144	0.00111	46.934	455	1.95833	0.00230	48.942
454	1.00100	0.00050	48.923	455	1.96144	0.00117	46.934	456	1.95833	0.00173	48.939
455	1.00100	0.00050	48.923	456	1.96144	0.00173	46.934	457	1.95833	0.00132	48.939
456	1.00100	0.00050	48.923	457	1.96144	0.00133	46.934	458	1.95833	0.00132	48.939
457	1.00100	0.00050	48.923	458	1.96144	0.00100	46.934	459	1.95833	0.00130	48.939
458	1.00100	0.00050	48.923	459	1.96144	0.00078	46.934	460	1.95833	0.00100	48.939
459	1.00100	0.00050	48.923	460	1.96144	0.00122	46.934	461	1.95833	0.00076	48.939
460	1.00100	0.00050	48.923	461	1.96144	0.00111	46.934	462	1.95833	0.00076	48.939
461	1.00100	0.00050	48.923	462	1.96144	0.00111	46.934	463	1.95833	0.00076	48.939
462	1.00100	0.00050	48.923	463	1.96144	0.00111	46.934	464	1.95833	0.00076	48.939
463	1.00100	0.00050	48.923	464	1.96144	0.00111	46.934	465	1.95833	0.00076	48.939
464	1.00100	0.00050	48.923	465	1.96144	0.00111	46.934	466	1.95833	0.00076	48.939
465	1.00100	0.00050	48.923	466	1.96144	0.00111	46.934	467	1.95833	0.00076	48.939
466	1.00100	0.00050	48.923	467	1.96144	0.00111	46.934	468	1.95833	0.00076	48.939
467	1.00100	0.00050	48.923	468	1.96144	0.00111	46.934	469	1.95833	0.00076	48.939
468	1.00100	0.00050	48.923	469	1.96144	0.00111	46.934	470	1.95833	0.00076	48.939
469	1.00100	0.00050	48.923	470	1.96144	0.00111	46.934	471	1.95833	0.00076	48.939
470	1.00100	0.00050	48.923	471	1.96144	0.00111	46.934	472	1.95833	0.00076	48.939
471	1.00100	0.00050	48.923	472	1.96144	0.00111	46.934	473	1.95833	0.00076	48.939
472	1.00100	0.00050	48.923	473	1.96144	0.0					

TABLE F4 (continued)

673	1.72756	0.00328	43.281	674	1.72856	0.00336	43.305	675	2.09744	0.00675	52.192
676	2.09900	0.00666	52.229	677	2.17011	0.00764	52.255	678	2.10178	0.00719	52.229
679	1.69922	0.00083	42.591	680	1.69933	0.00087	42.594	681	1.69959	0.00097	42.607
682	1.70044	0.00113	42.621	683	1.70100	0.00132	42.634	684	1.70122	0.00150	42.640
685	1.70267	0.00164	42.689	686	1.70401	0.00145	42.721	687	1.70412	0.00150	42.738
688	1.70413	0.00158	42.751	689	1.70421	0.00176	42.769	690	1.70431	0.00176	42.783
691	2.24033	0.00212	55.591	692	2.24200	0.00212	55.630	693	2.24369	0.00230	55.675
694	2.24422	0.00286	55.683	695	2.24367	0.00237	55.700	696	2.24344	0.00270	55.745
697	2.24867	0.00346	63.060	698	2.24667	0.00339	63.127	699	2.24633	0.00371	63.160
700	2.24844	0.00371	63.215	701	2.24567	0.00367	63.244	702	2.24578	0.00399	63.246
703	1.68022	0.00067	42.128	704	1.68289	0.00093	42.193	705	1.68300	0.00090	42.194
706	1.68378	0.00083	42.215	707	1.68544	0.00111	42.250	708	1.68700	0.00111	42.293
709	1.68956	0.00101	42.666	710	1.69100	0.00112	42.720	711	1.69110	0.00111	42.730
712	1.69121	0.00145	42.747	713	1.69123	0.00141	42.750	714	1.69127	0.00130	42.777
715	2.23500	0.00274	55.404	716	2.23744	0.00265	55.493	717	2.23667	0.00265	55.551
718	2.23711	0.00242	55.514	719	2.23769	0.00262	55.533	720	2.23833	0.00260	55.551
721	1.64033	0.00071	42.315	722	1.64044	0.00071	42.329	723	1.64096	0.00071	42.330
724	1.64033	0.00071	42.375	725	1.64056	0.00068	42.380	726	1.64022	0.00060	42.382
727	1.64122	0.00120	42.750	728	1.64133	0.00090	42.760	729	1.64157	0.00091	42.785
730	1.64172	0.00192	47.870	731	1.64178	0.00232	47.880	732	1.64185	0.00201	47.885
733	2.23544	0.00292	55.475	734	2.23567	0.00260	55.480	735	2.23600	0.00279	55.500
736	2.23767	0.00269	55.527	737	2.23722	0.00249	55.541	738	2.23933	0.00233	55.567

TABLE F5 (continued)

73	2.084	2.086	2.085	2.087	2.088	2.085	2.088	2.089	2.087
74	2.082	2.083	2.082	2.083	2.083	2.083	2.085	2.085	2.083
75	2.078	2.079	2.078	2.079	2.080	2.079	2.080	2.080	2.079
76	2.078	2.079	2.078	2.079	2.080	2.079	2.081	2.082	2.080
77	2.078	2.079	2.079	2.079	2.080	2.079	2.080	2.081	2.080
78	2.071	2.072	2.072	2.073	2.073	2.073	2.074	2.075	2.073
79	2.074	2.075	2.073	2.076	2.077	2.075	2.078	2.078	2.076
80	2.076	2.077	2.076	2.077	2.078	2.076	2.079	2.079	2.077
81	2.089	2.090	2.088	2.090	2.090	2.086	2.091	2.091	2.089
82	2.076	2.077	2.074	2.078	2.078	2.075	2.079	2.079	2.077
83	2.081	2.082	2.081	2.083	2.084	2.081	2.086	2.086	2.083
84	2.079	2.079	2.078	2.080	2.080	2.079	2.081	2.081	2.080
85	2.073	2.073	2.072	2.075	2.075	2.072	2.078	2.077	2.075
86	2.071	2.073	2.071	2.074	2.075	2.072	2.076	2.077	2.073
87	2.072	2.073	2.071	2.074	2.075	2.071	2.076	2.076	2.073
88	2.099	2.099	2.097	2.099	2.100	2.097	2.100	2.100	2.099
89	2.087	2.088	2.085	2.088	2.089	2.087	2.090	2.090	2.089
90	2.080	2.080	2.080	2.081	2.081	2.080	2.083	2.083	2.081
91	2.079	2.080	2.079	2.080	2.080	2.079	2.081	2.081	2.080
92	2.079	2.080	2.078	2.080	2.080	2.079	2.081	2.081	2.080
93	2.082	2.083	2.081	2.085	2.085	2.083	2.087	2.087	2.084
94	1.459	1.459	1.459	1.459	1.459	1.459	1.459	1.459	1.459
95	1.463	1.464	1.463	1.464	1.464	1.463	1.466	1.466	1.465
96	1.463	1.463	1.463	1.463	1.464	1.463	1.465	1.465	1.464
97	1.470	1.470	1.470	1.469	1.469	1.470	1.471	1.470	1.470
98	1.470	1.470	1.470	1.470	1.470	1.469	1.470	1.470	1.470
99	1.468	1.468	1.468	1.468	1.469	1.469	1.469	1.469	1.469
100	1.468	1.468	1.468	1.468	1.469	1.468	1.469	1.469	1.468
101	1.460	1.460	1.459	1.460	1.460	1.459	1.460	1.460	1.460
102	1.467	1.467	1.467	1.467	1.467	1.467	1.467	1.467	1.467
103	1.468	1.468	1.466	1.467	1.468	1.467	1.468	1.468	1.468
104	1.468	1.468	1.466	1.467	1.468	1.468	1.468	1.468	1.468
105	1.466	1.466	1.464	1.465	1.467	1.467	1.467	1.467	1.467
106	1.462	1.462	1.462	1.462	1.463	1.464	1.465	1.465	1.465
107	2.543	2.544	2.541	2.545	2.547	2.542	2.548	2.549	2.544
108	2.535	2.537	2.532	2.538	2.539	2.535	2.540	2.540	2.538
109	2.529	2.530	2.525	2.530	2.530	2.526	2.531	2.532	2.530
110	2.549	2.549	2.547	2.550	2.549	2.546	2.551	2.551	2.549
111	2.535	2.537	2.531	2.538	2.539	2.532	2.539	2.539	2.537
112	2.529	2.529	2.526	2.530	2.530	2.527	2.531	2.533	2.530
113	2.523	2.524	2.521	2.526	2.528	2.522	2.529	2.529	2.526
114	2.519	2.519	2.517	2.520	2.521	2.516	2.522	2.523	2.520
115	2.514	2.516	2.511	2.518	2.519	2.514	2.520	2.520	2.517
116	2.510	2.511	2.510	2.511	2.513	2.510	2.514	2.514	2.511
117	2.509	2.509	2.508	2.509	2.511	2.506	2.512	2.513	2.510
118	2.500	2.501	2.500	2.502	2.503	2.500	2.505	2.507	2.501
119	2.499	2.500	2.499	2.501	2.502	2.499	2.503	2.504	2.501
120	2.117	2.119	2.114	2.119	2.119	2.118	2.119	2.119	2.118
121	2.111	2.111	2.110	2.113	2.113	2.111	2.115	2.115	2.112
122	2.107	2.107	2.105	2.109	2.109	2.106	2.109	2.109	2.108
123	2.100	2.101	2.100	2.102	2.102	2.100	2.104	2.105	2.102
124	2.096	2.097	2.093	2.098	2.099	2.095	2.099	2.099	2.097
125	2.090	2.091	2.090	2.093	2.094	2.091	2.095	2.095	2.092
126	2.090	2.090	2.089	2.090	2.091	2.090	2.092	2.092	2.091
127	2.090	2.090	2.090	2.091	2.092	2.090	2.094	2.094	2.091
128	2.114	2.115	2.112	2.116	2.118	2.113	2.119	2.119	2.115
129	2.109	2.110	2.108	2.110	2.110	2.109	2.111	2.111	2.110
130	2.107	2.108	2.104	2.108	2.109	2.107	2.109	2.109	2.109
131	2.101	2.102	2.100	2.102	2.103	2.101	2.104	2.104	2.102
132	2.094	2.095	2.093	2.098	2.098	2.094	2.099	2.099	2.097
133	2.109	2.110	2.109	2.110	2.111	2.109	2.111	2.111	2.110
134	2.104	2.106	2.102	2.106	2.108	2.104	2.108	2.109	2.107
135	2.101	2.102	2.100	2.103	2.104	2.101	2.106	2.106	2.102
136	2.110	2.110	2.109	2.110	2.110	2.110	2.111	2.112	2.110
137	2.102	2.103	2.101	2.104	2.106	2.101	2.108	2.108	2.104
138	2.087	2.087	2.083	2.088	2.089	2.087	2.089	2.089	2.088
139	2.111	2.112	2.110	2.111	2.112	2.110	2.114	2.114	2.111
140	2.104	2.106	2.102	2.106	2.107	2.103	2.108	2.108	2.106
141	2.099	2.099	2.098	2.100	2.100	2.099	2.100	2.101	2.100
142	2.094	2.094	2.091	2.095	2.096	2.091	2.097	2.097	2.095
143	2.089	2.089	2.087	2.090	2.090	2.086	2.090	2.090	2.089
144	2.082	2.084	2.081	2.086	2.087	2.083	2.088	2.089	2.086
145	2.083	2.084	2.081	2.085	2.085	2.082	2.087	2.088	2.084
146	2.089	2.089	2.087	2.089	2.089	2.086	2.090	2.090	2.089
147	2.085	2.087	2.084	2.088	2.089	2.085	2.089	2.089	2.087
148	2.080	2.080	2.079	2.081	2.081	2.080	2.082	2.083	2.081
149	2.080	2.080	2.079	2.080	2.081	2.080	2.082	2.082	2.081

TABLE F5 (continued)

150	2.079	2.079	2.077	2.080	2.080	2.079	2.081	2.081	2.080
151	2.077	2.078	2.076	2.079	2.079	2.078	2.080	2.080	2.079
152	2.076	2.076	2.075	2.078	2.079	2.076	2.079	2.080	2.079
153	2.075	2.076	2.074	2.077	2.078	2.075	2.079	2.079	2.078
154	2.071	2.072	2.071	2.073	2.075	2.071	2.076	2.077	2.073
155	2.072	2.073	2.071	2.073	2.075	2.071	2.077	2.078	2.074
156	2.071	2.071	2.070	2.073	2.074	2.071	2.075	2.075	2.073
157	2.089	2.089	2.088	2.090	2.090	2.089	2.091	2.091	2.090
158	2.083	2.084	2.081	2.085	2.086	2.082	2.087	2.087	2.085
159	2.103	2.103	2.100	2.103	2.104	2.101	2.105	2.105	2.102
160	2.099	2.099	2.096	2.099	2.099	2.097	2.100	2.100	2.099
161	2.092	2.092	2.090	2.094	2.094	2.091	2.095	2.097	2.093
162	2.089	2.089	2.088	2.090	2.090	2.090	2.091	2.091	2.090
163	2.087	2.087	2.084	2.088	2.088	2.085	2.089	2.089	2.088
164	2.082	2.082	2.081	2.084	2.085	2.081	2.088	2.087	2.083
165	2.080	2.081	2.079	2.081	2.082	2.080	2.082	2.083	2.081
166	2.074	2.075	2.071	2.076	2.077	2.073	2.078	2.079	2.075
167	2.072	2.073	2.071	2.074	2.074	2.071	2.076	2.076	2.073
168	2.069	2.069	2.067	2.070	2.070	2.069	2.071	2.071	2.069
169	2.069	2.069	2.068	2.070	2.070	2.069	2.071	2.071	2.069
170	2.071	2.072	2.070	2.072	2.073	2.071	2.075	2.075	2.072
171	2.072	2.073	2.070	2.072	2.073	2.071	2.075	2.075	2.072
172	1.450	1.450	1.450	1.450	1.450	1.450	1.450	1.450	1.450
173	1.449	1.449	1.449	1.449	1.449	1.449	1.449	1.449	1.449
174	1.444	1.444	1.444	1.445	1.445	1.444	1.446	1.446	1.446
175	1.443	1.443	1.443	1.443	1.443	1.443	1.444	1.444	1.444
176	1.441	1.441	1.441	1.441	1.441	1.441	1.442	1.442	1.442
177	1.440	1.440	1.440	1.440	1.440	1.440	1.441	1.441	1.440
178	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440
179	1.440	1.440	1.440	1.440	1.440	1.440	1.441	1.441	1.440
180	1.440	1.440	1.440	1.440	1.441	1.441	1.441	1.441	1.441
181	1.441	1.441	1.441	1.441	1.441	1.441	1.442	1.442	1.442
182	1.441	1.441	1.440	1.441	1.441	1.440	1.442	1.442	1.441
183	1.441	1.441	1.440	1.441	1.441	1.441	1.442	1.442	1.442
184	1.441	1.441	1.441	1.441	1.441	1.441	1.442	1.442	1.442
185	2.495	2.496	2.492	2.498	2.498	2.494	2.499	2.499	2.498
186	2.500	2.501	2.498	2.502	2.503	2.499	2.505	2.506	2.501
187	2.499	2.500	2.498	2.502	2.502	2.499	2.502	2.504	2.500
188	2.522	2.522	2.519	2.524	2.524	2.520	2.527	2.528	2.522
189	2.507	2.508	2.503	2.509	2.509	2.504	2.510	2.510	2.506
190	2.551	2.552	2.549	2.553	2.553	2.549	2.556	2.557	2.553
191	2.539	2.539	2.535	2.540	2.540	2.537	2.541	2.542	2.539
192	2.530	2.530	2.527	2.531	2.532	2.529	2.534	2.534	2.530
193	2.510	2.512	2.509	2.513	2.514	2.510	2.516	2.516	2.511
194	2.509	2.509	2.509	2.505	2.510	2.500	2.512	2.511	2.509
195	2.503	2.503	2.500	2.505	2.507	2.501	2.508	2.508	2.503
196	2.500	2.501	2.499	2.502	2.503	2.499	2.505	2.506	2.501
197	2.502	2.503	2.499	2.503	2.505	2.500	2.508	2.508	2.502
198	2.099	2.099	2.097	2.099	2.099	2.097	2.099	2.099	2.099
199	2.093	2.093	2.091	2.094	2.095	2.091	2.097	2.097	2.094
200	2.090	2.090	2.089	2.091	2.091	2.089	2.092	2.092	2.090
201	2.088	2.089	2.087	2.089	2.089	2.087	2.090	2.090	2.089
202	2.087	2.086	2.083	2.088	2.088	2.084	2.089	2.089	2.086
203	2.082	2.083	2.080	2.084	2.084	2.081	2.087	2.087	2.083
204	2.081	2.083	2.080	2.083	2.084	2.081	2.086	2.086	2.082
205	2.081	2.081	2.079	2.081	2.082	2.080	2.083	2.084	2.081
206	2.080	2.080	2.079	2.081	2.081	2.080	2.082	2.082	2.081
207	2.079	2.079	2.077	2.079	2.079	2.078	2.080	2.080	2.079
208	2.079	2.079	2.077	2.079	2.080	2.078	2.080	2.080	2.079
209	2.078	2.079	2.075	2.079	2.079	2.077	2.080	2.080	2.079
210	2.071	2.072	2.070	2.073	2.074	2.072	2.075	2.075	2.073
211	2.078	2.078	2.074	2.079	2.079	2.077	2.080	2.080	2.078
212	2.079	2.079	2.077	2.079	2.080	2.078	2.080	2.080	2.079
213	2.078	2.079	2.075	2.079	2.079	2.077	2.080	2.080	2.079
214	2.078	2.079	2.075	2.079	2.079	2.077	2.080	2.080	2.079
215	2.078	2.078	2.076	2.079	2.079	2.078	2.080	2.080	2.079
216	2.099	2.099	2.098	2.099	2.099	2.099	2.099	2.099	2.099
217	2.095	2.094	2.092	2.097	2.097	2.093	2.098	2.099	2.095
218	2.091	2.091	2.089	2.092	2.092	2.090	2.094	2.094	2.091
219	2.089	2.089	2.087	2.090	2.090	2.088	2.090	2.091	2.089
220	2.085	2.086	2.083	2.087	2.088	2.084	2.089	2.089	2.087
221	2.083	2.084	2.082	2.085	2.087	2.083	2.088	2.088	2.084
222	2.081	2.082	2.080	2.082	2.083	2.080	2.084	2.084	2.082
223	2.078	2.079	2.076	2.079	2.079	2.077	2.080	2.080	2.079
224	2.071	2.071	2.070	2.072	2.072	2.070	2.073	2.073	2.071
225	2.071	2.071	2.069	2.072	2.072	2.070	2.073	2.073	2.072
226	2.069	2.070	2.068	2.070	2.071	2.069	2.072	2.071	2.070

TABLE F5 (continued)

227	2.071	2.071	2.070	2.072	2.073	2.073	2.070	2.073	2.074	2.072
228	2.071	2.072	2.070	2.073	2.073	2.073	2.071	2.075	2.075	2.073
229	2.067	2.067	2.064	2.068	2.068	2.068	2.065	2.069	2.069	2.068
230	2.068	2.068	2.065	2.069	2.069	2.069	2.067	2.070	2.070	2.069
231	2.068	2.068	2.067	2.069	2.069	2.069	2.066	2.070	2.070	2.069
232	2.072	2.072	2.070	2.073	2.073	2.073	2.071	2.075	2.075	2.073
233	2.073	2.073	2.071	2.074	2.074	2.074	2.072	2.077	2.077	2.074
234	2.073	2.074	2.072	2.075	2.075	2.075	2.073	2.078	2.078	2.075
235	2.073	2.073	2.071	2.074	2.074	2.074	2.072	2.077	2.077	2.074
236	2.074	2.074	2.072	2.075	2.075	2.075	2.073	2.078	2.078	2.075
237	2.072	2.073	2.070	2.073	2.073	2.073	2.071	2.075	2.075	2.072
238	2.069	2.069	2.067	2.070	2.070	2.070	2.068	2.071	2.071	2.069
239	2.067	2.067	2.064	2.068	2.068	2.068	2.066	2.069	2.069	2.068
240	2.066	2.066	2.062	2.067	2.067	2.067	2.063	2.069	2.069	2.065
241	2.071	2.071	2.069	2.072	2.072	2.072	2.070	2.073	2.073	2.071
242	2.071	2.071	2.070	2.073	2.073	2.073	2.070	2.073	2.073	2.072
243	2.071	2.072	2.070	2.072	2.072	2.072	2.070	2.073	2.073	2.072
244	2.071	2.071	2.070	2.072	2.072	2.072	2.070	2.073	2.073	2.072
245	2.071	2.071	2.070	2.072	2.072	2.072	2.070	2.073	2.073	2.072
246	2.071	2.071	2.070	2.072	2.072	2.072	2.070	2.073	2.073	2.072
247	2.071	2.072	2.070	2.073	2.073	2.073	2.071	2.074	2.074	2.072
248	2.072	2.073	2.071	2.073	2.073	2.073	2.072	2.076	2.077	2.073
249	2.072	2.073	2.071	2.073	2.073	2.073	2.071	2.075	2.075	2.073
250	1.443	1.443	1.443	1.444	1.444	1.444	1.444	1.444	1.444	1.443
251	1.442	1.442	1.442	1.442	1.442	1.442	1.443	1.444	1.444	1.443
252	1.442	1.442	1.442	1.442	1.442	1.442	1.442	1.443	1.443	1.443
253	1.442	1.442	1.442	1.442	1.442	1.442	1.442	1.442	1.442	1.442
254	1.441	1.441	1.440	1.441	1.441	1.441	1.442	1.441	1.442	1.442
255	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440
256	1.440	1.440	1.439	1.440	1.440	1.440	1.440	1.440	1.440	1.440
257	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440	1.440
258	1.439	1.439	1.439	1.440	1.440	1.440	1.440	1.440	1.440	1.440
259	1.438	1.438	1.438	1.438	1.438	1.438	1.438	1.438	1.438	1.439
260	1.439	1.439	1.438	1.439	1.439	1.439	1.439	1.439	1.439	1.439
261	1.439	1.439	1.438	1.439	1.439	1.439	1.439	1.439	1.439	1.439
262	1.439	1.439	1.439	1.439	1.439	1.439	1.439	1.439	1.439	1.439
263	2.504	2.505	2.503	2.506	2.506	2.506	2.509	2.510	2.510	2.506
264	2.508	2.508	2.503	2.509	2.509	2.509	2.506	2.510	2.510	2.509
265	2.510	2.511	2.509	2.512	2.512	2.512	2.513	2.515	2.515	2.512
266	2.511	2.512	2.510	2.513	2.513	2.513	2.510	2.517	2.517	2.512
267	2.512	2.513	2.510	2.514	2.514	2.514	2.511	2.518	2.518	2.513
268	2.512	2.513	2.510	2.514	2.514	2.514	2.511	2.518	2.518	2.513
269	2.512	2.513	2.510	2.514	2.514	2.514	2.511	2.518	2.518	2.513
270	2.515	2.515	2.512	2.517	2.517	2.517	2.514	2.519	2.519	2.517
271	2.515	2.515	2.512	2.517	2.517	2.517	2.514	2.519	2.519	2.517
272	2.515	2.515	2.512	2.517	2.517	2.517	2.514	2.519	2.519	2.517
273	2.515	2.515	2.512	2.517	2.517	2.517	2.514	2.519	2.519	2.517
274	2.513	2.513	2.510	2.515	2.515	2.515	2.512	2.519	2.519	2.514
275	2.513	2.513	2.510	2.515	2.515	2.515	2.512	2.519	2.519	2.514
276	2.517	2.517	2.514	2.519	2.519	2.519	2.516	2.520	2.520	2.517
277	2.512	2.512	2.511	2.513	2.513	2.513	2.511	2.514	2.514	2.512
278	2.511	2.511	2.510	2.512	2.512	2.512	2.510	2.513	2.513	2.511
279	2.511	2.511	2.510	2.512	2.512	2.512	2.510	2.513	2.513	2.511
280	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
281	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
282	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
283	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
284	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
285	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
286	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
287	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
288	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
289	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
290	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
291	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
292	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
293	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
294	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
295	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
296	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
297	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
298	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
299	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
300	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
301	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
302	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510
303	2.510	2.510	2.509	2.511	2.511	2.511	2.509	2.512	2.512	2.510

TABLE F5 (continued)

304	2.084	2.085	2.083	2.087	2.087	2.084	2.088	2.088	2.086
305	2.084	2.085	2.083	2.087	2.087	2.083	2.089	2.089	2.087
306	2.085	2.085	2.082	2.087	2.088	2.083	2.088	2.088	2.085
307	2.078	2.079	2.077	2.079	2.079	2.076	2.080	2.080	2.079
308	2.078	2.078	2.077	2.079	2.079	2.076	2.080	2.080	2.079
309	2.079	2.079	2.077	2.079	2.080	2.076	2.080	2.080	2.079
310	2.079	2.079	2.078	2.080	2.080	2.079	2.081	2.081	2.080
311	2.080	2.080	2.079	2.081	2.081	2.079	2.083	2.083	2.081
312	2.080	2.080	2.079	2.081	2.081	2.080	2.083	2.083	2.081
313	2.080	2.080	2.079	2.081	2.081	2.080	2.082	2.082	2.080
314	2.080	2.080	2.079	2.080	2.081	2.079	2.082	2.082	2.080
315	2.042	2.042	2.041	2.043	2.044	2.042	2.045	2.045	2.044
316	2.043	2.044	2.043	2.044	2.045	2.043	2.048	2.048	2.045
317	2.045	2.047	2.044	2.046	2.048	2.045	2.048	2.048	2.048
318	2.046	2.047	2.046	2.048	2.048	2.047	2.049	2.049	2.048
319	2.047	2.048	2.046	2.049	2.049	2.046	2.050	2.050	2.049
320	2.047	2.048	2.048	2.049	2.049	2.046	2.050	2.050	2.049
321	2.048	2.049	2.048	2.049	2.049	2.046	2.050	2.050	2.049
322	2.049	2.050	2.049	2.050	2.051	2.050	2.052	2.052	2.051
323	2.049	2.050	2.049	2.050	2.051	2.050	2.052	2.052	2.051
324	2.049	2.050	2.049	2.051	2.051	2.050	2.052	2.052	2.051
325	2.050	2.050	2.049	2.051	2.051	2.050	2.052	2.052	2.051
326	2.053	2.054	2.053	2.054	2.056	2.053	2.057	2.057	2.054
327	2.057	2.057	2.054	2.058	2.058	2.056	2.059	2.059	2.058
328	1.445	1.445	1.445	1.445	1.446	1.444	1.446	1.446	1.446
329	1.446	1.446	1.446	1.446	1.446	1.446	1.446	1.446	1.446
330	1.444	1.444	1.444	1.444	1.445	1.444	1.446	1.446	1.446
331	1.444	1.444	1.444	1.444	1.445	1.445	1.445	1.445	1.445
332	1.444	1.444	1.444	1.444	1.445	1.445	1.445	1.445	1.445
333	1.444	1.444	1.444	1.444	1.445	1.445	1.445	1.445	1.444
334	1.444	1.444	1.444	1.444	1.444	1.444	1.445	1.445	1.445
335	1.443	1.443	1.443	1.443	1.443	1.443	1.443	1.443	1.443
336	1.443	1.443	1.443	1.443	1.443	1.443	1.444	1.444	1.444
337	1.443	1.443	1.443	1.443	1.443	1.443	1.445	1.445	1.445
338	1.443	1.443	1.442	1.443	1.443	1.443	1.443	1.443	1.443
339	1.443	1.443	1.443	1.443	1.444	1.443	1.444	1.444	1.444
340	1.444	1.444	1.444	1.444	1.444	1.444	1.444	1.444	1.445
341	2.502	2.503	2.501	2.503	2.504	2.501	2.506	2.507	2.502
342	2.493	2.494	2.492	2.494	2.496	2.492	2.498	2.498	2.495
343	2.488	2.489	2.488	2.490	2.490	2.489	2.491	2.492	2.490
344	2.480	2.480	2.479	2.480	2.481	2.479	2.483	2.484	2.481
345	2.477	2.479	2.477	2.479	2.479	2.478	2.480	2.481	2.479
346	2.473	2.474	2.473	2.476	2.478	2.474	2.479	2.479	2.478
347	2.472	2.473	2.471	2.474	2.476	2.472	2.478	2.479	2.474
348	2.468	2.469	2.467	2.469	2.470	2.468	2.471	2.471	2.470
349	2.468	2.469	2.467	2.469	2.470	2.469	2.471	2.472	2.470
350	2.468	2.469	2.468	2.469	2.470	2.469	2.471	2.472	2.470
351	2.468	2.469	2.467	2.469	2.470	2.469	2.471	2.472	2.470
352	2.469	2.469	2.468	2.470	2.471	2.470	2.472	2.473	2.470
353	2.470	2.470	2.469	2.471	2.472	2.470	2.474	2.474	2.472
354	2.078	2.079	2.077	2.079	2.079	2.078	2.080	2.080	2.079
355	2.073	2.074	2.073	2.075	2.076	2.074	2.078	2.078	2.076
356	2.071	2.072	2.071	2.073	2.073	2.072	2.074	2.075	2.073
357	2.070	2.070	2.070	2.070	2.070	2.070	2.071	2.071	2.071
358	2.069	2.069	2.069	2.070	2.070	2.069	2.070	2.070	2.070
359	2.066	2.067	2.065	2.068	2.068	2.067	2.069	2.069	2.068
360	2.066	2.066	2.066	2.067	2.068	2.067	2.069	2.069	2.068
361	2.061	2.061	2.061	2.061	2.062	2.061	2.064	2.064	2.062
362	2.062	2.063	2.061	2.063	2.064	2.062	2.066	2.067	2.064
363	2.061	2.062	2.061	2.062	2.063	2.061	2.064	2.066	2.063
364	2.059	2.059	2.059	2.060	2.060	2.059	2.061	2.061	2.060
365	2.059	2.060	2.060	2.060	2.061	2.060	2.061	2.062	2.060
366	2.059	2.060	2.060	2.061	2.061	2.060	2.062	2.062	2.061
367	2.039	2.040	2.039	2.040	2.041	2.039	2.041	2.041	2.040
368	2.040	2.041	2.040	2.041	2.042	2.041	2.043	2.044	2.042
369	2.041	2.042	2.041	2.042	2.044	2.042	2.044	2.045	2.043
370	2.042	2.043	2.042	2.044	2.045	2.044	2.047	2.048	2.045
371	2.043	2.044	2.043	2.045	2.047	2.044	2.049	2.049	2.047
372	2.048	2.048	2.047	2.049	2.049	2.048	2.049	2.049	2.049
373	2.048	2.048	2.047	2.049	2.049	2.048	2.049	2.050	2.049
374	2.048	2.048	2.047	2.048	2.048	2.048	2.050	2.049	2.048
375	2.046	2.048	2.045	2.048	2.048	2.047	2.049	2.049	2.048
376	2.043	2.045	2.044	2.045	2.046	2.044	2.048	2.048	2.046
377	2.045	2.047	2.045	2.047	2.048	2.046	2.049	2.049	2.048
378	2.044	2.047	2.045	2.047	2.048	2.044	2.049	2.049	2.048
379	2.046	2.048	2.047	2.048	2.049	2.047	2.049	2.049	2.048
380	2.070	2.071	2.070	2.071	2.071	2.070	2.072	2.072	2.071

TABLE F5 (continued)

381	2.068	2.069	2.068	2.069	2.069	2.068	2.070	2.070	2.069
382	2.063	2.064	2.063	2.065	2.066	2.063	2.067	2.068	2.065
383	2.061	2.062	2.060	2.062	2.062	2.061	2.063	2.063	2.061
384	2.059	2.060	2.059	2.060	2.061	2.059	2.061	2.061	2.060
385	2.054	2.057	2.053	2.057	2.057	2.054	2.059	2.059	2.058
386	2.053	2.054	2.052	2.054	2.056	2.053	2.058	2.058	2.056
387	2.052	2.053	2.052	2.054	2.055	2.053	2.057	2.057	2.054
388	2.051	2.051	2.051	2.052	2.053	2.051	2.054	2.054	2.053
389	2.050	2.051	2.050	2.050	2.051	2.051	2.053	2.053	2.051
390	2.044	2.047	2.044	2.044	2.048	2.044	2.049	2.049	2.046
391	2.045	2.047	2.045	2.048	2.048	2.045	2.049	2.049	2.048
392	2.046	2.047	2.044	2.046	2.048	2.045	2.049	2.049	2.048
393	2.051	2.051	2.051	2.051	2.052	2.051	2.053	2.054	2.052
394	2.052	2.053	2.052	2.053	2.054	2.053	2.057	2.057	2.054
395	2.054	2.056	2.054	2.056	2.057	2.055	2.059	2.059	2.057
396	2.057	2.059	2.057	2.058	2.059	2.058	2.060	2.060	2.059
397	2.058	2.058	2.057	2.059	2.059	2.058	2.060	2.060	2.059
398	2.060	2.061	2.059	2.060	2.061	2.060	2.063	2.062	2.061
399	2.061	2.061	2.061	2.061	2.062	2.061	2.063	2.063	2.062
400	2.061	2.062	2.061	2.062	2.063	2.061	2.064	2.066	2.062
401	2.063	2.064	2.062	2.063	2.065	2.063	2.067	2.067	2.064
402	2.064	2.065	2.064	2.065	2.067	2.063	2.067	2.066	2.066
403	2.067	2.067	2.066	2.068	2.068	2.067	2.069	2.069	2.068
404	2.067	2.068	2.065	2.068	2.068	2.067	2.069	2.069	2.068
405	2.063	2.064	2.063	2.065	2.067	2.064	2.068	2.068	2.068
406	2.472	2.473	2.472	2.474	2.475	2.472	2.478	2.478	2.474
407	2.474	2.478	2.474	2.478	2.479	2.477	2.480	2.480	2.479
408	2.477	2.479	2.478	2.479	2.480	2.478	2.481	2.481	2.480
409	2.479	2.479	2.478	2.480	2.481	2.479	2.482	2.482	2.481
410	2.480	2.481	2.479	2.481	2.481	2.480	2.483	2.483	2.482
411	2.480	2.481	2.480	2.481	2.483	2.480	2.484	2.487	2.483
412	2.480	2.481	2.480	2.481	2.483	2.481	2.485	2.487	2.483
413	2.480	2.481	2.480	2.481	2.482	2.480	2.485	2.487	2.483
414	2.481	2.482	2.481	2.483	2.486	2.482	2.488	2.489	2.487
415	2.482	2.484	2.482	2.486	2.488	2.483	2.489	2.489	2.487
416	2.484	2.486	2.483	2.487	2.489	2.484	2.490	2.490	2.488
417	2.486	2.488	2.484	2.488	2.489	2.487	2.490	2.491	2.489
418	2.488	2.489	2.487	2.489	2.490	2.488	2.491	2.491	2.490
419	1.458	1.458	1.457	1.457	1.457	1.457	1.457	1.457	1.457
420	1.453	1.453	1.453	1.453	1.454	1.454	1.455	1.455	1.453
421	1.452	1.452	1.452	1.452	1.452	1.452	1.452	1.452	1.452
422	1.451	1.451	1.451	1.451	1.451	1.451	1.451	1.451	1.451
423	1.450	1.450	1.450	1.450	1.450	1.450	1.450	1.450	1.450
424	1.447	1.447	1.447	1.447	1.448	1.448	1.448	1.448	1.448
425	1.447	1.448	1.448	1.448	1.448	1.448	1.449	1.449	1.449
426	1.447	1.447	1.447	1.447	1.448	1.448	1.448	1.448	1.448
427	1.444	1.444	1.444	1.444	1.445	1.445	1.445	1.445	1.445
428	1.441	1.441	1.441	1.441	1.441	1.442	1.442	1.442	1.442
429	1.442	1.442	1.442	1.442	1.442	1.442	1.442	1.442	1.442
430	1.442	1.442	1.442	1.442	1.442	1.442	1.442	1.442	1.442
431	1.441	1.441	1.441	1.441	1.442	1.442	1.442	1.442	1.442
432	2.060	2.061	2.060	2.061	2.061	2.061	2.062	2.063	2.062
433	2.061	2.061	2.060	2.061	2.061	2.060	2.062	2.062	2.062
434	2.061	2.061	2.060	2.061	2.061	2.061	2.063	2.063	2.062
435	2.060	2.061	2.060	2.061	2.061	2.060	2.062	2.062	2.061
436	2.060	2.060	2.060	2.060	2.060	2.060	2.062	2.062	2.061
437	2.059	2.059	2.059	2.060	2.060	2.059	2.061	2.061	2.060
438	2.052	2.052	2.052	2.053	2.053	2.052	2.056	2.056	2.054
439	2.052	2.053	2.052	2.053	2.054	2.053	2.058	2.058	2.055
440	2.053	2.053	2.052	2.054	2.054	2.052	2.058	2.058	2.055
441	2.052	2.053	2.051	2.053	2.055	2.053	2.057	2.057	2.055
442	2.054	2.054	2.053	2.055	2.055	2.053	2.058	2.058	2.057
443	2.054	2.055	2.053	2.056	2.057	2.054	2.058	2.058	2.057
444	2.055	2.055	2.054	2.056	2.058	2.055	2.059	2.059	2.058
445	2.030	2.030	2.029	2.030	2.031	2.029	2.031	2.031	2.030
446	2.032	2.033	2.031	2.032	2.033	2.032	2.036	2.036	2.034
447	2.037	2.038	2.035	2.038	2.039	2.037	2.039	2.039	2.038
448	2.039	2.040	2.039	2.040	2.041	2.040	2.041	2.041	2.040
449	2.041	2.041	2.041	2.042	2.042	2.041	2.043	2.044	2.042
450	2.043	2.044	2.043	2.046	2.046	2.044	2.049	2.048	2.046
451	2.046	2.048	2.046	2.048	2.049	2.047	2.049	2.049	2.048
452	2.048	2.048	2.047	2.049	2.049	2.047	2.049	2.049	2.049
453	2.049	2.050	2.049	2.050	2.050	2.049	2.051	2.051	2.050
454	2.050	2.051	2.050	2.051	2.052	2.051	2.053	2.053	2.051
455	2.050	2.051	2.050	2.051	2.052	2.050	2.053	2.053	2.051
456	2.051	2.051	2.050	2.051	2.052	2.051	2.053	2.053	2.052
457	2.051	2.051	2.050	2.051	2.052	2.051	2.053	2.053	2.051

TABLE F5 (continued)

458	2.518	2.519	2.511	2.520	2.520	2.514	2.522	2.522	2.518
459	2.519	2.519	2.511	2.520	2.521	2.514	2.523	2.523	2.519
460	2.518	2.518	2.511	2.520	2.520	2.513	2.522	2.523	2.518
461	2.518	2.518	2.511	2.520	2.521	2.514	2.523	2.523	2.518
462	2.520	2.520	2.513	2.523	2.523	2.514	2.526	2.527	2.520
463	2.520	2.521	2.514	2.523	2.524	2.518	2.528	2.528	2.521
464	2.520	2.521	2.517	2.523	2.526	2.519	2.528	2.529	2.521
465	2.520	2.522	2.517	2.523	2.524	2.518	2.529	2.529	2.521
466	2.521	2.522	2.517	2.524	2.524	2.519	2.528	2.528	2.521
467	2.520	2.521	2.514	2.523	2.524	2.518	2.527	2.528	2.521
468	2.520	2.520	2.512	2.521	2.522	2.515	2.524	2.524	2.519
470	2.518	2.519	2.524	2.532	2.532	2.527	2.534	2.534	2.529
471	2.529	2.530	2.523	2.531	2.532	2.526	2.534	2.533	2.529
472	2.529	2.530	2.523	2.531	2.532	2.526	2.534	2.533	2.529
473	2.524	2.527	2.520	2.529	2.529	2.521	2.531	2.531	2.523
474	2.524	2.525	2.520	2.528	2.528	2.520	2.530	2.530	2.523
475	2.523	2.524	2.519	2.528	2.527	2.520	2.530	2.529	2.522
476	2.523	2.524	2.519	2.527	2.524	2.520	2.529	2.529	2.521
477	2.521	2.522	2.518	2.524	2.524	2.519	2.528	2.528	2.520
478	2.521	2.522	2.517	2.523	2.524	2.518	2.528	2.528	2.520
479	2.521	2.522	2.518	2.523	2.524	2.519	2.527	2.527	2.520
480	2.517	2.517	2.511	2.519	2.519	2.512	2.520	2.520	2.516
481	2.517	2.517	2.511	2.518	2.519	2.513	2.521	2.521	2.516
482	2.518	2.518	2.511	2.518	2.519	2.512	2.521	2.521	2.516
483	2.518	2.518	2.511	2.520	2.519	2.512	2.521	2.521	2.516
484	2.422	2.422	2.418	2.423	2.424	2.419	2.426	2.427	2.422
485	2.422	2.422	2.418	2.423	2.424	2.420	2.427	2.426	2.422
486	2.422	2.422	2.418	2.423	2.424	2.420	2.427	2.428	2.422
487	2.422	2.422	2.418	2.423	2.424	2.420	2.427	2.427	2.421
488	2.421	2.421	2.417	2.423	2.424	2.420	2.426	2.427	2.421
489	2.420	2.420	2.417	2.421	2.422	2.419	2.424	2.424	2.420
490	2.420	2.420	2.416	2.422	2.423	2.419	2.424	2.425	2.420
491	2.420	2.420	2.415	2.421	2.422	2.418	2.424	2.424	2.420
492	2.420	2.420	2.414	2.421	2.422	2.418	2.424	2.424	2.420
493	2.417	2.417	2.412	2.419	2.420	2.413	2.421	2.422	2.417
494	2.417	2.417	2.413	2.419	2.420	2.414	2.421	2.422	2.418
495	2.419	2.419	2.412	2.419	2.420	2.415	2.422	2.422	2.419
496	2.418	2.418	2.412	2.419	2.420	2.413	2.421	2.422	2.418
497	1.869	1.869	1.868	1.870	1.870	1.869	1.870	1.871	1.869
498	1.869	1.869	1.868	1.870	1.870	1.869	1.870	1.871	1.869
499	1.869	1.869	1.868	1.870	1.870	1.869	1.870	1.871	1.869
500	1.869	1.869	1.867	1.869	1.870	1.869	1.870	1.870	1.869
501	1.869	1.869	1.867	1.869	1.870	1.868	1.870	1.870	1.869
502	1.869	1.869	1.867	1.870	1.870	1.868	1.870	1.870	1.869
503	1.864	1.865	1.863	1.866	1.868	1.864	1.868	1.868	1.865
504	1.865	1.868	1.863	1.867	1.868	1.865	1.869	1.869	1.867
505	1.866	1.868	1.864	1.868	1.869	1.867	1.869	1.869	1.867
506	1.866	1.867	1.864	1.868	1.869	1.866	1.869	1.869	1.866
507	1.867	1.867	1.864	1.868	1.869	1.865	1.869	1.869	1.867
508	1.867	1.867	1.864	1.868	1.869	1.865	1.869	1.869	1.867
509	1.865	1.866	1.864	1.868	1.868	1.864	1.869	1.869	1.867
510	2.429	2.430	2.427	2.431	2.432	2.426	2.433	2.434	2.430
511	2.429	2.430	2.426	2.431	2.432	2.428	2.434	2.434	2.431
512	2.429	2.430	2.427	2.431	2.432	2.429	2.435	2.437	2.430
513	2.429	2.430	2.428	2.431	2.432	2.429	2.435	2.437	2.430
514	2.430	2.431	2.428	2.432	2.433	2.429	2.435	2.437	2.431
515	2.430	2.431	2.428	2.432	2.433	2.429	2.435	2.437	2.431
516	2.430	2.431	2.428	2.432	2.433	2.429	2.435	2.437	2.431
517	2.430	2.431	2.428	2.432	2.434	2.429	2.436	2.437	2.431
518	2.430	2.431	2.428	2.432	2.435	2.429	2.436	2.437	2.431
519	2.431	2.432	2.429	2.433	2.435	2.420	2.437	2.439	2.433
520	2.431	2.432	2.429	2.434	2.436	2.421	2.438	2.438	2.433
521	2.431	2.432	2.429	2.434	2.436	2.420	2.438	2.439	2.433
522	2.431	2.432	2.429	2.434	2.438	2.421	2.438	2.439	2.433
523	2.599	2.599	2.593	2.602	2.602	2.596	2.604	2.604	2.599
524	2.599	2.599	2.594	2.602	2.602	2.596	2.604	2.605	2.599
525	2.599	2.599	2.593	2.601	2.602	2.597	2.604	2.604	2.599
526	2.597	2.599	2.592	2.600	2.600	2.593	2.602	2.602	2.597
527	2.597	2.599	2.592	2.600	2.600	2.594	2.602	2.602	2.597
528	2.597	2.599	2.590	2.600	2.600	2.591	2.601	2.601	2.597
529	2.598	2.599	2.591	2.600	2.601	2.593	2.602	2.602	2.598
530	2.598	2.599	2.592	2.600	2.601	2.594	2.602	2.603	2.598
531	2.598	2.599	2.592	2.600	2.601	2.595	2.602	2.603	2.598
532	2.598	2.599	2.592	2.600	2.601	2.594	2.602	2.603	2.598
533	2.598	2.599	2.592	2.600	2.601	2.595	2.603	2.603	2.598
534	2.598	2.599	2.593	2.600	2.601	2.594	2.602	2.602	2.598

TABLE F5 (continued)

535	2.598	2.599	2.592	2.600	2.601	2.594	2.602	2.602	2.596
536	2.150	2.152	2.151	2.153	2.153	2.152	2.155	2.155	2.152
537	2.150	2.152	2.151	2.153	2.154	2.152	2.155	2.154	2.153
538	2.150	2.151	2.150	2.153	2.154	2.151	2.155	2.156	2.153
539	2.151	2.151	2.150	2.152	2.153	2.151	2.155	2.155	2.153
540	2.150	2.151	2.150	2.152	2.153	2.151	2.156	2.157	2.152
541	2.151	2.152	2.151	2.153	2.154	2.152	2.157	2.158	2.153
542	2.151	2.153	2.152	2.154	2.154	2.153	2.157	2.157	2.154
543	2.152	2.153	2.153	2.154	2.154	2.153	2.157	2.157	2.154
544	4.870	4.903	4.919	4.892	4.919	4.926	4.910	4.934	4.929
545	4.878	4.910	4.925	4.898	4.924	4.932	4.918	4.941	4.936
546	4.881	4.915	4.930	4.902	4.929	4.937	4.922	4.946	4.940
547	4.884	4.919	4.933	4.904	4.931	4.940	4.924	4.949	4.943
548	4.880	4.915	4.930	4.901	4.929	4.937	4.921	4.947	4.941
549	1.907	1.908	1.907	1.909	1.910	1.908	1.910	1.910	1.909
550	1.909	1.909	1.907	1.910	1.910	1.909	1.911	1.911	1.910
551	1.910	1.910	1.909	1.911	1.912	1.910	1.912	1.912	1.911
552	1.912	1.913	1.910	1.913	1.914	1.912	1.915	1.916	1.913
553	1.913	1.913	1.911	1.914	1.915	1.913	1.915	1.917	1.914
554	1.912	1.913	1.913	1.914	1.916	1.913	1.917	1.917	1.915
555	1.914	1.914	1.913	1.917	1.916	1.915	1.918	1.916	1.917
556	2.268	2.268	2.267	2.269	2.270	2.267	2.271	2.271	2.269
557	2.269	2.269	2.267	2.270	2.271	2.268	2.272	2.272	2.270
558	2.269	2.270	2.268	2.271	2.272	2.269	2.273	2.273	2.270
559	2.269	2.270	2.268	2.271	2.272	2.270	2.274	2.274	2.271
560	2.270	2.271	2.269	2.272	2.273	2.270	2.274	2.274	2.271
561	2.270	2.271	2.269	2.272	2.273	2.270	2.275	2.275	2.276
562	2.270	2.271	2.269	2.272	2.273	2.270	2.274	2.276	2.272
563	2.269	2.269	2.263	2.270	2.270	2.265	2.271	2.271	2.266
564	2.269	2.269	2.263	2.271	2.270	2.267	2.272	2.272	2.269
565	2.270	2.270	2.265	2.271	2.271	2.267	2.273	2.273	2.269
566	2.270	2.270	2.265	2.272	2.272	2.268	2.273	2.273	2.270
567	2.270	2.271	2.267	2.272	2.272	2.268	2.274	2.274	2.270
568	2.687	2.689	2.684	2.690	2.691	2.688	2.694	2.695	2.690
569	2.691	2.693	2.690	2.694	2.698	2.692	2.699	2.700	2.697
570	2.693	2.698	2.693	2.698	2.699	2.696	2.701	2.703	2.699
571	2.698	2.699	2.697	2.700	2.701	2.699	2.703	2.706	2.701
572	2.700	2.701	2.699	2.703	2.706	2.701	2.708	2.709	2.702
573	2.702	2.706	2.701	2.708	2.709	2.704	2.710	2.712	2.709
574	2.703	2.708	2.702	2.709	2.710	2.705	2.711	2.713	2.709
575	2.705	2.709	2.703	2.709	2.711	2.706	2.712	2.713	2.710
576	3.145	3.148	3.142	3.149	3.152	3.147	3.154	3.157	3.150
577	3.147	3.150	3.144	3.151	3.154	3.148	3.157	3.159	3.152
578	3.148	3.150	3.144	3.152	3.154	3.148	3.158	3.159	3.153
579	3.148	3.151	3.147	3.153	3.157	3.149	3.158	3.159	3.153
580	3.149	3.152	3.148	3.153	3.157	3.150	3.159	3.160	3.154
581	3.150	3.153	3.148	3.154	3.158	3.151	3.160	3.162	3.156
582	3.150	3.154	3.149	3.156	3.159	3.152	3.161	3.162	3.157
583	3.152	3.157	3.150	3.157	3.159	3.153	3.161	3.163	3.156
584	2.931	2.935	2.932	2.934	2.940	2.937	2.940	2.943	2.946
585	2.930	2.936	2.932	2.934	2.940	2.938	2.941	2.944	2.941
586	2.929	2.932	2.930	2.932	2.938	2.933	2.939	2.942	2.939
587	2.927	2.932	2.930	2.931	2.937	2.933	2.938	2.941	2.938
588	2.925	2.930	2.928	2.929	2.934	2.931	2.934	2.937	2.935
589	4.339	4.349	4.342	4.348	4.357	4.350	4.359	4.367	4.359
590	4.338	4.349	4.342	4.348	4.358	4.350	4.359	4.365	4.359
591	4.338	4.349	4.342	4.348	4.357	4.349	4.358	4.365	4.358
592	4.338	4.349	4.342	4.346	4.356	4.349	4.359	4.365	4.356
593	4.337	4.346	4.340	4.346	4.353	4.346	4.356	4.363	4.357
594	4.338	4.349	4.342	4.348	4.358	4.350	4.359	4.367	4.359
595	6.529	6.550	6.539	6.547	6.560	6.553	6.569	6.583	6.568
596	6.529	6.549	6.538	6.545	6.567	6.552	6.568	6.583	6.568
597	6.527	6.548	6.537	6.543	6.564	6.551	6.567	6.581	6.567
598	6.527	6.549	6.537	6.544	6.564	6.550	6.566	6.582	6.567
599	3.704	3.711	3.708	3.710	3.720	3.713	3.720	3.726	3.721
600	3.705	3.713	3.709	3.711	3.720	3.716	3.720	3.726	3.721
601	3.707	3.714	3.710	3.712	3.721	3.717	3.721	3.729	3.722
602	3.708	3.717	3.711	3.713	3.722	3.718	3.722	3.730	3.724
603	3.711	3.719	3.714	3.716	3.726	3.721	3.726	3.732	3.728
604	3.712	3.720	3.716	3.719	3.728	3.722	3.728	3.733	3.729
605	3.160	3.164	3.159	3.164	3.170	3.164	3.170	3.173	3.169
606	3.161	3.166	3.160	3.166	3.170	3.163	3.177	3.174	3.169
607	3.161	3.167	3.160	3.169	3.171	3.165	3.171	3.174	3.170
608	3.162	3.168	3.161	3.168	3.172	3.166	3.173	3.177	3.170
609	3.162	3.168	3.161	3.168	3.172	3.167	3.173	3.176	3.170
610	3.163	3.169	3.161	3.168	3.173	3.167	3.173	3.176	3.170
611	4.010	4.018	4.008	4.018	4.024	4.016	4.026	4.030	4.022

TABLE F5 (continued)

612	4.012	4.020	4.009	4.020	4.028	4.018	4.029	4.032	4.024
613	4.012	4.021	4.011	4.022	4.029	4.020	4.030	4.034	4.026
614	4.014	4.022	4.012	4.022	4.029	4.020	4.030	4.037	4.027
615	4.016	4.023	4.013	4.023	4.030	4.021	4.031	4.036	4.028
616	4.018	4.025	4.015	4.026	4.032	4.023	4.032	4.039	4.030
617	4.770	4.780	4.768	4.781	4.791	4.779	4.791	4.799	4.787
618	4.771	4.782	4.769	4.782	4.792	4.780	4.793	4.800	4.789
619	4.773	4.783	4.770	4.784	4.794	4.781	4.796	4.801	4.790
620	4.775	4.785	4.772	4.787	4.796	4.783	4.798	4.803	4.792
621	4.778	4.789	4.774	4.789	4.799	4.786	4.799	4.807	4.794
622	4.780	4.790	4.778	4.790	4.801	4.789	4.801	4.809	4.798
623	7.216	7.237	7.212	7.239	7.259	7.234	7.259	7.273	7.249
624	7.228	7.250	7.224	7.251	7.271	7.249	7.270	7.285	7.261
625	7.231	7.252	7.229	7.257	7.276	7.252	7.274	7.290	7.264
626	7.236	7.259	7.232	7.260	7.279	7.257	7.279	7.294	7.269
627	7.238	7.260	7.234	7.262	7.282	7.259	7.281	7.297	7.272
628	7.243	7.267	7.241	7.269	7.289	7.264	7.280	7.302	7.276
629	3.563	3.571	3.563	3.570	3.578	3.569	3.578	3.581	3.574
630	3.564	3.572	3.563	3.571	3.579	3.570	3.579	3.582	3.575
631	3.567	3.573	3.566	3.572	3.579	3.572	3.579	3.583	3.578
632	3.568	3.574	3.567	3.572	3.579	3.572	3.580	3.584	3.576
633	3.568	3.575	3.568	3.573	3.581	3.573	3.580	3.586	3.579
634	3.568	3.574	3.568	3.574	3.580	3.574	3.581	3.585	3.579
635	3.501	3.508	3.499	3.507	3.511	3.504	3.511	3.515	3.508
636	3.504	3.510	3.501	3.510	3.514	3.507	3.514	3.518	3.510
637	3.505	3.510	3.502	3.510	3.515	3.508	3.514	3.519	3.510
638	3.506	3.510	3.501	3.510	3.516	3.508	3.514	3.519	3.511
639	3.506	3.511	3.503	3.511	3.516	3.509	3.516	3.519	3.511
640	3.508	3.512	3.503	3.512	3.518	3.509	3.518	3.520	3.513
641	3.935	3.942	3.930	3.941	3.948	3.938	3.948	3.951	3.942
642	3.938	3.944	3.932	3.943	3.950	3.940	3.949	3.953	3.944
643	3.939	3.944	3.932	3.944	3.950	3.940	3.949	3.953	3.944
644	3.939	3.944	3.933	3.944	3.951	3.940	3.950	3.956	3.946
645	3.939	3.945	3.933	3.944	3.951	3.941	3.950	3.954	3.946
646	3.939	3.946	3.934	3.946	3.952	3.942	3.951	3.957	3.947
647	4.623	4.632	4.619	4.631	4.640	4.627	4.640	4.645	4.632
648	4.624	4.632	4.619	4.634	4.640	4.628	4.640	4.645	4.633
649	4.624	4.633	4.619	4.633	4.640	4.628	4.640	4.647	4.633
650	4.624	4.633	4.619	4.633	4.641	4.628	4.641	4.646	4.633
651	4.626	4.634	4.620	4.634	4.642	4.629	4.642	4.648	4.634
652	4.627	4.634	4.620	4.634	4.642	4.629	4.642	4.649	4.634
653	5.442	5.452	5.434	5.452	5.463	5.444	5.461	5.470	5.452
654	5.443	5.453	5.434	5.454	5.465	5.444	5.463	5.471	5.453
655	5.444	5.454	5.436	5.455	5.467	5.447	5.465	5.472	5.453
656	5.444	5.454	5.436	5.456	5.467	5.448	5.465	5.472	5.454
657	5.444	5.454	5.437	5.456	5.468	5.448	5.467	5.472	5.454
658	5.444	5.454	5.437	5.457	5.468	5.448	5.467	5.472	5.454
659	8.317	8.333	8.300	8.341	8.359	8.322	8.357	8.370	8.334
660	8.319	8.337	8.301	8.343	8.360	8.324	8.359	8.373	8.338
661	8.320	8.338	8.303	8.346	8.363	8.329	8.361	8.374	8.338
662	8.321	8.339	8.303	8.347	8.363	8.327	8.360	8.375	8.338
663	8.322	8.340	8.305	8.349	8.364	8.328	8.362	8.377	8.340
664	8.328	8.346	8.310	8.353	8.370	8.333	8.368	8.381	8.345
665	1.993	1.996	1.997	1.994	1.999	1.999	1.999	2.000	1.999
666	1.994	1.998	1.998	1.997	1.999	1.999	1.999	2.000	1.999
667	1.993	1.998	1.998	1.996	1.999	1.999	1.999	2.001	1.999
668	1.998	2.000	2.000	1.999	2.002	2.001	2.001	2.003	2.002
669	1.998	2.000	2.000	1.999	2.002	2.002	2.002	2.004	2.003
670	2.351	2.358	2.356	2.354	2.359	2.353	2.359	2.362	2.360
671	2.352	2.359	2.359	2.357	2.361	2.359	2.361	2.363	2.362
672	2.354	2.360	2.359	2.359	2.363	2.360	2.363	2.365	2.363
673	2.355	2.360	2.359	2.359	2.364	2.362	2.363	2.367	2.364
674	2.358	2.362	2.359	2.360	2.364	2.363	2.365	2.368	2.366
675	3.310	3.323	3.318	3.319	3.330	3.326	3.329	3.335	3.331
676	3.312	3.326	3.320	3.321	3.332	3.329	3.332	3.338	3.333
677	3.313	3.328	3.320	3.322	3.333	3.330	3.332	3.340	3.334
678	3.317	3.329	3.323	3.327	3.337	3.332	3.335	3.342	3.338
679	1.893	1.894	1.892	1.894	1.897	1.894	1.897	1.898	1.895
680	1.893	1.894	1.893	1.894	1.896	1.894	1.898	1.898	1.897
681	1.894	1.896	1.893	1.897	1.898	1.894	1.898	1.899	1.897
682	1.896	1.896	1.894	1.898	1.898	1.897	1.898	1.899	1.897
683	1.897	1.897	1.895	1.897	1.899	1.896	1.899	1.900	1.898
684	1.897	1.897	1.895	1.898	1.899	1.897	1.899	1.900	1.898
685	2.251	2.253	2.250	2.253	2.254	2.252	2.258	2.258	2.253
686	2.252	2.253	2.250	2.254	2.257	2.253	2.258	2.259	2.255
687	2.253	2.256	2.252	2.256	2.258	2.254	2.259	2.259	2.257
688	2.253	2.257	2.251	2.257	2.259	2.254	2.259	2.260	2.257

TABLE F5 (continued)

689	2.255	2.257	2.253	2.258	2.259	2.257	2.260	2.261	2.256
690	2.257	2.259	2.253	2.258	2.259	2.258	2.261	2.262	2.259
691	2.712	2.714	2.719	2.714	2.718	2.712	2.719	2.720	2.719
692	2.713	2.717	2.710	2.716	2.719	2.713	2.721	2.722	2.716
693	2.716	2.719	2.713	2.720	2.722	2.716	2.723	2.724	2.720
694	2.716	2.719	2.712	2.720	2.721	2.717	2.723	2.723	2.720
695	2.715	2.719	2.712	2.719	2.720	2.718	2.723	2.723	2.719
696	2.716	2.719	2.712	2.719	2.721	2.716	2.722	2.723	2.719
697	3.216	3.219	3.211	3.220	3.223	3.216	3.227	3.228	3.221
698	3.218	3.221	3.213	3.222	3.226	3.220	3.229	3.230	3.226
699	3.220	3.223	3.217	3.225	3.229	3.222	3.230	3.232	3.227
700	3.221	3.225	3.218	3.226	3.230	3.223	3.232	3.234	3.227
701	3.222	3.227	3.219	3.228	3.231	3.224	3.234	3.235	3.229
702	3.222	3.227	3.220	3.227	3.231	3.224	3.233	3.235	3.229
703	1.872	1.873	1.870	1.873	1.874	1.872	1.877	1.876	1.874
704	1.877	1.878	1.874	1.879	1.879	1.877	1.879	1.880	1.876
705	1.878	1.879	1.875	1.879	1.880	1.878	1.880	1.880	1.879
706	1.878	1.879	1.877	1.879	1.880	1.879	1.880	1.881	1.880
707	1.879	1.880	1.878	1.880	1.881	1.879	1.881	1.882	1.881
708	1.880	1.881	1.879	1.881	1.882	1.880	1.882	1.882	1.881
709	2.221	2.222	2.219	2.222	2.224	2.221	2.224	2.227	2.223
710	2.222	2.223	2.220	2.223	2.226	2.222	2.227	2.226	2.224
711	2.223	2.224	2.221	2.226	2.226	2.223	2.228	2.229	2.224
712	2.223	2.225	2.221	2.224	2.227	2.223	2.229	2.229	2.227
713	2.224	2.226	2.221	2.226	2.228	2.223	2.229	2.229	2.226
714	2.224	2.226	2.221	2.227	2.229	2.224	2.229	2.230	2.226
715	2.740	2.742	2.735	2.742	2.746	2.740	2.747	2.749	2.742
716	2.740	2.742	2.737	2.743	2.748	2.740	2.748	2.749	2.743
717	2.741	2.743	2.738	2.745	2.748	2.741	2.749	2.750	2.743
718	2.743	2.744	2.738	2.745	2.748	2.742	2.749	2.751	2.744
719	2.743	2.744	2.739	2.746	2.749	2.742	2.749	2.751	2.746
720	2.743	2.747	2.740	2.746	2.749	2.742	2.750	2.752	2.747
721	1.880	1.880	1.879	1.881	1.882	1.880	1.882	1.882	1.880
722	1.881	1.882	1.880	1.882	1.883	1.881	1.883	1.883	1.881
723	1.882	1.883	1.881	1.883	1.884	1.882	1.884	1.886	1.883
724	1.883	1.884	1.882	1.885	1.887	1.883	1.886	1.887	1.883
725	1.884	1.884	1.882	1.885	1.887	1.884	1.887	1.889	1.885
726	1.887	1.888	1.883	1.888	1.889	1.886	1.888	1.889	1.887
727	2.220	2.221	2.218	2.221	2.223	2.219	2.223	2.224	2.221
728	2.221	2.222	2.219	2.222	2.224	2.220	2.224	2.226	2.222
729	2.222	2.223	2.220	2.224	2.226	2.222	2.227	2.227	2.223
730	2.223	2.224	2.221	2.224	2.228	2.223	2.227	2.228	2.224
731	2.223	2.224	2.221	2.226	2.228	2.223	2.228	2.229	2.224
732	2.224	2.226	2.221	2.226	2.228	2.224	2.228	2.230	2.226
733	2.723	2.727	2.721	2.728	2.729	2.723	2.729	2.730	2.725
734	2.723	2.727	2.721	2.728	2.730	2.723	2.729	2.731	2.727
735	2.725	2.729	2.722	2.729	2.730	2.725	2.730	2.732	2.729
736	2.727	2.729	2.723	2.729	2.731	2.726	2.732	2.734	2.729
737	2.728	2.730	2.724	2.730	2.732	2.728	2.732	2.737	2.730
738	2.730	2.731	2.727	2.731	2.733	2.729	2.734	2.738	2.730

TABLE F6

[illegible]

TABLE F6 (continued)

214	217	220	223	226	229	232	235	238	241	244	247	250	253	256	259	262	265	268	271	274	277	280	283	286	289	292	295	298	301	304	307	310	313	316	319	322	325	328	331	334	337	340	343	346	349	352	355	358	361	364	367	370	373	376	379	382	385	388	391	394	397	400	403	406	409	412	415	418	421	424	427	430	433	436	439	442	445	448	451	454	457	460	463	466	469	472	475	478	481	484	487	490	493	496	499	502	505	508	511	514	517	520	523	526	529	532	535	538	541	544	547	550	553	556	559	562	565	568	571	574	577	580	583	586	589	592	595	598	601	604	607	610	613	616	619	622	625	628	631	634	637	640	643	646	649	652	655	658	661	664	667	670	673	676	679	682	685	688	691	694	697	700	703	706	709	712	715	718	721	724	727	730	733	736	739	742	745	748	751	754	757	760	763	766	769	772	775	778	781	784	787	790	793	796	799	802	805	808	811	814	817	820	823	826	829	832	835	838	841	844	847	850	853	856	859	862	865	868	871	874	877	880	883	886	889	892	895	898	901	904	907	910	913	916	919	922	925	928	931	934	937	940	943	946	949	952	955	958	961	964	967	970	973	976	979	982	985	988	991	994	997	1000
-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	------

TABLE F6 (continued)

676	3.32700	0.00508	80.710	677	3.32300	0.00529	80.733	678	3.33111	0.00793	80.803
679	1.89489	0.00203	47.332	680	1.89522	0.00205	47.340	681	1.89611	0.00196	47.362
682	1.89700	0.00150	47.383	683	1.89756	0.00159	47.396	684	1.89778	0.00146	47.402
685	2.25356	0.00279	55.904	686	2.25456	0.00296	55.928	687	2.25589	0.00267	55.959
688	2.25633	0.00304	55.970	689	2.25756	0.00246	55.999	690	2.25844	0.00255	56.020
691	2.27163	0.00328	66.748	692	2.27165	0.00397	66.754	693	2.27194	0.00347	66.821
694	2.27190	0.00354	66.810	695	2.27186	0.00350	66.803	696	2.27185	0.00343	66.800
697	3.22033	0.00529	78.299	698	3.22256	0.00539	78.349	699	3.22500	0.00423	78.405
700	3.22622	0.00519	78.432	701	3.22767	0.00534	78.463	702	3.22767	0.00487	78.485
703	1.87367	0.00250	46.820	704	1.87789	0.00176	46.922	705	1.87867	0.00156	46.941
706	1.87911	0.00117	46.952	707	1.88000	0.00122	46.973	708	1.88009	0.00103	46.994
709	2.22256	0.00210	55.169	710	2.22389	0.00262	55.201	711	2.22489	0.00257	55.224
712	2.22383	0.00283	55.235	713	2.22578	0.00273	55.246	714	2.22622	0.00291	55.256
715	2.24256	0.00425	67.356	716	2.24333	0.00418	67.374	717	2.24422	0.00409	67.395
718	2.24489	0.00395	67.410	719	2.24544	0.00384	67.423	720	2.24644	0.00397	67.446
721	1.88067	0.00112	46.989	722	1.88178	0.00109	47.016	723	1.88311	0.00143	47.048
724	1.88411	0.00176	47.072	725	1.88522	0.00211	47.099	726	1.88672	0.00186	47.147
727	2.22111	0.00193	55.185	728	2.22222	0.00217	55.181	729	2.22378	0.00244	55.193
730	2.22467	0.00345	55.219	731	2.22511	0.00276	55.230	732	2.22559	0.00267	55.248
733	2.22611	0.00322	66.975	734	2.22656	0.00347	66.983	735	2.22789	0.00316	67.016
736	2.22869	0.00350	67.039	737	2.23011	0.00355	67.068	738	2.23144	0.00321	67.099

TABLE F7

Raw Experimental Data

Thermocouple Wires Numbers 19 to 27

	MILLIVOLTS READ IN FOR POSITIONS 19 TO 27 ARE									
1	2.051	2.050	2.048	2.049	2.049	2.049	2.048			
2	2.054	2.054	2.050	2.053	2.053	2.053	2.052			
3	2.056	2.056	2.053	2.055	2.055	2.055	2.053			
4	2.058	2.057	2.055	2.057	2.057	2.057	2.056			
5	2.059	2.058	2.056	2.059	2.059	2.059	2.058			
6	2.060	2.059	2.057	2.059	2.059	2.059	2.058			
7	2.060	2.060	2.057	2.059	2.059	2.059	2.058			
8	2.067	2.067	2.064	2.067	2.067	2.067	2.065			
9	2.062	2.062	2.059	2.061	2.061	2.061	2.061			
10	2.062	2.062	2.059	2.061	2.061	2.061	2.060			
11	2.063	2.063	2.059	2.062	2.062	2.062	2.060			
12	2.063	2.063	2.060	2.063	2.063	2.063	2.061			
13	2.064	2.063	2.060	2.063	2.063	2.063	2.061			
14	2.064	2.064	2.061	2.064	2.064	2.064	2.062			
15	2.059	2.060	2.057	2.058	2.058	2.058	2.058			
16	2.061	2.060	2.058	2.060	2.060	2.060	2.059			
17	2.061	2.061	2.058	2.061	2.061	2.060	2.059			
18	2.062	2.061	2.059	2.061	2.061	2.060	2.060			
19	2.061	2.061	2.059	2.061	2.061	2.061	2.060			
20	2.060	2.060	2.058	2.060	2.060	2.060	2.059			
21	2.061	2.061	2.058	2.060	2.060	2.060	2.059			
22	2.062	2.061	2.059	2.060	2.060	2.060	2.059			
23	2.063	2.063	2.060	2.063	2.063	2.063	2.061			
24	2.064	2.063	2.062	2.064	2.064	2.064	2.063			
25	2.064	2.064	2.062	2.063	2.063	2.063	2.063			
26	2.064	2.064	2.061	2.063	2.063	2.063	2.061			
27	2.063	2.063	2.060	2.063	2.063	2.063	2.061			
28	2.063	2.063	2.060	2.062	2.062	2.062	2.061			
29	1.480	1.480	1.478	1.479	1.479	1.479	1.479			
30	1.477	1.477	1.477	1.477	1.477	1.477	1.477			
31	1.474	1.474	1.474	1.474	1.474	1.474	1.474			
32	1.468	1.467	1.466	1.467	1.467	1.467	1.467			
33	1.464	1.464	1.463	1.464	1.464	1.464	1.464			
34	1.451	1.451	1.451	1.451	1.451	1.451	1.451			
35	1.452	1.452	1.452	1.452	1.452	1.452	1.452			
36	1.453	1.453	1.452	1.453	1.453	1.453	1.453			
37	1.453	1.453	1.452	1.453	1.453	1.453	1.453			
38	1.456	1.456	1.454	1.455	1.455	1.455	1.455			
39	1.456	1.456	1.455	1.456	1.456	1.456	1.456			
40	1.457	1.457	1.456	1.457	1.457	1.457	1.457			
41	1.458	1.458	1.456	1.457	1.458	1.458	1.458			
42	1.458	1.458	1.457	1.458	1.458	1.458	1.458			
43	2.497	2.497	2.494	2.497	2.497	2.497	2.495			
44	2.498	2.496	2.494	2.497	2.497	2.497	2.493			
45	2.498	2.497	2.494	2.497	2.497	2.497	2.494			
46	2.499	2.498	2.494	2.497	2.497	2.497	2.494			
47	2.498	2.498	2.493	2.497	2.497	2.497	2.494			
48	2.498	2.497	2.493	2.497	2.497	2.497	2.494			
49	2.497	2.497	2.493	2.496	2.496	2.496	2.494			
50	2.503	2.501	2.499	2.501	2.501	2.501	2.499			
51	2.501	2.500	2.498	2.500	2.500	2.500	2.499			
52	2.502	2.500	2.498	2.500	2.500	2.500	2.499			
53	2.500	2.500	2.498	2.499	2.499	2.499	2.498			
54	2.499	2.498	2.495	2.498	2.498	2.498	2.496			
55	2.499	2.499	2.494	2.497	2.497	2.497	2.495			
56	2.107	2.107	2.104	2.107	2.107	2.107	2.104			
57	2.102	2.102	2.100	2.101	2.102	2.102	2.100			
58	2.097	2.097	2.095	2.097	2.097	2.097	2.096			
59	2.096	2.096	2.092	2.095	2.095	2.095	2.093			
60	2.092	2.092	2.090	2.093	2.093	2.093	2.090			
61	2.117	2.117	2.114	2.117	2.116	2.116	2.114			
62	2.111	2.111	2.109	2.111	2.111	2.111	2.110			
63	2.109	2.109	2.106	2.108	2.108	2.108	2.108			
64	2.107	2.107	2.105	2.107	2.107	2.107	2.105			
65	2.106	2.106	2.104	2.106	2.106	2.106	2.105			
66	2.102	2.102	2.101	2.101	2.101	2.101	2.101			
67	2.100	2.100	2.099	2.100	2.100	2.100	2.099			
68	2.100	2.100	2.099	2.100	2.100	2.100	2.099			
69	2.093	2.093	2.091	2.093	2.093	2.093	2.092			
70	2.092	2.092	2.090	2.091	2.091	2.091	2.090			
71	2.090	2.090	2.089	2.090	2.090	2.090	2.089			
72	2.089	2.089	2.088	2.089	2.089	2.089	2.088			

TABLE F7 (continued)

73	2.089	2.089	2.087	2.089	2.039	2.089	2.088
74	2.085	2.085	2.083	2.086	2.085	2.085	2.085
75	2.081	2.081	2.079	2.081	2.030	2.080	2.080
76	2.081	2.081	2.080	2.081	2.081	2.081	2.080
77	2.081	2.082	2.080	2.081	2.081	2.080	2.080
78	2.075	2.075	2.073	2.076	2.075	2.075	2.074
79	2.079	2.079	2.077	2.079	2.078	2.078	2.077
80	2.079	2.079	2.077	2.079	2.078	2.078	2.077
81	2.092	2.091	2.090	2.091	2.091	2.091	2.089
82	2.080	2.080	2.078	2.079	2.079	2.079	2.077
83	2.088	2.088	2.083	2.086	2.086	2.086	2.083
84	2.083	2.083	2.080	2.082	2.082	2.082	2.080
85	2.079	2.079	2.075	2.078	2.078	2.078	2.075
86	2.079	2.078	2.075	2.077	2.077	2.077	2.073
87	2.079	2.078	2.076	2.077	2.078	2.078	2.074
88	2.102	2.101	2.099	2.100	2.100	2.100	2.099
89	2.091	2.090	2.089	2.090	2.090	2.090	2.089
90	2.086	2.085	2.082	2.084	2.084	2.084	2.081
91	2.084	2.083	2.080	2.082	2.082	2.082	2.080
92	2.082	2.082	2.080	2.081	2.081	2.081	2.080
93	2.089	2.088	2.085	2.087	2.087	2.087	2.085
94	1.460	1.460	1.459	1.460	1.460	1.460	1.459
95	1.466	1.466	1.463	1.465	1.465	1.465	1.464
96	1.465	1.465	1.462	1.465	1.465	1.465	1.464
97	1.470	1.470	1.470	1.470	1.471	1.471	1.470
98	1.470	1.470	1.469	1.470	1.470	1.470	1.470
99	1.469	1.469	1.468	1.469	1.469	1.469	1.469
100	1.468	1.468	1.468	1.468	1.468	1.468	1.468
101	1.460	1.460	1.459	1.460	1.460	1.460	1.460
102	1.468	1.468	1.467	1.468	1.468	1.468	1.467
103	1.468	1.468	1.467	1.468	1.468	1.468	1.468
104	1.469	1.469	1.465	1.468	1.468	1.468	1.467
105	1.467	1.467	1.466	1.468	1.468	1.468	1.468
106	1.463	1.463	1.463	1.464	1.464	1.464	1.464
107	2.550	2.549	2.546	2.549	2.549	2.549	2.545
108	2.542	2.541	2.539	2.540	2.541	2.541	2.539
109	2.537	2.535	2.531	2.532	2.532	2.532	2.530
110	2.553	2.552	2.549	2.550	2.551	2.551	2.549
111	2.541	2.541	2.539	2.540	2.540	2.540	2.537
112	2.538	2.535	2.531	2.533	2.533	2.533	2.530
113	2.531	2.531	2.529	2.530	2.530	2.530	2.526
114	2.527	2.525	2.521	2.524	2.524	2.524	2.520
115	2.523	2.521	2.519	2.520	2.520	2.520	2.518
116	2.519	2.519	2.514	2.517	2.517	2.517	2.512
117	2.518	2.516	2.511	2.513	2.513	2.514	2.510
118	2.509	2.508	2.503	2.508	2.508	2.508	2.502
119	2.509	2.508	2.502	2.505	2.505	2.505	2.501
120	2.119	2.119	2.115	2.119	2.118	2.118	2.116
121	2.113	2.113	2.110	2.112	2.112	2.112	2.111
122	2.109	2.109	2.105	2.108	2.108	2.108	2.105
123	2.102	2.103	2.100	2.102	2.102	2.102	2.100
124	2.098	2.099	2.094	2.098	2.098	2.098	2.094
125	2.093	2.093	2.091	2.092	2.092	2.092	2.090
126	2.091	2.091	2.089	2.090	2.090	2.090	2.090
127	2.091	2.091	2.090	2.091	2.091	2.091	2.090
128	2.115	2.116	2.113	2.114	2.114	2.114	2.112
129	2.110	2.110	2.109	2.110	2.110	2.110	2.109
130	2.108	2.109	2.106	2.107	2.107	2.107	2.104
131	2.102	2.102	2.100	2.102	2.102	2.102	2.100
132	2.098	2.098	2.094	2.097	2.097	2.096	2.094
133	2.112	2.112	2.110	2.111	2.111	2.111	2.110
134	2.110	2.110	2.108	2.109	2.109	2.109	2.106
135	2.108	2.108	2.103	2.105	2.105	2.105	2.103
136	2.112	2.112	2.110	2.111	2.111	2.111	2.110
137	2.109	2.108	2.104	2.107	2.107	2.107	2.104
138	2.090	2.090	2.089	2.090	2.090	2.090	2.088
139	2.116	2.116	2.111	2.114	2.114	2.114	2.111
140	2.109	2.109	2.104	2.108	2.108	2.108	2.104
141	2.101	2.101	2.100	2.101	2.100	2.100	2.099
142	2.099	2.098	2.095	2.098	2.098	2.098	2.095
143	2.091	2.091	2.090	2.090	2.090	2.090	2.089
144	2.089	2.088	2.086	2.089	2.089	2.089	2.085
145	2.089	2.089	2.085	2.087	2.087	2.087	2.084
146	2.091	2.091	2.089	2.090	2.090	2.090	2.089
147	2.090	2.090	2.088	2.089	2.089	2.089	2.087
148	2.084	2.084	2.081	2.082	2.082	2.082	2.081
149	2.084	2.084	2.081	2.082	2.082	2.082	2.080

TABLE F7 (continued)

150	2.081	2.081	2.080	2.081	2.081	2.081	2.079
151	2.081	2.081	2.079	2.080	2.080	2.080	2.079
152	2.080	2.080	2.079	2.080	2.080	2.080	2.079
153	2.079	2.079	2.078	2.079	2.079	2.079	2.078
154	2.078	2.077	2.074	2.076	2.076	2.076	2.073
155	2.078	2.078	2.074	2.077	2.077	2.077	2.074
156	2.078	2.073	2.074	2.076	2.076	2.076	2.072
157	2.091	2.091	2.090	2.090	2.090	2.090	2.089
158	2.089	2.089	2.084	2.086	2.088	2.088	2.084
159	2.104	2.103	2.102	2.100	2.102	2.102	2.102
160	2.100	2.099	2.099	2.095	2.098	2.099	2.098
161	2.095	2.094	2.093	2.091	2.093	2.093	2.093
162	2.091	2.090	2.090	2.089	2.090	2.090	2.090
163	2.089	2.088	2.088	2.085	2.089	2.088	2.088
164	2.085	2.084	2.083	2.081	2.083	2.083	2.083
165	2.082	2.082	2.081	2.079	2.081	2.081	2.081
166	2.078	2.076	2.075	2.073	2.074	2.075	2.073
167	2.075	2.074	2.074	2.071	2.073	2.074	2.071
168	2.071	2.070	2.070	2.069	2.069	2.070	2.069
169	2.070	2.070	2.070	2.069	2.070	2.070	2.070
170	2.074	2.073	2.073	2.071	2.073	2.073	2.073
171	2.074	2.073	2.073	2.071	2.072	2.073	2.072
172	1.451	1.451	1.451	1.450	1.451	1.451	1.451
173	1.449	1.449	1.449	1.449	1.449	1.449	1.449
174	1.445	1.445	1.445	1.444	1.445	1.445	1.445
175	1.444	1.444	1.444	1.443	1.444	1.444	1.443
176	1.442	1.442	1.442	1.441	1.442	1.442	1.441
177	1.441	1.441	1.441	1.440	1.441	1.441	1.441
178	1.440	1.440	1.440	1.440	1.440	1.440	1.440
179	1.440	1.440	1.440	1.440	1.440	1.440	1.440
180	1.441	1.441	1.441	1.440	1.441	1.441	1.441
181	1.442	1.442	1.442	1.441	1.441	1.441	1.441
182	1.441	1.441	1.441	1.441	1.442	1.442	1.441
183	1.442	1.442	1.442	1.441	1.442	1.442	1.442
184	1.442	1.441	1.442	1.441	1.441	1.442	1.441
185	2.499	2.498	2.498	2.493	2.498	2.498	2.492
186	2.503	2.503	2.501	2.499	2.501	2.502	2.499
187	2.503	2.503	2.500	2.499	2.500	2.501	2.498
188	2.525	2.524	2.522	2.520	2.521	2.522	2.519
189	2.509	2.509	2.508	2.504	2.508	2.508	2.503
190	2.553	2.552	2.551	2.549	2.550	2.551	2.548
191	2.540	2.540	2.539	2.536	2.539	2.539	2.534
192	2.532	2.531	2.530	2.529	2.530	2.530	2.526
193	2.514	2.512	2.511	2.510	2.511	2.511	2.509
194	2.510	2.510	2.509	2.506	2.509	2.509	2.505
195	2.506	2.506	2.504	2.501	2.502	2.503	2.500
196	2.503	2.503	2.501	2.500	2.502	2.502	2.499
197	2.505	2.505	2.503	2.500	2.503	2.503	2.500
198	2.100	2.100	2.099	2.098	2.099	2.099	2.096
199	2.097	2.095	2.094	2.092	2.094	2.096	2.092
200	2.092	2.091	2.091	2.090	2.091	2.092	2.090
201	2.090	2.090	2.089	2.088	2.089	2.090	2.088
202	2.089	2.089	2.088	2.087	2.088	2.088	2.084
203	2.087	2.086	2.085	2.082	2.084	2.085	2.082
204	2.086	2.085	2.084	2.081	2.084	2.084	2.081
205	2.084	2.084	2.083	2.080	2.082	2.083	2.080
206	2.084	2.082	2.082	2.080	2.082	2.082	2.080
207	2.080	2.080	2.080	2.079	2.080	2.080	2.078
208	2.080	2.080	2.080	2.078	2.079	2.080	2.079
209	2.080	2.080	2.079	2.076	2.079	2.079	2.078
210	2.076	2.075	2.074	2.072	2.073	2.074	2.071
211	2.079	2.079	2.078	2.075	2.078	2.078	2.075
212	2.080	2.079	2.079	2.078	2.079	2.080	2.077
213	2.079	2.079	2.078	2.076	2.079	2.078	2.076
214	2.080	2.080	2.079	2.077	2.079	2.079	2.075
215	2.079	2.079	2.079	2.077	2.078	2.079	2.077
216	2.101	2.101	2.100	2.098	2.099	2.100	2.098
217	2.098	2.097	2.095	2.093	2.096	2.097	2.092
218	2.093	2.092	2.091	2.090	2.091	2.092	2.090
219	2.090	2.090	2.089	2.086	2.089	2.089	2.086
220	2.088	2.088	2.086	2.083	2.087	2.087	2.083
221	2.087	2.086	2.084	2.082	2.085	2.085	2.082
222	2.083	2.083	2.081	2.080	2.082	2.082	2.080
223	2.080	2.079	2.079	2.077	2.079	2.079	2.077
224	2.073	2.073	2.071	2.070	2.071	2.071	2.070
225	2.073	2.072	2.071	2.070	2.073	2.072	2.070
226	2.072	2.071	2.070	2.069	2.070	2.070	2.069

TABLE F7 (continued)

227	2.073	2.073	2.072	2.070	2.072	2.072	2.072	2.070
228	2.074	2.073	2.072	2.071	2.072	2.072	2.072	2.071
229	2.069	2.069	2.068	2.065	2.066	2.066	2.066	2.064
230	2.070	2.069	2.069	2.067	2.069	2.069	2.069	2.067
231	2.070	2.070	2.069	2.067	2.069	2.069	2.069	2.067
232	2.074	2.074	2.073	2.071	2.072	2.072	2.072	2.071
233	2.075	2.075	2.074	2.072	2.074	2.074	2.074	2.071
234	2.077	2.077	2.075	2.073	2.075	2.075	2.075	2.072
235	2.077	2.077	2.075	2.073	2.074	2.074	2.074	2.072
236	2.078	2.077	2.076	2.073	2.077	2.075	2.077	2.073
237	2.073	2.073	2.073	2.070	2.073	2.072	2.072	2.070
238	2.070	2.070	2.069	2.068	2.070	2.069	2.070	2.068
239	2.069	2.069	2.068	2.065	2.068	2.068	2.068	2.065
240	2.067	2.067	2.066	2.063	2.066	2.067	2.067	2.063
241	2.073	2.073	2.071	2.070	2.072	2.072	2.072	2.070
242	2.072	2.072	2.071	2.070	2.071	2.072	2.072	2.070
243	2.073	2.073	2.071	2.070	2.072	2.072	2.072	2.070
244	2.073	2.072	2.072	2.070	2.071	2.072	2.072	2.070
245	2.073	2.073	2.072	2.071	2.071	2.071	2.073	2.070
246	2.073	2.073	2.072	2.070	2.072	2.072	2.072	2.070
247	2.073	2.073	2.072	2.071	2.072	2.073	2.072	2.070
248	2.074	2.074	2.073	2.071	2.073	2.073	2.073	2.071
249	2.074	2.074	2.073	2.071	2.073	2.073	2.073	2.071
250	1.444	1.444	1.444	1.443	1.444	1.444	1.444	1.444
251	1.443	1.443	1.443	1.442	1.443	1.444	1.443	1.442
252	1.443	1.443	1.443	1.442	1.443	1.443	1.443	1.442
253	1.442	1.442	1.442	1.441	1.442	1.442	1.442	1.442
254	1.442	1.442	1.442	1.441	1.441	1.442	1.442	1.442
255	1.440	1.440	1.440	1.439	1.440	1.440	1.440	1.440
256	1.440	1.440	1.440	1.439	1.440	1.440	1.440	1.440
257	1.440	1.440	1.440	1.439	1.440	1.440	1.440	1.440
258	1.440	1.440	1.440	1.439	1.440	1.440	1.440	1.440
259	1.439	1.439	1.439	1.438	1.439	1.439	1.439	1.438
260	1.439	1.439	1.439	1.438	1.439	1.439	1.439	1.439
261	1.439	1.439	1.439	1.438	1.439	1.439	1.439	1.439
262	1.439	1.439	1.439	1.438	1.439	1.439	1.439	1.439
263	2.509	2.509	2.507	2.504	2.508	2.508	2.508	2.503
264	2.510	2.510	2.509	2.505	2.509	2.509	2.509	2.504
265	2.513	2.513	2.511	2.509	2.511	2.512	2.512	2.509
266	2.514	2.513	2.512	2.510	2.512	2.513	2.513	2.510
267	2.516	2.514	2.512	2.510	2.513	2.514	2.513	2.510
268	2.516	2.515	2.514	2.511	2.513	2.513	2.513	2.510
269	2.515	2.514	2.513	2.511	2.513	2.514	2.513	2.510
270	2.518	2.518	2.515	2.513	2.515	2.517	2.516	2.512
271	2.518	2.518	2.517	2.513	2.517	2.517	2.517	2.512
272	2.518	2.518	2.517	2.514	2.517	2.518	2.517	2.513
273	2.519	2.518	2.517	2.514	2.517	2.518	2.517	2.513
274	2.515	2.515	2.513	2.512	2.513	2.514	2.513	2.510
275	2.518	2.516	2.514	2.512	2.514	2.515	2.515	2.510
276	2.518	2.516	2.514	2.512	2.514	2.515	2.515	2.510
277	2.514	2.513	2.511	2.511	2.512	2.513	2.513	2.511
278	2.514	2.513	2.511	2.511	2.512	2.513	2.513	2.511
279	2.512	2.512	2.510	2.509	2.510	2.511	2.510	2.509
280	2.511	2.510	2.510	2.508	2.510	2.511	2.510	2.508
281	2.510	2.509	2.508	2.506	2.509	2.510	2.509	2.507
282	2.507	2.507	2.506	2.504	2.506	2.507	2.506	2.503
283	2.501	2.501	2.500	2.498	2.500	2.501	2.500	2.498
284	2.501	2.501	2.500	2.499	2.500	2.501	2.500	2.498
285	2.502	2.501	2.500	2.499	2.500	2.501	2.500	2.499
286	2.503	2.503	2.502	2.500	2.502	2.503	2.502	2.500
287	2.504	2.504	2.503	2.501	2.503	2.504	2.503	2.501
288	2.504	2.504	2.503	2.501	2.503	2.504	2.503	2.501
289	2.504	2.503	2.502	2.500	2.502	2.503	2.502	2.500
290	2.506	2.505	2.505	2.501	2.503	2.504	2.504	2.501
291	2.504	2.504	2.502	2.501	2.502	2.503	2.502	2.501
292	2.504	2.504	2.502	2.500	2.502	2.503	2.502	2.500
293	2.508	2.508	2.507	2.503	2.507	2.507	2.507	2.503
294	2.523	2.523	2.522	2.519	2.521	2.522	2.522	2.519
295	2.517	2.516	2.514	2.512	2.513	2.514	2.513	2.511
296	2.520	2.520	2.519	2.517	2.518	2.519	2.519	2.517
297	2.511	2.511	2.511	2.509	2.511	2.511	2.511	2.509
298	2.502	2.501	2.501	2.499	2.500	2.501	2.500	2.499
299	2.502	2.501	2.501	2.499	2.500	2.501	2.500	2.499
300	2.500	2.500	2.499	2.498	2.499	2.500	2.500	2.497
301	2.500	2.500	2.499	2.497	2.499	2.500	2.499	2.497
302	2.093	2.092	2.091	2.090	2.091	2.091	2.091	2.089
303	2.093	2.092	2.092	2.090	2.091	2.091	2.091	2.089

TABLE F7 (continued)

304	2.089	2.090	2.089	2.087	2.089	2.089	2.089	2.086
305	2.090	2.090	2.089	2.088	2.089	2.089	2.089	2.086
306	2.089	2.089	2.089	2.087	2.089	2.089	2.089	2.085
307	2.081	2.081	2.080	2.079	2.080	2.080	2.080	2.079
308	2.082	2.081	2.081	2.079	2.080	2.081	2.081	2.079
309	2.082	2.081	2.081	2.080	2.081	2.081	2.081	2.079
310	2.084	2.082	2.082	2.080	2.081	2.081	2.081	2.080
311	2.085	2.085	2.083	2.081	2.083	2.083	2.083	2.081
312	2.085	2.085	2.083	2.081	2.083	2.083	2.083	2.081
313	2.084	2.084	2.083	2.081	2.083	2.083	2.083	2.080
314	2.085	2.082	2.083	2.081	2.083	2.083	2.083	2.080
315	2.048	2.048	2.046	2.043	2.047	2.047	2.047	2.044
316	2.049	2.049	2.047	2.045	2.048	2.048	2.048	2.044
317	2.049	2.049	2.048	2.046	2.049	2.049	2.049	2.047
318	2.050	2.049	2.049	2.047	2.049	2.049	2.049	2.048
319	2.050	2.050	2.049	2.049	2.050	2.050	2.050	2.049
320	2.051	2.050	2.050	2.049	2.050	2.050	2.050	2.049
321	2.051	2.051	2.050	2.049	2.050	2.050	2.050	2.049
322	2.053	2.053	2.051	2.050	2.052	2.052	2.052	2.050
323	2.053	2.054	2.052	2.051	2.053	2.053	2.053	2.051
324	2.053	2.054	2.052	2.051	2.053	2.053	2.053	2.051
325	2.053	2.053	2.052	2.051	2.053	2.053	2.053	2.051
326	2.059	2.059	2.057	2.054	2.058	2.058	2.058	2.055
327	2.060	2.059	2.058	2.058	2.059	2.059	2.059	2.057
328	1.446	1.446	1.446	1.444	1.446	1.446	1.447	1.447
329	1.446	1.446	1.446	1.444	1.447	1.447	1.447	1.446
330	1.446	1.446	1.446	1.444	1.446	1.446	1.446	1.446
331	1.447	1.447	1.447	1.444	1.446	1.446	1.446	1.446
332	1.445	1.445	1.445	1.444	1.446	1.446	1.446	1.446
333	1.446	1.445	1.445	1.444	1.445	1.446	1.446	1.446
334	1.446	1.446	1.446	1.444	1.446	1.446	1.446	1.445
335	1.444	1.444	1.444	1.443	1.444	1.444	1.444	1.444
336	1.445	1.445	1.445	1.443	1.444	1.444	1.444	1.444
337	1.445	1.445	1.445	1.445	1.445	1.445	1.445	1.445
338	1.444	1.444	1.444	1.443	1.444	1.444	1.444	1.443
339	1.445	1.445	1.446	1.444	1.445	1.445	1.445	1.445
340	1.445	1.445	1.445	1.445	1.445	1.445	1.445	1.445
341	2.509	2.507	2.504	2.502	2.504	2.504	2.504	2.501
342	2.499	2.499	2.497	2.494	2.497	2.498	2.497	2.493
343	2.493	2.493	2.491	2.490	2.492	2.492	2.491	2.489
344	2.487	2.485	2.482	2.480	2.483	2.483	2.483	2.480
345	2.482	2.481	2.480	2.479	2.480	2.480	2.480	2.479
346	2.480	2.480	2.479	2.476	2.479	2.479	2.479	2.477
347	2.479	2.479	2.477	2.474	2.478	2.478	2.478	2.474
348	2.472	2.472	2.470	2.469	2.471	2.471	2.471	2.469
349	2.472	2.472	2.471	2.469	2.471	2.471	2.471	2.469
350	2.473	2.472	2.471	2.470	2.471	2.471	2.471	2.469
351	2.473	2.473	2.472	2.470	2.473	2.473	2.473	2.470
352	2.474	2.473	2.472	2.471	2.474	2.474	2.474	2.471
353	2.477	2.476	2.473	2.471	2.474	2.474	2.474	2.471
354	2.080	2.080	2.080	2.079	2.081	2.081	2.081	2.079
355	2.078	2.079	2.078	2.076	2.078	2.078	2.078	2.077
356	2.078	2.077	2.074	2.073	2.077	2.077	2.077	2.074
357	2.072	2.072	2.072	2.071	2.072	2.072	2.072	2.071
358	2.071	2.071	2.071	2.070	2.071	2.071	2.071	2.070
359	2.070	2.070	2.069	2.068	2.070	2.070	2.069	2.068
360	2.069	2.069	2.069	2.066	2.069	2.069	2.069	2.068
361	2.064	2.064	2.064	2.062	2.064	2.064	2.064	2.063
362	2.067	2.067	2.066	2.064	2.068	2.068	2.068	2.065
363	2.066	2.066	2.066	2.063	2.066	2.066	2.066	2.063
364	2.061	2.061	2.060	2.060	2.061	2.061	2.061	2.060
365	2.062	2.062	2.061	2.060	2.062	2.062	2.062	2.061
366	2.063	2.063	2.062	2.061	2.062	2.062	2.062	2.061
367	2.044	2.044	2.042	2.041	2.042	2.042	2.042	2.041
368	2.047	2.047	2.044	2.043	2.047	2.047	2.047	2.043
369	2.048	2.047	2.047	2.044	2.048	2.048	2.048	2.046
370	2.049	2.049	2.048	2.046	2.048	2.048	2.048	2.047
371	2.049	2.049	2.048	2.047	2.049	2.049	2.049	2.048
372	2.051	2.050	2.050	2.049	2.050	2.050	2.050	2.049
373	2.051	2.051	2.050	2.049	2.051	2.051	2.051	2.050
374	2.051	2.051	2.050	2.049	2.050	2.050	2.050	2.049
375	2.050	2.050	2.049	2.048	2.049	2.049	2.049	2.048
376	2.049	2.049	2.048	2.047	2.049	2.049	2.049	2.048
377	2.050	2.050	2.049	2.048	2.050	2.050	2.050	2.049
378	2.049	2.049	2.049	2.048	2.049	2.049	2.049	2.049
379	2.051	2.051	2.049	2.049	2.050	2.050	2.050	2.049
380	2.073	2.073	2.071	2.070	2.071	2.072	2.072	2.071

TABLE F7 (continued)

381	2.070	2.070	2.070	2.069	2.070	2.070	2.070	2.069
382	2.067	2.069	2.067	2.064	2.068	2.067	2.067	2.064
383	2.064	2.064	2.062	2.061	2.063	2.063	2.063	2.061
384	2.062	2.062	2.061	2.060	2.061	2.061	2.061	2.060
385	2.059	2.059	2.059	2.057	2.059	2.059	2.058	2.058
386	2.059	2.059	2.058	2.054	2.059	2.058	2.058	2.055
387	2.059	2.058	2.058	2.054	2.058	2.058	2.057	2.055
388	2.057	2.057	2.055	2.052	2.054	2.054	2.054	2.053
389	2.056	2.054	2.054	2.051	2.053	2.053	2.053	2.051
390	2.049	2.049	2.048	2.047	2.049	2.049	2.049	2.048
391	2.049	2.049	2.049	2.048	2.049	2.049	2.049	2.047
392	2.049	2.049	2.048	2.047	2.049	2.049	2.048	2.047
393	2.057	2.056	2.053	2.052	2.054	2.054	2.054	2.053
394	2.059	2.059	2.058	2.054	2.059	2.059	2.059	2.056
395	2.060	2.060	2.059	2.057	2.059	2.059	2.059	2.058
396	2.061	2.061	2.060	2.059	2.061	2.061	2.061	2.059
397	2.061	2.061	2.060	2.059	2.061	2.061	2.061	2.059
398	2.064	2.064	2.062	2.061	2.063	2.063	2.063	2.061
399	2.067	2.067	2.064	2.062	2.064	2.064	2.064	2.062
400	2.068	2.068	2.068	2.063	2.067	2.067	2.067	2.064
401	2.069	2.069	2.068	2.065	2.068	2.068	2.068	2.067
402	2.069	2.069	2.068	2.067	2.069	2.069	2.069	2.067
403	2.070	2.070	2.069	2.068	2.069	2.069	2.069	2.068
404	2.070	2.070	2.069	2.068	2.069	2.070	2.069	2.066
405	2.070	2.069	2.068	2.066	2.069	2.068	2.068	2.067
406	2.480	2.480	2.479	2.477	2.479	2.479	2.479	2.478
407	2.484	2.483	2.480	2.479	2.481	2.481	2.481	2.479
408	2.486	2.483	2.482	2.480	2.483	2.483	2.483	2.481
409	2.488	2.487	2.483	2.482	2.485	2.485	2.484	2.482
410	2.489	2.489	2.487	2.483	2.488	2.488	2.488	2.483
411	2.489	2.489	2.487	2.483	2.489	2.489	2.488	2.484
412	2.489	2.489	2.488	2.483	2.488	2.488	2.488	2.483
413	2.490	2.489	2.487	2.483	2.488	2.488	2.488	2.484
414	2.490	2.490	2.489	2.487	2.490	2.490	2.490	2.487
415	2.491	2.491	2.490	2.487	2.490	2.490	2.490	2.488
416	2.492	2.492	2.490	2.489	2.491	2.491	2.490	2.489
417	2.494	2.493	2.491	2.490	2.492	2.491	2.491	2.490
418	2.494	2.493	2.491	2.491	2.492	2.491	2.492	2.490
419	1.458	1.458	1.459	1.456	1.458	1.458	1.458	1.458
420	1.455	1.455	1.454	1.453	1.455	1.455	1.455	1.455
421	1.453	1.453	1.453	1.452	1.453	1.453	1.453	1.453
422	1.451	1.451	1.451	1.450	1.451	1.451	1.451	1.451
423	1.451	1.450	1.450	1.450	1.450	1.450	1.450	1.450
424	1.449	1.449	1.449	1.448	1.448	1.448	1.448	1.448
425	1.449	1.449	1.449	1.448	1.448	1.448	1.448	1.448
426	1.448	1.448	1.448	1.447	1.448	1.448	1.448	1.448
427	1.446	1.446	1.446	1.444	1.445	1.445	1.445	1.445
428	1.442	1.442	1.442	1.441	1.442	1.442	1.442	1.442
429	1.443	1.443	1.443	1.442	1.443	1.443	1.443	1.443
430	1.443	1.443	1.443	1.441	1.442	1.442	1.442	1.443
431	1.442	1.443	1.442	1.442	1.442	1.442	1.442	1.442
432	2.063	2.063	2.062	2.061	2.062	2.063	2.063	2.061
433	2.063	2.063	2.062	2.061	2.062	2.063	2.063	2.061
434	2.065	2.065	2.063	2.063	2.064	2.064	2.063	2.061
435	2.063	2.063	2.062	2.061	2.063	2.062	2.062	2.061
436	2.063	2.063	2.062	2.060	2.062	2.062	2.062	2.061
437	2.061	2.061	2.061	2.060	2.061	2.061	2.061	2.060
438	2.058	2.058	2.056	2.054	2.058	2.058	2.058	2.054
439	2.058	2.058	2.058	2.054	2.058	2.058	2.058	2.055
440	2.059	2.059	2.057	2.054	2.057	2.057	2.057	2.054
441	2.058	2.059	2.057	2.054	2.058	2.058	2.058	2.054
442	2.059	2.059	2.057	2.055	2.058	2.058	2.058	2.055
443	2.059	2.059	2.058	2.056	2.058	2.058	2.058	2.057
444	2.059	2.059	2.058	2.056	2.059	2.059	2.059	2.057
445	2.031	2.030	2.030	2.029	2.030	2.030	2.030	2.030
446	2.034	2.034	2.032	2.031	2.032	2.032	2.032	2.031
447	2.038	2.038	2.036	2.034	2.037	2.037	2.038	2.034
448	2.040	2.040	2.040	2.038	2.040	2.040	2.040	2.039
449	2.042	2.042	2.041	2.039	2.041	2.041	2.041	2.040
450	2.047	2.046	2.044	2.042	2.044	2.045	2.045	2.043
451	2.048	2.048	2.047	2.044	2.047	2.047	2.047	2.044
452	2.049	2.049	2.047	2.046	2.048	2.048	2.048	2.047
453	2.050	2.050	2.049	2.048	2.049	2.049	2.049	2.048
454	2.051	2.051	2.050	2.049	2.051	2.051	2.051	2.049
455	2.051	2.051	2.050	2.049	2.051	2.051	2.051	2.049
456	2.051	2.051	2.050	2.049	2.051	2.051	2.051	2.049
457	2.051	2.051	2.050	2.049	2.050	2.050	2.050	2.049

TABLE F7 (continued)

458	2.522	2.521	2.520	2.518	2.519	2.520	2.519	2.513
459	2.522	2.521	2.520	2.518	2.519	2.520	2.520	2.513
460	2.522	2.520	2.519	2.518	2.519	2.520	2.519	2.513
461	2.522	2.521	2.520	2.518	2.519	2.521	2.520	2.514
462	2.522	2.522	2.521	2.518	2.519	2.521	2.520	2.514
463	2.526	2.524	2.523	2.521	2.522	2.522	2.523	2.518
464	2.527	2.524	2.523	2.520	2.522	2.523	2.523	2.518
465	2.527	2.526	2.523	2.520	2.522	2.524	2.524	2.518
466	2.528	2.526	2.524	2.521	2.522	2.524	2.524	2.518
467	2.528	2.528	2.526	2.522	2.522	2.523	2.524	2.519
468	2.527	2.527	2.524	2.520	2.522	2.524	2.523	2.518
469	2.526	2.525	2.523	2.520	2.521	2.522	2.522	2.518
470	2.523	2.522	2.521	2.519	2.520	2.521	2.521	2.515
471	2.537	2.536	2.533	2.530	2.531	2.534	2.533	2.526
472	2.535	2.534	2.532	2.530	2.531	2.532	2.532	2.528
473	2.531	2.531	2.529	2.527	2.529	2.530	2.529	2.521
474	2.531	2.530	2.529	2.527	2.528	2.530	2.529	2.522
475	2.530	2.530	2.529	2.525	2.527	2.529	2.529	2.521
476	2.529	2.529	2.528	2.524	2.525	2.529	2.528	2.520
477	2.529	2.529	2.528	2.523	2.524	2.526	2.527	2.520
478	2.529	2.528	2.527	2.523	2.523	2.526	2.526	2.520
479	2.528	2.528	2.525	2.522	2.523	2.526	2.524	2.519
480	2.521	2.521	2.520	2.518	2.519	2.520	2.520	2.514
481	2.522	2.521	2.520	2.518	2.519	2.520	2.520	2.513
482	2.521	2.521	2.520	2.518	2.518	2.521	2.520	2.513
483	2.522	2.522	2.520	2.518	2.519	2.521	2.520	2.514
484	2.429	2.428	2.427	2.422	2.426	2.426	2.425	2.420
485	2.429	2.428	2.427	2.423	2.424	2.426	2.425	2.420
486	2.429	2.429	2.427	2.423	2.425	2.427	2.426	2.420
487	2.429	2.428	2.424	2.422	2.425	2.425	2.424	2.420
488	2.429	2.427	2.424	2.422	2.424	2.424	2.424	2.420
489	2.428	2.427	2.423	2.422	2.423	2.424	2.424	2.429
490	2.427	2.425	2.424	2.422	2.423	2.424	2.423	2.429
491	2.426	2.424	2.423	2.420	2.422	2.423	2.423	2.429
492	2.426	2.424	2.423	2.421	2.422	2.423	2.422	2.429
493	2.422	2.422	2.420	2.429	2.420	2.420	2.420	2.425
494	2.423	2.423	2.421	2.429	2.420	2.421	2.421	2.427
495	2.424	2.422	2.421	2.429	2.421	2.421	2.421	2.427
496	2.423	2.422	2.420	2.429	2.420	2.420	2.420	2.425
497	1.871	1.871	1.871	1.870	1.870	1.870	1.870	1.869
498	1.871	1.871	1.871	1.870	1.870	1.870	1.870	1.869
499	1.871	1.871	1.871	1.870	1.870	1.870	1.870	1.869
500	1.871	1.871	1.870	1.869	1.870	1.870	1.870	1.869
501	1.871	1.871	1.870	1.869	1.870	1.870	1.870	1.869
502	1.871	1.871	1.870	1.869	1.870	1.870	1.870	1.869
503	1.869	1.869	1.868	1.867	1.868	1.868	1.868	1.866
504	1.869	1.869	1.869	1.867	1.868	1.868	1.869	1.867
505	1.869	1.869	1.869	1.867	1.869	1.869	1.869	1.867
506	1.870	1.870	1.869	1.867	1.869	1.869	1.869	1.867
507	1.870	1.870	1.869	1.868	1.869	1.869	1.869	1.867
508	1.869	1.869	1.869	1.868	1.869	1.869	1.869	1.866
509	1.870	1.870	1.869	1.867	1.869	1.869	1.869	1.868
510	2.434	2.434	2.432	2.430	2.431	2.432	2.432	2.426
511	2.436	2.434	2.433	2.430	2.432	2.434	2.433	2.429
512	2.437	2.437	2.433	2.430	2.433	2.434	2.434	2.429
513	2.437	2.437	2.434	2.431	2.433	2.434	2.434	2.430
514	2.437	2.436	2.434	2.432	2.433	2.434	2.434	2.430
515	2.438	2.436	2.434	2.432	2.434	2.434	2.434	2.430
516	2.438	2.437	2.434	2.432	2.433	2.436	2.434	2.430
517	2.438	2.437	2.434	2.432	2.433	2.434	2.434	2.430
518	2.438	2.437	2.434	2.432	2.433	2.434	2.434	2.430
519	2.439	2.439	2.437	2.434	2.436	2.437	2.436	2.400
520	2.439	2.438	2.437	2.433	2.438	2.438	2.437	2.410
521	2.439	2.439	2.438	2.434	2.436	2.438	2.437	2.410
522	2.439	2.439	2.438	2.434	2.436	2.439	2.437	2.410
523	2.603	2.602	2.602	2.599	2.600	2.601	2.601	2.594
524	2.604	2.602	2.602	2.599	1.601	2.602	2.601	2.596
525	2.603	2.602	2.601	2.599	2.600	2.601	2.601	2.594
526	2.602	2.601	2.600	2.597	2.598	2.600	2.599	2.593
527	2.601	2.601	2.600	2.598	2.599	2.600	2.599	2.592
528	2.601	2.601	2.600	2.598	2.599	2.600	2.599	2.592
529	2.601	2.600	2.600	2.597	2.599	2.600	2.599	2.592
530	2.601	2.600	2.600	2.596	2.599	2.601	2.600	2.593
531	2.602	2.601	2.600	2.598	2.599	2.600	2.600	2.593
532	2.602	2.601	2.600	2.598	2.599	2.601	2.600	2.594
533	2.602	2.601	2.600	2.598	2.599	2.600	2.600	2.594
534	2.602	2.601	2.600	2.598	2.599	2.601	2.599	2.594

TABLE F7 (continued)

535	2.602	2.601	2.600	2.598	2.599	2.600	2.599	2.593
536	2.154	2.154	2.153	2.152	2.153	2.155	2.154	2.156
537	2.156	2.154	2.154	2.152	2.153	2.155	2.154	2.152
538	2.154	2.154	2.153	2.151	2.153	2.156	2.153	2.151
539	2.154	2.154	2.153	2.151	2.153	2.154	2.153	2.152
540	2.154	2.153	2.153	2.151	2.152	2.154	2.153	2.152
541	2.157	2.154	2.154	2.151	2.154	2.154	2.154	2.152
542	2.157	2.155	2.155	2.153	2.154	2.157	2.155	2.153
543	2.157	2.156	2.156	2.154	2.155	2.157	2.157	2.154
544	4.898	4.921	4.881	4.918	4.929	4.890	4.909	4.916
545	4.905	4.930	4.889	4.923	4.935	4.894	4.915	4.923
546	4.910	4.935	4.892	4.929	4.940	4.901	4.920	4.928
547	4.911	4.939	4.894	4.930	4.942	4.903	4.921	4.930
548	4.910	4.937	4.894	4.930	4.941	4.901	4.920	4.921
549	1.910	1.910	1.910	1.909	1.909	1.910	1.910	1.908
550	1.911	1.911	1.911	1.909	1.910	1.910	1.910	1.909
551	1.912	1.912	1.911	1.910	1.911	1.912	1.912	1.910
552	1.917	1.915	1.913	1.912	1.914	1.914	1.914	1.912
553	1.917	1.917	1.914	1.913	1.914	1.915	1.915	1.913
554	1.918	1.918	1.916	1.914	1.916	1.916	1.916	1.913
555	1.919	1.918	1.917	1.914	1.917	1.917	1.917	1.914
556	2.271	2.272	2.270	2.269	2.270	2.270	2.270	2.267
557	2.272	2.272	2.270	2.270	2.271	2.271	2.271	2.268
558	2.273	2.274	2.271	2.270	2.271	2.271	2.271	2.269
559	2.274	2.274	2.272	2.271	2.272	2.273	2.271	2.270
560	2.275	2.275	2.272	2.271	2.273	2.273	2.273	2.270
561	2.275	2.275	2.272	2.271	2.273	2.273	2.273	2.270
562	2.275	2.275	2.273	2.272	2.273	2.273	2.273	2.270
563	2.271	2.270	2.270	2.268	2.269	2.270	2.270	2.265
564	2.271	2.271	2.271	2.269	2.269	2.271	2.270	2.267
565	2.272	2.272	2.271	2.269	2.270	2.271	2.271	2.268
566	2.273	2.273	2.273	2.270	2.270	2.273	2.273	2.268
567	2.274	2.274	2.273	2.270	2.271	2.273	2.273	2.269
568	2.696	2.696	2.691	2.691	2.693	2.692	2.692	2.689
569	2.700	2.700	2.696	2.697	2.698	2.698	2.698	2.693
570	2.702	2.703	2.699	2.699	2.701	2.700	2.700	2.697
571	2.705	2.705	2.700	2.701	2.703	2.702	2.702	2.699
572	2.709	2.709	2.703	2.703	2.706	2.705	2.705	2.701
573	2.711	2.712	2.708	2.709	2.710	2.709	2.709	2.704
574	2.713	2.713	2.709	2.709	2.711	2.710	2.710	2.716
575	2.713	2.714	2.710	2.710	2.711	2.711	2.711	2.708
576	3.158	3.158	3.151	3.152	3.153	3.153	3.153	3.148
577	3.159	3.159	3.152	3.153	3.156	3.154	3.154	3.149
578	3.159	3.160	3.153	3.154	3.153	3.156	3.156	3.150
579	3.160	3.160	3.154	3.154	3.158	3.156	3.155	3.151
580	3.160	3.161	3.155	3.157	3.159	3.158	3.158	3.152
581	3.162	3.162	3.157	3.158	3.160	3.158	3.158	3.153
582	3.163	3.163	3.158	3.158	3.160	3.159	3.159	3.154
583	3.163	3.163	3.159	3.159	3.161	3.160	3.160	3.154
584	2.944	2.944	2.938	2.938	2.940	2.939	2.940	2.934
585	2.947	2.945	2.939	2.939	2.941	2.940	2.940	2.937
586	2.943	2.942	2.935	2.934	2.938	2.937	2.937	2.932
587	2.942	2.941	2.934	2.934	2.937	2.935	2.935	2.931
588	2.940	2.939	2.932	2.932	2.933	2.933	2.933	2.930
589	4.369	4.367	4.353	4.354	4.355	4.355	4.357	4.348
590	4.369	4.367	4.353	4.354	4.359	4.358	4.357	4.349
591	4.368	4.365	4.353	4.354	4.358	4.354	4.357	4.348
592	4.367	4.364	4.352	4.353	4.358	4.353	4.354	4.347
593	4.367	4.364	4.350	4.353	4.356	4.353	4.353	4.346
594	4.369	4.367	4.353	4.355	4.359	4.356	4.358	4.348
595	6.582	6.582	6.567	6.567	6.567	6.559	6.561	6.545
596	6.582	6.581	6.556	6.562	6.564	6.558	6.561	6.541
597	6.580	6.580	6.557	6.561	6.563	6.555	6.559	6.541
598	6.581	6.580	6.557	6.561	6.564	6.558	6.560	6.540
599	3.725	3.727	3.716	3.719	3.721	3.718	3.720	3.711
600	3.727	3.728	3.718	3.720	3.722	3.719	3.720	3.713
601	3.728	3.729	3.719	3.721	3.723	3.720	3.721	3.713
602	3.729	3.729	3.719	3.721	3.723	3.721	3.721	3.714
603	3.731	3.732	3.721	3.724	3.728	3.723	3.726	3.719
604	3.733	3.734	3.723	3.728	3.729	3.727	3.728	3.720
605	3.172	3.174	3.167	3.169	3.171	3.169	3.170	3.164
606	3.173	3.177	3.168	3.170	3.173	3.169	3.171	3.166
607	3.174	3.178	3.169	3.171	3.174	3.170	3.172	3.167
608	3.174	3.177	3.169	3.172	3.174	3.170	3.172	3.168
609	3.175	3.177	3.169	3.172	3.176	3.171	3.173	3.168
610	3.176	3.178	3.170	3.172	3.176	3.171	3.173	3.168
611	4.030	4.033	4.020	4.025	4.029	4.023	4.026	4.018

TABLE F7 (continued)

612	4.032	4.036	4.022	4.028	4.031	4.026	4.029	4.020
613	4.033	4.038	4.024	4.029	4.032	4.028	4.030	4.021
614	4.034	4.038	4.025	4.030	4.033	4.029	4.030	4.022
615	4.036	4.039	4.027	4.030	4.034	4.029	4.031	4.022
616	4.039	4.041	4.029	4.032	4.038	4.031	4.033	4.026
617	4.799	4.802	4.785	4.792	4.798	4.789	4.791	4.781
618	4.800	4.802	4.788	4.793	4.799	4.790	4.793	4.783
619	4.801	4.805	4.789	4.796	4.800	4.792	4.796	4.785
620	4.803	4.808	4.790	4.793	4.801	4.794	4.798	4.788
621	4.806	4.810	4.793	4.800	4.803	4.798	4.800	4.790
622	4.809	4.812	4.796	4.802	4.807	4.799	4.801	4.792
623	7.270	7.277	7.248	7.263	7.268	7.259	7.258	7.238
624	7.283	7.291	7.261	7.280	7.280	7.260	7.270	7.250
625	7.288	7.295	7.264	7.284	7.284	7.269	7.274	7.253
626	7.291	7.299	7.269	7.289	7.289	7.273	7.279	7.258
627	7.294	7.302	7.272	7.292	7.292	7.276	7.281	7.261
628	7.300	7.309	7.279	7.298	7.298	7.282	7.288	7.267
629	3.581	3.583	3.573	3.580	3.581	3.577	3.579	3.571
630	3.582	3.584	3.574	3.581	3.582	3.576	3.580	3.573
631	3.583	3.586	3.577	3.583	3.583	3.579	3.581	3.574
632	3.584	3.586	3.577	3.583	3.583	3.579	3.581	3.574
633	3.585	3.587	3.578	3.583	3.586	3.580	3.582	3.576
634	3.584	3.586	3.578	3.584	3.586	3.580	3.582	3.577
635	3.510	3.510	3.507	3.510	3.510	3.506	3.510	3.502
636	3.512	3.513	3.508	3.512	3.512	3.510	3.512	3.503
637	3.513	3.514	3.509	3.512	3.513	3.510	3.512	3.504
638	3.513	3.517	3.510	3.513	3.514	3.511	3.512	3.506
639	3.514	3.517	3.510	3.513	3.514	3.511	3.513	3.507
640	3.516	3.518	3.510	3.514	3.517	3.513	3.515	3.506
641	3.947	3.949	3.940	3.945	3.946	3.943	3.944	3.934
642	3.948	3.950	3.941	3.948	3.949	3.944	3.947	3.938
643	3.948	3.950	3.942	3.948	3.948	3.944	3.948	3.938
644	3.949	3.951	3.943	3.949	3.950	3.945	3.948	3.938
645	3.949	3.950	3.942	3.949	3.949	3.945	3.948	3.939
646	3.950	3.952	3.943	3.949	3.950	3.947	3.948	3.939
647	4.639	4.640	4.630	4.637	4.638	4.633	4.637	4.622
648	4.639	4.641	4.631	4.638	4.639	4.633	4.638	4.623
649	4.639	4.640	4.631	4.638	4.639	4.633	4.637	4.623
650	4.639	4.641	4.631	4.638	4.639	4.633	4.637	4.623
651	4.640	4.642	4.632	4.639	4.640	4.634	4.638	4.623
652	4.640	4.643	4.632	4.640	4.640	4.635	4.639	4.624
653	5.459	5.463	5.451	5.459	5.459	5.453	5.458	5.440
654	5.462	5.466	5.452	5.461	5.460	5.454	5.459	5.441
655	5.462	5.467	5.452	5.461	5.461	5.455	5.459	5.442
656	5.462	5.467	5.454	5.460	5.461	5.455	5.459	5.442
657	5.463	5.468	5.453	5.462	5.461	5.456	5.460	5.443
658	5.463	5.467	5.453	5.462	5.462	5.457	5.460	5.443
659	8.354	8.360	8.339	8.352	8.351	8.342	8.344	8.311
660	8.356	8.363	8.340	8.353	8.352	8.343	8.349	8.312
661	8.359	8.363	8.341	8.356	8.354	8.344	8.349	8.314
662	8.359	8.364	8.343	8.357	8.354	8.345	8.350	8.314
663	8.360	8.367	8.343	8.358	8.356	8.346	8.352	8.317
664	8.365	8.373	8.350	8.363	8.362	8.352	8.359	8.323
665	1.998	2.000	1.997	1.998	1.999	1.997	1.998	1.997
666	1.999	2.000	1.997	1.998	1.999	1.997	1.999	1.996
667	1.999	2.000	1.997	1.998	1.999	1.997	1.999	1.997
668	2.002	2.003	2.000	2.001	2.003	2.000	2.002	2.000
669	2.002	2.004	2.000	2.001	2.003	2.001	2.003	2.001
670	2.360	2.362	2.356	2.359	2.362	2.357	2.359	2.357
671	2.361	2.363	2.357	2.360	2.363	2.356	2.360	2.358
672	2.363	2.367	2.359	2.362	2.364	2.359	2.362	2.360
673	2.363	2.367	2.360	2.363	2.366	2.360	2.362	2.360
674	2.366	2.368	2.361	2.363	2.368	2.361	2.363	2.361
675	3.330	3.337	3.321	3.330	3.334	3.321	3.328	3.323
676	3.331	3.339	3.323	3.331	3.337	3.323	3.329	3.326
677	3.333	3.340	3.325	3.333	3.339	3.323	3.331	3.327
678	3.337	3.342	3.327	3.337	3.340	3.327	3.333	3.329
679	1.897	1.897	1.895	1.895	1.895	1.895	1.896	1.893
680	1.898	1.897	1.896	1.896	1.896	1.896	1.897	1.894
681	1.898	1.898	1.897	1.897	1.897	1.897	1.898	1.896
682	1.899	1.899	1.897	1.898	1.897	1.896	1.898	1.896
683	1.899	1.899	1.898	1.898	1.898	1.898	1.899	1.897
684	1.898	1.899	1.898	1.899	1.899	1.899	1.899	1.897
685	2.256	2.257	2.251	2.253	2.255	2.255	2.256	2.253
686	2.257	2.258	2.252	2.256	2.257	2.257	2.258	2.253
687	2.259	2.259	2.253	2.257	2.258	2.256	2.258	2.254
688	2.259	2.259	2.253	2.258	2.258	2.256	2.259	2.255

TABLE F7 (continued)

689	2.260	2.260	2.254	2.259	2.259	2.259	2.259	2.257
690	2.260	2.261	2.259	2.259	2.260	2.260	2.260	2.258
691	2.719	2.720	2.714	2.716	2.717	2.717	2.718	2.712
692	2.720	2.721	2.717	2.718	2.719	2.719	2.720	2.714
693	2.722	2.723	2.720	2.720	2.721	2.721	2.721	2.718
694	2.722	2.723	2.719	2.720	2.720	2.720	2.721	2.718
695	2.722	2.723	2.719	2.719	2.720	2.720	2.720	2.717
696	2.722	2.722	2.719	2.719	2.720	2.720	2.721	2.716
697	3.226	3.227	3.220	3.222	3.223	3.223	3.224	3.218
698	3.229	3.229	3.223	3.225	3.224	3.224	3.227	3.220
699	3.230	3.231	3.224	3.228	3.228	3.228	3.229	3.222
700	3.231	3.233	3.227	3.229	3.229	3.229	3.230	3.223
701	3.233	3.234	3.228	3.230	3.230	3.230	3.231	3.224
702	3.232	3.234	3.228	3.230	3.230	3.230	3.231	3.224
703	1.879	1.878	1.878	1.874	1.877	1.877	1.878	1.873
704	1.880	1.880	1.879	1.879	1.879	1.879	1.880	1.878
705	1.881	1.881	1.879	1.879	1.880	1.880	1.880	1.878
706	1.881	1.881	1.879	1.879	1.880	1.880	1.880	1.879
707	1.882	1.882	1.880	1.880	1.881	1.881	1.881	1.880
708	1.882	1.882	1.881	1.881	1.882	1.882	1.882	1.880
709	2.228	2.227	2.223	2.223	2.226	2.226	2.226	2.221
710	2.228	2.228	2.224	2.224	2.227	2.227	2.228	2.223
711	2.229	2.229	2.227	2.227	2.228	2.228	2.228	2.223
712	2.229	2.229	2.227	2.227	2.228	2.228	2.228	2.223
713	2.229	2.229	2.227	2.227	2.228	2.228	2.228	2.224
714	2.230	2.230	2.228	2.228	2.229	2.229	2.229	2.225
715	2.749	2.749	2.744	2.744	2.746	2.746	2.748	2.740
716	2.749	2.749	2.746	2.746	2.748	2.748	2.748	2.741
717	2.750	2.750	2.747	2.747	2.749	2.749	2.749	2.742
718	2.750	2.750	2.747	2.747	2.749	2.749	2.749	2.743
719	2.751	2.750	2.748	2.748	2.749	2.749	2.749	2.744
720	2.752	2.752	2.749	2.749	2.750	2.750	2.751	2.744
721	1.882	1.882	1.881	1.881	1.883	1.883	1.883	1.880
722	1.883	1.883	1.882	1.882	1.883	1.883	1.883	1.881
723	1.885	1.884	1.883	1.883	1.883	1.883	1.884	1.882
724	1.886	1.887	1.884	1.884	1.886	1.886	1.886	1.883
725	1.887	1.888	1.886	1.886	1.887	1.887	1.888	1.884
726	1.889	1.889	1.888	1.888	1.889	1.889	1.889	1.886
727	2.223	2.223	2.221	2.221	2.223	2.223	2.223	2.220
728	2.226	2.226	2.223	2.223	2.224	2.224	2.224	2.221
729	2.228	2.227	2.224	2.224	2.227	2.227	2.226	2.223
730	2.227	2.228	2.226	2.226	2.227	2.227	2.227	2.223
731	2.229	2.229	2.227	2.227	2.228	2.228	2.229	2.223
732	2.229	2.229	2.228	2.228	2.229	2.229	2.229	2.224
733	2.731	2.730	2.728	2.728	2.729	2.729	2.729	2.724
734	2.732	2.731	2.729	2.729	2.730	2.730	2.730	2.726
735	2.732	2.732	2.730	2.730	2.731	2.731	2.732	2.726
736	2.734	2.733	2.731	2.731	2.732	2.732	2.732	2.728
737	2.736	2.736	2.732	2.732	2.733	2.733	2.734	2.729
738	2.737	2.737	2.733	2.733	2.734	2.734	2.736	2.730

[illegible]

TABLE F8 (continued)

676	3.32988	0.00594	80.775	677	3.33138	0.00619	80.809	678	3.33460	0.00588	80.868
679	1.84538	0.00130	47.344	680	1.86925	0.00116	47.365	681	1.88972	0.00071	47.389
682	1.84775	0.00104	47.401	683	1.86955	0.00071	47.413	684	1.88965	0.00070	47.419
685	2.25550	0.00200	53.926	686	2.25500	0.00227	53.942	687	2.25700	0.00227	53.960
688	2.25738	0.00220	53.945	689	2.25557	0.00200	53.965	690	2.25963	0.00092	53.968
691	2.27166	0.00262	66.735	692	2.27111	0.00220	66.749	693	2.27207	0.00149	66.831
694	2.27203	0.00160	66.842	695	2.27200	0.00163	66.843	696	2.27196	0.00190	66.831
697	3.32258	0.00295	78.357	698	3.32231	0.00369	78.366	699	3.32273	0.00302	78.361
700	3.32288	0.00295	78.492	701	3.32230	0.00307	78.495	702	3.32298	0.00293	78.515
703	1.85767	0.00212	46.845	704	1.86749	0.00071	46.853	705	1.88797	0.00104	46.867
706	1.85788	0.00033	46.970	707	1.85658	0.00033	46.944	708	1.85519	0.00070	47.009
709	2.25500	0.00239	53.227	710	2.25222	0.00210	53.227	711	2.25273	0.00192	53.263
712	2.25738	0.00192	53.283	713	2.25222	0.00200	53.260	714	2.25285	0.00160	53.279
715	2.25755	0.00306	67.430	716	2.25222	0.00204	67.436	717	2.25285	0.00264	67.479
718	2.25700	0.00333	67.482	719	2.25222	0.00207	67.494	720	2.25285	0.00256	67.520
721	1.85113	0.00064	47.000	722	1.86883	0.00076	47.033	723	1.88836	0.00094	47.054
724	1.85125	0.00139	47.100	725	1.86883	0.00130	47.113	726	1.88837	0.00100	47.175
727	2.25213	0.00135	53.239	728	2.25222	0.00164	53.260	729	2.25257	0.00166	53.285
730	2.25637	0.00151	53.290	731	2.25222	0.00200	53.260	732	2.25281	0.00170	53.301
733	2.25650	0.00207	67.030	734	2.25229	0.00177	67.056	735	2.25305	0.00200	67.077
736	2.25163	0.00177	67.103	737	2.25313	0.00230	67.133	738	2.25342	0.00238	67.164

TABLE F9

Raw Experimental Data

Thermocouple Wires Numbers 28 to 32

	MILLIVOLTS READ IN FOR POSITIONS 28 TO 32 ARE				
1	1.974	1.977	1.976	1.976	1.976
2	1.978	1.979	1.979	1.978	1.979
3	1.979	1.981	1.981	1.981	1.981
4	1.981	1.983	1.983	1.983	1.983
5	1.982	1.983	1.984	1.984	1.984
6	1.984	1.984	1.984	1.984	1.984
7	1.983	1.985	1.984	1.984	1.984
8	1.990	1.992	1.992	1.991	1.992
9	1.985	1.987	1.986	1.986	1.986
10	1.985	1.987	1.986	1.985	1.985
11	1.985	1.988	1.986	1.986	1.986
12	1.986	1.988	1.988	1.988	1.988
13	1.987	1.988	1.987	1.987	1.987
14	1.987	1.989	1.988	1.988	1.988
15	1.981	1.983	1.983	1.983	1.983
16	1.981	1.984	1.983	1.983	1.983
17	1.983	1.984	1.984	1.984	1.984
18	1.983	1.985	1.984	1.984	1.984
19	1.984	1.985	1.984	1.984	1.984
20	1.983	1.984	1.984	1.984	1.984
21	1.983	1.984	1.984	1.984	1.984
22	1.983	1.984	1.984	1.984	1.984
23	1.985	1.987	1.987	1.987	1.987
24	1.986	1.987	1.986	1.986	1.986
25	1.986	1.988	1.986	1.986	1.986
26	1.984	1.987	1.986	1.986	1.986
27	1.984	1.987	1.985	1.985	1.985
28	1.984	1.985	1.986	1.986	1.986
29	1.462	1.462	1.462	1.462	1.462
30	1.458	1.458	1.458	1.458	1.458
31	1.456	1.456	1.455	1.455	1.455
32	1.448	1.448	1.448	1.448	1.448
33	1.446	1.446	1.446	1.446	1.446
34	1.434	1.434	1.434	1.434	1.434
35	1.436	1.436	1.436	1.436	1.436
36	1.438	1.438	1.438	1.438	1.438
37	1.437	1.437	1.437	1.437	1.437
38	1.438	1.439	1.439	1.439	1.439
39	1.439	1.440	1.440	1.440	1.440
40	1.440	1.440	1.440	1.440	1.440
41	1.441	1.441	1.441	1.441	1.441
42	1.440	1.441	1.441	1.441	1.441
43	2.368	2.372	2.370	2.370	2.370
44	2.367	2.369	2.369	2.369	2.369
45	2.368	2.371	2.369	2.369	2.369
46	2.368	2.371	2.370	2.370	2.370
47	2.368	2.371	2.370	2.371	2.370
48	2.368	2.371	2.369	2.369	2.369
49	2.368	2.370	2.369	2.369	2.369
50	2.373	2.376	2.374	2.375	2.374
51	2.373	2.376	2.374	2.374	2.374
52	2.373	2.376	2.374	2.374	2.374
53	2.371	2.374	2.373	2.373	2.373
54	2.369	2.372	2.370	2.371	2.371
55	2.369	2.371	2.370	2.371	2.371
56	2.030	2.033	2.032	2.032	2.032
57	2.027	2.029	2.028	2.028	2.029
58	2.023	2.024	2.024	2.024	2.024
59	2.020	2.023	2.021	2.021	2.021
60	2.019	2.020	2.020	2.019	2.019
61	2.039	2.041	2.040	2.040	2.040
62	2.035	2.037	2.036	2.037	2.037
63	2.031	2.034	2.034	2.034	2.034
64	2.030	2.033	2.032	2.032	2.032
65	2.030	2.031	2.031	2.031	2.031
66	2.026	2.028	2.028	2.028	2.028
67	2.025	2.028	2.027	2.027	2.027
68	2.025	2.027	2.027	2.026	2.026
69	2.020	2.022	2.021	2.021	2.021
70	2.019	2.020	2.020	2.020	2.020
71	2.017	2.020	2.020	2.020	2.020
72	2.017	2.019	2.018	2.018	2.018

TABLE F9 (continued)

73	2.017	2.019	2.018	2.018	2.018
74	2.013	2.016	2.014	2.014	2.015
75	2.009	2.011	2.011	2.011	2.011
76	2.010	2.011	2.011	2.011	2.011
77	2.009	2.010	2.010	2.010	2.010
78	2.003	2.007	2.006	2.006	2.006
79	2.006	2.009	2.008	2.008	2.008
80	2.007	2.009	2.009	2.009	2.009
81	1.967	1.969	1.968	1.968	1.968
82	1.955	1.959	1.958	1.958	1.958
83	1.962	1.964	1.964	1.964	1.964
84	1.960	1.961	1.961	1.960	1.961
85	1.954	1.958	1.957	1.957	1.957
86	1.953	1.953	1.955	1.955	1.955
87	1.954	1.957	1.956	1.955	1.956
88	1.974	1.973	1.975	1.975	1.976
89	1.967	1.969	1.969	1.969	1.969
90	1.961	1.963	1.962	1.962	1.962
91	1.960	1.961	1.960	1.960	1.960
92	1.959	1.960	1.960	1.960	1.960
93	1.963	1.965	1.963	1.964	1.965
94	1.431	1.431	1.431	1.431	1.431
95	1.437	1.437	1.437	1.437	1.437
96	1.436	1.436	1.436	1.436	1.436
97	1.441	1.441	1.441	1.441	1.441
98	1.441	1.441	1.441	1.441	1.441
99	1.440	1.440	1.440	1.440	1.440
100	1.439	1.439	1.439	1.439	1.439
101	1.431	1.431	1.431	1.431	1.431
102	1.439	1.439	1.439	1.439	1.439
103	1.439	1.439	1.439	1.439	1.439
104	1.439	1.439	1.439	1.439	1.439
105	1.439	1.439	1.439	1.439	1.439
106	1.437	1.438	1.438	1.437	1.437
107	2.349	2.352	2.351	2.351	2.351
108	2.344	2.349	2.347	2.347	2.348
109	2.338	2.340	2.339	2.339	2.339
110	2.351	2.354	2.354	2.353	2.353
111	2.343	2.348	2.346	2.347	2.347
112	2.339	2.341	2.340	2.340	2.341
113	2.333	2.339	2.337	2.337	2.337
114	2.329	2.331	2.330	2.330	2.330
115	2.326	2.329	2.329	2.329	2.329
116	2.321	2.327	2.324	2.324	2.325
117	2.320	2.322	2.321	2.321	2.321
118	2.311	2.316	2.314	2.314	2.314
119	2.310	2.313	2.312	2.312	2.312
120	1.978	1.979	1.979	1.979	1.979
121	1.974	1.977	1.976	1.976	1.976
122	1.969	1.970	1.970	1.970	1.970
123	1.965	1.968	1.967	1.967	1.966
124	1.959	1.960	1.960	1.960	1.960
125	1.958	1.959	1.959	1.959	1.959
126	1.954	1.957	1.956	1.956	1.956
127	1.956	1.959	1.958	1.958	1.958
128	1.974	1.977	1.975	1.976	1.976
129	1.971	1.972	1.971	1.971	1.971
130	1.969	1.970	1.970	1.970	1.970
131	1.964	1.968	1.965	1.966	1.968
132	1.959	1.961	1.960	1.960	1.960
133	1.981	1.984	1.983	1.983	1.983
134	1.980	1.981	1.980	1.980	1.981
135	1.978	1.979	1.979	1.979	1.979
136	1.982	1.984	1.983	1.983	1.984
137	1.979	1.980	1.980	1.979	1.979
138	1.961	1.963	1.962	1.962	1.962
139	1.985	1.988	1.987	1.986	1.988
140	1.980	1.981	1.981	1.981	1.981
141	1.975	1.977	1.976	1.975	1.976
142	1.970	1.972	1.971	1.971	1.971
143	1.965	1.968	1.967	1.967	1.967
144	1.961	1.963	1.962	1.962	1.962
145	1.960	1.962	1.961	1.961	1.961
146	1.961	1.962	1.962	1.962	1.962
147	1.960	1.961	1.960	1.960	1.960
148	1.956	1.958	1.957	1.957	1.957
149	1.956	1.958	1.957	1.957	1.957

TABLE F9 (continued)

150	1.954	1.956	1.956	1.956	1.956
151	1.952	1.954	1.953	1.953	1.953
152	1.951	1.953	1.951	1.951	1.951
153	1.950	1.952	1.951	1.951	1.951
154	1.949	1.950	1.949	1.949	1.950
155	1.949	1.950	1.950	1.950	1.950
156	1.949	1.950	1.949	1.949	1.949
157	1.962	1.963	1.962	1.962	1.962
158	1.960	1.960	1.960	1.960	1.960
159	1.931	1.933	1.933	1.933	1.933
160	1.929	1.930	1.929	1.929	1.929
161	1.924	1.922	1.923	1.927	1.927
162	1.920	1.922	1.921	1.921	1.921
163	1.919	1.921	1.920	1.920	1.921
164	1.917	1.919	1.918	1.918	1.919
165	1.914	1.918	1.917	1.916	1.916
166	1.909	1.910	1.908	1.909	1.909
167	1.907	1.909	1.909	1.909	1.909
168	1.902	1.904	1.903	1.903	1.903
169	1.902	1.905	1.903	1.903	1.904
170	1.906	1.909	1.908	1.908	1.908
171	1.906	1.909	1.908	1.909	1.909
172	1.414	1.414	1.414	1.414	1.414
173	1.411	1.411	1.411	1.411	1.411
174	1.409	1.409	1.409	1.409	1.409
175	1.408	1.408	1.408	1.408	1.408
176	1.405	1.405	1.405	1.405	1.405
177	1.404	1.405	1.405	1.404	1.404
178	1.403	1.403	1.403	1.403	1.403
179	1.404	1.404	1.404	1.404	1.404
180	1.404	1.405	1.405	1.405	1.404
181	1.407	1.407	1.407	1.407	1.407
182	1.405	1.405	1.405	1.405	1.405
183	1.406	1.406	1.406	1.406	1.406
184	1.405	1.405	1.405	1.405	1.405
185	2.230	2.234	2.232	2.231	2.232
186	2.238	2.240	2.239	2.238	2.239
187	2.235	2.239	2.238	2.238	2.238
188	2.253	2.259	2.258	2.258	2.257
189	2.240	2.244	2.242	2.241	2.242
190	2.277	2.280	2.279	2.279	2.279
191	2.267	2.270	2.269	2.269	2.269
192	2.259	2.262	2.260	2.259	2.260
193	2.241	2.248	2.245	2.244	2.245
194	2.240	2.244	2.242	2.241	2.242
195	2.234	2.239	2.238	2.237	2.238
196	2.234	2.239	2.238	2.238	2.238
197	2.237	2.240	2.239	2.239	2.239
198	1.930	1.932	1.932	1.931	1.932
199	1.928	1.929	1.929	1.929	1.929
200	1.925	1.929	1.928	1.928	1.928
201	1.923	1.926	1.925	1.924	1.924
202	1.921	1.923	1.922	1.922	1.922
203	1.919	1.921	1.920	1.920	1.920
204	1.919	1.920	1.920	1.920	1.920
205	1.918	1.920	1.920	1.919	1.919
206	1.918	1.920	1.919	1.919	1.919
207	1.914	1.918	1.917	1.917	1.917
208	1.913	1.918	1.917	1.917	1.917
209	1.913	1.917	1.916	1.915	1.915
210	1.909	1.910	1.910	1.910	1.910
211	1.907	1.909	1.908	1.908	1.909
212	1.908	1.910	1.909	1.909	1.909
213	1.907	1.910	1.909	1.908	1.909
214	1.908	1.910	1.909	1.909	1.909
215	1.907	1.910	1.909	1.908	1.909
216	1.927	1.929	1.929	1.926	1.929
217	1.922	1.927	1.924	1.924	1.924
218	1.921	1.922	1.922	1.921	1.921
219	1.918	1.920	1.920	1.919	1.919
220	1.913	1.918	1.918	1.917	1.917
221	1.913	1.918	1.915	1.915	1.915
222	1.911	1.914	1.913	1.911	1.912
223	1.908	1.910	1.909	1.909	1.909
224	1.903	1.907	1.905	1.904	1.906
225	1.903	1.907	1.906	1.905	1.905
226	1.902	1.904	1.903	1.902	1.903

TABLE F9 (continued)

227	1.903	1.906	1.906	1.905	1.907
228	1.904	1.908	1.907	1.905	1.907
229	1.899	1.900	1.900	1.899	1.900
230	1.900	1.902	1.901	1.900	1.901
231	1.900	1.902	1.901	1.900	1.901
232	1.905	1.909	1.908	1.907	1.907
233	1.907	1.909	1.908	1.908	1.909
234	1.907	1.910	1.909	1.909	1.909
235	1.907	1.909	1.909	1.909	1.909
236	1.908	1.910	1.909	1.909	1.909
237	1.899	1.901	1.900	1.900	1.900
238	1.896	1.899	1.898	1.898	1.898
239	1.892	1.897	1.895	1.895	1.895
240	1.892	1.894	1.894	1.893	1.894
241	1.899	1.900	1.900	1.899	1.900
242	1.899	1.901	1.901	1.900	1.900
243	1.899	1.901	1.901	1.900	1.900
244	1.899	1.902	1.900	1.900	1.900
245	1.899	1.902	1.901	1.900	1.902
246	1.899	1.902	1.901	1.900	1.900
247	1.900	1.902	1.901	1.901	1.901
248	1.900	1.902	1.902	1.901	1.902
249	1.900	1.902	1.902	1.901	1.902
250	1.405	1.406	1.405	1.405	1.405
251	1.405	1.406	1.406	1.406	1.406
252	1.404	1.404	1.404	1.404	1.404
253	1.403	1.404	1.404	1.404	1.404
254	1.403	1.404	1.403	1.403	1.403
255	1.402	1.402	1.402	1.402	1.402
256	1.402	1.402	1.402	1.402	1.402
257	1.402	1.402	1.402	1.402	1.402
258	1.401	1.401	1.401	1.401	1.401
259	1.400	1.400	1.400	1.400	1.400
260	1.400	1.400	1.400	1.400	1.400
261	1.400	1.401	1.400	1.401	1.401
262	1.401	1.401	1.401	1.401	1.401
263	2.228	2.232	2.230	2.230	2.231
264	2.229	2.233	2.232	2.231	2.232
265	2.231	2.238	2.235	2.233	2.236
266	2.232	2.238	2.237	2.236	2.238
267	2.233	2.239	2.238	2.237	2.238
268	2.234	2.239	2.238	2.237	2.239
269	2.233	2.239	2.238	2.237	2.238
270	2.237	2.240	2.240	2.239	2.240
271	2.237	2.240	2.240	2.239	2.240
272	2.237	2.241	2.239	2.240	2.240
273	2.237	2.240	2.239	2.239	2.240
274	2.233	2.239	2.238	2.237	2.239
275	2.234	2.239	2.238	2.238	2.239
276	1.939	1.941	1.940	1.940	1.940
277	1.939	1.940	1.939	1.939	1.940
278	1.939	1.940	1.939	1.939	1.939
279	1.936	1.939	1.937	1.937	1.938
280	1.935	1.938	1.936	1.937	1.937
281	1.932	1.936	1.933	1.934	1.934
282	1.931	1.933	1.931	1.932	1.932
283	1.927	1.929	1.928	1.929	1.929
284	1.928	1.929	1.928	1.928	1.928
285	1.928	1.929	1.928	1.929	1.929
286	1.929	1.931	1.930	1.930	1.930
287	1.930	1.932	1.931	1.931	1.931
288	1.930	1.932	1.930	1.930	1.931
289	1.942	1.944	1.943	1.943	1.943
290	1.943	1.947	1.944	1.944	1.944
291	1.943	1.945	1.943	1.943	1.944
292	1.942	1.945	1.943	1.943	1.943
293	1.965	1.967	1.965	1.964	1.964
294	1.961	1.963	1.962	1.962	1.962
295	1.958	1.960	1.959	1.959	1.959
296	1.952	1.957	1.955	1.955	1.955
297	1.951	1.953	1.951	1.951	1.951
298	1.942	1.943	1.943	1.942	1.942
299	1.942	1.944	1.943	1.943	1.943
300	1.940	1.942	1.941	1.942	1.942
301	1.940	1.942	1.941	1.941	1.941
302	1.935	1.938	1.937	1.937	1.937
303	1.935	1.938	1.937	1.937	1.937

TABLE F9 (continued)

304	1.931	1.932	1.931	1.931	1.932
305	1.931	1.933	1.932	1.932	1.932
306	1.931	1.933	1.932	1.932	1.932
307	1.924	1.928	1.926	1.926	1.926
308	1.925	1.928	1.927	1.927	1.927
309	1.926	1.928	1.928	1.928	1.928
310	1.928	1.929	1.929	1.929	1.929
311	1.929	1.930	1.929	1.929	1.929
312	1.929	1.930	1.929	1.929	1.929
313	1.929	1.930	1.929	1.929	1.929
314	1.928	1.929	1.929	1.929	1.929
315	1.952	1.954	1.954	1.953	1.953
316	1.953	1.958	1.957	1.957	1.956
317	1.956	1.959	1.958	1.957	1.958
318	1.956	1.959	1.959	1.958	1.959
319	1.957	1.959	1.959	1.958	1.959
320	1.958	1.960	1.960	1.959	1.960
321	1.958	1.960	1.960	1.959	1.960
322	1.959	1.961	1.961	1.960	1.961
323	1.959	1.962	1.962	1.960	1.961
324	1.960	1.962	1.961	1.961	1.961
325	1.960	1.962	1.961	1.961	1.961
326	1.962	1.965	1.964	1.964	1.966
327	1.963	1.967	1.967	1.964	1.966
328	1.424	1.424	1.424	1.424	1.424
329	1.424	1.424	1.425	1.425	1.425
330	1.424	1.424	1.424	1.424	1.424
331	1.424	1.424	1.424	1.424	1.424
332	1.424	1.424	1.424	1.424	1.424
333	1.424	1.424	1.424	1.424	1.424
334	1.423	1.424	1.424	1.424	1.424
335	1.422	1.423	1.423	1.423	1.423
336	1.423	1.423	1.423	1.423	1.423
337	1.423	1.424	1.424	1.424	1.424
338	1.423	1.423	1.423	1.423	1.423
339	1.424	1.424	1.424	1.424	1.424
340	1.424	1.424	1.424	1.424	1.424
341	2.352	2.357	2.355	2.354	2.356
342	2.344	2.349	2.349	2.347	2.349
343	2.340	2.344	2.342	2.342	2.343
344	2.332	2.338	2.337	2.335	2.337
345	2.330	2.334	2.333	2.331	2.333
346	2.329	2.332	2.331	2.330	2.331
347	2.328	2.330	2.330	2.329	2.330
348	2.320	2.324	2.323	2.322	2.324
349	2.321	2.325	2.324	2.323	2.324
350	2.321	2.326	2.325	2.323	2.324
351	2.321	2.327	2.324	2.323	2.325
352	2.322	2.328	2.328	2.325	2.327
353	2.323	2.329	2.328	2.327	2.329
354	1.989	1.991	1.990	1.990	1.990
355	1.985	1.989	1.989	1.987	1.989
356	1.983	1.987	1.987	1.984	1.987
357	1.981	1.983	1.983	1.931	1.982
358	1.980	1.982	1.981	1.980	1.981
359	1.978	1.980	1.980	1.979	1.980
360	1.972	1.976	1.975	1.974	1.975
361	1.974	1.978	1.978	1.976	1.978
362	1.973	1.977	1.977	1.976	1.976
363	1.970	1.972	1.971	1.971	1.971
364	1.971	1.973	1.972	1.972	1.973
365	1.971	1.974	1.973	1.972	1.973
366	1.953	1.957	1.956	1.954	1.956
367	1.956	1.959	1.959	1.959	1.959
368	1.958	1.960	1.959	1.959	1.959
369	1.959	1.960	1.960	1.960	1.960
370	1.959	1.961	1.961	1.960	1.960
371	1.961	1.962	1.962	1.962	1.962
372	1.961	1.963	1.962	1.962	1.962
373	1.961	1.963	1.963	1.962	1.962
374	1.960	1.962	1.961	1.961	1.961
375	1.960	1.962	1.961	1.961	1.961
376	1.958	1.961	1.960	1.961	1.961
377	1.960	1.961	1.961	1.961	1.961
378	1.960	1.961	1.961	1.961	1.961
379	1.961	1.962	1.961	1.961	1.961
380	1.981	1.983	1.983	1.983	1.983

TABLE F9 (continued)

381	1.980	1.981	1.980	1.980	1.980
382	1.978	1.979	1.978	1.979	1.979
383	1.973	1.977	1.977	1.975	1.975
384	1.971	1.973	1.972	1.972	1.971
385	1.969	1.970	1.969	1.969	1.969
386	1.968	1.970	1.969	1.969	1.969
387	1.967	1.969	1.969	1.968	1.968
388	1.966	1.969	1.968	1.968	1.968
389	1.964	1.968	1.967	1.967	1.967
390	1.960	1.961	1.960	1.960	1.960
391	1.960	1.961	1.961	1.960	1.961
392	1.959	1.961	1.960	1.960	1.960
393	1.962	1.966	1.964	1.964	1.965
394	1.964	1.968	1.968	1.967	1.968
395	1.968	1.969	1.969	1.969	1.969
396	1.969	1.971	1.971	1.970	1.970
397	1.969	1.971	1.970	1.970	1.971
398	1.971	1.974	1.973	1.972	1.972
399	1.971	1.976	1.974	1.972	1.974
400	1.973	1.977	1.976	1.974	1.976
401	1.974	1.979	1.978	1.977	1.978
402	1.974	1.979	1.978	1.978	1.979
403	1.977	1.979	1.979	1.978	1.979
404	1.977	1.980	1.979	1.979	1.979
405	1.974	1.979	1.979	1.977	1.978
406	2.331	2.337	2.335	2.333	2.337
407	2.333	2.340	2.339	2.338	2.339
408	2.336	2.341	2.340	2.339	2.340
409	2.338	2.342	2.341	2.340	2.341
410	2.339	2.343	2.343	2.341	2.343
411	2.339	2.344	2.343	2.341	2.343
412	2.339	2.343	2.343	2.341	2.342
413	2.340	2.344	2.342	2.341	2.343
414	2.340	2.347	2.344	2.342	2.344
415	2.341	2.348	2.347	2.344	2.348
416	2.342	2.349	2.348	2.347	2.349
417	2.344	2.350	2.349	2.348	2.349
418	2.344	2.350	2.350	2.349	2.349
419	1.438	1.438	1.438	1.438	1.438
420	1.434	1.435	1.435	1.434	1.434
421	1.433	1.433	1.433	1.433	1.433
422	1.431	1.432	1.432	1.431	1.431
423	1.430	1.430	1.430	1.430	1.431
424	1.428	1.426	1.428	1.428	1.428
425	1.428	1.429	1.429	1.429	1.429
426	1.428	1.428	1.428	1.428	1.428
427	1.425	1.427	1.427	1.427	1.426
428	1.422	1.423	1.422	1.422	1.422
429	1.423	1.423	1.423	1.423	1.423
430	1.422	1.423	1.423	1.423	1.423
431	1.422	1.422	1.422	1.422	1.422
432	1.971	1.974	1.973	1.973	1.973
433	1.972	1.974	1.973	1.973	1.973
434	1.973	1.975	1.975	1.973	1.974
435	1.971	1.973	1.973	1.972	1.973
436	1.971	1.973	1.973	1.972	1.973
437	1.970	1.972	1.971	1.971	1.971
438	1.965	1.969	1.969	1.968	1.968
439	1.966	1.969	1.968	1.968	1.968
440	1.965	1.969	1.968	1.968	1.968
441	1.965	1.969	1.968	1.968	1.968
442	1.967	1.969	1.968	1.968	1.969
443	1.967	1.969	1.969	1.969	1.969
444	1.968	1.969	1.969	1.969	1.969
445	1.929	1.931	1.930	1.930	1.930
446	1.931	1.934	1.932	1.932	1.932
447	1.934	1.939	1.936	1.936	1.936
448	1.938	1.940	1.939	1.939	1.939
449	1.939	1.941	1.941	1.941	1.941
450	1.942	1.946	1.944	1.944	1.944
451	1.944	1.948	1.947	1.946	1.946
452	1.945	1.948	1.948	1.948	1.948
453	1.948	1.950	1.950	1.950	1.950
454	1.949	1.951	1.950	1.950	1.950
455	1.949	1.951	1.950	1.950	1.950
456	1.949	1.951	1.950	1.950	1.950
457	1.949	1.951	1.950	1.950	1.950

TABLE F9 (continued)

458	1.965	1.967	1.968	1.967	1.968
459	1.967	1.968	1.968	1.969	1.969
460	1.967	1.968	1.968	1.968	1.969
461	1.967	1.968	1.968	1.968	1.969
462	1.968	1.968	1.969	1.968	1.969
463	1.968	1.969	1.969	1.969	1.969
464	1.969	1.969	1.969	1.969	1.969
465	1.968	1.969	1.969	1.969	1.969
466	1.968	1.969	1.969	1.969	1.969
467	1.968	1.969	1.969	1.969	1.969
468	1.969	1.969	1.969	1.969	1.969
469	1.968	1.969	1.969	1.969	1.969
470	1.964	1.967	1.967	1.967	1.968
471	1.960	1.961	1.961	1.961	1.961
472	1.959	1.959	1.960	1.960	1.960
473	1.955	1.955	1.957	1.955	1.957
474	1.955	1.955	1.956	1.955	1.958
475	1.953	1.954	1.954	1.954	1.956
476	1.954	1.954	1.954	1.954	1.954
477	1.954	1.954	1.954	1.954	1.954
478	1.953	1.953	1.953	1.952	1.953
479	1.952	1.952	1.952	1.951	1.952
480	1.947	1.947	1.948	1.948	1.947
481	1.945	1.946	1.947	1.947	1.948
482	1.947	1.947	1.947	1.947	1.947
483	1.947	1.948	1.948	1.947	1.948
484	2.024	2.024	2.024	2.024	2.024
485	2.024	2.024	2.024	2.024	2.024
486	2.024	2.024	2.026	2.024	2.024
487	2.024	2.024	2.024	2.025	2.024
488	2.023	2.023	2.024	2.022	2.022
489	2.023	2.023	2.024	2.023	2.023
490	2.023	2.023	2.024	2.022	2.022
491	2.022	2.022	2.023	2.022	2.022
492	2.022	2.022	2.023	2.022	2.022
493	2.021	2.021	2.021	2.021	2.021
494	2.021	2.021	2.021	2.021	2.021
495	2.021	2.021	2.021	2.021	2.021
496	2.020	2.020	2.021	2.020	2.020
497	1.672	1.672	1.672	1.672	1.672
498	1.672	1.672	1.672	1.672	1.672
499	1.671	1.671	1.671	1.671	1.671
500	1.671	1.671	1.671	1.671	1.671
501	1.670	1.670	1.671	1.670	1.670
502	1.671	1.671	1.671	1.670	1.670
503	1.669	1.669	1.669	1.669	1.669
504	1.669	1.669	1.669	1.669	1.669
505	1.669	1.669	1.670	1.670	1.670
506	1.670	1.670	1.670	1.670	1.670
507	1.670	1.670	1.670	1.670	1.670
508	1.669	1.669	1.669	1.669	1.669
509	1.669	1.669	1.670	1.670	1.670
510	2.020	2.020	2.020	2.020	2.020
511	2.021	2.021	2.021	2.021	2.021
512	2.021	2.021	2.021	2.021	2.021
513	2.021	2.021	2.021	2.021	2.021
514	2.021	2.021	2.021	2.021	2.021
515	2.022	2.022	2.022	2.022	2.022
516	2.022	2.022	2.023	2.022	2.022
517	2.022	2.022	2.022	2.022	2.022
518	2.021	2.021	2.021	2.021	2.021
519	2.024	2.024	2.024	2.024	2.024
520	2.024	2.024	2.026	2.024	2.024
521	2.024	2.025	2.025	2.025	2.025
522	2.026	2.025	2.026	2.024	2.024
523	1.971	1.970	1.970	1.969	1.969
524	1.971	1.970	1.970	1.969	1.969
525	1.971	1.970	1.970	1.969	1.969
526	1.970	1.966	1.969	1.968	1.968
527	1.970	1.968	1.969	1.968	1.968
528	1.970	1.968	1.969	1.967	1.967
529	1.970	1.968	1.969	1.967	1.967
530	1.970	1.968	1.969	1.967	1.967
531	1.970	1.968	1.969	1.967	1.967
532	1.969	1.967	1.967	1.965	1.965
533	1.969	1.967	1.967	1.967	1.967
534	1.969	1.967	1.967	1.964	1.964

TABLE F9 (continued)

535	1.969	1.967	1.967	1.965	1.965
536	2.079	2.079	2.080	2.079	2.079
537	2.079	2.079	2.080	2.079	2.079
538	2.079	2.079	2.080	2.079	2.079
539	2.079	2.079	2.080	2.079	2.079
540	2.079	2.079	2.080	2.079	2.080
541	2.080	2.080	2.080	2.079	2.079
542	2.080	2.080	2.081	2.080	2.080
543	2.081	2.081	2.081	2.080	2.080
544	4.342	4.376	4.406	4.356	4.356
545	4.350	4.383	4.413	4.360	4.361
546	4.354	4.389	4.419	4.366	4.366
547	4.358	4.390	4.420	4.369	4.368
548	4.358	4.390	4.419	4.368	4.368
549	1.728	1.728	1.729	1.728	1.728
550	1.729	1.729	1.729	1.729	1.729
551	1.730	1.730	1.730	1.730	1.730
552	1.731	1.732	1.732	1.731	1.731
553	1.731	1.732	1.733	1.731	1.731
554	1.732	1.732	1.734	1.732	1.732
555	1.733	1.734	1.736	1.732	1.732
556	1.980	1.980	1.980	1.980	1.980
557	1.980	1.980	1.981	1.980	1.980
558	1.980	1.982	1.982	1.980	1.980
559	1.980	1.982	1.984	1.981	1.981
560	1.981	1.982	1.983	1.981	1.981
561	1.981	1.983	1.984	1.981	1.981
562	1.980	1.982	1.983	1.980	1.980
563	1.680	1.680	1.681	1.680	1.680
564	1.680	1.680	1.681	1.680	1.680
565	1.680	1.680	1.681	1.680	1.680
566	1.681	1.681	1.682	1.681	1.681
567	1.681	1.682	1.683	1.681	1.681
568	2.259	2.261	2.263	2.260	2.260
569	2.262	2.267	2.269	2.263	2.263
570	2.267	2.269	2.270	2.267	2.267
571	2.268	2.271	2.272	2.269	2.269
572	2.270	2.273	2.274	2.271	2.271
573	2.272	2.277	2.279	2.274	2.274
574	2.273	2.277	2.279	2.274	2.274
575	2.273	2.277	2.279	2.274	2.274
576	2.564	2.569	2.571	2.567	2.567
577	2.567	2.570	2.573	2.568	2.568
578	2.567	2.571	2.573	2.569	2.569
579	2.567	2.571	2.573	2.569	2.569
580	2.568	2.571	2.574	2.569	2.569
581	2.569	2.572	2.575	2.570	2.570
582	2.569	2.573	2.577	2.570	2.570
583	2.569	2.573	2.578	2.572	2.572
584	2.442	2.443	2.447	2.443	2.443
585	2.440	2.442	2.444	2.442	2.442
586	2.440	2.441	2.443	2.441	2.441
587	2.438	2.439	2.440	2.440	2.440
588	2.437	2.438	2.440	2.440	2.440
589	3.334	3.338	3.343	3.340	3.341
590	3.334	3.338	3.342	3.339	3.339
591	3.330	3.333	3.339	3.334	3.334
592	3.329	3.331	3.337	3.332	3.332
593	3.328	3.330	3.337	3.331	3.330
594	3.328	3.330	3.337	3.331	3.331
595	4.607	4.611	4.623	4.614	4.614
596	4.606	4.610	4.622	4.613	4.613
597	4.604	4.610	4.622	4.613	4.613
598	4.606	4.611	4.623	4.614	4.614
599	2.922	2.925	2.930	2.927	2.927
600	2.923	2.926	2.930	2.928	2.928
601	2.923	2.928	2.931	2.928	2.928
602	2.926	2.929	2.932	2.930	2.930
603	2.929	2.930	2.936	2.932	2.932
604	2.930	2.932	2.938	2.933	2.933
605	2.417	2.420	2.423	2.419	2.419
606	2.418	2.420	2.423	2.420	2.420
607	2.419	2.422	2.426	2.421	2.421
608	2.420	2.421	2.426	2.421	2.421
609	2.420	2.422	2.425	2.421	2.421
610	2.420	2.422	2.427	2.422	2.422
611	2.898	2.900	2.907	2.900	2.900

TABLE F9 (continued)

612	2.899	2.901	2.909	2.901	2.901
613	2.900	2.903	2.910	2.902	2.902
614	2.901	2.903	2.911	2.903	2.903
615	2.903	2.907	2.913	2.904	2.904
616	2.904	2.907	2.913	2.907	2.907
617	3.330	3.332	3.340	3.330	3.330
618	3.330	3.333	3.342	3.331	3.331
619	3.331	3.334	3.343	3.332	3.332
620	3.333	3.338	3.347	3.335	3.335
621	3.337	3.340	3.349	3.339	3.339
622	3.338	3.341	3.350	3.340	3.340
623	4.639	4.640	4.657	4.637	4.637
624	4.647	4.649	4.664	4.643	4.645
625	4.651	4.651	4.669	4.649	4.649
626	4.653	4.653	4.670	4.650	4.650
627	4.656	4.657	4.673	4.652	4.652
628	4.661	4.662	4.679	4.658	4.658
629	2.675	2.678	2.683	2.678	2.678
630	2.677	2.679	2.684	2.678	2.678
631	2.678	2.680	2.684	2.679	2.679
632	2.678	2.680	2.686	2.679	2.679
633	2.679	2.681	2.686	2.680	2.680
634	2.680	2.683	2.688	2.681	2.681
635	2.793	2.795	2.799	2.791	2.791
636	2.793	2.796	2.799	2.793	2.793
637	2.795	2.797	2.800	2.793	2.793
638	2.796	2.798	2.800	2.794	2.794
639	2.798	2.799	2.801	2.797	2.797
640	2.798	2.799	2.802	2.798	2.798
641	3.067	3.069	3.073	3.064	3.064
642	3.069	3.070	3.074	3.068	3.068
643	3.070	3.071	3.074	3.068	3.068
644	3.070	3.070	3.076	3.068	3.068
645	3.070	3.071	3.076	3.069	3.069
646	3.070	3.072	3.077	3.069	3.069
647	3.507	3.509	3.513	3.503	3.503
648	3.508	3.509	3.514	3.504	3.504
649	3.509	3.509	3.514	3.509	3.509
650	3.509	3.509	3.516	3.504	3.504
651	3.509	3.509	3.517	3.506	3.506
652	3.509	3.509	3.517	3.508	3.508
653	4.025	4.027	4.034	4.022	4.022
654	4.028	4.029	4.035	4.021	4.021
655	4.028	4.029	4.037	4.022	4.022
656	4.028	4.029	4.037	4.022	4.022
657	4.028	4.029	4.037	4.022	4.022
658	4.029	4.030	4.038	4.023	4.023
659	5.801	5.794	5.812	5.782	5.782
660	5.801	5.796	5.813	5.783	5.783
661	5.802	5.797	5.813	5.783	5.783
662	5.803	5.798	5.814	5.784	5.784
663	5.805	5.798	5.816	5.786	5.786
664	5.806	5.799	5.820	5.779	5.779
665	1.574	1.574	1.577	1.576	1.576
666	1.574	1.576	1.578	1.576	1.576
667	1.576	1.578	1.579	1.578	1.578
668	1.578	1.579	1.580	1.579	1.579
669	1.579	1.579	1.581	1.580	1.580
670	1.720	1.721	1.724	1.722	1.722
671	1.722	1.723	1.726	1.722	1.722
672	1.723	1.724	1.728	1.724	1.724
673	1.723	1.724	1.728	1.724	1.724
674	1.723	1.724	1.729	1.725	1.725
675	2.095	2.098	2.106	2.099	2.100
676	2.096	2.099	2.107	2.100	2.100
677	2.098	2.100	2.109	2.101	2.101
678	2.099	2.101	2.109	2.102	2.102
679	1.694	1.694	1.696	1.695	1.695
680	1.694	1.696	1.697	1.696	1.696
681	1.695	1.696	1.697	1.696	1.696
682	1.696	1.698	1.698	1.697	1.697
683	1.698	1.697	1.699	1.698	1.698
684	1.698	1.698	1.699	1.698	1.698
685	1.931	1.933	1.934	1.932	1.932
686	1.932	1.934	1.936	1.933	1.933
687	1.933	1.934	1.937	1.933	1.933
688	1.933	1.935	1.938	1.934	1.934

TABLE F9 (continued)

689	1.934	1.936	1.939	1.936	1.936
690	1.937	1.938	1.939	1.937	1.937
691	2.231	2.233	2.235	2.232	2.232
692	2.232	2.234	2.238	2.234	2.234
693	2.234	2.237	2.240	2.236	2.236
694	2.234	2.236	2.239	2.235	2.235
695	2.233	2.237	2.239	2.234	2.234
696	2.234	2.237	2.239	2.234	2.234
697	2.550	2.550	2.553	2.550	2.550
698	2.550	2.552	2.556	2.552	2.552
699	2.552	2.553	2.559	2.553	2.553
700	2.552	2.554	2.559	2.553	2.553
701	2.553	2.557	2.560	2.555	2.555
702	2.553	2.556	2.560	2.553	2.553
703	1.675	1.676	1.677	1.678	1.678
704	1.678	1.676	1.679	1.679	1.679
705	1.678	1.679	1.679	1.679	1.679
706	1.679	1.679	1.679	1.679	1.679
707	1.679	1.680	1.680	1.679	1.679
708	1.680	1.680	1.681	1.680	1.680
709	1.902	1.903	1.903	1.903	1.903
710	1.904	1.904	1.907	1.903	1.903
711	1.906	1.906	1.907	1.906	1.906
712	1.906	1.907	1.908	1.907	1.907
713	1.906	1.907	1.908	1.907	1.907
714	1.907	1.908	1.909	1.908	1.908
715	2.229	2.230	2.230	2.230	2.230
716	2.229	2.230	2.231	2.230	2.230
717	2.229	2.230	2.231	2.230	2.230
718	2.230	2.231	2.232	2.231	2.231
719	2.230	2.232	2.233	2.232	2.232
720	2.231	2.232	2.233	2.232	2.232
721	1.677	1.677	1.678	1.678	1.678
722	1.679	1.679	1.679	1.679	1.679
723	1.679	1.680	1.680	1.679	1.679
724	1.680	1.681	1.681	1.681	1.681
725	1.680	1.681	1.681	1.681	1.681
726	1.682	1.682	1.682	1.682	1.682
727	1.900	1.900	1.900	1.900	1.900
728	1.900	1.901	1.902	1.900	1.900
729	1.901	1.902	1.902	1.902	1.902
730	1.902	1.903	1.903	1.902	1.902
731	1.902	1.903	1.903	1.902	1.902
732	1.902	1.903	1.904	1.903	1.903
733	2.216	2.218	2.219	2.217	2.217
734	2.217	2.219	2.219	2.217	2.217
735	2.217	2.219	2.220	2.218	2.218
736	2.219	2.220	2.221	2.219	2.219
737	2.219	2.220	2.221	2.220	2.220
738	2.220	2.222	2.222	2.220	2.220

TABLE F10 (continued)

214	1.409000	0.000671	47.672	215	1.408660	0.00114	47.663	216	1.492640	0.00089	48.139
217	1.424200	0.001179	48.0338	218	1.419120	0.000035	47.971	219	1.492200	0.00084	47.918
220	1.416600	0.00207	48.6355	221	1.415220	0.000179	47.622	222	1.492200	0.00130	47.749
223	1.409000	0.00071	47.672	224	1.415220	0.000136	47.576	225	1.460220	0.00140	47.7501
226	1.409000	0.00034	47.523	227	1.409000	0.000142	47.593	228	1.490220	0.00164	47.605
229	1.409000	0.00055	47.446	230	1.409000	0.000064	47.475	231	1.490000	0.00084	47.475
232	1.409000	0.00148	47.629	233	1.409000	0.000044	47.465	234	1.490880	0.00110	47.607
235	1.408660	0.00039	47.663	236	1.411000	0.00071	47.672	237	1.490000	0.00071	47.455
238	1.408660	0.00110	47.402	239	1.411000	0.00179	47.330	240	1.490000	0.00039	47.726
241	1.408660	0.00039	47.663	242	1.411000	0.000044	47.460	243	1.490000	0.00039	47.455
244	1.408660	0.00039	47.663	245	1.411000	0.000044	47.460	246	1.490000	0.00114	47.460
247	1.408660	0.00039	47.663	248	1.411000	0.000044	47.460	249	1.490000	0.00039	47.455
250	1.408660	0.00039	47.663	251	1.411000	0.000044	47.460	252	1.490000	0.00039	47.455
253	1.408660	0.00039	47.663	254	1.411000	0.000044	47.460	255	1.490000	0.00039	47.455
256	1.408660	0.00039	47.663	257	1.411000	0.000044	47.460	258	1.490000	0.00039	47.455
259	1.408660	0.00039	47.663	260	1.411000	0.000044	47.460	261	1.490000	0.00039	47.455
262	1.408660	0.00039	47.663	263	1.411000	0.000044	47.460	264	1.490000	0.00039	47.455
265	1.408660	0.00039	47.663	266	1.411000	0.000044	47.460	267	1.490000	0.00039	47.455
268	1.408660	0.00039	47.663	269	1.411000	0.000044	47.460	270	1.490000	0.00039	47.455
271	1.408660	0.00039	47.663	272	1.411000	0.000044	47.460	273	1.490000	0.00039	47.455
274	1.408660	0.00039	47.663	275	1.411000	0.000044	47.460	276	1.490000	0.00039	47.455
277	1.408660	0.00039	47.663	278	1.411000	0.000044	47.460	279	1.490000	0.00039	47.455
280	1.408660	0.00039	47.663	281	1.411000	0.000044	47.460	282	1.490000	0.00039	47.455
283	1.408660	0.00039	47.663	284	1.411000	0.000044	47.460	285	1.490000	0.00039	47.455
286	1.408660	0.00039	47.663	287	1.411000	0.000044	47.460	288	1.490000	0.00039	47.455
289	1.408660	0.00039	47.663	290	1.411000	0.000044	47.460	291	1.490000	0.00039	47.455
292	1.408660	0.00039	47.663	293	1.411000	0.000044	47.460	294	1.490000	0.00039	47.455
295	1.408660	0.00039	47.663	296	1.411000	0.000044	47.460	297	1.490000	0.00039	47.455
298	1.408660	0.00039	47.663	299	1.411000	0.000044	47.460	300	1.490000	0.00039	47.455
301	1.408660	0.00039	47.663	302	1.411000	0.000044	47.460				

TABLE F10 (continued)

445	1.93000	0.00071	46.176	446	1.93220	0.00110	48.231	447	1.93640	0.00179	46.327
446	1.93000	0.00071	46.395	447	1.93400	0.00069	48.433	450	1.94400	0.00121	48.515
447	1.93000	0.00071	46.599	448	1.93400	0.00134	48.597	453	1.94400	0.00069	48.649
448	1.93000	0.00071	46.744	449	1.93400	0.00071	48.659	456	1.95000	0.00071	48.699
449	1.93000	0.00071	46.899	450	1.93400	0.00122	48.706	459	1.95000	0.00054	48.799
450	1.93000	0.00071	47.044	451	1.93400	0.00071	48.800	462	1.95000	0.00054	48.901
451	1.93000	0.00071	47.199	452	1.93400	0.00071	48.900	465	1.95000	0.00043	48.999
452	1.93000	0.00071	47.344	453	1.93400	0.00043	49.000	468	1.95000	0.00040	49.111
453	1.93000	0.00071	47.499	454	1.93400	0.00132	49.050	471	1.95000	0.00040	49.211
454	1.93000	0.00071	47.644	455	1.93400	0.00110	49.100	474	1.95000	0.00040	49.311
455	1.93000	0.00071	47.799	456	1.93400	0.00040	49.150	477	1.95000	0.00040	49.411
456	1.93000	0.00071	47.944	457	1.93400	0.00040	49.200	480	1.95000	0.00040	49.511
457	1.93000	0.00071	48.099	458	1.93400	0.00040	49.250	483	1.95000	0.00040	49.611
458	1.93000	0.00071	48.244	459	1.93400	0.00040	49.300	486	1.95000	0.00040	49.711
459	1.93000	0.00071	48.399	460	1.93400	0.00040	49.350	489	1.95000	0.00040	49.811
460	1.93000	0.00071	48.544	461	1.93400	0.00040	49.400	492	1.95000	0.00040	49.911
461	1.93000	0.00071	48.699	462	1.93400	0.00040	49.450	495	1.95000	0.00040	50.011
462	1.93000	0.00071	48.844	463	1.93400	0.00040	49.500	498	1.95000	0.00040	50.111
463	1.93000	0.00071	48.999	464	1.93400	0.00040	49.550	501	1.95000	0.00040	50.211
464	1.93000	0.00071	49.144	465	1.93400	0.00040	49.600	504	1.95000	0.00040	50.311
465	1.93000	0.00071	49.299	466	1.93400	0.00040	49.650	507	1.95000	0.00040	50.411
466	1.93000	0.00071	49.444	467	1.93400	0.00040	49.700	510	1.95000	0.00040	50.511
467	1.93000	0.00071	49.599	468	1.93400	0.00040	49.750	513	1.95000	0.00040	50.611
468	1.93000	0.00071	49.744	469	1.93400	0.00040	49.800	516	1.95000	0.00040	50.711
469	1.93000	0.00071	49.899	470	1.93400	0.00040	49.850	519	1.95000	0.00040	50.811
470	1.93000	0.00071	50.044	471	1.93400	0.00040	49.900	522	1.95000	0.00040	50.911
471	1.93000	0.00071	50.199	472	1.93400	0.00040	49.950	525	1.95000	0.00040	51.011
472	1.93000	0.00071	50.344	473	1.93400	0.00040	50.000	528	1.95000	0.00040	51.111
473	1.93000	0.00071	50.499	474	1.93400	0.00040	50.050	531	1.95000	0.00040	51.211
474	1.93000	0.00071	50.644	475	1.93400	0.00040	50.100	534	1.95000	0.00040	51.311
475	1.93000	0.00071	50.799	476	1.93400	0.00040	50.150	537	1.95000	0.00040	51.411
476	1.93000	0.00071	50.944	477	1.93400	0.00040	50.200	540	1.95000	0.00040	51.511
477	1.93000	0.00071	51.099	478	1.93400	0.00040	50.250	543	1.95000	0.00040	51.611
478	1.93000	0.00071	51.244	479	1.93400	0.00040	50.300	546	1.95000	0.00040	51.711
479	1.93000	0.00071	51.399	480	1.93400	0.00040	50.350	549	1.95000	0.00040	51.811
480	1.93000	0.00071	51.544	481	1.93400	0.00040	50.400	552	1.95000	0.00040	51.911
481	1.93000	0.00071	51.699	482	1.93400	0.00040	50.450	555	1.95000	0.00040	52.011
482	1.93000	0.00071	51.844	483	1.93400	0.00040	50.500	558	1.95000	0.00040	52.111
483	1.93000	0.00071	51.999	484	1.93400	0.00040	50.550	561	1.95000	0.00040	52.211
484	1.93000	0.00071	52.144	485	1.93400	0.00040	50.600	564	1.95000	0.00040	52.311
485	1.93000	0.00071	52.299	486	1.93400	0.00040	50.650	567	1.95000	0.00040	52.411
486	1.93000	0.00071	52.444	487	1.93400	0.00040	50.700	570	1.95000	0.00040	52.511
487	1.93000	0.00071	52.599	488	1.93400	0.00040	50.750	573	1.95000	0.00040	52.611
488	1.93000	0.00071	52.744	489	1.93400	0.00040	50.800	576	1.95000	0.00040	52.711
489	1.93000	0.00071	52.899	490	1.93400	0.00040	50.850	579	1.95000	0.00040	52.811
490	1.93000	0.00071	53.044	491	1.93400	0.00040	50.900	582	1.95000	0.00040	52.911
491	1.93000	0.00071	53.199	492	1.93400	0.00040	50.950	585	1.95000	0.00040	53.011
492	1.93000	0.00071	53.344	493	1.93400	0.00040	51.000	588	1.95000	0.00040	53.111
493	1.93000	0.00071	53.499	494	1.93400	0.00040	51.050	591	1.95000	0.00040	53.211
494	1.93000	0.00071	53.644	495	1.93400	0.00040	51.100	594	1.95000	0.00040	53.311
495	1.93000	0.00071	53.799	496	1.93400	0.00040	51.150	597	1.95000	0.00040	53.411
496	1.93000	0.00071	53.944	497	1.93400	0.00040	51.200	600	1.95000	0.00040	53.511
497	1.93000	0.00071	54.099	498	1.93400	0.00040	51.250	603	1.95000	0.00040	53.611
498	1.93000	0.00071	54.244	499	1.93400	0.00040	51.300	606	1.95000	0.00040	53.711
499	1.93000	0.00071	54.399	500	1.93400	0.00040	51.350	609	1.95000	0.00040	53.811
500	1.93000	0.00071	54.544	501	1.93400	0.00040	51.400	612	1.95000	0.00040	53.911
501	1.93000	0.00071	54.699	502	1.93400	0.00040	51.450	615	1.95000	0.00040	54.011
502	1.93000	0.00071	54.844	503	1.93400	0.00040	51.500	618	1.95000	0.00040	54.111
503	1.93000	0.00071	54.999	504	1.93400	0.00040	51.550	621	1.95000	0.00040	54.211
504	1.93000	0.00071	55.144	505	1.93400	0.00040	51.600	624	1.95000	0.00040	54.311
505	1.93000	0.00071	55.299	506	1.93400	0.00040	51.650	627	1.95000	0.00040	54.411
506	1.93000	0.00071	55.444	507	1.93400	0.00040	51.700	630	1.95000	0.00040	54.511
507	1.93000	0.00071	55.599	508	1.93400	0.00040	51.750	633	1.95000	0.00040	54.611
508	1.93000	0.00071	55.744	509	1.93400	0.00040	51.800	636	1.95000	0.00040	54.711
509	1.93000	0.00071	55.899	510	1.93400	0.00040	51.850	639	1.95000	0.00040	54.811
510	1.93000	0.00071	56.044	511	1.93400	0.00040	51.900	642	1.95000	0.00040	54.911
511	1.93000	0.00071	56.199	512	1.93400	0.00040	51.950	645	1.95000	0.00040	55.011
512	1.93000	0.00071	56.344	513	1.93400	0.00040	52.000	648	1.95000	0.00040	55.111
513	1.93000	0.00071	56.499	514	1.93400	0.00040	52.050	651	1.95000	0.00040	55.211
514	1.93000	0.00071	56.644	515	1.93400	0.00040	52.100	654	1.95000	0.00040	55.311
515	1.93000	0.00071	56.799	516	1.93400	0.00040	52.150	657	1.95000	0.00040	55.411
516	1.93000	0.00071	56.944	517	1.93400	0.00040	52.200	660	1.95000	0.00040	55.511
517	1.93000	0.00071	57.099	518	1.93400	0.00040	52.250	663	1.95000	0.00040	55.611
518	1.93000	0.00071	57.244	519	1.93400	0.00040	52.300	666	1.95000	0.00040	55.711
519	1.93000	0.00071	57.399	520	1.93400	0.00040	52.350	669	1.95000	0.00040	55.811
520	1.93000	0.00071	57.544	521	1.93400	0.00040	52.400	672	1.95000	0.00040	55.911
521	1.93000	0.00071	57.699	522	1.93400	0.00040	52.450	675	1.95000	0.00040	56.011
522	1.93000	0.00071	57.844	523	1.93400	0.00040	52.500				

TABLE F10 (continued)

676	2.10040	0.00404	52.262	677	2.10180	0.00421	52.296	678	2.10260	0.00376	52.315
679	1.10098	0.00000	42.458	680	1.10098	0.00110	42.508	681	1.09600	0.00071	42.513
682	1.10098	0.00000	42.458	683	1.10098	0.00071	42.508	684	1.09600	0.00045	42.508
685	1.10098	0.00000	42.458	686	1.10098	0.00132	42.561	687	1.09600	0.00173	42.561
688	1.10098	0.00000	42.458	689	1.10098	0.00179	42.561	690	1.09600	0.00089	42.561
691	1.10098	0.00000	42.458	692	1.10098	0.00219	42.561	693	1.09600	0.00219	42.561
694	1.10098	0.00000	42.458	695	1.10098	0.00251	42.561	696	1.09600	0.00230	42.561
697	1.10098	0.00000	42.458	698	1.10098	0.00219	42.561	699	1.09600	0.00283	42.561
700	1.10098	0.00000	42.458	701	1.10098	0.00265	42.561	702	1.09600	0.00300	42.561
703	1.10098	0.00000	42.458	704	1.10098	0.00339	42.561	705	1.09600	0.00345	42.561
706	1.10098	0.00000	42.458	707	1.10098	0.00339	42.561	708	1.09600	0.00345	42.561
709	1.10098	0.00000	42.458	710	1.10098	0.00339	42.561	711	1.09600	0.00345	42.561
712	1.10098	0.00000	42.458	713	1.10098	0.00339	42.561	714	1.09600	0.00345	42.561
715	1.10098	0.00000	42.458	716	1.10098	0.00339	42.561	717	1.09600	0.00345	42.561
718	1.10098	0.00000	42.458	719	1.10098	0.00339	42.561	720	1.09600	0.00345	42.561
721	1.10098	0.00000	42.458	722	1.10098	0.00339	42.561	723	1.09600	0.00345	42.561
724	1.10098	0.00000	42.458	725	1.10098	0.00339	42.561	726	1.09600	0.00345	42.561
727	1.10098	0.00000	42.458	728	1.10098	0.00339	42.561	729	1.09600	0.00345	42.561
730	1.10098	0.00000	42.458	731	1.10098	0.00339	42.561	732	1.09600	0.00345	42.561
733	1.10098	0.00000	42.458	734	1.10098	0.00339	42.561	735	1.09600	0.00345	42.561
736	1.10098	0.00000	42.458	737	1.10098	0.00339	42.561	738	1.09600	0.00345	42.561

TABLE F11

Raw Experimental DataCurrent (amps) and Voltage (volts)

THE CURRENT AND VOLTAGE READ IN ARE				
K	AMPS1	AMPS2	VOLTS1	VOLTS2
1	0.5187	0.5189	35.420	35.430
2	0.5190	0.5190	35.440	35.450
3	0.5192	0.5191	35.450	35.460
4	0.5191	0.5189	35.460	35.450
5	0.5191	0.5190	35.450	35.440
6	0.5190	0.5189	35.440	35.430
7	0.5190	0.5189	35.440	35.430
8	0.5188	0.5188	35.420	35.420
9	0.5189	0.5187	35.420	35.420
10	0.5189	0.5188	35.440	35.430
11	0.5186	0.5189	35.430	35.450
12	0.5185	0.5186	35.430	35.430
13	0.5182	0.5183	35.400	35.410
14	0.5182	0.5181	35.400	35.400
15	0.5166	0.5179	35.460	35.460
16	0.5183	0.5182	35.460	35.460
17	0.5181	0.5182	35.460	35.460
18	0.5179	0.5178	35.440	35.440
19	0.5177	0.5177	35.450	35.450
20	0.5175	0.5176	35.440	35.440
21	0.5176	0.5175	35.430	35.440
22	0.5173	0.5176	35.440	35.460
23	0.5176	0.5174	35.460	35.450
24	0.5174	0.5174	35.450	35.450
25	0.5171	0.5173	35.420	35.440
26	0.5171	0.5172	35.420	35.430
27	0.5171	0.5172	35.430	35.430
28	0.5171	0.5173	35.430	35.430
29	0.2469	0.2467	17.020	17.020
30	0.2473	0.2469	17.020	17.020
31	0.2470	0.2474	17.030	17.030
32	0.2476	0.2476	17.020	17.030
33	0.2477	0.2478	17.030	17.030
34	0.2496	0.2482	17.070	17.070
35	0.2465	0.2452	17.080	17.080

TABLE F11 (continued)

36	0.2449	0.2445	17.090	17.090
37	0.2441	0.2435	17.090	17.080
38	0.2479	0.2480	17.090	17.090
39	0.2480	0.2464	17.090	17.080
40	0.2456	0.2452	17.070	17.080
41	0.2467	0.2461	17.080	17.090
42	0.2471	0.2472	17.090	17.090
43	0.6551	0.6551	44.610	44.610
44	0.6550	0.6549	44.590	44.590
45	0.6550	0.6551	44.600	44.590
46	0.6548	0.6550	44.580	44.590
47	0.6551	0.6548	44.590	44.580
48	0.6548	0.6547	44.570	44.580
49	0.6548	0.6548	44.570	44.580
50	0.6554	0.6554	44.620	44.610
51	0.6552	0.6552	44.630	44.630
52	0.6549	0.6549	44.600	44.610
53	0.6544	0.6547	44.570	44.590
54	0.6542	0.6546	44.560	44.590
55	0.6545	0.6544	44.580	44.580
56	0.5204	0.5206	35.510	35.520
57	0.5204	0.5205	35.510	35.510
58	0.5203	0.5203	35.510	35.500
59	0.5202	0.5203	35.500	35.500
60	0.5198	0.5193	35.500	35.510
61	0.5220	0.5230	35.480	35.480
62	0.5230	0.5230	35.480	35.480
63	0.5230	0.5220	35.470	35.470
64	0.5230	0.5230	35.470	35.470
65	0.5220	0.5230	35.480	35.480
66	0.5210	0.5220	35.470	35.470
67	0.5220	0.5220	35.460	35.460
68	0.5210	0.5220	35.470	35.460
69	0.5210	0.5200	35.420	35.420
70	0.5200	0.5200	35.430	35.430
71	0.5200	0.5200	35.440	35.450
72	0.5210	0.5210	35.450	35.450
73	0.5200	0.5200	35.460	35.440
74	0.5200	0.5190	35.440	35.430

TABLE F11 (continued)

75	0.5200	0.5190	35.440	35.450
76	0.5200	0.5200	35.450	35.460
77	0.5200	0.5200	35.460	35.460
78	0.5190	0.5190	35.420	35.430
79	0.5200	0.5190	35.440	35.440
80	0.5200	0.5200	35.450	35.450
81	0.5160	0.5160	35.420	35.430
82	0.5170	0.5160	35.450	35.450
83	0.5160	0.5160	35.430	35.430
84	0.5160	0.5160	35.420	35.420
85	0.5160	0.5160	35.440	35.440
86	0.5160	0.5160	35.440	35.450
87	0.5160	0.5160	35.430	35.450
88	0.5160	0.5150	35.440	35.430
89	0.5150	0.5150	35.420	35.420
90	0.5150	0.5160	35.420	35.420
91	0.5160	0.5160	35.440	35.450
92	0.5170	0.5180	35.460	35.460
93	0.5180	0.5170	35.460	35.460
94	0.2480	0.2480	17.050	17.050
95	0.2480	0.2480	17.040	17.040
96	0.2480	0.2480	17.050	17.050
97	0.2440	0.2440	17.040	17.040
98	0.2430	0.2440	17.050	17.050
99	0.2430	0.2440	17.050	17.050
100	0.2440	0.2440	17.050	17.060
101	0.2440	0.2430	17.040	17.040
102	0.2460	0.2460	17.040	17.050
103	0.2460	0.2470	17.050	17.050
104	0.2470	0.2460	17.060	17.050
105	0.2460	0.2460	17.060	17.050
106	0.2460	0.2470	17.060	17.050
107	0.6520	0.6510	44.610	44.600
108	0.6510	0.6520	44.600	44.600
109	0.6510	0.6500	44.580	44.590
110	0.6500	0.6530	44.600	44.620
111	0.6510	0.6510	44.590	44.610
112	0.6510	0.6500	44.590	44.560

TABLE F11 (continued)

113	0.6510	0.6500	44.600	44.600
114	0.6510	0.6500	44.600	44.590
115	0.6500	0.6500	44.590	44.590
116	0.6500	0.6500	44.560	44.570
117	0.6510	0.6510	44.570	44.590
118	0.6500	0.6500	44.610	44.600
119	0.6510	0.6510	44.590	44.610
120	0.5160	0.5150	35.450	35.460
121	0.5160	0.5150	35.460	35.440
122	0.5150	0.5160	35.450	35.440
123	0.5160	0.5160	35.460	35.450
124	0.5160	0.5150	35.440	35.440
125	0.5160	0.5150	35.440	35.440
126	0.5160	0.5160	35.440	35.430
127	0.5150	0.5150	35.440	35.430
128	0.5150	0.5160	35.430	35.440
129	0.5150	0.5160	35.440	35.450
130	0.5160	0.5150	35.460	35.450
131	0.5150	0.5160	35.450	35.450
132	0.5150	0.5160	35.440	35.440
133	0.5190	0.5200	35.420	35.430
134	0.5190	0.5180	35.430	35.420
135	0.5200	0.5190	35.420	35.430
136	0.5200	0.5200	35.440	35.450
137	0.5190	0.5200	35.420	35.430
138	0.5190	0.5190	35.410	35.410
139	0.5190	0.5190	35.410	35.410
140	0.5140	0.5150	35.440	35.450
141	0.5140	0.5170	35.420	35.420
142	0.5150	0.5150	35.410	35.410
143	0.5160	0.5160	35.420	35.420
144	0.5170	0.5170	35.410	35.410
145	0.5160	0.5160	35.410	35.410
146	0.5210	0.5210	35.480	35.460
147	0.5200	0.5190	35.470	35.470
148	0.5200	0.5200	35.460	35.470
149	0.5190	0.5190	35.460	35.470
150	0.5200	0.5200	35.470	35.460
151	0.5190	0.5200	35.460	35.470

TABLE F11 (continued)

152	0.5200	0.5200	35.460	35.460
153	0.5200	0.5200	35.460	35.460
154	0.5200	0.5200	35.470	35.480
155	0.5200	0.5200	35.460	35.460
156	0.5200	0.5200	35.480	35.480
157	0.5190	0.5180	35.490	35.480
158	0.5180	0.5180	35.490	35.490
159	0.5170	0.5170	35.490	35.490
160	0.5190	0.5190	35.490	35.500
161	0.5180	0.5190	35.490	35.480
162	0.5190	0.5190	35.490	35.490
163	0.5170	0.5180	35.490	35.490
164	0.5180	0.5170	35.500	35.490
165	0.5170	0.5180	35.490	35.490
166	0.5170	0.5170	35.480	35.480
167	0.5170	0.5170	35.480	35.500
168	0.5180	0.5170	35.490	35.470
169	0.5170	0.5190	35.480	35.480
170	0.5180	0.5180	35.500	35.500
171	0.5170	0.5170	35.500	35.500
172	0.2480	0.2470	17.000	17.010
173	0.2470	0.2480	17.010	17.010
174	0.2470	0.2470	17.000	17.000
175	0.2470	0.2470	17.000	17.000
176	0.2470	0.2480	17.000	17.000
177	0.2470	0.2480	17.010	17.010
178	0.2480	0.2470	17.000	17.000
179	0.2470	0.2480	17.000	17.000
180	0.2480	0.2480	17.010	17.000
181	0.2470	0.2470	17.010	17.010
182	0.2480	0.2480	17.010	17.010
183	0.2480	0.2470	17.010	17.010
184	0.2480	0.2480	17.010	17.010
185	0.6490	0.6490	44.620	44.620
186	0.6490	0.6490	44.630	44.630
187	0.6490	0.6480	44.630	44.630
188	0.6500	0.6490	44.620	44.620
189	0.6490	0.6490	44.610	44.610

TABLE F11 (continued)

190	0.6520	0.6520	44.640	44.640
191	0.6510	0.6520	44.650	44.640
192	0.6520	0.6510	44.620	44.630
193	0.6510	0.6510	44.610	44.620
194	0.6510	0.6500	44.620	44.620
195	0.6510	0.6510	44.630	44.640
196	0.6500	0.6500	44.620	44.620
197	0.6500	0.6510	44.620	44.620
198	0.5190	0.5190	35.470	35.470
199	0.5190	0.5190	35.470	35.470
200	0.5190	0.5190	35.470	35.460
201	0.5190	0.5190	35.470	35.460
202	0.5190	0.5190	35.460	35.450
203	0.5190	0.5190	35.440	35.450
204	0.5190	0.5190	35.450	35.450
205	0.5190	0.5190	35.450	35.450
206	0.5190	0.5190	35.460	35.460
207	0.5190	0.5200	35.460	35.460
208	0.5190	0.5290	35.470	35.470
209	0.5190	0.5290	35.460	35.470
210	0.5190	0.5290	35.460	35.470
211	0.5200	0.5210	35.560	35.570
212	0.5210	0.5200	35.570	35.560
213	0.5200	0.5210	35.550	35.550
214	0.5200	0.5200	35.550	35.560
215	0.5200	0.5200	35.560	35.550
216	0.5190	0.5190	35.550	35.550
217	0.5190	0.5190	35.560	35.560
218	0.5190	0.5190	35.560	35.560
219	0.5190	0.5190	35.570	35.570
220	0.5190	0.5190	35.570	35.570
221	0.5190	0.5200	35.580	35.580
222	0.5200	0.5190	35.570	35.580
223	0.5190	0.5190	35.560	35.560
224	0.5170	0.5170	35.450	35.450
225	0.5170	0.5170	35.450	35.460
226	0.5170	0.5170	35.440	35.440
227	0.5170	0.5170	35.450	35.440
228	0.5170	0.5170	35.450	35.450

TABLE F11 (continued)

229	0.5160	0.5170	35.410	35.420
230	0.5170	0.5170	35.420	35.430
231	0.5170	0.5170	35.430	35.440
232	0.5170	0.5170	35.450	35.450
233	0.5170	0.5170	35.460	35.460
234	0.5170	0.5170	35.460	35.460
235	0.5170	0.5170	35.460	35.460
236	0.5170	0.5170	35.470	35.470
237	0.5180	0.5180	35.460	35.450
238	0.5180	0.5180	35.460	35.460
239	0.5170	0.5170	35.460	35.470
240	0.5180	0.5180	35.470	35.470
241	0.5180	0.5190	35.470	35.480
242	0.5180	0.5180	35.480	35.480
243	0.5180	0.5180	35.460	35.460
244	0.5180	0.5180	35.470	35.460
245	0.5180	0.5180	35.460	35.470
246	0.5180	0.5180	35.460	35.470
247	0.5180	0.5180	35.460	35.470
248	0.5180	0.5180	35.470	35.470
249	0.5180	0.5180	35.470	35.470
250	0.2480	0.2480	17.010	17.010
251	0.2480	0.2480	17.010	17.010
252	0.2480	0.2480	17.010	17.010
253	0.2490	0.2480	17.010	17.010
254	0.2490	0.2480	17.010	17.010
255	0.2480	0.2480	17.010	17.010
256	0.2480	0.2480	17.010	17.010
257	0.2490	0.2490	17.010	17.010
258	0.2490	0.2480	17.010	17.010
259	0.2480	0.2480	17.010	17.010
260	0.2480	0.2480	17.010	17.010
261	0.2480	0.2480	17.010	17.010
262	0.2480	0.2490	17.010	17.010
263	0.6530	0.6530	44.620	44.630
264	0.6530	0.6530	44.620	44.620
265	0.6540	0.6530	44.640	44.630
266	0.6530	0.6530	44.630	44.640

TABLE F11 (continued)

267	0.6530	0.6530	44.640	44.640
268	0.6530	0.6530	44.630	44.640
269	0.6530	0.6530	44.610	44.620
270	0.6530	0.6530	44.620	44.620
271	0.6530	0.6530	44.620	44.620
272	0.6530	0.6530	44.620	44.630
273	0.6530	0.6530	44.630	44.630
274	0.6530	0.6530	44.610	44.610
275	0.6520	0.6530	44.610	44.620
276	0.5190	0.5190	35.480	35.480
277	0.5190	0.5190	35.480	35.490
278	0.5190	0.5190	35.500	35.500
279	0.5190	0.5200	35.510	35.510
280	0.5190	0.5190	35.510	35.500
281	0.5190	0.5190	35.510	35.510
282	0.5190	0.5200	35.500	35.500
283	0.5190	0.5190	35.460	35.480
284	0.5190	0.5190	35.490	35.480
285	0.5190	0.5190	35.480	35.480
286	0.5190	0.5200	35.490	35.500
287	0.5190	0.5190	35.500	35.510
288	0.5190	0.5200	35.500	35.500
289	0.5170	0.5170	35.400	35.410
290	0.5170	0.5170	35.410	35.410
291	0.5170	0.5170	35.420	35.420
292	0.5170	0.5170	35.420	35.420
293	0.5140	0.5130	35.380	35.390
294	0.5150	0.5150	35.390	35.400
295	0.5150	0.5150	35.400	35.410
296	0.5150	0.5150	35.400	35.400
297	0.5150	0.5140	35.400	35.410
298	0.5140	0.5140	35.380	35.380
299	0.5140	0.5140	35.390	35.390
300	0.5140	0.5140	35.390	35.390
301	0.5140	0.5140	35.400	35.400
302	0.5140	0.5140	35.430	35.440
303	0.5150	0.5150	35.440	35.440
304	0.5150	0.5150	35.430	35.420
305	0.5150	0.5150	35.430	35.430

TABLE F11 (continued)

306	0.5150	0.5150	35.430	35.430
307	0.5140	0.5140	35.400	35.400
308	0.5140	0.5140	35.400	35.400
309	0.5140	0.5140	35.410	35.410
310	0.5140	0.5140	35.420	35.420
311	0.5140	0.5140	35.430	35.440
312	0.5140	0.5140	35.430	35.410
313	0.5140	0.5140	35.430	35.410
314	0.5140	0.5140	35.430	35.420
315	0.5170	0.5170	35.420	35.420
316	0.5160	0.5160	35.410	35.410
317	0.5160	0.5160	35.410	35.420
318	0.5160	0.5170	35.410	35.420
319	0.5170	0.5170	35.410	35.400
320	0.5170	0.5160	35.400	35.410
321	0.5160	0.5160	35.420	35.430
322	0.5170	0.5170	35.430	35.440
323	0.5170	0.5160	35.420	35.430
324	0.5160	0.5160	35.420	35.400
325	0.5170	0.5170	35.430	35.420
326	0.5170	0.5170	35.450	35.450
327	0.5180	0.5160	35.450	35.450
328	0.2480	0.2480	17.010	17.020
329	0.2480	0.2480	17.010	17.020
330	0.2480	0.2480	17.020	17.020
331	0.2480	0.2480	17.020	17.020
332	0.2480	0.2480	17.020	17.020
333	0.2480	0.2480	17.020	17.030
334	0.2480	0.2480	17.020	17.020
335	0.2480	0.2480	17.020	17.020
336	0.2480	0.2480	17.020	17.030
337	0.2480	0.2480	17.030	17.030
338	0.2480	0.2480	17.030	17.020
339	0.2480	0.2480	17.030	17.030
340	0.2480	0.2480	17.030	17.030
341	0.6510	0.6520	44.600	44.600
342	0.6520	0.6520	44.600	44.600
343	0.6520	0.6520	44.590	44.600

TABLE F11 (continued)

344	0.6510	0.6510	44.600	44.590
345	0.6520	0.6510	44.580	44.560
346	0.6510	0.6520	44.600	44.600
347	0.6520	0.6510	44.590	44.610
348	0.6530	0.6520	44.610	44.610
349	0.6520	0.6520	44.620	44.610
350	0.6520	0.6520	44.600	44.590
351	0.6520	0.6520	44.590	44.600
352	0.6520	0.6520	44.600	44.600
353	0.6520	0.6520	44.600	44.600
354	0.5170	0.5170	35.430	35.430
355	0.5180	0.5170	35.440	35.440
356	0.5170	0.5180	35.450	35.460
357	0.5180	0.5170	35.460	35.450
358	0.5170	0.5170	35.460	35.460
359	0.5170	0.5170	35.450	35.460
360	0.5170	0.5170	35.460	35.460
361	0.5160	0.5160	35.450	35.450
362	0.5170	0.5170	35.450	35.460
363	0.5170	0.5160	35.460	35.460
364	0.5170	0.5160	35.420	35.420
365	0.5160	0.5160	35.430	35.430
366	0.5160	0.5160	35.440	35.440
367	0.5160	0.5160	35.410	35.400
368	0.5160	0.5160	35.400	35.400
369	0.5160	0.5160	35.400	35.400
370	0.5160	0.5160	35.400	35.400
371	0.5160	0.5160	35.400	35.400
372	0.5160	0.5160	35.410	35.410
373	0.5160	0.5140	35.410	35.410
374	0.5150	0.5150	35.410	35.410
375	0.5150	0.5160	35.410	35.410
376	0.5150	0.5140	35.400	35.390
377	0.5150	0.5150	35.400	35.400
378	0.5160	0.5160	35.390	35.410
379	0.5160	0.5150	35.420	35.420
380	0.5150	0.5140	35.420	35.410
381	0.5140	0.5130	35.420	35.410
382	0.5140	0.5140	35.420	35.410

TABLE F11 (continued)

383	0.5150	0.5140	35.420	35.410
384	0.5130	0.5140	35.410	35.410
385	0.5140	0.5140	35.410	35.410
386	0.5140	0.5140	35.410	35.410
387	0.5140	0.5140	35.420	35.410
388	0.5140	0.5140	35.420	35.410
389	0.5140	0.5150	35.410	35.430
390	0.5140	0.5150	35.430	35.430
391	0.5140	0.5140	35.430	35.430
392	0.5140	0.5130	35.430	35.420
393	0.5180	0.5180	35.460	35.460
394	0.5190	0.5190	35.470	35.460
395	0.5190	0.5190	35.460	35.470
396	0.5180	0.5180	35.460	35.450
397	0.5180	0.5180	35.450	35.450
398	0.5180	0.5190	35.450	35.450
399	0.5180	0.5180	35.450	35.460
400	0.5180	0.5190	35.450	35.450
401	0.5180	0.5180	35.450	35.460
402	0.5180	0.5180	35.460	35.460
403	0.5190	0.5190	35.480	35.470
404	0.5190	0.5190	35.470	35.480
405	0.5180	0.5190	35.470	35.470
406	0.6520	0.6520	44.610	44.600
407	0.6510	0.6520	44.600	44.590
408	0.6530	0.6520	44.600	44.590
409	0.6520	0.6520	44.600	44.600
410	0.6520	0.6520	44.590	44.500
411	0.6520	0.6510	44.580	44.500
412	0.6520	0.6520	44.580	44.580
413	0.6530	0.6520	44.580	44.590
414	0.6520	0.6520	44.580	44.500
415	0.6530	0.6530	44.580	44.590
416	0.6520	0.6520	44.590	44.600
417	0.6520	0.6520	44.600	44.610
418	0.6520	0.6520	44.610	44.620
419	0.2460	0.2460	17.020	17.030
420	0.2450	0.2460	17.020	17.020

TABLE F11 (continued)

421	0.2460	0.2450	17.020	17.030
422	0.2450	0.2450	17.030	17.030
423	0.2450	0.2450	17.030	17.030
424	0.2450	0.2450	17.020	17.020
425	0.2450	0.2440	17.020	17.020
426	0.2450	0.2440	17.020	17.020
427	0.2440	0.2440	17.020	17.020
428	0.2450	0.2450	17.030	17.040
429	0.2450	0.2440	17.030	17.040
430	0.2440	0.2450	17.030	17.030
431	0.2440	0.2450	17.030	17.030
432	0.5150	0.5150	35.430	35.430
433	0.5150	0.5150	35.440	35.430
434	0.5150	0.5150	35.440	35.440
435	0.5150	0.5150	35.440	35.440
436	0.5150	0.5150	35.440	35.430
437	0.5150	0.5150	35.430	35.430
438	0.5150	0.5150	35.430	35.430
439	0.5150	0.5150	35.430	35.430
440	0.5150	0.5150	35.440	35.440
441	0.5150	0.5150	35.440	35.440
442	0.5150	0.5150	35.440	35.440
443	0.5140	0.5140	35.440	35.440
444	0.5170	0.5170	35.440	35.440
445	0.5160	0.5160	35.400	35.410
446	0.5150	0.5160	35.410	35.410
447	0.5150	0.5150	35.400	35.400
448	0.5160	0.5160	35.410	35.400
449	0.5150	0.5150	35.410	35.400
450	0.5150	0.5160	35.400	35.400
451	0.5160	0.5150	35.400	35.400
452	0.5150	0.5150	35.400	35.410
453	0.5150	0.5150	35.400	35.400
454	0.5150	0.5150	35.390	35.390
455	0.5150	0.5150	35.400	35.400
456	0.5150	0.5150	35.400	35.400
457	0.5150	0.5150	35.400	35.400
458	0.7270	0.7270	49.600	49.600
459	0.7270	0.7240	49.600	49.600

TABLE F11 (continued)

460	0.7240	0.7250	49.600	49.610
461	0.7270	0.7270	49.610	49.620
462	0.7250	0.7280	49.630	49.630
463	0.7280	0.7270	49.640	49.640
464	0.7280	0.7280	49.650	49.650
465	0.7280	0.7260	49.630	49.630
466	0.7280	0.7280	49.630	49.630
467	0.7280	0.7280	49.630	49.630
468	0.7270	0.7280	49.630	49.630
469	0.7280	0.7240	49.630	49.630
470	0.7270	0.7270	49.630	49.620
471	0.7270	0.7270	49.700	49.680
472	0.7280	0.7270	49.690	49.690
473	0.7270	0.7260	49.680	49.650
474	0.7260	0.7260	49.670	49.660
475	0.7250	0.7260	49.630	49.670
476	0.7260	0.7260	49.670	49.680
477	0.7260	0.7260	49.690	49.670
478	0.7260	0.7260	49.670	49.680
479	0.7260	0.7260	49.680	49.680
480	0.7260	0.7260	49.640	49.650
481	0.7260	0.7250	49.640	49.650
482	0.7250	0.7260	49.650	49.660
483	0.7260	0.7260	49.650	49.650
484	0.7240	0.7240	49.670	49.680
485	0.7230	0.7230	49.670	49.670
486	0.7230	0.7230	49.680	49.680
487	0.7230	0.7220	49.680	49.680
488	0.7220	0.7230	49.660	49.650
489	0.7230	0.7240	49.670	49.680
490	0.7230	0.7240	49.670	49.680
491	0.7230	0.7240	49.650	49.670
492	0.7230	0.7240	49.650	49.680
493	0.7220	0.7220	49.670	49.660
494	0.7230	0.7230	49.670	49.670
495	0.7240	0.7230	49.670	49.690
496	0.7220	0.7220	49.660	49.660
497	0.5140	0.5130	35.400	35.390

TABLE F11 (continued)

498	0.5140	0.5130	35.390	35.390
499	0.5130	0.5130	35.380	35.390
500	0.5150	0.5150	35.400	35.390
501	0.5150	0.5150	35.400	35.410
502	0.5150	0.5150	35.400	35.390
503	0.5150	0.5140	35.400	35.400
504	0.5140	0.5140	35.390	35.390
505	0.5150	0.5150	35.400	35.410
506	0.5140	0.5140	35.400	35.400
507	0.5140	0.5140	35.390	35.400
508	0.5140	0.5140	35.390	35.390
509	0.5140	0.5140	35.390	35.390
510	0.7260	0.7270	49.670	49.600
511	0.7260	0.7260	49.660	49.600
512	0.7260	0.7250	49.670	49.650
513	0.7250	0.7260	49.660	49.670
514	0.7250	0.7260	49.650	49.600
515	0.7250	0.7260	49.650	49.600
516	0.7260	0.7250	49.650	49.650
517	0.7250	0.7250	49.650	49.640
518	0.7260	0.7260	49.640	49.640
519	0.7250	0.7250	49.650	49.650
520	0.7250	0.7260	49.650	49.650
521	0.7250	0.7260	49.650	49.650
522	0.7260	0.7260	49.650	49.650
523	0.7240	0.7240	49.580	49.590
524	0.7250	0.7230	49.590	49.590
525	0.7230	0.7230	49.600	49.600
526	0.7240	0.7230	49.590	49.500
527	0.7220	0.7230	49.580	49.590
528	0.7230	0.7220	49.590	49.500
529	0.7240	0.7240	49.570	49.500
530	0.7240	0.7240	49.570	49.550
531	0.7240	0.7250	49.590	49.590
532	0.7250	0.7240	49.620	49.600
533	0.7240	0.7240	49.600	49.590
534	0.7240	0.7240	49.600	49.590
535	0.7240	0.7240	49.590	49.600
536	0.7230	0.7240	49.660	49.640

TABLE F11 (continued)

537	0.7230	0.7230	49.640	49.630
538	0.7230	0.7230	49.630	49.630
539	0.7230	0.7220	49.630	49.630
540	0.7220	0.7230	49.620	49.630
541	0.7230	0.7230	49.640	49.640
542	0.7230	0.7230	49.650	49.650
543	0.7240	0.7240	49.650	49.650
544	1.9660	1.9660	132.600	132.500
545	1.9660	1.9670	132.500	132.600
546	1.9670	1.9680	132.600	132.600
547	1.9680	1.9680	132.600	132.600
548	1.9700	1.9690	132.700	132.700
549	0.5180	0.5180	35.400	35.400
550	0.5180	0.5180	35.400	35.400
551	0.5180	0.5180	35.400	35.400
552	0.5180	0.5180	35.410	35.400
553	0.5180	0.5180	35.410	35.410
554	0.5180	0.5180	35.410	35.410
555	0.5170	0.5180	35.410	35.410
556	0.6540	0.6540	44.580	44.590
557	0.6540	0.6540	44.590	44.590
558	0.6530	0.6530	44.590	44.600
559	0.6540	0.6540	44.610	44.600
560	0.6530	0.6530	44.610	44.600
561	0.6530	0.6520	44.610	44.590
562	0.6540	0.6540	44.610	44.590
563	0.5170	0.5170	35.430	35.430
564	0.5170	0.5170	35.430	35.430
565	0.5170	0.5170	35.430	35.430
566	0.5170	0.5170	35.440	35.440
567	0.5170	0.5170	35.430	35.440
568	0.8080	0.8080	54.920	54.950
569	0.8080	0.8080	54.950	54.950
570	0.8080	0.8090	54.990	55.000
571	0.8090	0.8090	54.970	55.010
572	0.8090	0.8110	55.040	55.050
573	0.8100	0.8100	55.070	55.100
574	0.8090	0.8110	55.080	55.080

TABLE F11 (continued)

575	0.8110	0.8110	55.070	55.100
576	0.9420	0.9430	63.800	63.820
577	0.9420	0.9430	63.810	63.810
578	0.9420	0.9420	63.780	63.780
579	0.9420	0.9420	63.800	63.790
580	0.9430	0.9430	63.830	63.830
581	0.9440	0.9430	63.870	63.890
582	0.9440	0.9440	63.860	63.870
583	0.9440	0.9440	63.860	63.880
584	0.9390	0.9390	64.000	64.000
585	0.9410	0.9420	64.050	64.080
586	0.9340	0.9350	64.080	64.090
587	0.9420	0.9420	64.100	64.100
588	0.9360	0.9370	64.090	64.090
589	1.3220	1.3220	90.080	90.080
590	1.3220	1.3230	90.070	90.110
591	1.3210	1.3210	90.120	90.090
592	1.3190	1.3200	90.080	90.080
593	1.3200	1.3200	90.110	90.120
594	1.3240	1.3250	90.090	90.090
595	1.7820	1.7800	120.380	120.350
596	1.7810	1.7810	120.300	120.380
597	1.7820	1.7810	120.420	120.360
598	1.7820	1.7800	120.370	120.340
599	1.1690	1.1680	79.240	79.240
600	1.1680	1.1670	79.240	79.170
601	1.1680	1.1680	79.180	79.180
602	1.1680	1.1680	79.200	79.210
603	1.1680	1.1670	79.190	79.210
604	1.1670	1.1680	79.200	79.200
605	0.9530	0.9520	64.610	64.580
606	0.9520	0.9520	64.560	64.580
607	0.9530	0.9520	64.550	64.560
608	0.9520	0.9520	64.550	64.560
609	0.9520	0.9520	64.560	64.570
610	0.9520	0.9520	64.570	64.540
611	1.1660	1.1680	79.040	79.010
612	1.1680	1.1670	79.020	79.020
613	1.1680	1.1670	79.030	79.030

TABLE F11 (continued)

614	1.1670	1.1670	79.020	79.020
615	1.1670	1.1670	79.000	78.970
616	1.1680	1.1680	78.990	79.060
617	1.3290	1.3290	89.880	89.840
618	1.3290	1.3280	89.870	89.890
619	1.3290	1.3300	89.900	89.940
620	1.3290	1.3290	89.970	89.990
621	1.3300	1.3300	89.960	89.950
622	1.3300	1.3310	89.950	90.000
623	1.7860	1.7890	120.560	120.670
624	1.7920	1.7920	120.860	120.830
625	1.7900	1.7890	120.760	120.770
626	1.7910	1.7910	120.800	120.800
627	1.7890	1.7890	120.720	120.770
628	1.7890	1.7900	120.780	120.790
629	1.0430	1.0440	70.730	70.740
630	1.0440	1.0450	70.740	70.740
631	1.0430	1.0430	70.720	70.760
632	1.0450	1.0450	70.750	70.750
633	1.0450	1.0440	70.740	70.740
634	1.0430	1.0460	70.780	70.780
635	0.9370	0.9360	63.640	63.560
636	0.9360	0.9360	63.560	63.520
637	0.9360	0.9360	63.490	63.480
638	0.9370	0.9370	63.520	63.540
639	0.9360	0.9360	63.520	63.540
640	0.9360	0.9370	63.520	63.520
641	1.0380	1.0380	70.500	70.460
642	1.0380	1.0370	70.480	70.450
643	1.0370	1.0380	70.440	70.430
644	1.0370	1.0370	70.420	70.410
645	1.0360	1.0370	70.410	70.400
646	1.0370	1.0380	70.400	70.380
647	1.1790	1.1790	80.010	79.990
648	1.1790	1.1790	79.990	79.980
649	1.1790	1.1790	79.980	80.000
650	1.1790	1.1790	79.980	79.970
651	1.1780	1.1790	79.990	79.960

TABLE F11 (continued)

652	1.1790	1.1790	79.990	80.000
653	1.3270	1.3260	89.960	89.830
654	1.3260	1.3260	89.840	89.810
655	1.3260	1.3270	89.810	89.830
656	1.3260	1.3260	89.820	89.810
657	1.3260	1.3250	89.800	89.800
658	1.3260	1.3270	89.800	89.800
659	1.7800	1.7810	120.600	120.560
660	1.7810	1.7820	120.580	120.560
661	1.7810	1.7810	120.520	120.560
662	1.7810	1.7800	120.530	120.540
663	1.7810	1.7820	120.560	120.560
664	1.7810	1.7830	120.560	120.650
665	0.5170	0.5140	35.470	35.470
666	0.5140	0.5140	35.470	35.470
667	0.5140	0.5150	35.480	35.470
668	0.5160	0.5150	35.480	35.480
669	0.5140	0.5140	35.460	35.460
670	0.6470	0.6470	44.500	44.510
671	0.6470	0.6480	44.520	44.520
672	0.6480	0.6480	44.530	44.520
673	0.6480	0.6480	44.510	44.510
674	0.6480	0.6480	44.510	44.510
675	0.9420	0.9420	64.390	64.420
676	0.9420	0.9420	64.440	64.450
677	0.9430	0.9430	64.480	64.500
678	0.9420	0.9430	64.500	64.490
679	0.5140	0.5130	35.400	35.400
680	0.5130	0.5140	35.400	35.400
681	0.5140	0.5130	35.400	35.410
682	0.5140	0.5140	35.400	35.410
683	0.5130	0.5140	35.410	35.410
684	0.5140	0.5140	35.410	35.420
685	0.6520	0.6520	44.530	44.540
686	0.6520	0.6530	44.540	44.550
687	0.6520	0.6520	44.550	44.550
688	0.6520	0.6530	44.560	44.560
689	0.6520	0.6530	44.570	44.570
690	0.6520	0.6530	44.550	44.570

TABLE F11 (continued)

691	0.7980	0.7980	54.480	54.470
692	0.7980	0.7980	54.460	54.460
693	0.7980	0.7990	54.430	54.470
694	0.7980	0.7990	54.430	54.460
695	0.7980	0.7980	54.420	54.420
696	0.7980	0.7980	54.460	54.450
697	0.9450	0.9450	64.320	64.310
698	0.9450	0.9450	64.310	64.300
699	0.9450	0.9450	64.330	64.310
700	0.9450	0.9450	64.320	64.310
701	0.9450	0.9450	64.310	64.320
702	0.9420	0.9450	64.250	64.310
703	0.5140	0.5150	35.410	35.420
704	0.5140	0.5140	35.420	35.410
705	0.5140	0.5140	35.410	35.400
706	0.5150	0.5140	35.410	35.410
707	0.5150	0.5140	35.400	35.400
708	0.5140	0.5140	35.400	35.400
709	0.6480	0.6480	44.540	44.550
710	0.6480	0.6480	44.550	44.550
711	0.6490	0.6490	44.550	44.560
712	0.6480	0.6490	44.560	44.570
713	0.6480	0.6480	44.570	44.560
714	0.6490	0.6480	44.570	44.560
715	0.8220	0.8220	56.270	56.260
716	0.8220	0.8210	56.270	56.260
717	0.8210	0.8210	56.250	56.250
718	0.8220	0.8200	56.260	56.210
719	0.8220	0.8210	56.200	56.230
720	0.8210	0.8210	56.230	56.220
721	0.5180	0.5180	35.400	35.410
722	0.5180	0.5180	35.410	35.420
723	0.5180	0.5180	35.420	35.420
724	0.5180	0.5180	35.420	35.420
725	0.5180	0.5180	35.430	35.430
726	0.5180	0.5180	35.440	35.430
727	0.6510	0.6510	44.510	44.520
728	0.6510	0.6520	44.520	44.530

TABLE F11 (continued)

729	0.6520	0.6520	44.530	44.540
730	0.6520	0.6520	44.540	44.540
731	0.6520	0.6520	44.540	44.550
732	0.6520	0.6510	44.550	44.560
733	0.8160	0.8160	55.870	55.860
734	0.8170	0.8170	55.840	55.830
735	0.8170	0.8170	55.810	55.810
736	0.8170	0.8160	55.810	55.820
737	0.8170	0.8180	55.820	55.820
738	0.8180	0.8170	55.840	55.840

بسم الله الرحمن الرحيم

73 72 71 70 69 68 67 66 65 64 63 62 61 60 59 58 57 56 55 54 53 52 51 50 49 48 47 46 45 44 43 42 41 40 39 38 37 36 35 34 33 32 31 30 29 28 27 26 25 24 23 22 21 20 19 18 17 16 15 14 13 12 11 10 9 8 7 6 5 4 3 2 1

151	152	153	154	155	156	157	158	159	160	161	162	163	164	165	166	167	168	169	170	171	172	173	174	175	176	177	178	179	180	181	182	183	184	185	186	187	188	189	190	191	192	193	194	195	196	197	198	199	200	201	202	203	204	205	206	207	208	209	210	211	212	213	214	215	216	217	218	219	220	221	222	223	224	225	226	227	228	229	230	231	232	233	234	235	236	237	238	239	240	241	242	243	244	245	246	247	248	249	250	251	252	253	254	255	256	257	258	259	260	261	262	263	264	265	266	267	268	269	270	271	272	273	274	275	276	277	278	279	280	281	282	283	284	285	286	287	288	289	290	291	292	293	294	295	296	297	298	299	300	301	302	303	304	305	306	307	308	309	310	311	312	313	314	315	316	317	318	319	320	321	322	323	324	325	326	327	328	329	330	331	332	333	334	335	336	337	338	339	340	341	342	343	344	345	346	347	348	349	350	351	352	353	354	355	356	357	358	359	360	361	362	363	364	365	366	367	368	369	370	371	372	373	374	375	376	377	378	379	380	381	382	383	384	385	386	387	388	389	390	391	392	393	394	395	396	397	398	399	400	401	402	403	404	405	406	407	408	409	410	411	412	413	414	415	416	417	418	419	420	421	422	423	424	425	426	427	428	429	430	431	432	433	434	435	436	437	438	439	440	441	442	443	444	445	446	447	448	449	450	451	452	453	454	455	456	457	458	459	460	461	462	463	464	465	466	467	468	469	470	471	472	473	474	475	476	477	478	479	480	481	482	483	484	485	486	487	488	489	490	491	492	493	494	495	496	497	498	499	500	501	502	503	504	505	506	507	508	509	510	511	512	513	514	515	516	517	518	519	520	521	522	523	524	525	526	527	528	529	530	531	532	533	534	535	536	537	538	539	540	541	542	543	544	545	546	547	548	549	550	551	552	553	554	555	556	557	558	559	560	561	562	563	564	565	566	567	568	569	570	571	572	573	574	575	576	577	578	579	580	581	582	583	584	585	586	587	588	589	590	591	592	593	594	595	596	597	598	599	600	601	602	603	604	605	606	607	608	609	610	611	612	613	614	615	616	617	618	619	620	621	622	623	624	625	626	627	628	629	630	631	632	633	634	635	636	637	638	639	640	641	642	643	644	645	646	647	648	649	650	651	652	653	654	655	656	657	658	659	660	661	662	663	664	665	666	667	668	669	670	671	672	673	674	675	676	677	678	679	680	681	682	683	684	685	686	687	688	689	690	691	692	693	694	695	696	697	698	699	700	701	702	703	704	705	706	707	708	709	710	711	712	713	714	715	716	717	718	719	720	721	722	723	724	725	726	727	728	729	730	731	732	733	734	735	736	737	738	739	740	741	742	743	744	745	746	747	748	749	750	751	752	753	754	755	756	757	758	759	760	761	762	763	764	765	766	767	768	769	770	771	772	773	774	775	776	777	778	779	780	781	782	783	784	785	786	787	788	789	790	791	792	793	794	795	796	797	798	799	800	801	802	803	804	805	806	807	808	809	810	811	812	813	814	815	816	817	818	819	820	821	822	823	824	825	826	827	828	829	830	831	832	833	834	835	836	837	838	839	840	841	842	843	844	845	846	847	848	849	850	851	852	853	854	855	856	857	858	859	860	861	862	863	864	865	866	867	868	869	870	871	872	873	874	875	876	877	878	879	880	881	882	883	884	885	886	887	888	889	890	891	892	893	894	895	896	897	898	899	900	901	902	903	904	905	906	907	908	909	910	911	912	913	914	915	916	917	918	919	920	921	922	923	924	925	926	927	928	929	930	931	932	933	934	935	936	937	938	939	940	941	942	943	944	945	946	947	948	949	950	951	952	953	954	955	956	957	958	959	960	961	962	963	964	965	966	967	968	969	970	971	972	973	974	975	976	977	978	979	980	981	982	983	984	985	986	987	988	989	990	991	992	993	994	995	996	997	998	999	1000
-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	-----	------

459
460
461
462
463
464
465
466
467
468
469
470
471
472
473
474
475
476
477
478
479
480
481
482
483
484
485
486
487
488
489
490
491
492
493
494
495
496
497
498
499
500
501
502
503
504
505
506
507
508
509
510
511
512
513
514
515
516
517
518
519
520
521
522
523
524
525
526
527
528
529
530
531
532
533
534
535
536
537
538
539
540
541
542
543
544
545
546
547
548
549
550
551
552
553
554
555
556
557
558
559
560
561
562
563
564
565
566
567
568
569
570
571
572
573
574
575
576
577
578
579
580
581
582
583
584
585
586
587
588
589
590
591
592
593
594
595
596
597
598
599
600
601
602
603
604
605
606
607
608
609
610
611
612
613
614
615
616
617
618
619
620
621
622
623
624
625
626
627
628
629
630
631
632
633
634
635
636
637
638
639
640
641
642
643
644
645
646
647
648
649
650
651
652
653
654
655
656
657
658
659
660
661
662
663
664
665
666
667
668
669
670
671
672
673
674
675
676
677
678
679
680
681
682
683
684
685
686
687
688
689
690
691
692
693
694
695
696
697
698
699
700
701
702
703
704
705
706
707
708
709
710
711
712
713
714
715
716
717
718
719
720
721
722
723
724
725
726
727
728
729
730
731
732
733
734
735
736
737
738
739
740
741
742
743
744
745
746
747
748
749
750
751
752
753
754
755
756
757
758
759
760
761
762
763
764
765
766
767
768
769
770
771
772
773
774
775
776
777
778
779
780
781
782
783
784
785
786
787
788
789
790
791
792
793
794
795
796
797
798
799
800
801
802
803
804
805
806
807
808
809
810
811
812
813
814
815
816
817
818
819
820
821
822
823
824
825
826
827
828
829
830
831
832
833
834
835
836
837
838
839
840
841
842
843
844
845
846
847
848
849
850
851
852
853
854
855
856
857
858
859
860
861
862
863
864
865
866
867
868
869
870
871
872
873
874
875
876
877
878
879
880
881
882
883
884
885
886
887
888
889
890
891
892
893
894
895
896
897
898
899
900
901
902
903
904
905
906
907
908
909
910
911
912
913
914
915
916
917
918
919
920
921
922
923
924
925
926
927
928
929
930
931
932
933
934
935
936
937
938
939
940
941
942
943
944
945
946
947
948
949
950
951
952
953
954
955
956
957
958
959
960
961
962
963
964
965
966
967
968
969
970
971
972
973
974
975
976
977
978
979
980
981
982
983
984
985
986
987
988
989
990
991
992
993
994
995
996
997
998
999
1000

TABLE F13 (continued)

TABLE F14

RUNS	THE MEAN THERMAL CONDUCTIVITIES AND STD DEVIATIONS			
	TOP SPECIMEN		BOTTOM SPECIMEN	
	CONDUCTIVITY	STD DEVIATION	CONDUCTIVITY	STD DEVIATION
1-- 14	0.1934	0.00192	0.1777	0.00150
15-- 28	0.1965	0.00113	0.1765	0.00120
29-- 42	0.1942	0.01716	0.1775	0.01234
43-- 55	0.2031	0.00065	0.1730	0.00127
56-- 68	0.1825	0.00194	0.1856	0.00216
69-- 80	0.1812	0.00164	0.1946	0.00162
81-- 93	0.2053	0.00214	0.2193	0.00179
94--106	0.2010	0.00415	0.2086	0.00667
107--119	0.2030	0.00218	0.2232	0.00177
120--132	0.2195	0.00224	0.1953	0.00260
133--145	0.2053	0.00161	0.2113	0.00190
146--158	0.2035	0.00112	0.2123	0.00207
159--171	0.1779	0.00099	0.1613	0.00155
172--184	0.1765	0.00402	0.1645	0.00376
185--197	0.1816	0.00131	0.1621	0.00133
198--210	0.1741	0.00156	0.1632	0.00166
211--223	0.1763	0.00060	0.1583	0.00071
224--236	0.1761	0.00029	0.1606	0.00099
237--249	0.1754	0.00115	0.1561	0.00054
250--262	0.1650	0.00392	0.1563	0.00220
263--275	0.1760	0.00050	0.1566	0.00036
276--288	0.1714	0.00120	0.1549	0.00124
289--301	0.1566	0.00099	0.1673	0.00231
302--314	0.1595	0.00075	0.1724	0.00139
315--327	0.1509	0.00055	0.1470	0.00142
328--340	0.1444	0.00348	0.1407	0.00295
341--353	0.1518	0.00066	0.1474	0.00094
354--366	0.1421	0.00183	0.1482	0.00731
367--379	0.1422	0.00156	0.1506	0.00263
380--392	0.1439	0.00123	0.1530	0.00170
393--405	0.1426	0.00172	0.1493	0.00067
406--418	0.1453	0.00070	0.1511	0.00100
419--431	0.1402	0.00549	0.1505	0.00262
432--444	0.1435	0.00121	0.1515	0.00039
445--457	0.1642	0.00180	0.1312	0.00041

TABLE F14 (continued)

458--470	0.1663	0.00024	0.1696	0.00029
471--483	0.1739	0.00092	0.1636	0.00026
484--496	0.2251	0.00033	0.2247	0.00033
497--509	0.2203	0.00124	0.2247	0.00049
510--522	0.2259	0.00039	0.2196	0.00089
523--535	0.1427	0.00039	0.1508	0.01003
536--548	0.6947	0.00397	0.6167	0.00435
549--561	0.8044	0.00042	0.6881	0.00215
562--574	0.1512	0.00047	0.1455	0.00082
575--587	0.1532	0.00021	0.1472	0.00036
588--600	0.0522	0.00002	0.0513	0.00005
601--613	0.1551	0.00012	0.1534	0.00029
614--626	0.1559	0.00022	0.1560	0.00015
627--639	0.2075	0.00061	0.1976	0.00052
640--652	0.2093	0.00046	0.1998	0.00064
653--665	0.2120	0.00008	0.2018	0.00011
666--678	0.2033	0.00009	0.1956	0.00020
679--691	0.1437	0.00017	0.1343	0.00011
692--704	0.1469	0.00010	0.1384	0.00006
705--717	0.1486	0.00006	0.1418	0.00018
718--730	0.1580	0.00024	0.1532	0.00018
731--743	0.1413	0.00013	0.1365	0.00016
744--756	0.1622	0.00022	0.1386	0.00017
757--769	0.1651	0.00022	0.1411	0.00011
770--782	0.1689	0.00005	0.1450	0.00012
783--795	0.1719	0.00015	0.1482	0.00013
796--808	0.1859	0.00009	0.1625	0.00015
809--821	0.0631	0.00009	0.0628	0.00013
822--834	0.0669	0.00005	0.0664	0.00007
835--847	0.0750	0.00007	0.0749	0.00007
848--860	0.1333	0.00020	0.1310	0.00028
861--873	0.1347	0.00012	0.1322	0.00020
874--886	0.1360	0.00015	0.1340	0.00011
887--899	0.1391	0.00012	0.1372	0.00028
900--912	0.2300	0.00105	0.2225	0.00066
913--925	0.2301	0.00020	0.2240	0.00068
926--938	0.2319	0.00100	0.2270	0.00044
939--951	0.2326	0.00091	0.2202	0.00122
952--964	0.2352	0.00068	0.2231	0.00061
965--977	0.2362	0.00017	0.2261	0.00027

APPENDIX GERROR ANALYSIS

G1	<u>PROCESS ERRORS</u>	432
G2	<u>MEASUREMENT ERRORS</u>	433
G3	<u>SYSTEMATIC ERRORS</u>	434
G4	<u>EXPERIMENTAL ERROR</u>	435

G1 PROCESS ERRORS

These are defined as errors generated by random disturbances in the process or non-steady-state error.

In all the experimental runs, the Kipps-Zonen BD5 recorder indicated that the guarded hot plate was at steady-state. As is evident from Appendix F, during a series of runs, for example, runs 1 to 14, the indicated millivolts and power input into the guarded hot plate varied. The temperatures of all the plates varied due to the varying power input. Since two stage voltage regulation was used (a.c. regulator followed by a d.c. regulator), no further improvements to the power supply circuit could be made. The process error due to electrical power supply was minimised by taking readings every hour and consequently allowing the guarded hot plate to come to new equilibrium temperatures. The thermal conductivities and conductances were evaluated at these new equilibrium temperatures.

An estimate of the process error is given by the 'probable error' of the mean of the millivolt readings. Consider for example run 549:

For thermocouple wires 1 to 9:

$$\text{mean} = 1.733\text{mV}$$

$$\text{standard deviation} = 0.001$$

$$\text{hence probable error} = \frac{0.001}{\sqrt{9}}$$

$$= 0.00033$$

$$\text{As a percentage of the mean} = 0.00033 \times 100/1.733$$

$$= \underline{0.02\%}$$

This is so small that it can be ignored.

G2 MEASUREMENT ERRORS

G2.1 PLATES

The plates were machined to within $\pm 0.03\text{mm}$.

Considering plate 5 (11mm thick perspex), the error due to its non-flatness is estimated as:

$$\frac{0.03}{11.15} \times 100$$

$$= 0.3\%$$

For the aluminium hot and cold plates, the errors are:

$$\frac{0.03\text{mm}}{6.35\text{mm}} \times 100 = \underline{0.5\%} \text{ (for each)}$$

G2.2 TEMPERATURES

The uncertainties in the temperatures indicated by the thermocouple wires are discussed in Chapters 1 and 2. The surface temperature uncertainty (from Chapter 1) =

$$\frac{0.02^{\circ}\text{C}}{45.14^{\circ}\text{C}} \times 100$$

$$= \underline{0.04\%}$$

The calibration uncertainty (0.04°C) in indicating the temperature of run 549 for example is:

$$\frac{0.04^{\circ}\text{C}}{47.66^{\circ}\text{C}} \times 100$$

$$= \underline{0.1\%}$$

The uncertainty due to the potentiometer = 0.1%.

G2.3 HEAT INPUT

The resolution of the current measuring digital multi-meter is 0.005%. The voltage measuring multimeter has the same resolution too. The uncertainty in product of the

voltage and the current is 0.01%.

G3 SYSTEMATIC ERRORS

The difference in the 'temperature-drops' across the specimens for any run is termed the 'systematic error' of the experiment. This is discussed in Chapter 2. Consider for example run 549:

The temperature drop across perspex plate 5 = 4.25°C
and the temperature drop across perspex plate 6 = 4.39°C

Estimate the systematic error for run 549 to be:

$$\frac{(4.39 - 4.25)}{(4.39 + 4.25)/2} \times 100 = 3\%$$

From the positioning experiments described in Chapter 2, runs II to VI use the same conditions applicable to experimental runs I to 738. (Run I used polystyrene insulation completely filling the stainless steel enclosure).

Using the above systematic error definition, the errors in runs II to VI (Chapter 2) were:

TABLE G1
Systematic Errors

Run	Systematic Error
II	9.5%
III	7.9%
IV	6.0%
V	3.5%
VI	3.8%

From Table G1, the systematic error chosen to take account of all the possible positionings of the apparatus in runs 1 to 738 is 10%.

G4 EXPERIMENTAL ERROR

The experimental error is the sum of the process, measurement, and systematic errors.

Sum of process errors = 0.04%

Sum of measurement errors = 1.8%

The systematic error = 10%

Hence the experimental error = 12%

APPENDIX HNUMERICAL SIMULATION RESULTS

H1	<u>NODAL-POINT TEMPERATURES</u>	437
H2	<u>HEAT FLUX PROFILE</u>	458
H3	<u>CONDUCTANCES OF RUN 568A</u>	470

H1 NODAL-POINT TEMPERATURES

Tables H1 to H20 show the nodal-point temperatures of the numerical simulation runs described in Table 3-6 (Chapter 3), (with the emissivity of aluminium equal to 0.04). In each case, the decimal point is not shown, for example, in run 159, the hot boundary temperature is 52.324°C in Table H1.

Temperature Profile of Simulation Run 159

[illegible]

TABLE H2

Temperature Profile of Simulation Run 172

[illegible]

TABLE H3

Temperature Profile of Simulation Run 186

[illegible]

TABLE H4

Temperature Profile of Simulation Run 201

[illegible]

TABLE H5

Temperature Profile of Simulation Run 315

[illegible]

TABLE H6

Temperature Profile of Simulation Run 331

[illegible]

TABLE H7

Temperature Profile of Simulation Run 341

[illegible]

TABLE 148

Temperature Profile of Simulation Run 549

[illegible]

TABLE H9

Temperature Profile of Simulation Run 556

[illegible]

TABLE H10

Temperature Profile of Simulation Run 568

[illegible]

Temperature Profile of Simulation Run 576

448

Temperature Profile of Simulation Run 605

449

TABLE H13

Temperature Profile of Simulation Run 611

[illegible]

1. 2. 3. 4. 5. 6. 7. 8. 9. 10. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. 101. 102. 103. 104. 105. 106. 107. 108. 109. 110. 111. 112. 113. 114. 115. 116. 117. 118. 119. 120. 121. 122. 123. 124. 125. 126. 127. 128. 129. 130. 131. 132. 133. 134. 135. 136. 137. 138. 139. 140. 141. 142. 143. 144. 145. 146. 147. 148. 149. 150. 151. 152. 153. 154. 155. 156. 157. 158. 159. 160. 161. 162. 163. 164. 165. 166. 167. 168. 169. 170. 171. 172. 173. 174. 175. 176. 177. 178. 179. 180. 181. 182. 183. 184. 185. 186. 187. 188. 189. 190. 191. 192. 193. 194. 195. 196. 197. 198. 199. 200. 201. 202. 203. 204. 205. 206. 207. 208. 209. 210. 211. 212. 213. 214. 215. 216. 217. 218. 219. 220. 221. 222. 223. 224. 225. 226. 227. 228. 229. 230. 231. 232. 233. 234. 235. 236. 237. 238. 239. 240. 241. 242. 243. 244. 245. 246. 247. 248. 249. 250. 251. 252. 253. 254. 255. 256. 257. 258. 259. 260. 261. 262. 263. 264. 265. 266. 267. 268. 269. 270. 271. 272. 273. 274. 275. 276. 277. 278. 279. 280. 281. 282. 283. 284. 285. 286. 287. 288. 289. 290. 291. 292. 293. 294. 295. 296. 297. 298. 299. 300. 301. 302. 303. 304. 305. 306. 307. 308. 309. 310. 311. 312. 313. 314. 315. 316. 317. 318. 319. 320. 321. 322. 323. 324. 325. 326. 327. 328. 329. 330. 331. 332. 333. 334. 335. 336. 337. 338. 339. 340. 341. 342. 343. 344. 345. 346. 347. 348. 349. 350. 351. 352. 353. 354. 355. 356. 357. 358. 359. 360. 361. 362. 363. 364. 365. 366. 367. 368. 369. 370. 371. 372. 373. 374. 375. 376. 377. 378. 379. 380. 381. 382. 383. 384. 385. 386. 387. 388. 389. 390. 391. 392. 393. 394. 395. 396. 397. 398. 399. 400. 401. 402. 403. 404. 405. 406. 407. 408. 409. 410. 411. 412. 413. 414. 415. 416. 417. 418. 419. 420. 421. 422. 423. 424. 425. 426. 427. 428. 429. 430. 431. 432. 433. 434. 435. 436. 437. 438. 439. 440. 441. 442. 443. 444. 445. 446. 447. 448. 449. 450. 451. 452. 453. 454. 455. 456. 457. 458. 459. 460. 461. 462. 463. 464. 465. 466. 467. 468. 469. 470. 471. 472. 473. 474. 475. 476. 477. 478. 479. 480. 481. 482. 483. 484. 485. 486. 487. 488. 489. 490. 491. 492. 493. 494. 495. 496. 497. 498. 499. 500. 501. 502. 503. 504. 505. 506. 507. 508. 509. 510. 511. 512. 513. 514. 515. 516. 517. 518. 519. 520. 521. 522. 523. 524. 525. 526. 527. 528. 529. 530. 531. 532. 533. 534. 535. 536. 537. 538. 539. 540. 541. 542. 543. 544. 545. 546. 547. 548. 549. 550. 551. 552. 553. 554. 555. 556. 557. 558. 559. 560. 561. 562. 563. 564. 565. 566. 567. 568. 569. 570. 571. 572. 573. 574. 575. 576. 577. 578. 579. 580. 581. 582. 583. 584. 585. 586. 587. 588. 589. 590. 591. 592. 593. 594. 595. 596. 597. 598. 599. 600. 601. 602. 603. 604. 605. 606. 607. 608. 609. 610. 611. 612. 613. 614. 615. 616. 617. 618. 619. 620. 621. 622. 623. 624. 625. 626. 627. 628. 629. 630. 631. 632. 633. 634. 635. 636. 637. 638. 639. 640. 641. 642. 643. 644. 645. 646. 647. 648. 649. 650. 651. 652. 653. 654. 655. 656. 657. 658. 659. 660. 661. 662. 663. 664. 665. 666. 667. 668. 669. 670. 671. 672. 673. 674. 675. 676. 677. 678. 679. 680. 681. 682. 683. 684. 685. 686. 687. 688. 689. 690. 691. 692. 693. 694. 695. 696. 697. 698. 699. 700. 701. 702. 703. 704. 705. 706. 707. 708. 709. 710. 711. 712. 713. 714. 715. 716. 717. 718. 719. 720. 721. 722. 723. 724. 725. 726. 727. 728. 729. 730. 731. 732. 733. 734. 735. 736. 737. 738. 739. 740. 741. 742. 743. 744. 745. 746. 747. 748. 749. 750. 751. 752. 753. 754. 755. 756. 757. 758. 759. 760. 761. 762. 763. 764. 765. 766. 767. 768. 769. 770. 771. 772. 773. 774. 775. 776. 777. 778. 779. 780. 781. 782. 783. 784. 785. 786. 787. 788. 789. 790. 791. 792. 793. 794. 795. 796. 797. 798. 799. 800. 801. 802. 803. 804. 805. 806. 807. 808. 809. 810. 811. 812. 813. 814. 815. 816. 817. 818. 819. 820. 821. 822. 823. 824. 825. 826. 827. 828. 829. 830. 831. 832. 833. 834. 835. 836. 837. 838. 839. 840.

[illegible]

TABLE H16

Temperature Profile of Simulation Run 629

[illegible]

Temperature Profile of Simulation Run 679

[illegible]

TABLE H18

Temperature Profile of Simulation Run 686

[illegible]

Temperature Profile of Simulation Run 692

[illegible]

Temperature Profile of Simulation Run 698

[illegible]

H2 HEAT FLUX PROFILE

Table H21 shows the heat flows between nodal points (results of run 568A - 11mm thick perspex with the aluminium emissivity equal to 0.04).

Tables H23 and H24 show the corresponding radiation flows.

Table H22 shows the values of dQ_r/dT for the surface points.

TABLE H21 - Heat Flows (W) - Run 568A

| PT NO | QYX(K) | QYX(K+126) | QXY(K-1) | QXY(K) | QZX(K-14) | QZX(K) | TOTAL HEAT FLOW | % ERROR |
|-------|--------------------------------|----------------------------|--------------------|--|----------------------------|------------|-----------------|---------|
| 146 | -.8679E-03
HEAT INTO POINT= | -.8337E-03
-.901114E-03 | -.2716E-04
HEAT | -.1424E-04
CONDUCTED AWAY FROM POINT= | -.4024E-04
-.901120E-03 | -.1897E-04 | .5439E-06 | 0.001 |
| 147 | -.3337E-03
HEAT INTO POINT= | -.3322E-03
-.346437E-03 | -.1424E-04
HEAT | 0.
CONDUCTED AWAY FROM POINT= | 0.
-.346440E-03 | -.7720E-05 | .3521E-06 | 0.001 |
| 159 | -.7049E-03
HEAT INTO POINT= | -.6724E-03
-.753036E-03 | -.2836E-04
HEAT | -.1111E-04
CONDUCTED AWAY FROM POINT= | -.5231E-04
-.753044E-03 | -.3701E-04 | .6010E-06 | 0.001 |
| 160 | -.5943E-03
HEAT INTO POINT= | -.5818E-03
-.611886E-03 | -.1111E-04
HEAT | -.5127E-05
CONDUCTED AWAY FROM POINT= | -.1697E-04
-.611893E-03 | -.1246E-04 | .7626E-06 | 0.001 |
| 161 | -.4653E-03
HEAT INTO POINT= | -.4603E-03
-.473116E-03 | -.5127E-05
HEAT | -.2924E-05
CONDUCTED AWAY FROM POINT= | -.7720E-05
-.473125E-03 | -.4895E-05 | .8535E-06 | 0.002 |
| 162 | -.1600E-03
HEAT INTO POINT= | -.1590E-03
-.161903E-03 | -.2924E-05
HEAT | 0.
CONDUCTED AWAY FROM POINT= | 0.
-.161907E-03 | -.1920E-05 | .4619E-06 | 0.003 |
| 172 | -.4035E-03
HEAT INTO POINT= | -.3757E-03
-.506353E-03 | -.7326E-05
HEAT | -.6743E-05
CONDUCTED AWAY FROM POINT= | -.1234E-05
-.506364E-03 | -.9409E-04 | .1691E-07 | 0.002 |
| 173 | -.5124E-03
HEAT INTO POINT= | -.4969E-03
-.542686E-03 | -.8743E-05
HEAT | -.3696E-05
CONDUCTED AWAY FROM POINT= | -.3701E-04
-.542706E-03 | -.2656E-04 | .1423E-07 | 0.003 |
| 174 | -.3024E-03
HEAT INTO POINT= | -.2980E-03
-.314173E-03 | -.3696E-05
HEAT | -.1826E-05
CONDUCTED AWAY FROM POINT= | -.1248E-04
-.314190E-03 | -.1001E-04 | .1685E-07 | 0.005 |
| 175 | -.2370E-03
HEAT INTO POINT= | -.2352E-03
-.241925E-03 | -.1826E-05
HEAT | -.1035E-05
CONDUCTED AWAY FROM POINT= | -.4695E-05
-.241943E-03 | -.3926E-05 | .1755E-07 | 0.007 |
| 176 | -.1630E-03
HEAT INTO POINT= | -.1623E-03
-.165256E-03 | -.1035E-05
HEAT | -.6686E-06
CONDUCTED AWAY FROM POINT= | -.1920E-05
-.165273E-03 | -.1559E-05 | .1549E-07 | 0.009 |
| 177 | -.4155E-04
HEAT INTO POINT= | -.4142E-04
-.421075E-04 | -.6886E-06
HEAT | 0.
CONDUCTED AWAY FROM POINT= | 0.
-.421143E-04 | -.5643E-06 | .6991E-08 | 0.017 |
| 185 | -.7567E-03
HEAT INTO POINT= | -.6895E-03
-.852057E-03 | .4274E-05
HEAT | -.1045E-04
CONDUCTED AWAY FROM POINT= | -.1668E-05
-.852057E-03 | -.8494E-04 | -.4182E-09 | -0.000 |
| 186 | -.7045E-03 | -.6633E-03 | -.1045E-04 | -.1267E-04 | -.9409E-04 | -.5067E-04 | -.8313E-09 | -0.000 |

TABLE H21 (continued)

| | HEAT INTO POINT= -.767866E-03 | | HEAT CONDUCTED AWAY FROM POINT= -.767867E-03 | | | |
|-----|---|------------|--|--------------------------|--------------------------|--------|
| 187 | -.6259E-03
HEAT INTO POINT= -.648570E-03 | -.6093E-03 | -.1267E-04
HEAT CONDUCTED AWAY FROM POINT= -.648569E-03 | -.5706E-05
-.2656E-04 | -.1697E-04
-.8112E-09 | -0.000 |
| 188 | -.5297E-03
HEAT INTO POINT= -.538696E-03 | -.5230E-03 | -.5706E-05
HEAT CONDUCTED AWAY FROM POINT= -.538695E-03 | -.2826E-05
-.1001E-04 | -.6201E-05
-.5404E-09 | -0.000 |
| 189 | -.4152E-03
HEAT INTO POINT= -.419257E-03 | -.4125E-03 | -.2826E-05
HEAT CONDUCTED AWAY FROM POINT= -.419257E-03 | -.1602E-05
-.3926E-05 | -.2411E-05
.3252E-09 | 0.000 |
| 190 | -.2857E-03
HEAT INTO POINT= -.287752E-03 | -.2846E-03 | -.1602E-05
HEAT CONDUCTED AWAY FROM POINT= -.287755E-03 | -.1071E-05
-.1559E-05 | -.9696E-06
.2341E-06 | 0.001 |
| 191 | -.1456E-03
HEAT INTO POINT= -.146835E-03 | -.1452E-03 | -.1071E-05
HEAT CONDUCTED AWAY FROM POINT= -.146846E-03 | -.8810E-06
-.5643E-06 | -.3563E-06
.1663E-07 | 0.007 |
| 192 | -.1276E-03
HEAT INTO POINT= -.128153E-03 | -.1273E-03 | -.8810E-06
HEAT CONDUCTED AWAY FROM POINT= -.128152E-03 | 0.
0. | -.5616E-06
-.1566E-06 | -0.001 |
| 198 | -.6467E-03
HEAT INTO POINT= -.659041E-03 | -.6241E-03 | 0.
HEAT CONDUCTED AWAY FROM POINT= -.659042E-03 | -.1607E-05
-.3496E-04 | -.1395E-04
.7074E-09 | 0.000 |
| 199 | -.1270E-02
HEAT INTO POINT= -.130777E-02 | -.1224E-02 | -.1607E-05
HEAT CONDUCTED AWAY FROM POINT= -.130777E-02 | -.6580E-05
-.8494E-04 | -.3126E-04
.1306E-06 | 0.000 |
| 200 | -.1191E-02
HEAT INTO POINT= -.121894E-02 | -.1162E-02 | -.6580E-05
HEAT CONDUCTED AWAY FROM POINT= -.121895E-02 | -.8370E-05
-.5067E-04 | -.1960E-04
.1918E-06 | 0.000 |
| 201 | -.1066E-02
HEAT INTO POINT= -.107860E-02 | -.1053E-02 | -.8370E-05
HEAT CONDUCTED AWAY FROM POINT= -.107860E-02 | -.4632E-05
-.1697E-04 | -.7535E-05
.2781E-06 | 0.000 |
| 202 | -.9049E-03
HEAT INTO POINT= -.910184E-03 | -.8994E-03 | -.4632E-05
HEAT CONDUCTED AWAY FROM POINT= -.910186E-03 | -.2458E-05
-.6201E-05 | -.2801E-05
.3847E-08 | 0.000 |
| 203 | -.7100E-03
HEAT INTO POINT= -.712520E-03 | -.7077E-03 | -.2458E-05
HEAT CONDUCTED AWAY FROM POINT= -.712525E-03 | -.1437E-05
-.2411E-05 | -.1082E-05
.5103E-06 | 0.001 |
| 204 | -.4889E-03
HEAT INTO POINT= -.490275E-03 | -.4879E-03 | -.1437E-05
HEAT CONDUCTED AWAY FROM POINT= -.490282E-03 | -.1001E-05
-.9696E-06 | -.4256E-06
.7635E-06 | 0.001 |
| 205 | -.2492E-03
HEAT INTO POINT= -.250162E-03 | -.2488E-03 | -.1001E-05
HEAT CONDUCTED AWAY FROM POINT= -.250179E-03 | -.8689E-06
-.3563E-06 | -.1454E-06
.1684E-07 | 0.007 |
| 206 | -.4367E-03
HEAT INTO POINT= -.437599E-03 | -.4362E-03 | -.8689E-06
HEAT CONDUCTED AWAY FROM POINT= -.437596E-03 | -.8582E-06
-.5616E-06 | -.2160E-06
.1723E-06 | 0.000 |

TABLE H21 (continued)

| | | | | | | | | |
|-----|--------------------------------|----------------------------|------------------|---|----------------------------|------------|------------|--------|
| 207 | -.3738E-03
HEAT INTO POINT= | -.3735E-03
-.374111E-03 | -.6582E-06
0. | 0.
HEAT CONDUCTED AWAY FROM POINT= | -.374112E-03 | -.3267E-06 | .9269E-09 | 0.000 |
| 212 | -.6425E-03
HEAT INTO POINT= | -.6320E-03
-.645961E-03 | 0. | .2442E-06
HEAT CONDUCTED AWAY FROM POINT= | -.1395E-04
-.645962E-03 | -.3686E-05 | .6304E-09 | 0.000 |
| 213 | -.1261E-02
HEAT INTO POINT= | -.1240E-02
-.127127E-02 | .2442E-06 | -.2783E-05
HEAT CONDUCTED AWAY FROM POINT= | -.3126E-04
-.127127E-02 | -.7930E-05 | .1166E-08 | 0.000 |
| 214 | -.1185E-02
HEAT INTO POINT= | -.1171E-02
-.119367E-02 | -.2783E-05 | -.3670E-05
HEAT CONDUCTED AWAY FROM POINT= | -.1960E-04
-.119368E-02 | -.5108E-05 | .1717E-08 | 0.000 |
| 215 | -.1064E-02
HEAT INTO POINT= | -.1057E-02
-.106866E-02 | -.3670E-05 | -.2381E-05
HEAT CONDUCTED AWAY FROM POINT= | -.7535E-05
-.106866E-02 | -.2105E-05 | .2490E-08 | 0.000 |
| 216 | -.9041E-03
HEAT INTO POINT= | -.9011E-03
-.906261E-03 | -.2381E-05 | -.1376E-05
HEAT CONDUCTED AWAY FROM POINT= | -.2601E-05
-.906265E-03 | -.7909E-06 | .3439E-08 | 0.000 |
| 217 | -.7097E-03
HEAT INTO POINT= | -.7094E-03
-.710818E-03 | -.1376E-05 | -.8325E-06
HEAT CONDUCTED AWAY FROM POINT= | -.1082E-05
-.710823E-03 | -.3086E-06 | .4534E-08 | 0.001 |
| 218 | -.4887E-03
HEAT INTO POINT= | -.4882E-03
-.489410E-03 | -.6325E-06 | -.5704E-06
HEAT CONDUCTED AWAY FROM POINT= | -.4256E-06
-.489416E-03 | -.1185E-06 | .6195E-08 | 0.001 |
| 219 | -.2491E-03
HEAT INTO POINT= | -.2489E-03
-.249617E-03 | -.5704E-06 | -.4730E-06
HEAT CONDUCTED AWAY FROM POINT= | -.1454E-06
-.249632E-03 | -.3778E-07 | .1401E-07 | 0.006 |
| 220 | -.4367E-03
HEAT INTO POINT= | -.4363E-03
-.436997E-03 | -.4730E-06 | -.2801E-06
HEAT CONDUCTED AWAY FROM POINT= | -.2160E-06
-.436997E-03 | -.5312E-07 | -.6944E-09 | -0.000 |
| 221 | -.7475E-03
HEAT INTO POINT= | -.7471E-03
-.747695E-03 | -.2861E-06 | -.1651E-06
HEAT CONDUCTED AWAY FROM POINT= | -.3267E-06
-.747698E-03 | -.7943E-07 | .2953E-08 | 0.000 |
| 222 | -.3737E-03
HEAT INTO POINT= | -.3736E-03
-.373759E-03 | -.1651E-06 | 0.
HEAT CONDUCTED AWAY FROM POINT= | 0.
-.373760E-03 | -.4921E-07 | .1324E-08 | 0.000 |
| 226 | -.3207E-03
HEAT INTO POINT= | -.3170E-03
-.320708E-03 | 0. | -.1686E-09
HEAT CONDUCTED AWAY FROM POINT= | -.3686E-05
-.320708E-03 | 0. | .9196E-10 | 0.000 |
| 227 | -.6291E-03
HEAT INTO POINT= | -.6221E-03
-.630034E-03 | -.1686E-09 | -.9363E-06
HEAT CONDUCTED AWAY FROM POINT= | -.7930E-05
-.630034E-03 | 0. | .6935E-10 | 0.000 |
| 228 | -.5918E-03
HEAT INTO POINT= | -.5870E-03
-.593039E-03 | -.9363E-06 | -.1255E-05
HEAT CONDUCTED AWAY FROM POINT= | -.5108E-05
-.593039E-03 | 0. | .1437E-09 | 0.000 |
| 229 | -.5318E-03 | -.5293E-03 | -.1255E-05 | -.8815E-06 | -.2105E-05 | 0. | .2793E-09 | 0.000 |

TABLE H21 (continued)

| | HEAT INTO POINT= | HEAT INTO POINT= | HEAT CONDUCTED AWAY FROM POINT= | | | |
|-----|--------------------------------|----------------------------|---|--|------------------------|--------|
| | -.532663E-03 | | -.532663E-03 | | | |
| 230 | -.4519E-03
HEAT INTO POINT= | -.4508E-03
-.452467E-03 | -.5815E-06
HEAT CONDUCTED AWAY FROM POINT= | -.5337E-06
-.7989E-06
-.452466E-03 | 0.
.5330E-09 | 0.000 |
| 231 | -.3549E-03
HEAT INTO POINT= | -.3544E-03
-.355212E-03 | -.5337E-06
HEAT CONDUCTED AWAY FROM POINT= | -.3274E-06
-.3086E-06
-.355213E-03 | 0.
.9992E-09 | 0.000 |
| 232 | -.2443E-03
HEAT INTO POINT= | -.2441E-03
-.244561E-03 | -.3274E-06
HEAT CONDUCTED AWAY FROM POINT= | -.2171E-06
-.1185E-06
-.244563E-03 | 0.
.1946E-08 | 0.001 |
| 233 | -.1246E-03
HEAT INTO POINT= | -.1245E-03
-.124716E-03 | -.2171E-06
HEAT CONDUCTED AWAY FROM POINT= | -.1699E-06
-.3778E-07
-.124725E-03 | 0.
.6299E-08 | 0.005 |
| 234 | -.1246E-03
HEAT INTO POINT= | -.1245E-03
-.124690E-03 | -.1699E-06
HEAT CONDUCTED AWAY FROM POINT= | -.1373E-06
-.5312E-07
-.124699E-03 | 0.
-.1243E-08 | -0.001 |
| 235 | -.3737E-03
HEAT INTO POINT= | -.3736E-03
-.373791E-03 | -.1373E-06
HEAT CONDUCTED AWAY FROM POINT= | -.6742E-07
-.7943E-07
-.373791E-03 | 0.
.2255E-09 | 0.000 |
| 236 | -.3737E-03
HEAT INTO POINT= | -.3736E-03
-.373724E-03 | -.6742E-07
HEAT CONDUCTED AWAY FROM POINT= | -.2028E-07
-.4921E-07
-.373724E-03 | 0.
.2541E-09 | 0.000 |
| 237 | -.9342E-04
HEAT INTO POINT= | -.9340E-04
-.934246E-04 | -.2028E-07
HEAT CONDUCTED AWAY FROM POINT= | 0.
0.
-.934244E-04 | 0.
-.1581E-09 | -0.000 |
| 272 | -.8337E-03
HEAT INTO POINT= | -.8695E-03
-.793498E-03 | .2833E-04
HEAT CONDUCTED AWAY FROM POINT= | .1626E-04
.4765E-04
-.793502E-03 | .2390E-04
.4233E-08 | 0.001 |
| 273 | -.3322E-03
HEAT INTO POINT= | -.3340E-03
-.322765E-03 | .1626E-04
HEAT CONDUCTED AWAY FROM POINT= | 0.
0.
-.322768E-03 | .9433E-05
.2891E-08 | 0.001 |
| 285 | -.6724E-03
HEAT INTO POINT= | -.7042E-03
-.620871E-03 | .1561E-04
HEAT CONDUCTED AWAY FROM POINT= | .9425E-05
.6773E-04
-.620876E-03 | .4206E-04
.5044E-08 | 0.001 |
| 286 | -.5818E-03
HEAT INTO POINT= | -.5945E-03
-.561163E-03 | .9425E-05
HEAT CONDUCTED AWAY FROM POINT= | .5157E-05
.2390E-04
-.561169E-03 | .1548E-04
.6498E-08 | 0.001 |
| 287 | -.4603E-03
HEAT INTO POINT= | -.4655E-03
-.450862E-03 | .5157E-05
HEAT CONDUCTED AWAY FROM POINT= | .3304E-05
.9433E-05
-.450869E-03 | .6096E-05
.7366E-08 | 0.002 |
| 288 | -.1590E-03
HEAT INTO POINT= | -.1600E-03
-.156703E-03 | .3304E-05
HEAT CONDUCTED AWAY FROM POINT= | 0.
0.
-.156707E-03 | .2272E-05
.4077E-08 | 0.003 |
| 298 | -.3757E-03
HEAT INTO POINT= | -.3999E-03
-.300071E-03 | .5255E-05
HEAT CONDUCTED AWAY FROM POINT= | .4631E-05
.9457E-04
-.300081E-03 | .7045E-04
.9977E-08 | 0.003 |

TABLE H21 (continued)

| | | | | | |
|-----|---|---|-----------|------------|--------|
| 499 | -.8969E-03
HEAT INTO POINT= -.5116E-03
-.464873E-03 | .4631E-05
HEAT CONDUCTED AWAY FROM POINT= .2703E-05
.4206E-04
-.464686E-03 | .2935E-04 | .1294E-07 | 0.003 |
| 400 | -.2980E-03
HEAT INTO POINT= -.3023E-03
-.284132E-03 | .2703E-05
HEAT CONDUCTED AWAY FROM POINT= .1656E-05
.1548E-04
-.284148E-03 | .1220E-04 | .1550E-07 | 0.005 |
| 301 | -.2352E-03
HEAT INTO POINT= -.2370E-03
-.229244E-03 | .1656E-05
HEAT CONDUCTED AWAY FROM POINT= .1080E-05
.6096E-05
-.229260E-03 | .4665E-05 | .1617E-07 | 0.007 |
| 302 | -.1623E-03
HEAT INTO POINT= -.1630E-03
-.159678E-03 | .1080E-05
HEAT CONDUCTED AWAY FROM POINT= .7649E-06
.2272E-05
-.159692E-03 | .1845E-05 | .1429E-07 | 0.009 |
| 303 | -.4142E-04
HEAT INTO POINT= -.4155E-04
-.407640E-04 | .7649E-06
HEAT CONDUCTED AWAY FROM POINT= 0.
0.
-.407905E-04 | .6282E-06 | .6505E-06 | 0.016 |
| 311 | -.6895E-03
HEAT INTO POINT= -.7481E-03
-.620395E-03 | .2398E-05
HEAT CONDUCTED AWAY FROM POINT= .7423E-05
.1253E-05
-.620394E-03 | .6172E-04 | -.6100E-09 | -0.000 |
| 312 | -.6633E-03
HEAT INTO POINT= -.6988E-03
-.620471E-03 | .7423E-05
HEAT CONDUCTED AWAY FROM POINT= .6539E-05
.7095E-04
-.620470E-03 | .3632E-04 | -.1136E-08 | -0.000 |
| 313 | -.6093E-03
HEAT INTO POINT= -.6247E-03
-.588839E-03 | .6539E-05
HEAT CONDUCTED AWAY FROM POINT= .3955E-05
.2935E-04
-.588837E-03 | .1655E-04 | -.1242E-06 | -0.000 |
| 314 | -.5230E-03
HEAT INTO POINT= -.5245E-03
-.513365E-03 | .3955E-05
HEAT CONDUCTED AWAY FROM POINT= .2454E-05
.1220E-04
-.513363E-03 | .7166E-05 | -.1084E-06 | -0.000 |
| 315 | -.4125E-03
HEAT INTO POINT= -.4152E-03
-.407924E-03 | .2454E-05
HEAT CONDUCTED AWAY FROM POINT= .1613E-05
.4665E-05
-.407924E-03 | .2968E-05 | -.2785E-09 | -0.000 |
| 316 | -.2646E-03
HEAT INTO POINT= -.2857E-03
-.282253E-03 | .1613E-05
HEAT CONDUCTED AWAY FROM POINT= .1156E-05
.1845E-05
-.282255E-03 | .1161E-05 | .1730E-08 | 0.001 |
| 317 | -.1452E-03
HEAT INTO POINT= -.1456E-03
-.143819E-03 | .1156E-05
HEAT CONDUCTED AWAY FROM POINT= .9546E-06
.6282E-06
-.143829E-03 | .4171E-06 | .9757E-08 | 0.007 |
| 318 | -.1273E-03
HEAT INTO POINT= -.1276E-03
-.126829E-03 | .9546E-06
HEAT CONDUCTED AWAY FROM POINT= 0.
0.
-.126828E-03 | .6447E-06 | -.1685E-06 | -0.001 |
| 324 | -.6241E-03
HEAT INTO POINT= -.6443E-03
-.609669E-03 | 0.
HEAT CONDUCTED AWAY FROM POINT= .1907E-05
.3467E-04
-.609670E-03 | .1251E-04 | .5368E-09 | 0.000 |
| 325 | -.1224E-02
HEAT INTO POINT= -.1262E-02
-.119865E-02 | .1907E-05
HEAT CONDUCTED AWAY FROM POINT= .4296E-05
.6172E-04
-.119865E-02 | .2149E-04 | .8979E-09 | 0.000 |
| 326 | -.1162E-02
-.1186E-02 | .4296E-05
.3692E-05
.3632E-04 | .1307E-04 | .1311E-08 | 0.000 |

TABLE H21 (continued)

| | HEAT INTO POINT= | HEAT CONDUCTED AWAY FROM POINT= | | | | | |
|-----|---|---------------------------------|--|-----------|-----------|-----------|-----------|
| 327 | -.1053E-02
HEAT INTO POINT= -.104432E-02 | -.1065E-02 | .3692E-05
HEAT CONDUCTED AWAY FROM POINT= | .2457E-05 | .1655E-04 | .6477E-05 | .1966E-08 |
| 328 | -.9994E-03
HEAT INTO POINT= -.894762E-03 | -.9044E-03 | .2457E-05
HEAT CONDUCTED AWAY FROM POINT= | .1627E-05 | .7106E-05 | .2960E-05 | .2838E-08 |
| 329 | -.7077E-03
HEAT INTO POINT= -.705240E-03 | -.7090E-03 | .1627E-05
HEAT CONDUCTED AWAY FROM POINT= | .1129E-05 | .2968E-05 | .1279E-05 | .3999E-08 |
| 330 | -.4879E-03
HEAT INTO POINT= -.486477E-03 | -.4888E-03 | .1129E-05
HEAT CONDUCTED AWAY FROM POINT= | .8647E-06 | .1181E-05 | .5205E-06 | .5972E-08 |
| 331 | -.2488E-03
HEAT INTO POINT= -.247855E-03 | -.2491E-03 | .8647E-06
HEAT CONDUCTED AWAY FROM POINT= | .7558E-06 | .4171E-06 | .1763E-06 | .1552E-07 |
| 332 | -.4362E-03
HEAT INTO POINT= -.435276E-03 | -.4367E-03 | .7558E-06
HEAT CONDUCTED AWAY FROM POINT= | .6221E-06 | .6447E-06 | .2652E-06 | .1637E-08 |
| 333 | -.3735E-03
HEAT INTO POINT= -.373126E-03 | -.3737E-03 | .6221E-06
HEAT CONDUCTED AWAY FROM POINT= | 0. | 0. | .3259E-06 | .4360E-09 |
| 338 | -.6320E-03
HEAT INTO POINT= -.628085E-03 | -.6406E-03 | 0.
HEAT CONDUCTED AWAY FROM POINT= | .8429E-06 | .1251E-04 | .3085E-05 | .4752E-09 |
| 339 | -.1240E-02
HEAT INTO POINT= -.123351E-02 | -.1256E-02 | .8429E-06
HEAT CONDUCTED AWAY FROM POINT= | .1531E-05 | .2149E-04 | .5210E-05 | .8087E-09 |
| 340 | -.1171E-02
HEAT INTO POINT= -.116703E-02 | -.1182E-02 | .1531E-05
HEAT CONDUCTED AWAY FROM POINT= | .1234E-05 | .1307E-04 | .3226E-05 | .1206E-08 |
| 341 | -.1057E-02
HEAT INTO POINT= -.105491E-02 | -.1063E-02 | .1234E-05
HEAT CONDUCTED AWAY FROM POINT= | .8670E-06 | .6477E-05 | .1673E-05 | .1797E-08 |
| 342 | -.9011E-03
HEAT INTO POINT= -.899670E-03 | -.9035E-03 | .8670E-06
HEAT CONDUCTED AWAY FROM POINT= | .6145E-06 | .2960E-05 | .7917E-06 | .2577E-08 |
| 343 | -.7084E-03
HEAT INTO POINT= -.707556E-03 | -.7095E-03 | .6145E-06
HEAT CONDUCTED AWAY FROM POINT= | .4472E-06 | .1279E-05 | .3506E-06 | .3585E-08 |
| 344 | -.4882E-03
HEAT INTO POINT= -.487663E-03 | -.4886E-03 | .4472E-06
HEAT CONDUCTED AWAY FROM POINT= | .3402E-06 | .5205E-06 | .1436E-06 | .5274E-08 |
| 345 | -.2499E-03
HEAT INTO POINT= -.248565E-03 | -.2491E-03 | .3402E-06
HEAT CONDUCTED AWAY FROM POINT= | .2752E-06 | .1763E-06 | .4814E-07 | .1347E-07 |

TABLE H21 (continued)

| | | | | | | | | |
|---|---|----------------------------|--|---------------------------|---------------------------|-----------|------------|--------|
| 346 | -.4393E-03
HEAT INTO POINT= -.4386E-03 | -.4386E-03
-.438656E-03 | .2752E-06
HEAT CONDUCTED AWAY FROM POINT= | .1828E-06
-.438655E-03 | .2652E-06
-.438655E-03 | .7095E-07 | -.1167E-08 | -0.000 |
| 347 | -.7471E-03
HEAT INTO POINT= -.746872E-03 | -.7474E-03
-.746872E-03 | .1828E-06
HEAT CONDUCTED AWAY FROM POINT= | .1264E-06
-.746874E-03 | .3259E-06
-.746874E-03 | .8199E-07 | .2062E-08 | 0.000 |
| 348 | -.3736E-03
HEAT INTO POINT= -.373554E-03 | -.3737E-03
-.373554E-03 | .1264E-06
HEAT CONDUCTED AWAY FROM POINT= | 0.
-.373555E-03 | 0.
-.373555E-03 | .3893E-07 | .9428E-09 | 0.000 |
| 352 | -.3170E-03
HEAT INTO POINT= -.316748E-03 | -.3198E-03
-.316748E-03 | 0.
HEAT CONDUCTED AWAY FROM POINT= | .2743E-06
-.316748E-03 | .3085E-06
-.316748E-03 | 0. | .2906E-10 | 0.000 |
| 353 | -.6221E-03
HEAT INTO POINT= -.621663E-03 | -.6271E-03
-.621663E-03 | .2743E-06
HEAT CONDUCTED AWAY FROM POINT= | .4411E-06
-.621663E-03 | .5210E-06
-.621663E-03 | 0. | -.6966E-10 | -0.000 |
| 354 | -.5870E-03
HEAT INTO POINT= -.586664E-03 | -.5903E-03
-.586664E-03 | .4411E-06
HEAT CONDUCTED AWAY FROM POINT= | .3308E-06
-.586664E-03 | .3226E-06
-.586664E-03 | 0. | -.5265E-10 | -0.000 |
| 355 | -.5293E-03
HEAT INTO POINT= -.529066E-03 | -.5311E-03
-.529066E-03 | .3308E-06
HEAT CONDUCTED AWAY FROM POINT= | .2366E-06
-.529066E-03 | .1673E-06
-.529066E-03 | 0. | .1195E-10 | 0.000 |
| 356 | -.4508E-03
HEAT INTO POINT= -.450611E-03 | -.4516E-03
-.450611E-03 | .2366E-06
HEAT CONDUCTED AWAY FROM POINT= | .1760E-06
-.450611E-03 | .7917E-06
-.450611E-03 | 0. | .1986E-09 | 0.000 |
| 357 | -.3544E-03
HEAT INTO POINT= -.354238E-03 | -.3548E-03
-.354238E-03 | .1760E-06
HEAT CONDUCTED AWAY FROM POINT= | .1311E-06
-.354238E-03 | .3506E-06
-.354238E-03 | 0. | .6257E-09 | 0.000 |
| 358 | -.2441E-03
HEAT INTO POINT= -.244019E-03 | -.2443E-03
-.244019E-03 | .1311E-06
HEAT CONDUCTED AWAY FROM POINT= | .9462E-07
-.244021E-03 | .1436E-06
-.244021E-03 | 0. | .1593E-08 | 0.001 |
| 359 | -.1245E-03
HEAT INTO POINT= -.124392E-03 | -.1245E-03
-.124392E-03 | .9462E-07
HEAT CONDUCTED AWAY FROM POINT= | .6621E-07
-.124397E-03 | .4014E-07
-.124397E-03 | 0. | .5797E-08 | 0.005 |
| 360 | -.1245E-03
HEAT INTO POINT= -.124397E-03 | -.1245E-03
-.124397E-03 | .6621E-07
HEAT CONDUCTED AWAY FROM POINT= | .7219E-07
-.124395E-03 | .7035E-07
-.124395E-03 | 0. | -.1308E-08 | -0.001 |
| 361 | -.3736E-03
HEAT INTO POINT= -.373533E-03 | -.3737E-03
-.373533E-03 | .7219E-07
HEAT CONDUCTED AWAY FROM POINT= | .4165E-07
-.373533E-03 | .8199E-07
-.373533E-03 | 0. | -.1153E-09 | -0.000 |
| 362 | -.3736E-03
HEAT INTO POINT= -.373594E-03 | -.3737E-03
-.373594E-03 | .4165E-07
HEAT CONDUCTED AWAY FROM POINT= | .1316E-07
-.373594E-03 | .3893E-07
-.373594E-03 | 0. | -.3845E-10 | -0.000 |
| 363 | -.9340E-04
HEAT INTO POINT= -.934045E-04 | -.9342E-04
-.934045E-04 | .1316E-07
HEAT CONDUCTED AWAY FROM POINT= | 0.
-.934043E-04 | 0.
-.934043E-04 | 0. | -.2131E-09 | -0.000 |
| QXY(131)= -.3151E-05 QRAD(1,3)= -.7250E-04 QYX(255)= -.3688E-03 HEATIN= -.4648E-03
QZX(132)= -.4029E-04 QYX(132)= -.4245E-03 HEATOUT= -.4648E-03 TURFLU= .2911E-08 HEAT BALANCE ERROR = 0.001 | | | | | | | | |

TABLE H21 (continued)

| | | | | |
|-------------------------|-----------------------|----------------------|---------------------|----------------------------|
| QXY(257)= .9439E-05 | QRAD(1,4)= .7575E-04 | QYX(384)= -.4263E-03 | HEATIN= -.3412E-03 | |
| QZX(258)= .4765E-04 | QYX(256)= -.3888E-03 | HEATOUT= -.3412E-03 | TOTFLC= .2342E-08 | HEAT BALANCE ERROR = 0.001 |
| QZX(131)= -.6249E-05 | QRAD(2,3)= -.3456E-03 | QYX(271)= -.7695E-03 | HEATIN= -.9413E-03 | |
| PT N0145QYX= -.8619E-03 | QXY= -.2716E-04 | QZX= -.5231E-04 | HEATOUT= -.9413E-03 | TOTFLO= .5666E-08 |
| QZX(257)= .1903E-04 | QRAD(2,4)= .1515E-03 | QYX(397)= -.8640E-03 | HEATIN= -.6934E-03 | ΔERROR= 0.001 |
| PT N0271QYX= -.7845E-03 | QXY= .2633E-04 | QZX= .6773E-04 | HEATOUT= -.6934E-03 | TOTFLO= .4605E-08 |
| QXY(157)= -.8431E-04 | QRAD(3,3)= -.1456E-03 | QYX(284)= -.6665E-03 | HEATIN= -.9024E-03 | ΔERROR= 0.001 |
| PT N0158QYX= -.7507E-03 | QXY= -.2836E-04 | QZX= -.1234E-03 | HEATOUT= -.9024E-03 | TOTFLO= .5490E-08 |
| QXY(283)= .3159E-04 | QRAD(3,4)= .1515E-03 | QYX(410)= -.7414E-03 | HEATIN= -.5583E-03 | ΔERROR= 0.001 |
| PT N0284QYX= -.6685E-03 | QXY= .1561E-04 | QZX= .9457E-04 | HEATOUT= -.5583E-03 | TOTFLO= .4666E-08 |
| QZX(157)= -.8843E-04 | QRAD(4,3)= -.1456E-03 | QYX(297)= -.5058E-03 | HEATIN= -.7399E-03 | ΔERROR= 0.001 |
| PT N0171QYX= -.5657E-03 | QXY= -.7326E-05 | QZX= -.1668E-03 | HEATOUT= -.7399E-03 | TOTFLO= .7828E-08 |
| QZX(283)= .3177E-04 | QRAD(4,4)= .1515E-03 | QYX(423)= -.5585E-03 | HEATIN= -.3752E-03 | ΔERROR= 0.001 |
| PT N0297QYX= -.5058E-03 | QXY= .5255E-05 | QZX= .1253E-03 | HEATOUT= -.3752E-03 | TOTFLO= .7101E-08 |
| QXY(183)= .9840E-06 | QRAD(5,3)= -.7280E-04 | QYX(310)= -.4597E-03 | HEATIN= -.5315E-03 | ΔERROR= 0.002 |
| PT N0184QYX= -.5009E-03 | QXY= .4278E-05 | QZX= -.3496E-04 | HEATOUT= -.5315E-03 | TOTFLO= .7463E-09 |
| QXY(309)= .5899E-06 | QRAD(5,4)= .7575E-04 | QYX(436)= -.4990E-03 | HEATIN= -.4227E-03 | ΔERROR= 0.000 |
| PT N0310QYX= -.4597E-03 | QXY= .2398E-05 | QZX= .3467E-04 | HEATOUT= -.4227E-03 | TOTFLO= .5993E-09 |
| QXY(128)= .1069E-05 | QYX(255)= -.2495E-03 | HEATIN= -.2485E-03 | | ΔERROR= 0.000 |
| PT N0129QYX= -.2967E-03 | QXY= .2366E-06 | QZX= .4802E-04 | HEATOUT= -.2485E-03 | TOTFLO= .3553E-14 |
| QXY(254)= .3825E-06 | QYX(381)= -.2780E-03 | HEATIN= -.2777E-03 | | ΔERROR= 0.000 |
| PT N0255QYX= -.2495E-03 | QXY= -.9006E-05 | QZX= -.1912E-04 | HEATOUT= -.2777E-03 | TOTFLO= .1776E-13 |

| REGION NUMBER | SUM OF QYX | SUM OF QYX | SUM OF QZX | SUM OF QY, QX AND QZ |
|---------------|--------------|--------------|--------------|----------------------|
| C2 | -.297138E-01 | -.184403E-03 | -.898165E-03 | .307963E-01 |
| C3 | -.290786E-01 | .146351E-03 | .789799E-03 | .300147E-01 |
| C4 | -.296520E-01 | 0. | 0. | .296520E-01 |

TOTAL HEAT CONDUCTED IN SOLID=TOSOCO= .904630E-01

| REGION NUMBER | QYXAIR(J) | QYXAIR(J) | QZXAIR(J) | SUM OF REGIONAL AIR CONDUCTION |
|---------------|--------------|--------------|--------------|--------------------------------|
| C2 | -.401885E-02 | -.902457E-04 | -.466554E-04 | .415575E-02 |
| C3 | -.198802E-02 | .326132E-04 | .316738E-04 | .205230E-02 |
| C4 | -.364376E-02 | 0. | 0. | .364376E-02 |

TOTAL HEAT CONDUCTED BY AIR= .985182E-02 IN WATTS

| | | | |
|----------------------|--------------------|---------------------|------------------------------|
| SOLIDCU= .307963E-01 | AIRCU= .415575E-02 | TOTRAU= .130561E-02 | HEAT TRANSFERED= .362576E-01 |
|----------------------|--------------------|---------------------|------------------------------|

HEAT TRANSFERED BY THE THREE MODES FOR THE WHOLE PLATE IN THE EXPERIMENT IS

| | | | |
|-------------------------------|-----------------------------|------------------------|------------------------------------|
| SOLID CONDUCTION= .394192E+01 | AIR CONDUCTION= .531936E+00 | RADIATION= .167119E+00 | TOTAL HEAT TRANSFERED= .464098E+01 |
|-------------------------------|-----------------------------|------------------------|------------------------------------|

TABLE H22

Values of dQ_r/dT For Run 568A

| J | DQDT(I,J) W/ ^o C | | | | |
|---|-----------------------------|-----------|-----------|-----------|-----------|
| | I | | | | |
| | 1 | 2 | 3 | 4 | 5 |
| 2 | -0.000021 | -0.000043 | -0.000043 | -0.000043 | -0.000021 |
| 3 | -0.000034 | -0.000068 | -0.000068 | -0.000068 | -0.000034 |
| 4 | -0.000033 | -0.000066 | -0.000066 | -0.000066 | -0.000033 |
| 5 | -0.000020 | -0.000039 | -0.000039 | -0.000039 | -0.000020 |

TABLE H23Net Radiation Flows For Run 568A

| I | QRADTO(I) in Watts |
|---|--------------------|
| 1 | -0.001698 |
| 2 | -0.006417 |
| 3 | -0.004659 |
| 4 | 0.004848 |
| 5 | 0.006283 |
| 6 | 0.001643 |

where QRADTO(I) is the net
radiative loss from surface I
resulting from radiation in the
enclosure

TABLE H24
Radiation Flows Towards Surface Points

| J | QRAD(I,J) in Watts | | | | |
|---|--------------------|------------|------------|------------|------------|
| | I | | | | |
| | 1 | 2 | 3 | 4 | 5 |
| 2 | -0.0001033 | -0.0002005 | -0.0002005 | -0.0002005 | -0.0001003 |
| 3 | -0.0000728 | -0.0001456 | -0.0001456 | -0.0001456 | -0.0000728 |
| 4 | 0.0000758 | 0.0001515 | 0.0001515 | 0.0001515 | 0.0000758 |
| 5 | 0.0000982 | 0.0001964 | 0.0001964 | 0.0001064 | 0.0000982 |

where QRAD(I,J) is the radiation flow to the surface point as defined in Appendix B

H3 CONDUCTANCES

Table H25 shows the conductances between nodal points (results of run 568A).

TABLE H25 - Conductances For Simulation Run 568A

NX= 14

NY= 4

NZ= 4

THE THERMAL CONDUCTIVITY OF PERSPEX=0.2000 IN WATTS PER METRE PER DEGREE C
 THE THICKNESS OF PERSPEX DIVIDED BY 3 IN METRES=.370E-02

| | CONDUCTANCE | MC | AC | DC | | |
|-----------|-------------|----------|----------|----------|-----------|----------|
| CXY(145)= | 0.000530 | 0.715200 | 1.000000 | 1.000000 | CXY(271)= | 0.000530 |
| CXY(146)= | 0.000645 | 0.871400 | 1.000000 | 1.000000 | CXY(272)= | 0.000645 |
| CXY(153)= | 0.000320 | 0.431900 | 1.000000 | 1.000000 | CXY(284)= | 0.000320 |
| CXY(154)= | 0.000365 | 1.000000 | 1.325000 | 2.690000 | CXY(285)= | 0.000365 |
| CXY(160)= | 0.000444 | 1.000000 | 1.325000 | 2.208000 | CXY(286)= | 0.000444 |
| CXY(161)= | 0.000598 | 0.807900 | 1.000000 | 1.000000 | CXY(287)= | 0.000598 |
| CXY(171)= | 0.000150 | 0.202900 | 1.000000 | 1.000000 | CXY(297)= | 0.000150 |
| CXY(172)= | 0.000163 | 1.000000 | 0.675500 | 3.068000 | CXY(298)= | 0.000163 |
| CXY(173)= | 0.000166 | 1.000000 | 0.675500 | 2.690000 | CXY(299)= | 0.000166 |
| CXY(174)= | 0.000227 | 1.000000 | 0.675500 | 2.208000 | CXY(300)= | 0.000227 |
| CXY(175)= | 0.000305 | 1.000000 | 0.675500 | 1.640000 | CXY(301)= | 0.000305 |
| CXY(176)= | 0.000495 | 0.608800 | 1.000000 | 1.000000 | CXY(302)= | 0.000495 |
| CXY(184)= | 0.000253 | 0.341900 | 1.000000 | 1.000000 | CXY(310)= | 0.000253 |
| CXY(185)= | 0.000263 | 1.000000 | 1.184000 | 3.330000 | CXY(311)= | 0.000263 |
| CXY(186)= | 0.000286 | 1.000000 | 1.184000 | 3.068000 | CXY(312)= | 0.000286 |
| CXY(187)= | 0.000326 | 1.000000 | 1.184000 | 2.690000 | CXY(313)= | 0.000326 |
| CXY(188)= | 0.000397 | 1.000000 | 1.184000 | 2.208000 | CXY(314)= | 0.000397 |
| CXY(189)= | 0.000535 | 1.000000 | 1.184000 | 1.640000 | CXY(315)= | 0.000535 |
| CXY(190)= | 0.000868 | 1.000000 | 1.184000 | 1.010000 | CXY(316)= | 0.000868 |
| CXY(191)= | 0.002571 | 2.472100 | 1.000000 | 1.000000 | CXY(317)= | 0.002571 |
| CXY(198)= | 0.000433 | 1.000000 | 2.027000 | 3.463000 | CXY(324)= | 0.000433 |
| CXY(199)= | 0.000451 | 1.000000 | 2.027000 | 3.330000 | CXY(325)= | 0.000451 |
| CXY(200)= | 0.000489 | 1.000000 | 2.027000 | 3.068000 | CXY(326)= | 0.000489 |
| CXY(201)= | 0.000558 | 1.000000 | 2.027000 | 2.690000 | CXY(327)= | 0.000558 |
| CXY(202)= | 0.000660 | 1.000000 | 2.027000 | 2.208000 | CXY(328)= | 0.000660 |
| CXY(203)= | 0.000915 | 1.000000 | 2.027000 | 1.640000 | CXY(329)= | 0.000915 |
| CXY(204)= | 0.001486 | 1.000000 | 2.027000 | 1.010000 | CXY(330)= | 0.001486 |
| CXY(205)= | 0.004401 | 1.000000 | 2.027000 | 0.341000 | CXY(331)= | 0.004401 |
| CXY(206)= | 0.001481 | 1.000000 | 2.000000 | 1.000000 | CXY(332)= | 0.001481 |
| CXY(212)= | 0.000433 | 1.000000 | 2.027000 | 3.463000 | CXY(338)= | 0.000433 |
| CXY(213)= | 0.000451 | 1.000000 | 2.027000 | 3.330000 | CXY(339)= | 0.000451 |
| CXY(214)= | 0.000489 | 1.000000 | 2.027000 | 3.068000 | CXY(340)= | 0.000489 |
| CXY(215)= | 0.000558 | 1.000000 | 2.027000 | 2.690000 | CXY(341)= | 0.000558 |

TABLE H25 (continued)

| | | | | | | |
|-----------|----------|----------|----------|----------|-----------|----------|
| CXY(216)= | 0.000660 | 1.000000 | 2.027000 | 2.208000 | CXY(342)= | 0.000680 |
| CXY(217)= | 0.000915 | 1.000000 | 2.027000 | 1.640000 | CXY(343)= | 0.000915 |
| CXY(218)= | 0.001486 | 1.000000 | 2.027000 | 1.010000 | CXY(344)= | 0.001486 |
| CXY(219)= | 0.004401 | 1.000000 | 2.027000 | 0.341000 | CXY(345)= | 0.004401 |
| CXY(220)= | 0.000740 | 1.000000 | 2.027000 | 2.027000 | CXY(346)= | 0.000740 |
| CXY(221)= | 0.000740 | 1.000000 | 1.000000 | 1.000000 | CXY(347)= | 0.000740 |
| CXY(226)= | 0.000217 | 1.000000 | 1.013500 | 3.463000 | CXY(352)= | 0.000217 |
| CXY(227)= | 0.000225 | 1.000000 | 1.013500 | 3.330000 | CXY(353)= | 0.000225 |
| CXY(228)= | 0.000245 | 1.000000 | 1.013500 | 3.068000 | CXY(354)= | 0.000245 |
| CXY(229)= | 0.000279 | 1.000000 | 1.013500 | 2.690000 | CXY(355)= | 0.000279 |
| CXY(230)= | 0.000340 | 1.000000 | 1.013500 | 2.208000 | CXY(356)= | 0.000340 |
| CXY(231)= | 0.000458 | 1.000000 | 1.013500 | 1.640000 | CXY(357)= | 0.000458 |
| CXY(232)= | 0.000743 | 1.000000 | 1.013500 | 1.010000 | CXY(358)= | 0.000743 |
| CXY(233)= | 0.002201 | 1.000000 | 1.013500 | 0.341000 | CXY(359)= | 0.002201 |
| CXY(234)= | 0.000370 | 1.000000 | 1.013500 | 2.027000 | CXY(360)= | 0.000370 |
| CXY(235)= | 0.000370 | 1.000000 | 1.013500 | 2.027000 | CXY(361)= | 0.000370 |
| CXY(236)= | 0.000370 | 0.500000 | 1.000000 | 1.000000 | CXY(362)= | 0.000370 |

THE CONDUCTANCES OF CYX AND CYZ ARE

| | | | | | | | |
|-----------|----------|-----------|----------|-----------|----------|-----|----------|
| CYX(132)= | 0.000073 | CYX(258)= | 0.000073 | CYX(384)= | 0.000073 | AC= | 1.351800 |
| CYX(145)= | 0.000150 | CYX(271)= | 0.000150 | CYX(397)= | 0.000150 | AC= | 2.704600 |
| CYX(146)= | 0.000255 | CYX(272)= | 0.000255 | CYX(398)= | 0.000255 | AC= | 4.711900 |
| CYX(147)= | 0.000100 | CYX(273)= | 0.000100 | CYX(399)= | 0.000100 | AC= | 1.050900 |
| CYX(158)= | 0.000114 | CYX(284)= | 0.000114 | CYX(410)= | 0.000114 | AC= | 2.119300 |
| CYX(159)= | 0.000206 | CYX(285)= | 0.000206 | CYX(411)= | 0.000206 | AC= | 3.614700 |
| CYX(160)= | 0.000175 | CYX(286)= | 0.000175 | CYX(412)= | 0.000175 | AC= | 3.244900 |
| CYX(161)= | 0.000138 | CYX(287)= | 0.000138 | CYX(413)= | 0.000138 | AC= | 2.549300 |
| CYX(162)= | 0.000047 | CYX(288)= | 0.000047 | CYX(414)= | 0.000047 | AC= | 0.677600 |
| CYX(171)= | 0.000062 | CYX(297)= | 0.000062 | CYX(423)= | 0.000062 | AC= | 1.147200 |
| CYX(172)= | 0.000117 | CYX(298)= | 0.000117 | CYX(424)= | 0.000117 | AC= | 2.160900 |
| CYX(173)= | 0.000151 | CYX(299)= | 0.000151 | CYX(425)= | 0.000151 | AC= | 2.787400 |
| CYX(174)= | 0.000089 | CYX(300)= | 0.000089 | CYX(426)= | 0.000089 | AC= | 1.054300 |
| CYX(175)= | 0.000070 | CYX(301)= | 0.000070 | CYX(427)= | 0.000070 | AC= | 1.299700 |
| CYX(176)= | 0.000046 | CYX(302)= | 0.000046 | CYX(428)= | 0.000046 | AC= | 0.695000 |
| CYX(177)= | 0.000012 | CYX(303)= | 0.000012 | CYX(429)= | 0.000012 | AC= | 0.226200 |
| CYX(184)= | 0.000095 | CYX(310)= | 0.000095 | CYX(436)= | 0.000095 | AC= | 1.754900 |
| CYX(185)= | 0.000217 | CYX(311)= | 0.000217 | CYX(437)= | 0.000217 | AC= | 4.021500 |
| CYX(186)= | 0.000205 | CYX(312)= | 0.000205 | CYX(438)= | 0.000205 | AC= | 3.797600 |
| CYX(187)= | 0.000184 | CYX(313)= | 0.000184 | CYX(439)= | 0.000184 | AC= | 3.406700 |
| CYX(188)= | 0.000157 | CYX(314)= | 0.000157 | CYX(440)= | 0.000157 | AC= | 2.694600 |

TABLE H25 (continued)

| | | | | | | | |
|-----------|----------|-----------|----------|-----------|----------|-----|----------|
| CYX(189)= | 0.000123 | CYX(315)= | 0.000123 | CYX(441)= | 0.000123 | AC= | 2.276000 |
| CYX(190)= | 0.000085 | CYX(316)= | 0.000085 | CYX(442)= | 0.000085 | AC= | 1.568800 |
| CYX(191)= | 0.000043 | CYX(317)= | 0.000043 | CYX(443)= | 0.000043 | AC= | 0.799800 |
| CYX(192)= | 0.000038 | CYX(318)= | 0.000038 | CYX(444)= | 0.000038 | AC= | 0.700900 |
| CYX(193)= | 0.000190 | CYX(324)= | 0.000190 | CYX(450)= | 0.000190 | AC= | 3.509800 |
| CYX(199)= | 0.000372 | CYX(325)= | 0.000372 | CYX(451)= | 0.000372 | AC= | 6.664700 |
| CYX(200)= | 0.000350 | CYX(326)= | 0.000350 | CYX(452)= | 0.000350 | AC= | 6.484400 |
| CYX(201)= | 0.000315 | CYX(327)= | 0.000315 | CYX(453)= | 0.000315 | AC= | 5.635700 |
| CYX(202)= | 0.000268 | CYX(328)= | 0.000268 | CYX(454)= | 0.000268 | AC= | 4.964100 |
| CYX(203)= | 0.000211 | CYX(329)= | 0.000211 | CYX(455)= | 0.000211 | AC= | 3.699000 |
| CYX(204)= | 0.000145 | CYX(330)= | 0.000145 | CYX(456)= | 0.000145 | AC= | 2.685600 |
| CYX(205)= | 0.000074 | CYX(331)= | 0.000074 | CYX(457)= | 0.000074 | AC= | 1.369200 |
| CYX(206)= | 0.000130 | CYX(332)= | 0.000130 | CYX(458)= | 0.000130 | AC= | 2.400600 |
| CYX(207)= | 0.000111 | CYX(333)= | 0.000111 | CYX(459)= | 0.000111 | AC= | 2.654400 |
| CYX(212)= | 0.000190 | CYX(338)= | 0.000190 | CYX(464)= | 0.000190 | AC= | 3.509800 |
| CYX(213)= | 0.000372 | CYX(339)= | 0.000372 | CYX(465)= | 0.000372 | AC= | 6.664700 |
| CYX(214)= | 0.000350 | CYX(340)= | 0.000350 | CYX(466)= | 0.000350 | AC= | 6.484400 |
| CYX(215)= | 0.000315 | CYX(341)= | 0.000315 | CYX(467)= | 0.000315 | AC= | 5.635700 |
| CYX(216)= | 0.000268 | CYX(342)= | 0.000268 | CYX(468)= | 0.000268 | AC= | 4.964100 |
| CYX(217)= | 0.000211 | CYX(343)= | 0.000211 | CYX(469)= | 0.000211 | AC= | 3.699000 |
| CYX(218)= | 0.000145 | CYX(344)= | 0.000145 | CYX(470)= | 0.000145 | AC= | 2.685600 |
| CYX(219)= | 0.000074 | CYX(345)= | 0.000074 | CYX(471)= | 0.000074 | AC= | 1.369200 |
| CYX(220)= | 0.000130 | CYX(346)= | 0.000130 | CYX(472)= | 0.000130 | AC= | 2.400600 |
| CYX(221)= | 0.000222 | CYX(347)= | 0.000222 | CYX(473)= | 0.000222 | AC= | 4.103700 |
| CYX(222)= | 0.000111 | CYX(348)= | 0.000111 | CYX(474)= | 0.000111 | AC= | 2.654400 |
| CYX(226)= | 0.000095 | CYX(352)= | 0.000095 | CYX(476)= | 0.000095 | AC= | 1.754900 |
| CYX(227)= | 0.000186 | CYX(353)= | 0.000186 | CYX(479)= | 0.000186 | AC= | 3.442400 |
| CYX(228)= | 0.000175 | CYX(354)= | 0.000175 | CYX(480)= | 0.000175 | AC= | 3.242200 |
| CYX(229)= | 0.000158 | CYX(355)= | 0.000158 | CYX(481)= | 0.000158 | AC= | 2.917900 |
| CYX(230)= | 0.000134 | CYX(356)= | 0.000134 | CYX(482)= | 0.000134 | AC= | 2.482100 |
| CYX(231)= | 0.000105 | CYX(357)= | 0.000105 | CYX(483)= | 0.000105 | AC= | 1.950900 |
| CYX(232)= | 0.000073 | CYX(358)= | 0.000073 | CYX(484)= | 0.000073 | AC= | 1.342900 |
| CYX(233)= | 0.000037 | CYX(359)= | 0.000037 | CYX(485)= | 0.000037 | AC= | 0.684600 |
| CYX(234)= | 0.000037 | CYX(360)= | 0.000037 | CYX(486)= | 0.000037 | AC= | 0.684600 |
| CYX(235)= | 0.000111 | CYX(361)= | 0.000111 | CYX(487)= | 0.000111 | AC= | 2.654400 |
| CYX(236)= | 0.000111 | CYX(362)= | 0.000111 | CYX(488)= | 0.000111 | AC= | 2.654400 |
| CYX(237)= | 0.000028 | CYX(363)= | 0.000028 | CYX(489)= | 0.000028 | AC= | 0.513600 |

TABLE H25 (continued)

| | CONDUCTANCE | AC | AC | DC | | |
|-----------|-------------|----------|----------|----------|-----------|----------|
| CZx(132)= | 0.000821 | 1.109100 | 1.000000 | 1.000000 | CZx(258)= | 0.000621 |
| CZx(145)= | 0.001300 | 1.755500 | 1.000000 | 1.000000 | CZx(271)= | 0.001300 |
| CZx(146)= | 0.000977 | 1.000000 | 2.165000 | 1.640000 | CZx(272)= | 0.000977 |
| CZx(147)= | 0.000869 | 1.173200 | 1.000000 | 1.000000 | CZx(273)= | 0.000869 |
| CZx(158)= | 0.002345 | 3.167300 | 1.000000 | 1.000000 | CZx(284)= | 0.002345 |
| CZx(159)= | 0.002111 | 1.000000 | 2.679000 | 1.010000 | CZx(285)= | 0.002111 |
| CZx(160)= | 0.001795 | 1.000000 | 2.449000 | 1.010000 | CZx(286)= | 0.001795 |
| CZx(161)= | 0.001410 | 1.000000 | 1.924000 | 1.010000 | CZx(287)= | 0.001410 |
| CZx(162)= | 0.000971 | 1.311900 | 1.000000 | 1.000000 | CZx(288)= | 0.000971 |
| CZx(171)= | 0.007374 | 9.958900 | 1.000000 | 1.000000 | CZx(297)= | 0.007374 |
| CZx(172)= | 0.006946 | 1.000000 | 3.199000 | 0.341000 | CZx(298)= | 0.006946 |
| CZx(173)= | 0.006251 | 1.000000 | 2.879000 | 0.341000 | CZx(299)= | 0.006251 |
| CZx(174)= | 0.005317 | 1.000000 | 2.449000 | 0.341000 | CZx(300)= | 0.005317 |
| CZx(175)= | 0.004178 | 1.000000 | 1.924000 | 0.341000 | CZx(301)= | 0.004178 |
| CZx(176)= | 0.002877 | 1.000000 | 1.325000 | 0.341000 | CZx(302)= | 0.002877 |
| CZx(177)= | 0.001467 | 1.980900 | 1.000000 | 1.000000 | CZx(303)= | 0.001467 |
| CZx(184)= | 0.000632 | 1.000000 | 1.731500 | 2.027000 | CZx(310)= | 0.000632 |
| CZx(185)= | 0.001241 | 1.000000 | 3.396500 | 2.027000 | CZx(311)= | 0.001241 |
| CZx(186)= | 0.001168 | 1.000000 | 3.199000 | 2.027000 | CZx(312)= | 0.001168 |
| CZx(187)= | 0.001052 | 1.000000 | 2.879000 | 2.027000 | CZx(313)= | 0.001052 |
| CZx(188)= | 0.000895 | 1.000000 | 2.449000 | 2.027000 | CZx(314)= | 0.000895 |
| CZx(189)= | 0.000703 | 1.000000 | 1.924000 | 2.027000 | CZx(315)= | 0.000703 |
| CZx(190)= | 0.000484 | 1.000000 | 1.325000 | 2.027000 | CZx(316)= | 0.000484 |
| CZx(191)= | 0.000247 | 1.000000 | 0.675500 | 2.027000 | CZx(317)= | 0.000247 |
| CZx(192)= | 0.000432 | 0.564100 | 1.000000 | 1.000000 | CZx(318)= | 0.000432 |
| CZx(198)= | 0.000632 | 1.000000 | 1.731500 | 2.027000 | CZx(324)= | 0.000632 |
| CZx(199)= | 0.001241 | 1.000000 | 3.396500 | 2.027000 | CZx(325)= | 0.001241 |
| CZx(200)= | 0.001168 | 1.000000 | 3.199000 | 2.027000 | CZx(326)= | 0.001168 |
| CZx(201)= | 0.001052 | 1.000000 | 2.879000 | 2.027000 | CZx(327)= | 0.001052 |
| CZx(202)= | 0.000895 | 1.000000 | 2.449000 | 2.027000 | CZx(328)= | 0.000895 |
| CZx(203)= | 0.000703 | 1.000000 | 1.924000 | 2.027000 | CZx(329)= | 0.000703 |
| CZx(204)= | 0.000484 | 1.000000 | 1.325000 | 2.027000 | CZx(330)= | 0.000484 |
| CZx(205)= | 0.000247 | 1.000000 | 0.675500 | 2.027000 | CZx(331)= | 0.000247 |
| CZx(206)= | 0.000432 | 1.000000 | 1.184000 | 2.027000 | CZx(332)= | 0.000432 |
| CZx(207)= | 0.000740 | 1.000000 | 1.000000 | 1.000000 | CZx(333)= | 0.000740 |
| CZx(212)= | 0.000632 | 1.000000 | 1.731500 | 2.027000 | CZx(338)= | 0.000632 |

TABLE H25 (continued)

| | | | | | | |
|-----------|----------|----------|----------|----------|-----------|----------|
| CZX(213)= | 0.001241 | 1.000000 | 3.396500 | 2.027000 | CZX(339)= | 0.001241 |
| CZX(214)= | 0.001168 | 1.000000 | 3.199000 | 2.027000 | CZX(340)= | 0.001168 |
| CZX(215)= | 0.001052 | 1.000000 | 2.879000 | 2.027000 | CZX(341)= | 0.001052 |
| CZX(216)= | 0.000895 | 1.000000 | 2.449000 | 2.027000 | CZX(342)= | 0.000895 |
| CZX(217)= | 0.000703 | 1.000000 | 1.924000 | 2.027000 | CZX(343)= | 0.000703 |
| CZX(218)= | 0.000484 | 1.000000 | 1.325000 | 2.027000 | CZX(344)= | 0.000484 |
| CZX(219)= | 0.000247 | 1.000000 | 0.675500 | 2.027000 | CZX(345)= | 0.000247 |
| CZX(220)= | 0.000432 | 1.000000 | 1.184000 | 2.027000 | CZX(346)= | 0.000432 |
| CZX(221)= | 0.000740 | 1.000000 | 2.027000 | 2.027000 | CZX(347)= | 0.000740 |
| CZX(222)= | 0.000740 | 1.000000 | 1.000000 | 1.000000 | CZX(348)= | 0.000740 |

R1= .10000E-02 R2= .51875E-02 R3= .93750E-02 R4= .13563E-01

IN METRES.

THE CONDUCTANCES OF POINTS ASSOCIATED WITH AIR IN THE CAVITY ARE

| | | |
|-----------------------|-----------------------|-----------------------|
| CXY(127)= .999900E+31 | CYX(127)=0. | CZX(127)= .999900E+31 |
| CXY(128)= .464281E-03 | CYX(128)=0. | CZX(128)=0. |
| CXY(129)= .139284E-04 | CYX(129)= .816120E-04 | CZX(129)= .185713E-04 |
| CXY(130)= .999900E+31 | CYX(130)=0. | CZX(130)=0. |
| CXY(131)= .162779E-04 | CYX(131)= .176589E-03 | CZX(131)= .325559E-04 |
| CXY(132)=0. | CYX(132)= .122738E-03 | CZX(132)= .821178E-03 |
| CXY(141)=0. | CYX(141)=0. | CZX(141)= .999900E+31 |
| CXY(142)=0. | CYX(142)=0. | CZX(142)=0. |
| CXY(143)=0. | CYX(143)=0. | CZX(143)= .999900E+31 |
| CXY(144)=0. | CYX(144)=0. | CZX(144)=0. |
| CXY(145)= .529534E-03 | CYX(145)= .249042E-03 | CZX(145)= .129977E-02 |
| CXY(155)=0. | CYX(155)=0. | CZX(155)= .999900E+31 |
| CXY(156)=0. | CYX(156)=0. | CZX(156)=0. |
| CXY(157)= .325559E-04 | CYX(157)= .236119E-03 | CZX(157)= .325559E-04 |
| CXY(158)= .319779E-03 | CYX(158)= .213909E-03 | CZX(158)= .234507E-02 |
| CXY(169)=0. | CYX(169)=0. | CZX(169)= .999900E+31 |
| CXY(170)=0. | CYX(170)=0. | CZX(170)=0. |
| CXY(171)= .150227E-03 | CYX(171)= .161392E-03 | CZX(171)= .737357E-02 |
| CXY(183)= .162779E-04 | CYX(183)= .595297E-04 | CZX(183)=0. |
| CXY(184)= .253143E-03 | CYX(184)= .144516E-03 | CZX(184)= .632463E-03 |
| CXY(253)= .999900E+31 | CYX(253)=0. | CZX(253)= .999900E+31 |
| CXY(254)= .464281E-03 | CYX(254)=0. | CZX(254)=0. |
| CXY(255)= .139284E-04 | CYX(255)= .816120E-04 | CZX(255)= .185713E-04 |
| CXY(256)= .999900E+31 | CYX(256)=0. | CZX(256)=0. |
| CXY(257)= .162779E-04 | CYX(257)= .176589E-03 | CZX(257)= .325559E-04 |
| CXY(258)=0. | CYX(258)= .122738E-03 | CZX(258)= .821178E-03 |
| CXY(267)=0. | CYX(267)=0. | CZX(267)= .999900E+31 |

TABLE H25 (continued)

| | | | |
|----------------------|----------------------|----------------------|----------------------|
| CXY(268)=0. | CYX(268)=0. | CZX(268)=0. | |
| CXY(269)=0. | CYX(269)=0. | CZX(269)=.999900E+31 | |
| CXY(270)=0. | CYX(270)=0. | CZX(270)=0. | |
| CXY(271)=.529534E-03 | CYX(271)=.249042E-03 | CZX(271)=.129977E-02 | |
| CXY(281)=0. | CYX(281)=0. | CZX(281)=.999900E+31 | |
| CXY(282)=0. | CYX(282)=0. | CZX(282)=0. | |
| CXY(283)=.325559E-04 | CYX(283)=.238119E-03 | CZX(283)=.325559E-04 | |
| CXY(284)=.319779E-03 | CYX(284)=.213909E-03 | CZX(284)=.234507E-02 | |
| CXY(295)=0. | CYX(295)=0. | CZX(295)=.999900E+31 | |
| CXY(296)=0. | CYX(296)=0. | CZX(296)=0. | |
| CXY(297)=.150227E-03 | CYX(297)=.161392E-03 | CZX(297)=.737357E-02 | |
| CXY(309)=.162779E-04 | CYX(309)=.595297E-04 | CZX(309)=0. | |
| CXY(310)=.253143E-03 | CYX(310)=.144516E-03 | CZX(310)=.632463E-03 | |
| CYX(379)=0. | CYX(380)=0. | CYX(381)=.816120E-04 | CYX(382)=0. |
| CYX(383)=.178589E-03 | CYX(384)=.122738E-03 | CYX(385)=0. | CYX(386)=0. |
| CYX(393)=0. | CYX(394)=0. | CYX(395)=0. | CYX(396)=0. |
| CYX(397)=.249042E-03 | CYX(398)=0. | CYX(399)=.238119E-03 | CYX(400)=.213909E-03 |
| CYX(407)=0. | CYX(408)=0. | CYX(409)=.161392E-03 | CYX(410)=.595297E-04 |
| CYX(421)=0. | CYX(422)=0. | CYX(423)=0. | |
| CYX(436)=.144516E-03 | CYX(437)=0. | | |

THE THERMAL CONDUCTIVITY OF AIR IN THE CAVITY IS TKAIN IN W/M DEGREE C=0.02659

THE EMISSIVITIES USED ARE

E(1)=0.0400 E(2)=0.9000 E(3)=0.9000 E(4)=0.9000 E(5)=0.9000 E(6)=0.0400.

THE RADIUS OF THE HOLES DRILLED IN THE PERSPEX IN METRES IS .177500E-01

| | | | | | |
|---------------|---------------|---------------|---------------|---------------|---------------|
| F(1,1)=0.0000 | F(1,2)=0.0990 | F(1,3)=0.1687 | F(1,4)=0.1352 | F(1,5)=0.0569 | F(1,6)=0.5401 |
| F(2,1)=0.4746 | F(2,2)=0.0508 | F(2,3)=0.0921 | F(2,4)=0.0766 | F(2,5)=0.0328 | F(2,6)=0.2730 |
| F(3,1)=0.4045 | F(3,2)=0.0461 | F(3,3)=0.0989 | F(3,4)=0.0882 | F(3,5)=0.0383 | F(3,6)=0.3241 |
| F(4,1)=0.3241 | F(4,2)=0.0383 | F(4,3)=0.0882 | F(4,4)=0.0989 | F(4,5)=0.0461 | F(4,6)=0.4045 |
| F(5,1)=0.2730 | F(5,2)=0.0328 | F(5,3)=0.0766 | F(5,4)=0.0921 | F(5,5)=0.0508 | F(5,6)=0.4746 |
| F(6,1)=0.5401 | F(6,2)=0.0569 | F(6,3)=0.1352 | F(6,4)=0.1687 | F(6,5)=0.0990 | F(6,6)=0.0000 |

THE AREAS ASSOCIATED WITH RADIATION AT THE POINTS INSIDE THE CYLINDER IN SQUARE METRES ARE

| | | | | | |
|---------------------|---------------------|---------------------|---------------------|---------------------|-----------------|
| AA(1,2)=.322556E-05 | AA(2,2)=.645113E-05 | AA(3,2)=.645113E-05 | AA(4,2)=.645113E-05 | AA(5,2)=.322556E-05 | |
| AA(1,3)=.645113E-05 | AA(2,3)=.129023E-04 | AA(3,3)=.129023E-04 | AA(4,3)=.129023E-04 | AA(5,3)=.645113E-05 | |
| AA(1,4)=.645113E-05 | AA(2,4)=.129023E-04 | AA(3,4)=.129023E-04 | AA(4,4)=.129023E-04 | AA(5,4)=.645113E-05 | |
| AA(1,5)=.322556E-05 | AA(2,5)=.645113E-05 | AA(3,5)=.645113E-05 | AA(4,5)=.645113E-05 | AA(5,5)=.322556E-05 | |
| AR(1)=0.0004898 | AR(2)=0.0002064 | AR(3)=0.0004129 | AR(4)=0.0004129 | AR(5)=0.0002064 | AR(6)=0.0004898 |

APPENDIX I

LISTING OF THE CAVITY PROBLEM

SIMULATION PROGRAM


```

C
C CALL RADIOS(TR,E,F,QQ,RGELG,IER)
C
C THE MATRIX OF OUTGOING FLUXES QQ HAS BEEN SOLVED
C THE ANSWERS ARE IN ARRAY RGELG
C QQ IS IN WATTS PER SQUARE METRE
C DO 121 I=1,6
C   QQ(I)=RGELG(I)
121 CONTINUE
122 WRITE(6,122)IER
122 FORMAT(/,10X,'THE RESULTING ERROR PARAMETER IN INVERTING THE FLUX
5 MATRIX IS IER=',I4)
123 WRITE(6,123)(I,QQ(I),I=1,6)
123 FORMAT(/,3X,6('QOC(',I1,')=',E12.5,3X))
C
C NOW THAT QQ(K) HAS BEEN COMPUTED, QKADTO(K) IS FOUND
C QKADTO(K) CAN BE REGARDED AS EITHER THE ENERGY SUPPLIED TO
C SURFACE K BY EXTERNAL MEANS OR THE NET RADIATIVE
C LOSS FROM SURFACE K RESULTING FROM RADIATION IN THE
C ENCLOSURE
C
C   SIGMA=5.6697E-08
C   DO 124 I=1,6
C     QKADTO(I)=AR(I)*E(I)/(1.-E(I))*(SIGMA*(TR(I)**4)-QQ(I))
C     QKADTO(I)=-QKADTO(I)
124 CONTINUE
125 WRITE(6,125)(I,QKADTO(I),I=1,6)
125 FORMAT(/,3X,6('QKADTO(',I1,')=',F9.6,2X))
C
C CONSIDER FOR EXAMPLE K=3
C QKADTO(K)=TOTAL RADIATION ON SURFACE 3
C BUT SURFACE 3 CONSISTS OF TEMP. POINTS 132,145,158,171
C AND 184. " THE RADIATION TO EACH OF THESE IS "
C QKAD(1,3),QKAD(2,3),QKAD(3,3),QKAD(4,3),AND QKAD(5,3) RESPECTIVELY
C
C HENCE QKAD(1,3)=QKADTO(3)*AA(1,3)/AR(3),AND IN GENERAL
C QKAD(I,J)=QKADTO(J)*AA(I,J)/AR(J)
C WITH I = AS THE NUMBER COUNTER
C J = AS THE PLANE COUNTER
C
C START WITH RADIATION REGION 2
C
C DO 110 J=2,5
C   QKAR2=QKADTO(J)/AR(J)
C   DO 111 I=1,5
C     QKAD(I,J)=QKAR2*AA(I,J)
111 CONTINUE
110 CONTINUE
C DO 126 J=2,5
C   WRITE(6,127)(I,J,QKAD(I,J),I=1,5)
127 FORMAT(/,3X,5('QKAD(',I1,',',I1,')=',F11.7,4X))
126 CONTINUE
C IF(NPITER.GT.4) GO TO 160
C
C START EVALUATING QQ BY DT FOR EACH TEMP REGION
C ASSUME QQ BY DT IS CONSTANT WITH TEMP. IN EACH REGION
C HENCE CALCULATE IT ONLY ONCE
C
C CALL DQBYDT(DQDT,QQ,QKAD,E,F,TR,RGELG,AA)
C
C 160 CONTINUE
C
C NOW PERFORM THE OVER-ALL HEAT BALANCE
C ACHIEVED USING SUBROUTINE RADREL
C THAT IS RADIATION RELAXATION
C
C CALL RELAX(CXY,CYX,CZX,T,RES,HX,HY,NZ,CRAD,QQDT,QKAD,TR)
C THE RADIATION RESIDUAL ITERATION HAS BEEN PERFORMED.
C REPEAT THE WHOLE PROGRAM UNTIL NO FURTHER
C SIGNIFICANT CHANGES OCCUR IN THE TEMPS. OF THE
C INSIDE OF THE CYLINDER. THAT IS, GO BACK TO STMT
C WITH "146"CONTINUE"
C WRITE(6,148)NPITER
148 FORMAT(/,10X,'THE NUMBER OF TOTAL PROGRAM ITERATIONS=',I3)
C IF(NPITER.EQ.10)GO TO 147
C NPITER=NPITER+1
C GO TO 146
C
C 147 CONTINUE
C EVALUATING THE HEAT FLOW BETWEEN POINTS USING HEATFL
C
C WRITE(6,406)
C 406 FORMAT(1H1)
C WRITE(6,51)
C 51 FORMAT(/,11X,'THE HEAT FLUX PROFILE IS')
C CALL HEATFL(CXY,CYX,CZX,T,QXY,QYX,QZX,HX,HY,NZ,QAIR,CAIR,TR,AN,DEL
C 1 AY,TKAIR,QKAD,SECAR1,SECAR2,QKADT)
C CONTINUE
C STOP
C END

```

```

00148000
00149000
00150000
00151000
00152000
00153000
00154000
00155000
00156000
00157000
00158000
00159000
00160000
00161000
00162000
00163000
00164000
00165000
00166000
00167000
00168000
00169000
00170000
00171000
00172000
00173000
00174000
00175000
00176000
00177000
00178000
00179000
00180000
00181000
00182000
00183000
00184000
00185000
00186000
00187000
00188000
00189000
00190000
00191000
00192000
00193000
00194000
00195000
00196000
00197000
00198000
00199000
00200000
00201000
00202000
00203000
00204000
00205000
00206000
00207000
00208000
00209000
00210000
00211000
00212000
00213000
00214000
00215000
00216000
00217000
00218000
00219000
00220000
00221000
00222000
00223000
00224000
00225000
00226000
00227000
00228000
00229000
00230000
00231000
00232000
00233000
00234000
00235000
00236000
00237000

```

```

SUBROUTINE CONDOC(CXY,CXZ,CYX,CYZ,CZX,CZY,HA,HY,HZ,DELTAY,TKAIR,R, 00238000
1 SECAR1,SECAR2) 00239000
DIMENSION CXY(1),CXZ(1),CYX(1),CYZ(1),CZX(1),CZY(1) 00240000
DIMENSION CAIR(5,5) 00241000
CONDOC EVALUATES THE CONDUCTANCES BETWEEN ANY POINTS. 00242000
00243000
NOTES ON NOMENCLATURE 00244000
CXY=CONDUCTANCE IN X DIRECTION WHEN CONSIDERING THE XY PLANE. 00245000
CXZ=CONDUCTANCE IN X DIRECTION WHEN CONSIDERING THE XZ PLANE. 00246000
HENCE CXY(I)=H*HA/D=H*(DELTAY*DELTAY)/DELTAY 00247000
SIMILAR DEFINITIONS APPLY FOR CYX,CYZ,CZX AND CZY 00248000
00249000
TKP=THERMAL CONDUCTIVITY OF PERSPEX 00250000
THICKNESS OF PERSPEX DIVIDED BY 3=DELTAY IN METRES 00251000
READING IN TKP AND DELTAY 00252000
READ(5,10)TKP,DELTAY 00253000
10 FORMAT(F9.7,E9.3) 00254000
WRITE(6,52)TKP,DELTAY 00255000
52 FORMAT(/,10X,'THE THERMAL CONDUCTIVITY OF PERSPEX=', 00256000
1F6.4,' IN WATTS PER METRE PER DEGREE C',/,10X, 00257000
2'THE THICKNESS OF PERSPEX DIVIDED BY 3 IN METRES=',E9.3) 00258000
COMPUTING CONDUCTANCES THAT ARE NEITHER B.C.S. 00259000
OR THOSE OF INFINITE CONDUCTANCE STARTS HERE" 00260000
CONDUCTANCES OF CXY AND CXZ 00261000
READ IN THE COEFFICIENT OF H, THAT IS, HC 00262000
READ IN THE COEFFICIENT OF AREA, THAT IS, AC 00263000
READ IN THE COEFFICIENT OF DISTANCE, THAT IS, DC 00264000
CXY(1)=CXZ(1)=(TKP*HC)*(DELTAY*AC)/DC 00265000
WRITE(6,30) 00266000
30 FORMAT(/,13X,'CONDUCTANCE',17X,'HC',20X,'AC',22X,'DC') 00267000
DO 15 I=145,146,1 00268000
READ(5,14)HC,AC,DC 00269000
14 FORMAT(3F12.7) 00270000
CXY(I)=(TKP*HC)*(DELTAY*AC)/DC 00271000
CXZ(I+126)=CXY(I) 00272000
WRITE(6,56)I,CXY(I),HC,AC,DC,(I+126),CXY(I+126) 00273000
56 FORMAT(/,1X,'CXY(',13,')=',F12.6,3(10X,F12.6),10X,'CXY(',13,')=', 00274000
5F12.6) 00275000
15 CONTINUE 00276000
DO 16 I=158,161,1 00277000
READ(5,14)HC,AC,DC 00278000
CXY(I)=(TKP*HC)*(DELTAY*AC)/DC 00279000
CXZ(I+126)=CXY(I) 00280000
WRITE(6,56)I,CXY(I),HC,AC,DC,(I+126),CXY(I+126) 00281000
16 CONTINUE 00282000
DO 17 I=171,176,1 00283000
READ(5,14)HC,AC,DC 00284000
CXY(I)=(TKP*HC)*(DELTAY*AC)/DC 00285000
CXZ(I+126)=CXY(I) 00286000
WRITE(6,56)I,CXY(I),HC,AC,DC,(I+126),CXY(I+126) 00287000
17 CONTINUE 00288000
DO 18 I=184,191,1 00289000
READ(5,14)HC,AC,DC 00290000
CXY(I)=(TKP*HC)*(DELTAY*AC)/DC 00291000
CXZ(I+126)=CXY(I) 00292000
WRITE(6,56)I,CXY(I),HC,AC,DC,(I+126),CXY(I+126) 00293000
18 CONTINUE 00294000
DO 19 I=198,206,1 00295000
READ(5,14)HC,AC,DC 00296000
CXY(I)=(TKP*HC)*(DELTAY*AC)/DC 00297000
CXZ(I+126)=CXY(I) 00298000
WRITE(6,56)I,CXY(I),HC,AC,DC,(I+126),CXY(I+126) 00299000
19 CONTINUE 00300000
DO 20 I=212,221,1 00301000
READ(5,14)HC,AC,DC 00302000
CXY(I)=(TKP*HC)*(DELTAY*AC)/DC 00303000
CXZ(I+126)=CXY(I) 00304000
WRITE(6,56)I,CXY(I),HC,AC,DC,(I+126),CXY(I+126) 00305000
20 CONTINUE 00306000
DO 21 I=226,236,1 00307000
00308000
00309000
00310000
00311000
00312000

```

```

READ(5,14)HC,AC,DC
CXY(I)=(TKP*HC)*(DELTAY*AC)/DC
CXY(I+126)=CXY(I)
WRITE(6,56)I,CXY(I),HC,AC,DC,(I+126),CXY(I+126)
21 CONTINUE
CONDUCTANCES OF CYX AND CYZ EVALUATED
USING SUBROUTINE CONYX

CXY(I)=CYZ(I)=TKP*(AC*1.E+06)/DELTAY

SINCE TKP AND DELTAY ARE FIXED AND READ IN ALREADY,
AC, THAT IS, THE AREA COEFFT IS THE ONLY VARIABLE

WRITE(6,59)
59 FORMAT(/,10X,'THE CONDUCTANCES OF CYX AND CYZ ARE')
INITIAL=132
IFINAL=132
CALL CONYX(CYX,CYZ,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=145
IFINAL=147
CALL CONYX(CYX,CYZ,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=158
IFINAL=162
CALL CONYX(CYX,CYZ,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=171
IFINAL=177
CALL CONYX(CYX,CYZ,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=184
IFINAL=192
CALL CONYX(CYX,CYZ,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=198
IFINAL=207
CALL CONYX(CYX,CYZ,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=212
IFINAL=222
CALL CONYX(CYX,CYZ,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=226
IFINAL=237
CALL CONYX(CYX,CYZ,INITIAL,IFINAL,TKP,DELTAY)

CONDUCTANCES OF CZX AND CZY
EVALUATED USING SUBROUTINE COCZX

CZX(I)=CZY(I)=(TKP*HC)*(DELTAY*AC)/DC

WRITE(6,405)
405 WRITE(6,30)
FORMAT(1H1)
INITIAL=132
IFINAL=132
CALL COCZX(CZX,CZY,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=145
IFINAL=147
CALL COCZX(CZX,CZY,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=158
IFINAL=162
CALL COCZX(CZX,CZY,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=171
IFINAL=177
CALL COCZX(CZX,CZY,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=184
IFINAL=192
CALL COCZX(CZX,CZY,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=198
IFINAL=207
CALL COCZX(CZX,CZY,INITIAL,IFINAL,TKP,DELTAY)
INITIAL=212
IFINAL=222
CALL COCZX(CZX,CZY,INITIAL,IFINAL,TKP,DELTAY)

AIR CONDUCTANCE EVALUATION STARTS HERE
INCLUDING CORRECTIONS OF SURFACE CONDUCTANCES IN Y DIRECTION

R1=1.E+03
R2=(R-R1)/4. +R1
R3=(R-R1)/2. +R1

```



```

R4=R3*(R-R1)/4
WRITE(6,192)R1,R2,R3,R4
192 FORMAT(/,10X,'R1=',E12.5,6X,'R2=',E12.5,6X,'R3=',E12.5,6X,'R4=',E1
12.5,6X,'IN METRES')
C
C CONDUCTANCES FROM INNER AIR CORE TO OUTER AIR CYLINDER
C THAT IS TOWARDS TEMP. 129
C
PI=3.1415927
AIRXC=TKAIR*2.*PI*DELTAY/(ALOG(R3/R1))
CXY(128)=AIRXC/64.
CXY(254)=CXY(128)
CZX(129)=AIRXC/16.
CZX(255)=CZX(129)
CXY(129)=AIRXC*3./64.
CXY(255)=CXY(129)
C
C AIR CONDUCTANCES IN OUTER REGION TOWARDS SURFACE POINTS
C
AIRXCO=TKAIR*2.*PI*DELTAY/(ALOG(R/R3))
CXY(131)=AIRXCO/64.
CXY(257)=CXY(131)
CZX(131)=AIRXCO/32.
CZX(257)=CZX(131)
CXY(157)=CZX(131)
CXY(283)=CZX(131)
CZX(157)=CZX(131)
CZX(283)=CZX(131)
CXY(183)=CXY(131)
CXY(309)=CXY(131)
C
C AIR CONDUCTANCES EVALUATION IN Y-DIRECTION
C
CYX(129)=TKAIR*PI*R2*R2/8./DELTAY
CYX(255)=CYX(129)
CYX(381)=CYX(129)
C
C CONDUCTANCES IN Y DIRM ON RADIUS=R3, THAT IS THOSE
C ASSOCIATED WITH POINTS 183,157 AND 131
C
SEGARA=TKAIR*(R4-R2)*(R4+R2)*0.5/DELTAY
SEGARA=SECTOR AREA OF ANNULUS BTWN RADII R2 AND R4
CYX(183)=SEGARA*11.25/2.*PI/180.
CYX(157)=SEGARA*22.5*PI/180.
CYX(131)=SEGARA*(11.25+(11.25/2.))*PI/180.
CYX(309)=CYX(183)
CYX(435)=CYX(183)
CYX(283)=CYX(157)
CYX(409)=CYX(157)
CYX(257)=CYX(131)
CYX(383)=CYX(131)
C
C RE-EVALUATION OF SURFACE CONDUCTANCES IN Y DIRM
C TAKING INTO ACCOUNT AIR CONDUCTANCE WHICH IS IN
C PARALLEL TO SOLID CONDUCTANCE
C
SECARA=TKAIR*(R-R4)*(R+R4)*0.5/DELTAY
SECARA=SECTOR AREA OF ANNULUS BTWN R4 AND SURFACE POINT
SECAR1=SECARA*11.25/2.*PI/180.
SECAR2=SECAR1*2
CYX(184)=CYX(184)+SECAR1
CYX(171)=CYX(171)+SECAR2
CYX(158)=CYX(158)+SECAR2
CYX(145)=CYX(145)+SECAR2
CYX(132)=CYX(132)+SECAR1
DO 188 I=132,184,13
CYX(I+126)=CYX(I)
CYX(I+252)=CYX(I)
188 CONTINUE
C
C SETTING UP INFINITE CONDUCTANCES CONNECTING
C AIR TEMPS. TO INNER CORE AIR TEMP. THAT IS T(129)
C
CI=9.999E+30
DO 189 I=127,169,14
CZX(I)=CI

```

```

00390000
00391000
00392000
00393000
00394000
00395000
00396000
00397000
00398000
00399000
00400000
00401000
00402000
00403000
00404000
00405000
00406000
00407000
00408000
00409000
00410000
00411000
00412000
00413000
00414000
00415000
00416000
00417000
00418000
00419000
00420000
00421000
00422000
00423000
00424000
00425000
00426000
00427000
00428000
00429000
00430000
00431000
00432000
00433000
00434000
00435000
00436000
00437000
00438000
00439000
00440000
00441000
00442000
00443000
00444000
00445000
00446000
00447000
00448000
00449000
00450000
00451000
00452000
00453000
00454000
00455000
00456000
00457000
00458000
00459000
00460000
00461000
00462000
00463000
00464000
00465000
00466000

```

```

      CZX(I+126)=CI
189  CONTINUE
      CXY(127)=CI
      CXY(253)=CI
      CZX(143)=CI
      CZX(269)=CI
      CXY(130)=CI
      CXY(256)=CI
      WRITE(6,193)
193  FORMAT(/,10X,'THE CONDUCTANCES OF POINTS ASSOCIATED WITH AIR IN TH
      IE CAVITY ARE')
      DO 195 I=127,132,1
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
194  FORMAT(/,10X,'CXY(',I3,')='E12.6,6X,'CYX(',I3,')='E12.6,6X,'CZX(
      I',I3,')='E12.6)
195  CONTINUE
      DO 196 I=141,145,1
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
196  CONTINUE
      DO 197 I=155,158,1
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
197  CONTINUE
      DO 198 I=169,171,1
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
198  CONTINUE
      DO 200 I=183,184
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
200  CONTINUE
      DO 199 I=253,258,1
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
199  CONTINUE
      DO 200 I=267,271,1
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
200  CONTINUE
      DO 201 I=281,284,1
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
201  CONTINUE
      DO 202 I=295,297,1
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
202  CONTINUE
      DO 210 I=309,310
      WRITE(6,194)I,CXY(I),I,CYX(I),I,CZX(I)
210  CONTINUE
      WRITE(6,203)(I,CYX(I),I=379,384)
203  FORMAT(/,1X,4(10X,'CYX(',I3,')='E12.6))
      WRITE(6,203)(I,CYX(I),I=393,397)
      WRITE(6,203)(I,CYX(I),I=407,410)
      WRITE(6,203)(I,CYX(I),I=421,423),(K,CYX(K),K=435,436)
      WRITE(6,150)TKAIR
150  FORMAT(/,10X,'THE THERMAL CONDUCTIVITY OF AIR IN THE CAVITY IS TKA
      AIR IN W/H DEGREE C='F7.5)
      RETURN
      END

```

```

00467000
00468000
00469000
00470000
00471000
00472000
00473000
00474000
00475000
00476000
00477000
00478000
00479000
00480000
00481000
00482000
00483000
00484000
00485000
00486000
00487000
00488000
00489000
00490000
00491000
00492000
00493000
00494000
00495000
00496000
00497000
00498000
00499000
00500000
00501000
00502000
00503000
00504000
00505000
00506000
00507000
00508000
00509000
00510000
00511000
00512000
00513000
00514000
00515000
00516000
00517000
00518000
00519000

```

```

C
C
C
C
SUBROUTINE CONYX(CYX,CYZ,INITAL,IFINAL,TKP,DELTAY)
DIMENSION CYX(1),CYZ(1)
CONYX*COMPUTES THE CONDUCTANCES CYX AND CYZ
USING THE READ-IN AREAS ONLY, AS THE THERMAL CONDUCTIVITY
AND THICKNESS OF PERSPEX ARE ALREADY READ IN.
DO 23 I=INITAL,IFINAL,1
READ(5,24)AC
24  FORMAT(F12.7)
CYX(I)=TKP*(AC*1.E-06)/DELTAY
CYX(I+126)=CYX(I)
CYX(I+252)=CYX(I)
58  WRITE(6,58)I,CYX(I),(I+126),CYX(I+126),(I+252),CYX(I+252),AC
23  FORMAT(/,10X,3('CYX(',I3,')= ',F12.6,10X),',AC= ',F10.6)
23  CONTINUE
RETURN
END
00520000
00521000
00522000
00523000
00524000
00525000
00526000
00527000
00528000
00529000
00530000
00531000
00532000
00533000
00534000
00535000
00536000
00537000

```

```

C
C
C
C
SUBROUTINE COCZX(CZX,CZY,INITAL,IFINAL,TKP,DELTAY)
DIMENSION CZX(1),CZY(1)
COCZX*COMPUTES THE CONDUCTANCES OF CZX AND CZY
USING THE FORMULA
CZX(I)=CZY(I)=(TKP*HC)*(DELTAY*AC)/DC
DO 25 I=INITAL,IFINAL,1
READ(5,26)HC,AC,DC
26  FORMAT(3F12.7)
CZX(I)=(TKP*HC)*(DELTAY*AC)/DC
CZX(I+126)=CZX(I)
60  WRITE(6,60)I,CZX(I),HC,AC,DC,(I+126),CZX(I+126)
1  FORMAT(/,1X,'CZX(',I3,')= ',F12.6,3(10X,F12.6),10X,'CZX(',I3,')= ',
25  F12.6)
25  CONTINUE
RETURN
END
00538000
00539000
00540000
00541000
00542000
00543000
00544000
00545000
00546000
00547000
00548000
00549000
00550000
00551000
00552000
00553000
00554000
00555000

```

```

SURROUTINE RELAX(CXY,CYX,CZX,T,RES,NX,NZ,CRAD,DQDT,GRAD,TR)
DIMENSION CXY(1),CYX(1),CZX(1),T(1),RES(1)
DIMENSION TR(504),DQDT(5,5),GRAD(5,5)
DIMENSION TR(6)

RELAX=EVALUATES THE TEMPERATURES BY RELAXATION

SETTING THE RADIATION CONDUCTANCE VALUES FOR SURFACE POINTS

CXY(132)=DQDT(1,3)
CXY(144)=DQDT(2,3)
CZX(144)=DQDT(3,3)
CXY(170)=DQDT(4,3)
CZX(170)=DQDT(5,3)
CXY(258)=DQDT(1,4)
CXY(270)=DQDT(2,4)
CZX(270)=DQDT(3,4)
CXY(296)=DQDT(4,4)
CZX(296)=DQDT(5,4)
DO 205 I=132,258,126
WRITE(6,204)I,CXY(I),(I+12),CXY(I+12),(I+12),CZX(I+12),(I+36),CXY(
1+38),(I+38),CZX(I+38)
204 FORMAT(/,3X,2('CXY(',I3,')=',E12.5,4X),('CZX(',I3,')=',E12.5,4X),('C
2Y(',I3,')=',E12.5,4X),('CZX(',I3,')=',E12.5)
205 CONTINUE

SETTING THE VALUES OF CRAD(I)
CRAD(I)=CONSTANT VALUE IN RELAXATION EQUATION
CRAD(I)=0 FOR INTERIOR NODAL POINTS
CRAD(I)=GRAD(I,J)FOR SURFACE POINTS

I=1
J=3
DO 206 IJ=132,184,13
CRAD(IJ)=GRAD(I,J)
CRAD(IJ+126)=GRAD(I,J+1)
I=I+1
206 CONTINUE
WRITE(6,207)(I,CRAD(I),I=132,184,13),(I,CRAD(I),I=258,310,13)
207 FORMAT(/,3X,5('CRAD(',I3,')=',F11.7,4X))
W=1.26
W=IS THE OVERRELAXATION FACTOR
KI=1
KI=IS THE RESIDUALS ITERATIONS COUNTER
LL=1
L=1
LL AND L ARE THE WRITE UP COUNTERS
TOL=0.00001
K IS THE TEMPERATURE COUNTER
40 NR=1
TOLM=0.00001
J=3
K=(NX*NZ)+1
33 CONTINUE
MR=(NX*NZ)+(NX*(NZ-1))
31 CONTINUE
IF(K.GT.MR)GO TO 32
IF(K.EQ.133.OR.K.EQ.144) GO TO 212
IF(K.EQ.259.OR.K.EQ.270) GO TO 212
IF(K.EQ.170.OR.K.EQ.296) GO TO 212
K1=K-1
K2=K+1
KNX1=K-NX
KNY2=K+NX
KNXZ1=K-(NX*NZ)
KNYZ2=K+(NX*NZ)
IF(K.EQ.132.OR.K.EQ.258) T(K2)=T(K)
IF(K.EQ.145.OR.K.EQ.271) T(K1)=T(K)
IF(K.EQ.158.OR.K.EQ.284) T(KNX1)=T(K)
IF(K.EQ.171.OR.K.EQ.297) T(K1)=T(K)
IF(K.EQ.184.OR.K.EQ.310) T(KNX1)=T(K)
DEN=(CXY(K1)*T(K1))+(CXY(K)*T(K+1))+(CYX(KNXZ2)*T(KNXZ2))+CRAD(K)
DEN=DEN+(CYX(K)*T(KNXZ1))+(CZX(KNX1)*T(KNX1))+(CZX(K)*T(KNX2))
DENUM1=CXY(K1)+CXY(K)+CYX(KNXZ2)+CYX(K)+CZX(KNX1)+CZX(K)

```

```

      IF (DENOM1.EQ.0.0) GO TO 208
      DENUM=DEN/DENOM1
      RES(K)=DENUM*T(K)
      T(K)=T(K)+(H*RES(K))
212  CONTINUE
208  CONTINUE
      K=K+1
      GO TO 31
32  K=K+NX
      NR=NR+1
      MR=MR+(NX*NZ)
      NZ1=NZ-1
      IF (NR.EQ.3) GO TO 34
      J=J+1
      GO TO 31
34  CONTINUE
C
C      THE FIRST ESTIMATE OF TEMPS HAS BEEN OBTAINED.
C      RESIDUALS ITERATING STARTS HERE.
      WRITE(6,300)(RES(J),J=1,504)
300  FORMAT(/,(1X,14(F7.3,2X)))
      NR=1
      K=(NX*NZ)+1
39  MR=(NX*NZ)+(NX*(NZ-1))
35  CONTINUE
      IF (K.GT.MR) GO TO 37
      IF (ABS(RES(K)).GT.ABS(TOLM)) GO TO 36
      K=K+1
      GO TO 35
36  TOLM=RES(K)
      K=K+1
      GO TO 35
37  K=K+NX
      NR=NR+1
      MR=MR+(NX*NZ)
      NZ1=NZ-1
      IF (NR.EQ.3) GO TO 64
      GO TO 35
64  IF (ABS(TOLM).LE.TOL) GO TO 42
      IF (KI.GT.20) GO TO 42
      IF (KI.EQ.L) GO TO 41
      KI=KI+1
      GO TO 40
41  CONTINUE
      WRITE(6,65)KI
65  FORMAT(///,11X,'THE NUMBER OF RESIDUAL ITERATIONS FOR THE TEMPERAT
      URE PROFILE SHOWN BELOW*',I3)
C      NXYZ=NX*NY*NZ
      SF=SCALING FACTOR FOR WRITING FORMAT
      SF=1000.
      DO 66 I=1,NXYZ
      TT(I)=T(I)*SF
66  CONTINUE
      WRITE(6,67)(TT(I),I=1,NXYZ,1)
67  FORMAT(///,(1X,14(I5,3X)))
      KI=KI+1
      LL=LL+1
      L=1*LL
      GO TO 40
42  CONTINUE
      WRITE(6,74)TOLM,TOL
74  FORMAT(/,10X,'TOLM=',F7.4,5X,'TOL=',F7.4)
      WRITE(6,65)KI
      NXYZ=NX*NY*NZ
      SF=1000.
      DO 68 I=1,NXYZ
      TT(I)=T(I)*SF
68  CONTINUE
      WRITE(6,67)(TT(I),I=1,NXYZ,1)
      RETURN
      END

```

```

00632000
00633000
00634000
00635000
00636000
00637000
00638000
00639000
00640000
00641000
00642000
00643000
00644000
00645000
00646000
00647000
00648000
00649000
00650000
00651000
00652000
00653000
00654000
00655000
00656000
00657000
00658000
00659000
00660000
00661000
00662000
00663000
00664000
00665000
00666000
00667000
00668000
00669000
00670000
00671000
00672000
00673000
00674000
00675000
00676000
00677000
00678000
00679000
00680000
00681000
00682000
00683000
00684000
00685000
00686000
00687000
00688000
00689000
00690000
00691000
00692000
00693000
00694000
00695000
00696000
00697000
00698000
00699000
00700000
00701000
00702000
00703000

```

```

SUBROUTINE HEATFL(CXY,CYX,CZX,T,QXY,QYX,QZX,NX,NY,NZ,QAIR,CAIR,TR, 00704000
1AR,DELTA,T,TKAIR,GRAD,SECAR1,SECAR2,GRADT) 00705000
DIMENSION CXY(1),CYX(1),CZX(1),T(1),QXY(1),QYX(1),QZX(1) 00706000
DIMENSION QAIR(5,5),CAIR(5,5),TR(6),AR(6) 00707000
DIMENSION GRAD(5,5) 00708000
DIMENSION GRADT(6),SUMQXY(6),SUMQYX(6),SUMQZX(6) 00709000
DIMENSION SQXYZ(6),QYXAIR(6),QYXAIR(6),QZXAIR(6),SQAIR(6) 00710000
C 00711000
C 00712000
C 00713000
HEATFL=COMPUTES THE HEAT FLUX BETWEEN POINTS 00714000
NR=1 00715000
KPLANE=1 00716000
C 00717000
C 00718000
ALTERING SUBROUTINE HEATFLOW 00719000
K=(NX*NZ)+1 00720000
CONTINUE 00721000
71 MR=(NX*NZ)+(NX*(NZ-1)) 00722000
47 CONTINUE 00723000
IF(K.GT.MR) GO TO 73 00724000
K2=K+1 00725000
KNX2=K+NX 00726000
KNXZ1=K-(NX*NZ) 00727000
QXY(K)=CXY(K)*(T(K)-T(K2)) 00728000
QYX(K)=CYX(K)*(T(K)-T(KNXZ1)) 00729000
QZX(K)=CZX(K)*(T(K)-T(KNX2)) 00730000
K=K+1 00731000
GO TO 47 00732000
73 CONTINUE 00733000
K=K+NX 00734000
NR=NR+1 00735000
MR=MR+(NX*NZ) 00736000
IF(NR.EQ.3) GO TO 49 00737000
GO TO 47 00738000
49 CONTINUE 00739000
IF(K.GT.MR) GO TO 187 00740000
KNXZ1=K-(NX*NZ) 00741000
QYX(K)=CYX(K)*(T(K)-T(KNXZ1)) 00742000
K=K+1 00743000
GO TO 49 00744000
C 00745000
187 CONTINUE 00746000
WRITE(6,213) 00747000
213 FORMAT(/,10X,'THE HEAT BALANCE OF ALL INTERIOR POINTS IS') 00748000
WRITE(6,185) 00749000
185 FORMAT(1X,'PT NO',6X,'QYX(K)',7X,'QYX(K+126)',6X,'QXY(K-1)',10X,'Q 00750000
1XY(K)',10X,'QZX(K-14)',6X,'QZX(K)',7X,'TOTAL HEAT FLOW',4X,'% ERRO 00751000
2R') 00752000
IHB=0 00753000
186 CONTINUE 00754000
INITAL=146+IHB 00755000
IFINAL=147+IHB 00756000
CALL HBPONT(QYX,QXY,QZX,TOTFLO,INITAL,IFINAL) 00757000
INITAL=159+IHB 00758000
IFINAL=162+IHB 00759000
CALL HBPONT(QYX,QXY,QZX,TOTFLO,INITAL,IFINAL) 00760000
INITAL=172+IHB 00761000
IFINAL=177+IHB 00762000
CALL HBPONT(QYX,QXY,QZX,TOTFLO,INITAL,IFINAL) 00763000
INITAL=185+IHB 00764000
IFINAL=192+IHB 00765000
CALL HBPONT(QYX,QXY,QZX,TOTFLO,INITAL,IFINAL) 00766000
INITAL=198+IHB 00767000
IFINAL=207+IHB 00768000
CALL HBPONT(QYX,QXY,QZX,TOTFLO,INITAL,IFINAL) 00769000
INITAL=212+IHB 00770000
IFINAL=222+IHB 00771000
CALL HBPONT(QYX,QXY,QZX,TOTFLO,INITAL,IFINAL) 00772000
INITAL=226+IHB 00773000
IFINAL=237+IHB 00774000
CALL HBPONT(QYX,QXY,QZX,TOTFLO,INITAL,IFINAL) 00775000
IF(IHB.GT.1) GO TO 250 00776000
IHB=IHB+126 00777000
GO TO 186 00778000
250 CONTINUE 00779000

```

```

C
C
C      HEAT BALANCE FOR SURFACE POINTS
C      J=3
C      I=1
C      DO 215 IJ=132,258,126
C      HEATIN=QXY(IJ-1)+ORAD(I,J)+QYX(IJ+126)
C      HITOUT=QZX(IJ)+QYX(IJ)
C      TOTFLO=HEATIN-HITOUT
C      PECERR=TOTFLO/((ABS(HEATIN+HITOUT))/2.)*100.
C      WRITE(6,216)(IJ-1),QXY(IJ-1),I,J,ORAD(I,J),(IJ+126),QYX(IJ+126),HE
1ATIN
216  FORMAT(/,5X,'QXY(',I3,')=',E11.4,7X,'ORAD(',I1,','I1,')=',E11.4,7
2X,'QYX(',I3,')=',E11.4,7X,'HEATIN=',E11.4)
C      WRITE(6,217)IJ,QZX(IJ),IJ,QYX(IJ),HITOUT,TOTFLO,PECERR
217  FORMAT(/,5X,'QZX(',I3,')=',E11.4,6X,'QYX(',I3,')=',E11.4,6X,'HEATU
1UT=',E11.4,6X,'TOTFLO=',E11.4,6X,'HEAT BALANCE ERROR %=',F6.3)
C      J=J+1
215  CONTINUE
C
C
C      HEAT BALANCE FOR POINT 145
C      I=2
C      J=3
C      DO 218 IJ=145,271,126
C      HEATIN=QZX(IJ-14)+QYX(IJ+126)+ORAD(I,J)
C      HITOUT=QYX(IJ)+QXY(IJ)+QZX(IJ)
C      TOTFLO=HEATIN-HITOUT
C      PECERR=TOTFLO/((ABS(HEATIN+HITOUT))/2.)*100.
C      WRITE(6,219)(IJ-14),QZX(IJ-14),I,J,ORAD(I,J),(IJ+126),QYX(IJ+126),
1HEATIN
219  FORMAT(/,5X,'QZX(',I3,')=',E11.4,7X,'ORAD(',I1,','I1,')=',E11.4,7
1X,'QYX(',I3,')=',E11.4,7X,'HEATIN=',E11.4)
C      WRITE(6,220)IJ,QYX(IJ),QXY(IJ),QZX(IJ),HITOUT,TOTFLO,PECERR
220  FORMAT(/,1X,'PT NO',I3,'QYX=',E11.4,5X,'QXY=',E11.4,5X,'QZX=',E11.
14,5X,'HEATOUT=',E11.4,6X,'TOTFLO=',E11.4,6X,'%ERROR=',F6.3)
C      J=J+1
218  CONTINUE
C
C
C      HEAT BALANCE FOR POINT 158
C      I=3
C      J=3
C      DO 221 IJ=158,284,126
C      HEATIN=QXY(IJ-1)+ORAD(I,J)+QYX(IJ+126)
C      HITOUT=QYX(IJ)+QXY(IJ)+QZX(IJ)
C      TOTFLO=HEATIN-HITOUT
C      PECERR=TOTFLO/((ABS(HEATIN+HITOUT))/2.)*100.
C      WRITE(6,216)(IJ-1),QXY(IJ-1),I,J,ORAD(I,J),(IJ+126),QYX(IJ+126),HE
1ATIN
C      WRITE(6,220)IJ,QYX(IJ),QXY(IJ),QZX(IJ),HITOUT,TOTFLO,PECERR
C      J=J+1
221  CONTINUE
C
C
C      HEAT BALANCE FOR POINT 171
C      I=4
C      J=3
C      DO 222 IJ=171,297,126
C      HEATIN=QZX(IJ-14)+ORAD(I,J)+QYX(IJ+126)
C      HITOUT=QYX(IJ)+QXY(IJ)+QZX(IJ)
C      TOTFLO=HEATIN-HITOUT
C      PECERR=TOTFLO/((ABS(HEATIN+HITOUT))/2.)*100.
C      WRITE(6,219)(IJ-14),QZX(IJ-14),I,J,ORAD(I,J),(IJ+126),QYX(IJ+126),
1HEATIN
C      WRITE(6,220)IJ,QYX(IJ),QXY(IJ),QZX(IJ),HITOUT,TOTFLO,PECERR
C      J=J+1
222  CONTINUE
C
C
C      HEAT BALANCE FOR POINT 184
C      I=5
C      J=3
C      DO 223 IJ=184,310,126
C      HEATIN=QXY(IJ-1)+ORAD(I,J)+QYX(IJ+126)
C      HITOUT=QYX(IJ)+QXY(IJ)+QZX(IJ)
C      TOTFLO=HEATIN-HITOUT

```

```

PECERR=TOTFLO/((ABS(HEATIN+HITOUT))/2.)*100.
WRITE(6,216)(IJ=1),QXY(IJ=1),I,J,QPAD(I,J),(IJ+126),QYX(IJ+126),HE
1ATIN
WRITE(6,220)IJ,QYX(IJ),QXY(IJ),QZX(IJ),HITOUT,TOTFLO,PECERR
J=J+1
223 CONTINUE
HEAT BALANCE FOR NODAL POINTS ASSOCIATED WITH AIR
CONSIDER POINT 129
DO 224 IJ=129,255,126
HEATIN=QXY(IJ=1)*QYX(IJ+126)
HITOUT=QYX(IJ)*QXY(IJ)+QZX(IJ)
TOTFLO=HEATIN+HITOUT
PECERR=TOTFLO/((ABS(HEATIN+HITOUT))/2.)*100.
WRITE(6,225)(IJ=1),QXY(IJ=1),(IJ+126),QYX(IJ+126),HEATIN
225 FORMAT(7,5X,'QXY(',I3,')= ',E11.4,7X,'HEATIN= ',E11.4)
IN=1,E11.4)
WRITE(6,220)IJ,QYX(IJ),QXY(IJ),QZX(IJ),HITOUT,TOTFLO,PECERR
224 CONTINUE
SUMMING THE SOLID CONDUCTION HEAT FLOWS
THE HEAT FLOWS NEXT TO SURFACE ARE RE-EVALUATED
SO THAT AIR CONDUCTION IS SEPARATED
DO 230 I=1,6
SUMQXY(I)=0.0
SUMQYX(I)=0.0
SUMQZX(I)=0.0
230 CONTINUE
J=3
ISUM=0
ISUM IS USED FOR REGION COUNTING
START WITH QXY
SUMQXY(3)=QXY(145)+QXY(146)
SUMQXY(4)=QXY(271)+QXY(272)
231 CONTINUE
INITAL=150+ISUM
IFINAL=161+ISUM
DO 171 I=INITAL,IFINAL
SUMQXY(J)=SUMQXY(J)+QXY(I)
171 CONTINUE
INITAL=171+ISUM
IFINAL=176+ISUM
DO 172 I=INITAL,IFINAL
SUMQXY(J)=SUMQXY(J)+QXY(I)
172 CONTINUE
INITAL=184+ISUM
IFINAL=191+ISUM
DO 173 I=INITAL,IFINAL
SUMQXY(J)=SUMQXY(J)+QXY(I)+QXY(I+NX)+QXY(I+(2*NX))+QXY(I+(3*NX))
173 CONTINUE
I=206+ISUM
SUMQXY(J)=SUMQXY(J)+QXY(I)+QXY(I+14)+QXY(I+15)+QXY(I+28)
SUMQXY(J)=SUMQXY(J)+QXY(I+29)+QXY(I+30)
IF(ISUM.GT.1) GO TO 232
ISUM=ISUM+126
J=J+1
GO TO 231
232 CONTINUE
QAIR(1,J)=DEFINE THIS AS THE AIR HEAT FLOW
IN Y-DIRECTION ASSOCIATED WITH SURFACE POINTS
I=1
J=3
DO 233 IJ=132,364,126
QAIR(I,J)=SECAR1*(T(IJ)-T(IJ=126))
QAIR(I+4,J)=SECAR1*(T(IJ+52)-T(IJ=74))
QAIR(I+1,J)=SECAR2*(T(IJ+13)-T(IJ=113))
QAIR(I+2,J)=SECAR2*(T(IJ+26)-T(IJ=100))
QAIR(I+3,J)=SECAR2*(T(IJ+39)-T(IJ=87))
J=J+1
233 CONTINUE

```



```

C      SUBTRACTING AIR CONDUCTION FROM(SOLID+AIR)CONDUCTION
C      IN Y-DIRECTION
C
      I=1
      J=3
      DO 234 IJ=132,184,13
      QYX(IJ)=QYX(IJ)-QAIR(I,J)
      QYX(IJ+126)=QYX(IJ+126)-QAIR(I,J+1)
      QYX(IJ+252)=QYX(IJ+252)-QAIR(I,J+2)
      I=I+1
234  CONTINUE
C
C      CONSIDERING QYX AND QZX
C
      J=3
      ISUM=0
      SUMQYX(3)=SUMQYX(3)+QYX(132)+QYX(145)+QYX(146)+QYX(147)
      SUMQYX(4)=SUMQYX(4)+QYX(258)+QYX(271)+QYX(272)+QYX(273)
      SUMQYX(5)=SUMQYX(5)+QYX(384)+QYX(397)+QYX(398)+QYX(399)
      SUMQZX(3)=SUMQZX(3)+QZX(132)+QZX(145)+QZX(146)+QZX(147)
      SUMQZX(4)=SUMQZX(4)+QZX(258)+QZX(271)+QZX(272)+QZX(273)
235  CONTINUE
      INITIAL=158+ISUM
      IFINAL=162+ISUM
      DO 174 I=INITIAL,IFINAL
      SUMQYX(J)=SUMQYX(J)+QYX(I)
      SUMQZX(J)=SUMQZX(J)+QZX(I)
174  CONTINUE
      INITIAL=171+ISUM
      IFINAL=177+ISUM
      DO 175 I=INITIAL,IFINAL
      SUMQYX(J)=SUMQYX(J)+QYX(I)
      SUMQZX(J)=SUMQZX(J)+QZX(I)
175  CONTINUE
      INITIAL=184+ISUM
      IFINAL=192+ISUM
      DO 176 I=INITIAL,IFINAL
      SUMQYX(J)=SUMQYX(J)+QYX(I)+QYX(I+NX)+QYX(I+(2*NX))
      SUMQZX(J)=SUMQZX(J)+QZX(I)+QZX(I+NX)+QZX(I+(2*NX))
176  CONTINUE
      I=207+ISUM
      SUMQYX(J)=SUMQYX(J)+QYX(I)+QYX(I+14)+QYX(I+15)
      SUMQZX(J)=SUMQZX(J)+QZX(I)+QZX(I+14)+QZX(I+15)
      INITIAL=226+ISUM
      IFINAL=237+ISUM
      DO 177 I=INITIAL,IFINAL
      SUMQYX(J)=SUMQYX(J)+QYX(I)
177  CONTINUE
      IF(ISUM.GE.252) GO TO 236
      ISUM=ISUM+126
      J=J+1
      GO TO 235
236  CONTINUE
C
C      PUTTING Y-DIRECTION SURFACE HEAT FLOWS TO WHAT THEY
C      WERE BEFORE
C
      I=1
      J=3
      DO 237 IJ=132,184,13
      QYX(IJ)=QYX(IJ)+QAIR(I,J)
      QYX(IJ+126)=QYX(IJ+126)+QAIR(I,J+1)
      QYX(IJ+252)=QYX(IJ+252)+QAIR(I,J+2)
      I=I+1
237  CONTINUE
C
C      WRITING THE HEAT FLOW IN SOLID CONDUCTION
C
      DO 240 I=3,5
      SQXYZ(I)=ABS(SUMQYX(I))+ABS(SUMQXY(I))+ABS(SUMQZX(I))
240  CONTINUE
      TOSUCD=SQXYZ(3)+SQXYZ(4)+SQXYZ(5)
      TOSUCD IS THE TOTAL SOLID CONDUCTION
      WRITE(6,238)
238  FORMAT(/,10X,'REGION NUMBER',10X,'SUM OF QYX',14X,'SUM OF QXY',13
      1X,'SUM OF QZX',11X,'SUM OF QY,QX AND QZ')

```

```

WRITE(6,239)(1,SUMQYX(1),SUMQXY(1),SUMQZX(1),SQXYZ(1),I=3,5)
239 FORMAT(/,14X,I4,15X,E13.6,10X,E13.6,10X,E13.6,10X,E13.6)
WRITE(6,241)TOSUCU
241 FORMAT(/,20X,'TOTAL HEAT CONDUCTED IN SOLID=TOUSUCU=',E13.6)
CCC
COMPUTING AIR CONDUCTION
DO 244 I=1,6
QYXAIR(I)=0.0
QXYAIR(I)=0.0
QZXAIR(I)=0.0
SQAIR(I)=0.0
244 CONTINUE
CCC
QYXAIR(I)=SUM OF AIR CONDUCTION IN Y DIRECTION
QXYAIR(I)=SUM OF AIR CONDUCTION IN X DIRECTION
QZXAIR(I)=SUM OF AIR CONDUCTION IN Z DIRECTION
DO 242 J=3,5
DO 242 I=1,5
QYXAIR(J)=QYXAIR(J)+QAIR(I,J)
242 CONTINUE
J=3
DO 243 I=129,381,126
QYXAIR(J)=QYXAIR(J)+QYX(I)+QYX(I+2)+QYX(I+26)+QYX(I+54)
QXYAIR(J)=QXYAIR(J)+QXY(I)+QXY(I+2)+QXY(I+26)+QXY(I+54)
QZXAIR(J)=QZXAIR(J)+QZX(I)+QZX(I+2)+QZX(I+26)+QZX(I+54)
J=J+1
243 CONTINUE
DO 245 J=3,5
SQAIR(J)=ABS(QYXAIR(J))+ABS(QXYAIR(J))+ABS(QZXAIR(J))
245 CONTINUE
TOAIR=SQAIR(3)+SQAIR(4)+SQAIR(5)
TOAIR=IS THE TOTAL HEAT CONDUCTED BY AIR
WRITE(6,246)
246 FORMAT(/,10X,'REGION NUMBER',10X,'QYXAIR(J)',15X,'QXYAIR(J)',14X,
1,'QZXAIR(J)',10X,'SUM OF REGIONAL AIR CONDUCTION')
WRITE(6,239)(1,QYXAIR(I),QXYAIR(I),QZXAIR(I),SQAIR(I),I=3,5)
WRITE(6,247)TOAIR
247 FORMAT(/,20X,'TOTAL HEAT CONDUCTED BY AIR=',E13.6,' IN WATTS')
CCC
SUMMING RADIATION TRANSFERED
TOTRAD=ABS((GRADTU(1)+GRADTU(2)+(GRADTU(3)/2.))/8.)
TOTRAD=IS THE TOTAL HEAT TRANSFERED BY RADIATION
HEATR=SQXYZ(3)+SQAIR(3)+TOTRAD
WRITE(6,248)SQXYZ(3),SQAIR(3),TOTRAD,HEATR
248 FORMAT(/,14X,'SOLIDCO=',E13.6,10X,'AIRCO=',E13.6,10X,'TOTRAD=',E13
1,6,10X,'HEAT TRANSFERED=',E13.6)
HTAIR=SQAIR(3)*16.*8.
HTRAD=TOTRAD*16.*8.
HTSOLI=SQXYZ(3)*16.*8.
CONRAD=HTAIR+HTRAD+HTSOLI
WRITE(6,249)HTSOLI,HTAIR,HTRAD,CONRAD
249 FORMAT(/,20X,'HEAT TRANSFERED BY THE THREE MODES FOR THE WHOLE PLA
1TE IN THE EXPERIMENT IS',/,1X,'SOLID CONDUCTION=',E13.6,5X,'AIR C
2NDUCTION=',E13.6,5X,'RADIATION=',E13.6,5X,'TOTAL HEAT TRANSFERED=
3',E13.6)
RETURN
END

```

```

SUBROUTINE SHAPEF(F,R,DELTAY,AR)
DIMENSION F(6,6),AR(6)
F(1,1)=1./2.*(H/R*(SORT(4.*(H*H/(F*R))))*(H*H/(R*R)))
FRITRI(H1,H2,R)=(H2/2./R)+(1./4.*(SORT(4.*(H1*H1)/(R*R)))+(H2/H1
1)*(SORT(4.*(H2*H2)/(R*R))))-(H1+H2)/H1*(SORT(4.*(H1*H2)*(H1*H2)/
2(R*R))))))
C
C SHAPEF-COMPUTES THE SHAPE FACTORS FOR THE CYLINDRICAL HOLE
C
C FOR A CYLINDER DIVIDED INTO 4 RADIATION REGIONS
C THE SHAPE FACTORS ARE
C 1-FROM ONE RING TO ANOTHER RING-E.G. F(2,3),F(3,4),F(4,5)
C 2-FROM ANY RING TO A DISK-E.G.F(2,1),F(3,1),F(5,6),F(4,6)
C 3-FROM A DISK TO ANOTHER DISK-E.G.F(1,6)
C
C F(1,1)-SHAPE FACTOR EQN FOR SOLVING DISK TO RING FACTORS
C FRITRI-SHAPE FACTOR EQN FOR SOLVING RING TO RING FACTORS
C THE HOLE THRU THE PERSPEX IS DIVIDED INTO 4 RING REGIONS
C THAT IS,2,3,4, AND 5
C THE TWO END DISK REGIONS ARE 1 AND 6
C
C THE RADIATION SURFACE AREAS IN SQUARE METRES ARE -
C PI=3.1416
C AR(1)=PI*R*R
C AR(6)=AR(1)
C THE ABOVE ARE THE DISK AREAS
C THE RING AREAS ARE
C AR(2)=PI*R*DELTAY
C AR(5)=AR(2)
C AR(3)=2.*PI*R*DELTAY
C AR(4)=AR(3)
C
C SHAPE FACTOR EVALUATION STARTS HERE
C
C SHAPE FACTORS OF DISK TO DISK
C H=DELTAY*3.
C F(1,6)=1.-F(1,1)
C F(6,1)=F(1,6)
C
C SHAPE FACTORS OF DISK TO RING
C
C COMPUTING F(1,2)
C H=DELTAY/2.
C F(1,2)=F(1,1)
C F(6,5)=F(1,2)
C COMPUTING F(1,3)
C H=DELTAY*(DELTAY/2.)
C F123=F(1,1)
C F(1,3)=F123-F(1,2)
C F(6,4)=F(1,3)
C COMPUTING F(1,4)
C H=DELTAY*DELTAY*(DELTAY/2.)
C F1234=F(1,1)
C F(1,4)=F1234-F(1,2)-F(1,3)
C F(6,3)=F(1,4)
C COMPUTING F(1,5)
C H=3.*DELTAY
C F12345=F(1,1)
C F(1,5)=F12345-F(1,2)-F(1,3)-F(1,4)
C F(6,2)=F(1,5)
C COMPUTING F(1,1)
C F(1,1)=1.-F(1,2)-F(1,3)-F(1,4)-F(1,5)
C F(6,6)=F(1,1)
C
C SHAPE FACTORS FOR RING TO RING
C
C COMPUTING F(2,3)
C H1=DELTAY/2.
C H2=DELTAY
C F(2,3)=FRITRI(H1,H2,R)
C F(5,4)=F(2,3)
C COMPUTING F(2,4)
C H1=DELTAY/2.
C H2=DELTAY+DELTAY
C F234=FRITRI(H1,H2,R)

```

```

F(2,4)=F234-F(2,3)
F(5,3)=F(2,4)
C COMPUTING F(2,5)
H1=DELTAY/2.
H2=DELTAY*DELTAY+(DELTAY/2.)
F2345=FRITRI(H1,H2,R)
F(2,5)=F2345-F(2,3)-F(2,4)
F(5,2)=F(2,5)
C COMPUTING F(3,4)
H1=DELTAY
H2=DELTAY
F(3,4)=FRITRI(H1,H2,R)
F(4,3)=F(3,4)
C
C ALL THE SHAPE FACTORS THAT ARE NECESSARY TO FIND
C ALL THE OTHER SHAPE FACTORS HAVE NOW BEEN EVALUATED
C NOW USING CONFIGURATION-FACTOR ALGEBRA, FIND THE OTHER
C SHAPE FACTORS.
C
C STARTING WITH SHAPE FACTORS F(2,J)
F(2,1)=AR(1)*F(1,2)/AR(2)
F(2,6)=AR(6)*F(6,2)/AR(2)
F(2,2)=1.-(F(2,1)+F(2,3)+F(2,4)+F(2,5)+F(2,6))
C
C CONSIDERING SHAPE FACTORS F(3,J)
F(3,1)=AR(1)*F(1,3)/AR(3)
F(3,2)=AR(2)*F(2,3)/AR(3)
F(3,5)=AR(5)*F(5,3)/AR(3)
F(3,6)=AR(6)*F(6,3)/AR(3)
F(3,3)=1.-(F(3,1)+F(3,2)+F(3,4)+F(3,5)+F(3,6))
C CONSIDERING SHAPE FACTORS F(4,J)
F(4,1)=AR(1)*F(1,4)/AR(4)
F(4,2)=AR(2)*F(2,4)/AR(4)
F(4,5)=F(3,2)
F(4,6)=F(3,1)
F(4,4)=1.-(F(4,1)+F(4,2)+F(4,3)+F(4,5)+F(4,6))
C CONSIDERING SHAPE FACTORS F(5,J)
F(5,1)=F(2,6)
F(5,6)=AR(6)*F(6,5)/AR(5)
F(5,5)=1.-(F(5,1)+F(5,2)+F(5,3)+F(5,4)+F(5,6))
DO 104 I=1,6
WRITE(6,105)(I,J,F(I,J),J=1,6)
105 FORMAT(//,10X,6('F(',I1,',',I1,',')=',F6,4,5X))
104 CONTINUE
RETURN
END

```

```

01145000
01146000
01147000
01148000
01149000
01150000
01151000
01152000
01153000
01154000
01155000
01156000
01157000
01158000
01159000
01160000
01161000
01162000
01163000
01164000
01165000
01166000
01167000
01168000
01169000
01170000
01171000
01172000
01173000
01174000
01175000
01176000
01177000
01178000
01179000
01180000
01181000
01182000
01183000
01184000
01185000
01186000
01187000
01188000
01189000
01190000

```

```

SUBROUTINE RADIOS(TR,E,F,QU,R,IER)                                01191000
DIMENSION TR(6),E(6),F(6,6),QU(6),R(6),A(6,6)                  01192000
RADIOS=EVALUATES THE RADIOSITIES QU BY MATRIX INVERSION          01193000
SET UP MATRIX OF COEFFICIENTS A(M,M)                            01194000
R.H.S. OF MATRIX IS R(M,N)                                       01195000
BOTH OF THESE MATRICES ARE DESTROYED ON INVERSION                01196000
SOLN STORED IN R-AFTER USING SUBROUTINE GELG                     01197000
                                                                    01198000
                                                                    01199000
C                                                                    01200000
C                                                                    01201000
C                                                                    01202000
C                                                                    01203000
C                                                                    01204000
C                                                                    01205000
C                                                                    01206000
C                                                                    01207000
C                                                                    01208000
C                                                                    01209000
C                                                                    01210000
C                                                                    01211000
C                                                                    01212000
C                                                                    01213000
C                                                                    01214000
C                                                                    01215000
C                                                                    01216000
C                                                                    01217000
C                                                                    01218000
C                                                                    01219000
C                                                                    01220000
C                                                                    01221000
C                                                                    01222000
C                                                                    01223000
C                                                                    01224000
C                                                                    01225000
C                                                                    01226000
C                                                                    01227000
C                                                                    01228000
C                                                                    01229000
C                                                                    01230000
C                                                                    01231000
C                                                                    01232000
C                                                                    01233000
C                                                                    01234000
C                                                                    01235000
C                                                                    01236000
C                                                                    01237000
C                                                                    01238000
C                                                                    01239000
C                                                                    01240000
C                                                                    01241000
C                                                                    01242000
C                                                                    01243000
C                                                                    01244000
C                                                                    01245000
C                                                                    01246000
C                                                                    01247000
C                                                                    01248000
C                                                                    01249000
C                                                                    01250000
C                                                                    01251000
C                                                                    01252000
C                                                                    01253000
C                                                                    01254000
C                                                                    01255000
C                                                                    01256000
C                                                                    01257000
C                                                                    01258000
C                                                                    01259000
C                                                                    01260000
C                                                                    01261000

112 CONTINUE
A(1,1)=1.-((1.-E(1))*F(1,1))
DO 112 I=2,6
A(I,1)=((1.-E(I))*F(I,1))
CONTINUE
A(1,2)=((1.-E(1))*F(1,2))
A(2,2)=1.-((1.-E(2))*F(2,2))
DO 113 I=3,6
A(I,2)=((1.-E(I))*F(I,2))
CONTINUE
DO 114 I=1,2
A(I,3)=((1.-E(I))*F(I,3))
CONTINUE
A(3,3)=1.-((1.-E(3))*F(3,3))
DO 115 I=4,6
A(I,3)=((1.-E(I))*F(I,3))
CONTINUE
DO 116 I=1,3
A(I,4)=((1.-E(I))*F(I,4))
CONTINUE
A(4,4)=1.-((1.-E(4))*F(4,4))
DO 117 I=5,6
A(I,4)=((1.-E(I))*F(I,4))
CONTINUE
DO 118 I=1,4
A(I,5)=((1.-E(I))*F(I,5))
CONTINUE
A(5,5)=1.-((1.-E(5))*F(5,5))
A(6,5)=((1.-E(6))*F(6,5))
DO 119 I=1,5
A(I,6)=((1.-E(I))*F(I,6))
CONTINUE
A(6,6)=1.-((1.-E(6))*F(6,6))
WRITE(6,161)
161 FORMAT(/,10X,'THE MATRIX OF CUEFFTS OF RADIOSITY EQNS USED IS')
DO 162 J=1,6
WRITE(6,163)(I,J,A(I,J)),I=1,6
163 FORMAT(/,4X,6('A(',I1,',',I1,',')='F11.7,3X))
162 CONTINUE

R IS THE M*N MATRIX OF RIGHT HAND SIDES
COMPUTED BELOW
SIGMA=5.6697E-08
DO 120 I=1,6
R(I)=E(I)*SIGMA*(TR(I)**4)
CONTINUE
WRITE(6,164)(I,R(I)),I=1,6
164 FORMAT(/,10X,'R.H.S. OF RADIOSITY EQUATIONS ARE ',/5X,6('R(',I1,',',I1,',',E13.6,3X))

THE REST OF THE ARGUMENTS IN GELG ARE SET BELOW

M=6
N=1
EPS=1.E-08
CALL GELG(R,A,M,N,EPS,IER)

THE SYSTEM OF QU EQNS HAS BEEN SOLVED
THE ANSWERS ARE IN R

RETURN
END

```

```

SUBROUTINE DQBYDT(DQDT,QQ,QRAD,E,F,IP,RGELG,AA)
DIMENSION DQDT(5,5),QQ(6),QRAD(5,5),E(6),F(6,6),TR(6)
DIMENSION RGELG(6),AA(5,5)
SIGMA=5.6697E-08
DELTAT=0.3
C
C START WITH RADIATION REGION 2
C J=RADIATION REGION COUNTER
C I=TEMP COUNTER FOR A GIVEN RADIATION REGION
C
DO 129 J=2,5
  TR(J)=TR(J)+DELTAT
  SIGT4=4,*(TR(J)**3)/((TR(J)**4)-((TR(J)-DELTAT)**4))
  CALL RADIUS(TR,E,F,QQ,RGELG,IER)
  C VALUE OF OUTGOING RADIATIVE FLUX IS IN RGELG(J)
  QRDQTJ=E(J)/(1.-E(J))*(SIGMA*(TR(J)**4)-RGELG(J))
  C QRDQTJ=-QRDQTJ
  C QRDQTJ=J*RDQT(J) TO BE USED IN DQ/DV CALC-N PER UNIT AREA
  DO 128 I=1,5
    QRAD12=QRDQTJ*AA(I,J)
    QDQT(I,J)=(QRAD12-QRAD(I,J))*SIGT4
  128 CONTINUE
  TR(J)=TR(J)-DELTAT
  129 CONTINUE
  DO 131 J=2,5
    WRITE(6,130)(I,J,DQDT(I,J),I=1,5)
  130 FORMAT(/,3X,5('DQDT(',I1,',',I1,',',F11.6,'4X))
  131 CONTINUE
  RETURN
END
01262000
01263000
01264000
01265000
01266000
01267000
01268000
01269000
01270000
01271000
01272000
01273000
01274000
01275000
01276000
01277000
01278000
01279000
01280000
01281000
01282000
01283000
01284000
01285000
01286000
01287000
01288000
01289000
01290000
01291000

```

```

SUBROUTINE GELG(R,A,M,N,EPS,IER)
DIMENSION A(1),R(1)
.....

SUBROUTINE GELG
PURPOSE
  TO SOLVE A GENERAL SYSTEM OF SIMULTANEOUS LINEAR EQUATIONS.
USAGE
  CALL GELG(R,A,M,N,EPS,IER)
DESCRIPTION OF PARAMETERS
  R  = THE M BY N MATRIX OF RIGHT HAND SIDES. (DESTROYED)
      ON RETURN R CONTAINS THE SOLUTION OF THE EQUATIONS.
  A  = THE M BY M COEFFICIENT MATRIX. (DESTROYED)
  M  = THE NUMBER OF EQUATIONS IN THE SYSTEM.
  N  = THE NUMBER OF RIGHT HAND SIDE VECTORS.
  EPS = AN INPUT CONSTANT WHICH IS USED AS RELATIVE
        TOLERANCE FOR TEST ON LOSS OF SIGNIFICANCE.
  IER = RESULTING ERROR PARAMETER CODED AS FOLLOWS
        IER=0  " NO ERROR
        IER=-1 " NO RESULT BECAUSE OF M LESS THAN 1 OR
                PIVOT ELEMENT AT ANY ELIMINATION STEP
                EQUAL TO 0.
        IER=K  " WARNING DUE TO POSSIBLE LOSS OF SIGNIFI-
                CANCE INDICATED AT ELIMINATION STEP K+1,
                WHERE PIVOT ELEMENT WAS LESS THAN OR
                EQUAL TO THE INTERNAL TOLERANCE EPS TIMES
                ABSOLUTELY GREATEST ELEMENT OF MATRIX A.

REMARKS
  INPUT MATRICES R AND A ARE ASSUMED TO BE STORED COLUMNWISE
  IN M*N RESP. M*M SUCCESSIVE STORAGE LOCATIONS. ON RETURN
  SOLUTION MATRIX R IS STORED COLUMNWISE TOO.
  THE PROCEDURE GIVES RESULTS IF THE NUMBER OF EQUATIONS M IS
  GREATER THAN 0 AND PIVOT ELEMENTS AT ALL ELIMINATION STEPS
  ARE DIFFERENT FROM 0. HOWEVER WARNING IER=K " IF GIVEN "
  INDICATES POSSIBLE LOSS OF SIGNIFICANCE. IN CASE OF A WELL
  SCALED MATRIX A AND APPROPRIATE TOLERANCE EPS, IER=K MAY BE
  INTERPRETED THAT MATRIX A HAS THE RANK K. NO WARNING IS
  GIVEN IN CASE M=1.

SUBROUTINES AND FUNCTION SUBPROGRAMS REQUIRED
  NONE

METHOD
  SOLUTION IS DONE BY MEANS OF GAUSS-ELIMINATION WITH
  COMPLETE PIVOTING.
.....

IF(M)23,23,1
SEARCH FOR GREATEST ELEMENT IN MATRIX A
1  IER=0
  PIV=0.
  MN=M*N
  NN=M*M
  DO 3 L=1,MN
    TB=ABS(A(L))
    IF(TB>PIV)3,3,2
2  PIV=TB
  I=L
3  CONTINUE
  TOL=EPS*PIV
  A(I) IS PIVOT ELEMENT. PIV CONTAINS THE ABSOLUTE VALUE OF A(I).

START ELIMINATION LOOP
LST=1
DO 17 K=1,N

```

| | | |
|----|--|----------|
| C | TEST ON SINGULARITY | 01368000 |
| | IF(PIV)23,23,4 | 01369000 |
| 4 | IF(1ER)7,5,7 | 01370000 |
| 5 | IF(PIV-TOL)6,6,7 | 01371000 |
| 6 | 1ER=K-1 | 01372000 |
| 7 | PIV=1./A(I) | 01373000 |
| | J=(I-1)/N | 01374000 |
| | I=1-J*M=K | 01375000 |
| | J=J+1=K | 01376000 |
| | I+K IS ROW=INDEX, J+K COLUMN=INDEX OF PIVOT ELEMENT | 01377000 |
| C | PIVOT ROW REDUCTION AND ROW INTERCHANGE IN RIGHT HAND SIDE K | 01378000 |
| C | DO 8 L=K,MM,M | 01379000 |
| | LL=L+1 | 01380000 |
| | TH=PIV*A(LL) | 01381000 |
| | R(LL)=R(L) | 01382000 |
| 8 | R(L)=TB | 01383000 |
| C | IS ELIMINATION TERMINATED | 01384000 |
| C | IF(K=M)9,18,18 | 01385000 |
| C | COLUMN INTERCHANGE IN MATRIX A | 01386000 |
| 9 | LEND=LST+H-K | 01387000 |
| | IF(J)12,12,10 | 01388000 |
| 10 | II=J*M | 01389000 |
| | DO 11 L=LST,LEND | 01390000 |
| | TB=A(L) | 01391000 |
| | LL=L+II | 01392000 |
| | A(L)=A(LL) | 01393000 |
| 11 | A(LL)=TB | 01394000 |
| C | ROW INTERCHANGE AND PIVOT ROW REDUCTION IN MATRIX A | 01395000 |
| C | DO 13 L=LST,MM,M | 01396000 |
| | LL=L+1 | 01397000 |
| | TB=PIV*A(LL) | 01398000 |
| | A(LL)=A(L) | 01399000 |
| 13 | A(L)=TB | 01400000 |
| C | SAVE COLUMN INTERCHANGE INFORMATION | 01401000 |
| C | A(LST)=J | 01402000 |
| C | ELEMENT REDUCTION AND NEXT PIVOT SEARCH | 01403000 |
| | PIV=0. | 01404000 |
| | LST=LST+1 | 01405000 |
| | J=0 | 01406000 |
| | DO 16 II=LST,LEND | 01407000 |
| | PIV=A(II) | 01408000 |
| | IST=II+M | 01409000 |
| | J=J+1 | 01410000 |
| | DO 15 L=IST,MM,M | 01411000 |
| | LL=L-J | 01412000 |
| | A(L)=A(L)+PIV*A(LL) | 01413000 |
| | TB=ABS(A(L)) | 01414000 |
| | IF(TB-PIV)15,15,14 | 01415000 |
| 14 | PIV=TB | 01416000 |
| | I=L | 01417000 |
| 15 | CONTINUE | 01418000 |
| | DO 16 L=K,MM,M | 01419000 |
| | LL=L+J | 01420000 |
| 16 | R(LL)=R(LL)+PIV*R(L) | 01421000 |
| 17 | LST=LST+H | 01422000 |
| | END OF ELIMINATION LOOP | 01423000 |
| C | BACK SUBSTITUTION AND BACK INTERCHANGE. | 01424000 |
| 18 | IF(M-1)23,22,19 | 01425000 |
| 19 | IST=MM+H | 01426000 |
| | LST=M+1 | 01427000 |
| | DO 21 I=2,M | 01428000 |
| | II=LST-I | 01429000 |
| | IST=IST-LST | 01430000 |
| | L=IST-M | 01431000 |
| | L=A(L)+.5 | 01432000 |
| | DO 21 J=II,MM,M | 01433000 |
| | TB=R(J) | 01434000 |
| | LL=J | 01435000 |
| | DO 20 K=IST,MM,M | 01436000 |
| | LL=LL+1 | 01437000 |
| 20 | TB=TB-A(K)*R(LL) | 01438000 |
| | K=J+L | 01439000 |
| | R(J)=R(K) | 01440000 |
| 21 | R(K)=TB | 01441000 |
| 22 | RETURN | 01442000 |
| C | ERROR RETURN | 01443000 |
| C | IF(1ER)1 | 01444000 |
| 23 | RETURN | 01445000 |
| | END | 01446000 |


```

C
C
C
SUBROUTINE HBPONT(QYX,QXY,QZX,TOTFLO,INITAL,IFINAL)
DIMENSION QYX(504),QXY(504),QZX(504)
HBPONT=EVALUATES THE HEAT BALANCE BETWEEN INTERIOR
NODAL POINTS
DO 184 K=INITAL,IFINAL
HEATIN=QYX(K+126)+QXY(K-1)+QZX(K-14)
HITOUT=QYX(K)+QXY(K)+QZX(K)
TOTFLO=QYX(K)+QYX(K+126)+QXY(K-1)+QXY(K)+QZX(K-14)+QZX(K)
PECERR=TOTFLO/((ABS(HEATIN + HITOUT))/2.)*100.
WRITE(6,183)K,QYX(K),QYX(K+126),QXY(K-1),QXY(K),QZX(K-14),QZX(K),T
4TOTFLO,PECERR
183 FORMAT(/,/,1X,I4,3X,7(E11.4,6X,),F6.3)
WRITE(6,214)HEATIN,HITOUT
214 FORMAT(10X,'HEAT INTO POINT=',E13.6,10X,'HEAT CONDUCTED AWAY FROM
1POINT=',E13.6)
184 CONTINUE
RETURN
END

```

```

01457000
01458000
01459000
01460000
01461000
01462000
01463000
01464000
01465000
01466000
01467000
01468000
01469000
01470000
01471000
01472000
01473000
01474000
01475000
01476000

```